

STEAM TABLES AND DIAGRAMS

MARKS AND DAVIS

TABLES AND DIAGRAMS

OF

THE THERMAL PROPERTIES OF SATURATED AND SUPERHEATED STEAM

BY

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PREFACE

THE tables of the properties of saturated steam which have appeared up to the present time have all been based upon the classic investigations of Regnault, carried out more than sixty years ago. It has been apparent for some time that the total heats of dry and saturated steam, as determined by those admirable researches, are below the correct values. The great difficulty in obtaining steam which is exactly dry and saturated has not been appreciated until very recently; and it is undoubtedly true that Regnault was investigating steam containing a small amount of moisture when he thought that he was dealing with dry steam. Fortunately, the recent investigations of Dieterici, Smith Griffiths, Henning and Joly give a trustworthy body of new values of the total heat of dry steam at pressures below atmospheric pressure; while the method recently elaborated by Davis, when applied to the throttling experiments of Grindley, of Peake, and of Griessmann, gives remarkably accordant determinations at pressures above atmospheric pressure. The table which we have prepared is based entirely upon these new values, and is probably correct to one tenth of one per cent within the range of steam pressures usual in engineering practice. Regnault's formula gives results which are too high by 18 B. t. u. at 32° F.; too low by 6 B. t. u. at 275° F.; and again too high at 380° F.; the error increasing rapidly at higher temperatures.

The investigations of Knoblauch, of Thomas and of Henning are the necessary basis for any determinations of the properties of superheated steam. These investigations have been subjected to a careful analysis, both as to the probable errors resulting from the methods of experimentation, and also as to the relation of the experimental results to the values deduced from thermodynamic theory, so far as this latter throws any light on the matter. Where the results of the separate investigations are not closely accordant, a critical estimate has been made of the relative values to be given to each, in the region under consideration. The properties of superheated steam are tabulated for every pound pressure, and for every ten degrees of superheat, within a range which exceeds present practice. All the information relating to superheated steam of any pressure is given on one double-page; an arrangement which permits the immediate finding of any desired quantity. Supplementary tables extend the superheated steam table to very high temperatures and give the properties of water, metric conversion factors, Naperian logarithms and other quantities.

Beside the tables, we have prepared two large diagrams showing the properties of saturated and superheated steam. These diagrams can be used, instead of the tables, for finding the total heat, entropy and specific volume of steam of any known quality or superheat (within an extended range); but their chief purpose is to facilitate certain calculations. In consequence of the variation of the specific heat of super-

PREFACE

heated steam with both pressure and temperature, the solution of commonly occurring problems involving superheated steam is either laborious or approximate. If the tables are arranged in such a manner as to aid the solution of problems of one class, they become inconvenient for other purposes. The total heat-entropy diagram, devised by Mollier, makes it possible to solve immediately many of the problems which arise in connection with either saturated or superheated steam. A total heat-pressure diagram, showing specific volumes, permits the solution of problems involving volumes. By the use of the two diagrams, either separately or together, a large number of the steam problems occurring in the design of engines and turbines, or in connection with the flow of steam, or its throttling, can be solved without any calculation. These two diagrams have been plotted with great care from the data given in the tables, and should prove useful to all engineers or students engaged in making calculations which involve saturated or superheated steam.

The authors desire to express their indebtedness to Professor E. V. Huntington for the use of the plates of his four-place tables of logarithms, and to Mr. M. R. Wolfard, S. B., for his patient and skilful assistance in the arduous work of computation and in drawing the diagrams.

L. S. M. H. N. D

CAMBRIDGE, MASS., December, 1908.

Note to the 1916 Reprint. The experimental information which has become available since these tables were computed does not justify any appreciable change in them except in one respect. The work of Holborn and Baumann* on the pressure-temperature relations of saturated steam at high pressures should apparently be accepted in preference to all previous work. The pressures involved are from 400 lb. per sq. in. to the critical pressure and are consequently outside the range of usual engineering experience. The last few entries in Tables 1,2,3, and 6 have been changed to bring them into agreement with this new information.

A new Mollier chart has been prepared which will be found to be more convenient than the earlier Diagram I.

L. S. M. H. N. D.

CAMBRIDGE, MASS., August, 1916.

* Marks, Trans. Am. Soc. Mech. Eng., vol. 33 (1911).

CONTENTS

PART I. TABLES AND DIAGRAMS	
DESCRIPTION OF TABLES	. (
Description of diagrams	. ;
Tables	
I. SATURATED STEAM: TEMPERATURE TABLE	. 8
2. SATURATED STEAM: PRESSURE TABLE	. 10
3. SATURATED AND SUPERHEATED STEAM	. 2
4. Superheated steam at high superheats	. 60
5. Boiling points, for thermometer calibrations	. 6
6. Thermal properties of water	, 68
7. Conversion tables	. 70
8. Logarithms to the base 10	. 72
9. Logarithms to the base e	. 70
DIAGRAMS (AT END OF BOOK)	·
I. TOTAL HEAT-ENTROPY DIAGRAM	
II. Total heat-pressure diagram	
PART II. THE USE OF THE DIAGRAMS	
GENERAL DISCUSSION	. 78
SOLUTIONS OF ILLUSTRATIVE PROBLEMS	. 80
PART III. DISCUSSION OF SOURCES	
1. Absolute temperature	. 8
2. The specific heat of water	. 88
3. THE MECHANICAL EQUIVALENT OF HEAT	. 92
4. The pressure-temperature relation	. 93
5. The specific heat of superheated steam	. 95
6. The specific volume of superheated steam	. 98
7. THE TOTAL HEAT OF SATURATED STEAM	. 98
8. The specific volume of saturated steam	. 10:
9. The volume of saturated steam at high temperatures	. 10
10. THE COMPUTATION OF THE TABLES	. 100

THE TABLES

Of the three main steam tables, the first and second are for water and saturated steam only, and give explicitly all of the properties that are ordinarily needed. Table 3 is primarily for superheated steam, but includes saturated steam as the special case of zero superheat.

In Table 1, the argument is the temperature. This table is useful for hygrometric and other purposes as well as for steam engineering. To facilitate the handling of condenser vacuums, all pressures below one atmosphere are given in inches of mercury as well as in lbs. per sq. in. The use of this table in accurate calorimetry is made possible by giving the heat of the liquid to hundredths of a mean B. t. u. between 32° and 212°.

The data upon which steam tables must be based are well known only to about 400°. It is, however, often convenient to be able to work roughly at much higher temperatures. Table I has, therefore, been extended to the critical point itself, but the values above 400° should not be used with too much confidence (see the discussion of sources in Part III of this book).

In Tables 2 and 3, the argument is the pressure. These tables extend to 600 lbs., the values above 250 lbs. being less certain than those below. Table 3 can be extended to very high superheats by means of Table 4.

There is also a table of boiling points for use in calibrating thermometers, a table of the thermal properties of water, a full set of conversion tables, particularly for energy units, and tables of four-place logarithms, both common and Naperian.

The unit of heat and of energy in these tables is a "mean B. t. u.," that is, 1/180 of the heat needed to raise one pound of water from the freezing to the boiling point. The use of such a unit instead of the B. t. u. at 60° F. corresponds to the rapidly increasing use of the Bunsen or mean calorie in the metric system, and has many advantages, among which is the ease with which tables based on the two mean units can be compared. The most important reason for such a choice in these tables is that, at the present time, the value of the mean unit is better known than that of the 60° unit, because of the rapidity with which the specific heat of water changes with the temperature near 60°. The mean B. t. u. is larger than the 60° B. t. u. by between three and ten hundredths of one per cent, a difference that is negligible for engineering purposes.

THE DIAGRAMS

In order to facilitate the solution of many problems of common occurrence, two large diagrams have been prepared to accompany this book.

The Total Heat-Entropy Diagram (Diagram I) has two families of curves: (a) curves of constant pressure, and (b) curves of constant quality and constant superheat. The ordinates are total heat (i. e. heat of formation measured above water at 32° F.); the abscissæ are entropies. Vertical lines are lines of constant entropy and show the change in the condition of steam during adiabatic expansion. Measurements along vertical lines give the change in the total heat of steam during adiabatic expansion (which is equal to the work done in the Rankine ideal cycle); the same measurements transferred to the velocity scale give the theoretical velocity of escape of steam through a properly shaped orifice or nozzle. Horizontal lines are lines of constant total heat; they show the change in the condition of steam which results from throttling.

The Total Heat-Pressure Diagram (Diagram II) has two families of curves: (a) curves of constant specific volume, and (b) curves of constant quality and constant superheat. The ordinates are total heats; the abscissæ, pressures. Vertical lines are lines of constant pressure; measurements along vertical lines give the heat supply accompanying changes of volume or quality at constant pressure. Horizontal lines are lines of constant total heat; they show the change of volume and condition of the steam resulting from throttling. The scale of abscissæ is a uniform scale of temperatures of saturated steam, which gives a varying scale of steam pressures. This varying scale has the advantage of spreading out the specific volume curves at low pressures.

The use of total heats as ordinates has certain special advantages. The energy given up by steam that is passing through any appliance is equal to the difference between the total heat of the entering and of the leaving steam. This difference is represented by vertical measurements on the diagram.

The method of using these diagrams for the solution of problems is explained in detail in Part II.

Table 1 Saturated Steam: Temperature Table

Temp.	Prese lbs. per	sure inches	Sp. Vol.	Density lbs per	Heat of the	Latent heat of	Total	Internal B. t	Energy		Entrepy		Temp.
Fahr.	sq. in.	of Hg.	ců, ft. per lb.	lbs per cu. ft.	liquid	evap.	steam	Evap.	Steam	Water	Evap.	Steam	Fahr.
t	p		y or s	1/y		Lorr	Н	l or p	E		L/T or r/T		t
32°	0.0886			0.000304		1073.4		1019.3			2.1832		32°
33 34	0.0922	0.1878		0.000316 0.000328		1072.8 1072.2		1018.6 1018.0			2.1777 2.1721		33 34 ₅
-	0.0300	0.2555		0.0000			207 1,2	2020.0	2020.0	0.0012		2,2,02	-0-0-C
35°	0.0999			0.000340		1071.7		1017.3		0.0062	2.1666	2.1728	35°
36		0.2117		0.000353		1071.1			1020.7		2.1611		36
37 38		0,2202 0,2290		0.000367 0.000381		1070.6 1070.0		1016.0 1015.3			2.1557 2.1503		37 38
39		0.2382		0.000395		1069.4		1013.3			2.1303		39
40°		0.2477		0.000410		1068.9		1014.0			2.1394		40°
41 42		0.2575 0.2677		0.000425 0.000441		1068.3 1067.8		1013.3 1012.6			2.1341 2.1287		41 42
43		0.2782		0.000458		1067.2		1012.0			2.1234		43
44		0.2890		0.000475		1066.7		1011.3			2.1181		44
45°	0.1475			0.000492		1066.1		1010.6			2.1127		45°
46 47		0.3118 0.3238		0.000510 0.000529		1065.6 1065.0		1010.0 1009.3			2.1074 2.1022		46 47
48		0.3363		0.000548		1064.5		1009.5			2.1022		48
49		0,3492		0.000567		1063,9		1007.9			2.0917		49
50°		0.3625		0.000587		1063.3			1025.4		2.0865		50°
51 52		0.3762 0.3903		0.000608 0.000630		1062.8 1062.2		1006.6	1025.7		2.0814 2.0763		51 52
53		0.4049		0.000653		1061.7			1026.4		2.0712		53
54		0.4201		0.000676		1061.1		1004.6			2,0660		54
55°	0.0740	0.4357	1420	0.000700	02.00	1060.6	1002 6	1004.0	10071	0.0450	0.000	0.1060	55°
56		0.4337		0.000700		1060.0			1027.1	0.0459 0.0478	2.0609		56
57		0.4684		0.000749		1059.5			1027.7		2,0508		57
58	0.2385	0.4856	1291.	0.000775			1085.0		1028.1		2.0458		58
59	0.2472	0.5034	1249.	0.000801	27.08	1058.3	1085.4	1001.3	1028,4	0.0536	2,0408	2.0944	59
60°	0,2562	0.522	1208	0.000828	28.08	1057.8	1085.9	1000.7	1028.7	0.0555	2.0358	2.0913	60°
61	0.2654			0.000856		1057.2			1029.1		2,0308		61
62		0.560		0.000885			1086.8		1029.4		2,0258		62
63		0.580		0.000915			1087.2		1029.8		2,0209		63
64	0,2949	0.601	1058.	0.000946	32.07	1055.6	1087.6	998.0	1030.1	0.0631	2,0160	2,0791	64
65°	0.3054	0.622	1024.	0,000977	33.07	1055.0	1088,1	997.4	1030,4	0.0650	2,0110	2.0760	65°
66	0.3161	0.644	991.	0.001009			1088.5		1030 8		2.0062		66
67		0.667		0.001043			1089.0		1031.1	0.0688	2.0013	2.0701	67
68 69		0.690		0.001077 0.001112			1089.4 1089.9		1031.4 1031.8		1.9965 1.9916		68 69
05	0.5504	0.714	099.	0.001112	37.00	1032.0	1009.9	994.7	1031,6	0.0720	1,9910	2,0012	09
70°		0.739	871.	0.001148	38.06	1052,3	1090.3	994.0	1032.1	0.0745	1.9868	2.0613	70°
71		0.764		0.001186			1090.8		1032,4		1.9821		71
72 73		0.790		0.001224			1091.2		1032.8		1.9773		72 73
73 74		0.817		0.001263 0.001304			1091.6		1033.1		1,9726 1,9678		73 7 4
75°		0.873		0.001346			1092.5		1033.8		1.9631		75°
76 77		0.903		0.001389 0.001433			1093.0		1034.1		1.9585 1.9538		76 77
78		0.964		0.001433			1093.4		1034.4		1,9336		78
79		0,996		0.001523			1094.3		1035.1		1.9445		79
quo.	= tº + 45	9.61 J		lhe ner R.t.n.									

Table 1: Temperatures

T and		1 0111	- ,	ui Ui									
Tamn.	Press lbs. per	ure	Sp. Vol.	Density	Heat	Latent heat of	Total .	Interna	i Energy	,	Entropy		Temp.
Fahr.	sq. in.	of Hg.	ců. ft. per lb.	lbs. per cu. ft.	of the liquid	evap.	steam	8. t Evap.	Steam	Water	Evap.	Steam	Fahr.
t	p	_	v or s	1/y	horq	Lorr	Н	l or e	E	n or e L	/Torr/T		t
		1 000	626 0		•						• •		
	0.505			0.001570		1046.7			1035.4		1,9398		80°
81	0.522			0.001619		1046.2			1035.8		1.9352		81
82	0.539			0.001670		1045.6			1036.1		1.9306		82
83	0.557			0.001723		1045.1			1036.4		1.9260		83
84	0.575	1.171	562.9	0.001777	52.02	1044.5	1096.5	984.8	1036.8	0.1005	1.9215	2.0220	84
					#2 2 2								
85°	0.594			0.001832		1044.0			1037.1		1.9169		85°
86	0.613			0.001889		1043.4			1037.4		1.9124		86
87	0,633			0.001947		1042.8			1037.8		1.9079		87
88	0.654			0.002007		1042.2			1038.1		1.9034		88
89	0,675	1.373	483.6	0.002068	57,00	1041.7	1098.7	981.4	1038.4	0.1096	1.8989	2.0085	89
90°	0.696			0.002131		1041.2			1038.8		1:8944		90°
91	0.718			0.002195		1040.6			1039.1		1.8900		91
92	0.741	-		0.002261		1040,0			1039.4		1.8856		92
93	0.765			0.002329		1039.5			1039.8		1.8812		93
94	0.789	1,605	417.0	0.002398	61.99	1039.0	1101.0	978.1	1040.1	0,1187	1,8767	1,9954	94
											_		
95°	0.813		405.0	0.002469		1038.4			1040.4		1.8723		95°
96	0.838	1.706	393.4	0.002542	63.98	1037.8	1101.8	976.8	1040.8	0.1223	1.8680	1.9903	96
97	0.864	1.759	382.2	0.002617	64.98	1037.3	1102.3	976.1	1041.1	0.1241	1.8636	1.9877	97
98	0,891	1.813	371.4	0.002693	65.98	1036,7	1102.8	975,5	1041,4	0,1259	1,8592	1.9851	98
99	0.918	1,869	360.9	0.002771	66.97	1036.2	1103.2	974.8	1041.8	0.1277	1.8549	1,9826	99
100°	0.946	1.926	350.8	0.002851	67.97	1035.6	1103.6	974.1	1042.1	0.1295	1.8505	1.9800	100°
101	0.975	1.985	341.0	0.002933	68.97	1035.1	1104.0	973.5	1042.4	0.1313	1.8463	1.9776	101
102	1,005	2,045	331.5	0.003017	69.96	1034.5	1104.5	972.8	1042.8	0.1330	1.8420	1.9750	102
103	1.035	2.107	322.2	0.003104	70.96	1034.0	1104.9	972.1	1043.1	0.1347	1.8377	1.9724	103
104	1,066	2.171	313.3	0.003192	71.96	1033,4	1105.3	971.5	1043,4	0.1365	1,8335	1.9700	104
105°	1,098	2,236	304.7	0.003282	72.95	1032.8	1105.8	970.8	1043.8	0.1383	1.8292	1.9675	105°
106	1,131	2,303	296,4	0.003374	73,95	1032,3	1106.2	970,1	1044,1	0.1401	1.8250	1.9651	106
107	1,165	2,372	288,3	0.003469	74,95	1031,7	1106.7	969.5	1044.4	0.1418	1,8208	1.9626	107
108	1.199	2,443	280.5	0.003565	75.95	1031.2	1107.1	968.8	1044.8		1.8166		108
109		2.515		0.003664		1030.6		968.2	1045,1		1.8124		109
110°	1.271	2,589	265.5	0.003766	77,94	1030.0	11.08.0	967.5	1045.4	0.1471	1.8082	1.9553	110°
111	1,308	2.665	258.3	0.003871	78.94	1029.5	1108.4	966.8	1045.8		1.8041		111
112		2,740	251.4	0.003978	79.93	1028.9	1108.8	966.2	1046.1		1.8000		112
113	1.386			0.004087	80.93	1028,4	1109.3	965.5	1046.4		1,7959		113
114	1.426			0.004198		1027.8			1046.8		1.7917		114
	-•												
115°	1,467	2,987	231.9	0.004312	82.92	1027.2	1110.2	964.2	1047,1	0.1559	1.7876	1.9435	115°
116		3.073		0.004429		1026.7			1047.4		1.7836		116
117	1.553			0.004548		1026.1			1047.8		1.7795		117
118		3.252		0.004671		1025.5			1048,1		1,7755		118
119		3.344		0.004796			1111.9		1048.4		1.7715		119
		0,0		0.00							_,,,	-,,,,,,,,	
120°	1,689	3.438	203.1	0.004924	87.91	1024.4	1112.3	960.8	1048.7	0.1645	1.7674	1.9319	.120°
121		3,535		0.005054		1023.9		~~~	1049.1		1.7634		121
122		3.635		0.005187		1023.3			1049.4		1,7594		122
123	1,835			0.005323		1022.7			1049.7		1.7555		123
124	1.886			0.005462		1022.2			1050.0		1.7515		124
	4.000	J.0 11	100.1	0.003 102	72.70	_000.0		JJ 0.2	_0.00.0	0.2720	-,,,,,,,	,,,,,,,,,	
125°	1.938	3 948	178 4	0.005605	92.90	1021.6	1114.5	957.5	1050.4	0.1730	1.7475	1 9205	125°
126		4.057		0.005751		1021.1			1050.7				126
127	2.047			0.005900		1020.5			1051.0		1,7397		127
128	2.103			0.006052		1019.9			1051.3		1,7358		128
129	2,160			0.006207		1019.4			1051.7		1,7318		129
	(-		
40	O.L.ARO	R. T-7	77 5 24 1	he was Dee	flam-f	90 071	1. A-1/	T 1 000	2 Y 7 A-8.	3 4 4 A 0	TORO [1	T 08	7041

T°=4°+459.6; J=777.5 ft. lbs. per B.t.u. $[\log = 2.89\ 071]$; A=1/ σ =1.286×10⁻³; 144 A=0.1852 $[\log = \overline{1}.26\ 764]$. For water, at 95° (0.81 lbs.), sp. vol., v' or σ =0.0161 cu. ft. per lb.; 1/v'=62.0 lbs. per cu. ft.; 144 Apv'=0.002 B.t.u.; at 120° (1.69 lbs.), • v'@ σ =0.0162 " i1/v'=61.7 " ; 144 Apv'=0.005 " .

(9)

Table 1: Temperatures

130° 2.219 4.52 157.1 0.00637 97.89 101.88 111.67 954.1 1052.0 0.1816 1.779 1.9095 130° 131 2279 4.64 153.2 0.00653 98.99 101.82 111.71 953.4 1052.3 0.1833 1.740 1.9073 131 132 2.340 4.76 4.99 4.90 4.90669 99.88 101.7 111.75 952.8 1052.3 0.1836 1.7716 1.903 133 134 2.467 5.02 142.2 0.00703 101.88 101.65 111.84 952.1 1053.0 0.1866 1.7164 1.903 133 134 2.467 5.02 142.2 0.00703 103.88 101.65 111.84 952.1 1053.0 0.1866 1.7164 1.903 134 1357 136 2.600 5.29 1554 0.00739 103.88 101.65 111.84 951.4 1053.3 0.1868 1.7125 1.9008 134 1357 136 2.600 5.29 1554 0.00739 104.87 101.43 111.91 940.1 1054.0 1.917 1.7048 1.8965 136 138 2.81 5.77 125.8 0.0076 105.87 101.43 112.01 940.8 1054.0 1.917 1.0048 1.896 138 137 138 2.740 5.58 128.9 0.0076 105.87 101.43 112.01 947.4 1054.3 0.1931 1.6934 1.891 139 139 2.812 5.73 123.8 0.0094 103.8 101.54 111.9 947.4 1055.3 0.1984 1.6986 1.898 140 141 2.900 60.3 119.9 0.00834 108.87 101.20 112.18 940.1 1055.9 0.2007 1.6821 1.8938 142 143 135 143 143 143 143 143 143 143 143 143 143 143 143 143 144 1.915 1.0518 1.055.0 0.2007 1.6921 1.8938 142 143 1	lemp. Fahr.	Pres ibs. per sq. in.	sure inches	Sp. Vol.	Density lbs. per cu. ft.	Heat of the liquid h or q	Latent heat of evap. L or r	Total heat of steam H	Internal Energy B. t. u. Evap. Steam I or P E	Entropy Water Evap. Steam n or 0 L/T or r/T N or 0	Temp. Fahr. t
131 2279 4.64 4.76 1440 4.00669 98.89 1017 1117.5 95.81 105.27 0.1849 1.7020 1.9051 132 133 2.403 4.89 45.8 0.00666 100.88 1017.1 1118.0 95.21 105.30 0.1866 1.7164 1.9030 133 133 2.403 4.89 45.8 0.00666 100.88 1017.1 1118.0 95.21 105.30 0.1866 1.7164 1.9030 133 133 2.403 4.89 45.8 0.00703 101.88 1016.5 1118.4 951.4 105.33 0.1866 1.7164 1.9030 133 133 2.240 2.600 5.29 135.4 0.00739 103.88 1015.4 1119.3 950.1 1054.0 0.1917 1.7048 1.8965 136 137 2.669 5.43 132.1 0.00757 104.87 10148 1119.7 944 1054.3 0.1931 1.7010 1.8965 136 137 138 2.740 5.58 128.9 0.00776 105.87 1014.3 1120.1 944.8 1054.6 0.1950 1.6972 1.8922 138 139 2.812 5.73 125.8 0.00795 106.87 1013.7 1120.6 948.1 1055.0 0.1967 1.6934 1.8901 139 141 2.900 6.03 119.9 0.00844 109.87 1012.6 1121.4 946.8 1055.6 0.2000 1.6859 1.8859 141 142 3.037 6.18 117.1 0.00854 109.87 1012.0 112.4 946.1 1055.9 0.2007 1.6821 1.8338 142 1.433 1.54 1.043 0.00875 110.87 1011.4 112.2 944.7 1055.3 0.1984 1.6996 1.8836 144 143 1.955 6.51 111.6 0.00896 113.86 10097 1123.6 944.7 1056.0 0.2005 1.6746 1.8796 144 148 1.353 1.634 143.3 0.00985 113.86 10097 1123.6 944.7 1055.5 0.2003 1.6747 1.8317 143 143 143 143 143 143 143 143 143 143 143 143 143 143 143 144 145 1	t	P 0.010	4 50							•	
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TO-40 LARGE B. T-777 F.M. IL DA. G 0 00 0717. A-1/+- 1 000 V 10-8. 144 A-0 1000 G 7 00 7047											

 $\begin{array}{l} T^{o}=t^{o}+459.6; \ J=777.5 \ ft. \ lbs. \ per \ B.t.u. \ [log=2.89\ 071]; \ A=1/\sigma=1.286\times 10^{-3}; \ 144\ A=0.1852 \ [log=\overline{1}.26764]. \\ For \ water, at 145^{o}(3.28\ lbs.), \ sp. \ vol., \ v'or \ \sigma=0.0163 \ cu. \ ft. \ per \ lb.; \ 1/v'=61.3 \ lbs. \ per \ cu. \ ft.; \ 144\ Apv'=0.01\ B.t.u.; \ 17v'=60.8; \ c'' \ ; \ 144\ Apv'=0.02 \ '' \ . \end{array}$

Table 1: Temperatures

	Presa	ure	en Val	Density	Heat	Latent		Interna	l Energy		Entropy		Temp.
Temp. Fahr.	lbs. per sq. in.	inches	cu. ft. per lb.	ibs. per cu. ft.	of the liquid	evap.	heat of steam	Evap.	t. u. Steam	Water	Evap.	Steam	Fahr.
t	P	-	A OL 8	1/ _V	horq	L or r	Н	l or p	E	n or ø 1	_/T or r/1	Γ N or φ	t
180°	7.51			0.01994	147.88				1068.1		1.5476		180°
181		15.63		0.02036	148.88				1068.4		1.5443		181
182		15.98		0.02078	149.89				1068.7		1.5409		182
183		16.34	-	0.02121 0.02165	150.89 151.89				1069.0 1069.3		1.5376 1.5343		183 184
184	8.20	16.70	40.10	0.02103	131.09	301.3	1135.7	717,7	1009.5	0.2090	1,3373	1.0033	70=
185°		17.07	-	0.02210			1139.8		1069.6		1.5310		185°
186	8.57			0.02255			1140.2		1069.9		1.5277		186
187		17.83		0.02301	155,90		1140.6		1070.2		1.5244		187 188
188 189		18.22 18.61	-	0.02348			1141.4		1070.5 1070.8		1.5211 1.5179		189
109	7.17	10,01	71./7	0.02590	150.50	301,3	1171.7	910.9	1070.0	0.2707	1,3119	1,7510	100
190°	9.34	19.02	40.91	0.02444	157.91				1071.1		1.5146		190°
191		19.43		0.02493	158.91				1071.4		1.5113		191
192		19.85		0.02544			1142.6		1071.7		1.5081		192
193		20.27		0.02595	160.91				1072.0		1.5048		193 194
194	10.17	20.71	31.10	0.02647	161.92	301.3	1145.4	910.4	1072.3	0,2043	1.5016	1.7001	104
195°	10.39	21,15	37.04	0.02700	162,92	980.9	1143.8	909,7	1072.6		1.4984		195°
196	10.61			0.02753	163.92				1072.9		1.4952		196
197	10.83			0.02807	164.93				1073.2		1.4920		197
198	11.06			0.02863	165.93				1073.5		1.4888		198
199	11.29	44,99	34.20	0.02919	166,94	9/0.4	1145.4	900,9	1073.8	0.2921	1.4856	1.////	199
200 °	11.52			0.02976	167.94				1074.1	0.2937	1.4824	1.7761	200°
201	11.76			0.03034	168.94				1074.4		1.4792	-	201
202	12.01	-		0.03093	169.95				1074.7		1.4760		202
203 204	12.26 12.51			0.03153 0.03214	170.95 171.96				1075.0 1075.3		1.4729 1.4697		203 204
202	14.51	23,70	31,12	0.03214	171,50	313. T	1147,3	903,3	1075.5	0.2997	1,707/	1.7094	40%
205°	12,77			0.03276			1147.7		1075.6	0.3012	1.4666	1.7678	205°
206	13.03			0.03339	173.97	-	-		1075.9		1.4635		206
207	13.30			0.03402	174.97				1076.1		1.4603	•	207
208 209	13.57 13.85			0.03466 0.03531	175.98		1148.9		1076.4 1076.7		1.4572 1.4541		208 209
205	13,03	20,19	20.32	0.03331	170.98	314,4	1179.2	055,7	1070.7	0,3072	19041	1,7013	209
210 °	14.13			0.03597			1149.6	899.0	1076.9	0.3087	1.4510	1.7597	210°
211	14.41			0.03664			1150.0		1077.2		1.4478		211
212	14.70			0.03732			1150.4		1077.5		1,4447		212
213 214		1.020*		0.03802	181.0		1150.7		1077.8		1.4416	-	213
214	15.29	1,041	23.82	0.03873	182.0	909.1	1151,1	090.1	1078.1	0.3148	1.4385	1.7533	214
215°		1.062*		0.03945	183.0		1151.5		1078.3		1.4354		215°
216	15.91			0.04018	184.0		1151.8		1078,6		1.4323		216
217	16.22		-	0.04092	185.0		1152.2		1078.9		1.4292		217
218 219	16.54 16.86			0.04167 0.04243	186.1 187.1		1152.6 1152.9		1079.2 1079.4		1.4261		218
410	10,00	1,14/	۵.51	0,04243	107.1	905,9	1132,9	074,4	1079,4	0,3223	1.4230	1.7455	219
220°				0.04320	188.1		1153.3		1079.7			1.7437	
221	17.53			0.04398	189.1		1153.7		1080.0		1.4169		221
222	17.87			0.04477	190.1		1154.0		1080.2		1.4139		222
223 224	18.21 18.56			0.04558	191,1 192,1		1154.4 1154.8		1080.5 1080.8		1.4110 1.4081		223 224
225° 226		1.287*		0.04723	193.1		1155.1		1081.1		1.4052		225°
226 227	19,27 19,64			0.04807	194.1		1155.5 1155.8		1081.3		1.4023		226
228	20.01			0.04892	195.2 196.2		1156.2		1081.6 1081.9		1.3993	1.7334	227 228
229	20.39			0.05067	197.2		1156.5		1082.1			1.7304	229
				1,0007						0.00,0	L.UJUT	±.,,00 f	

^{*}In standard atmospheres. 1 atmo=760 mms. of Hg. by definition=29.921 ins. of Hg. = 14.696 lbs. per sq. in. For water, at 195° (10.4 lbs.), sp. vol., v' or $\sigma = 0.0166$ cu. ft. per lb.; $\frac{1}{2}$ = 60.3 lbs. per cu. ft.; $\frac{144 \text{ Apv'} = 0.03 \text{ B.t.u.}}{144 \text{ Apv'} = 0.05}$ at 220° (17.2 lbs.), • ev' or $\sigma = 0.0168$ " ; $\frac{1}{2}$ = 0.05 " .

Table 1: Temperatures

TADI		I CIII	heran		,					
Temp.	Pres	sure	Sp. Vol.	Density	Heat	Latent	Total	Internal Energy	Entropy	Temp.
Fahr.	lbs.	Atmos*	per lb.	lbs. per cu. ft.	liquid	evap.	heat of steam	B. t. u. Evap. Steam	Water Evap. Steam	Fahr.
t	p	-	V OF 8	1/y	h or q	-	Н	lor P E	n or θ L/Torr/T N or Φ	ŧ
	-	1 412			-			-	• •	
230°		1.413		0.0516			1156.9	884.3 1082.4	0.3384 1.3905 1.7289	230
231		1.440		0.0525	-		1157.2	883.6 1082.7	0.3399 1.3875 1.7274	231
232		1.467		0.0534			1157.6	882.8 1083.0	0.3414 1.3844 1.7258	232
	21.96			0.0543			1158.0	882.1 1083.2	0.3429 •1.3814 1.7243	233
234	22.37	1.522	18.09	0.0553	202.2	956.1	1158.3	881.3 1083.5	0.3443 1.3784 1.7227	234
235°	00.70	1 550	17 70	0.0560	202.0	055.4	1150 7	000 6 1002 0	0 2459 1 2754 1 7010	OOF
236		1.550		0.0562			1158.7	880.6 1083.8	0.3458 1.3754 1.7212	235
237		1.579 1.609		0.0572			1159.0	879.8 1084.0	0.3472 1.3725 1.7197	236
				0.0582			1159.4	879.1 1084.3	0.3487 1.3695 1.7182	237
238		1.638		0.0592			1159.7	878.3 1084.5	0.3501 1.3666 1.7167	238
239	24.54	1.668	10.00	0.0602	207.3	952,8	1160.0	877.6 1084.8	0.3516 1.3636 1.7152	239
240°	24 97	1.699	16 32	0.0613	208.3	052 1	1160.4	876.8 1085.0	0.3531 1.3607 1.7138	240
241		1:730		0.0623			1160.7	876.1 1085.3	0.3546 1.3578 1.7124	241
242		1.761		0.0634			1161.1	875.3 1085.6	0.3560 1.3550 1.7110	242
243		1.793		0.0644			1161.4	874.6 1085.8	0.3575 1.3521 1.7096	243
244		1.826		0.0655	-		1161.4	873.8 1086.1		244
44	20.65	1.020	13,20	0.0055	212.4	949.4	1101.0	0/3.0 1000.1	0.3589 1.3493 1.7082	244
245°	27.31	1.859	15 01	0.0666	213.4	948 7	1162.1	873.1 1086.4	0.3603 1.3465 1.7068	245
246		1.892		0.0678			1162.4	872,3 1086.6	0.3617 1.3437 1.7054	246
247		1.926		0.0689	-		1162.8	871.6 1086.9	0,3631 1,3408 1,7039	247
248		1.960		0.0700			1163,1	870.8 1087.1	0,3646 1,3379 1,7025	248
249		1.994		0.0712			1163.4	870.0 1087.4	0.3661 1.3350 1.7011	249
		.,,,,,	_ 1,00	0.0, 12	227	J .O.O	1100.1	0,0.0 100,	0.0001 1.0000 1.7011	220
250°	29.82	2.029	13.82	0.0724	218.5	945.3	1163.8	869.2 1087.6	0.3675 1.3321 1.6996	250
251		2.065	13.59	0.0736			1164.1	868.5 1087.9	0,3689 1,3292 1,6981	251
252	30.88	2.101		0.0748			1164.4	867.7 1088.1	0.3704 1.3263 1.6967	252
253		2.138		0.0760			1164,8	867.0 1088.4	0,3718 1,3235 1,6953	253
254		2,175		0.0772			1165.1	866.2 1088.6	0.3732 1.3207 1.6939	254
255°	32,53	2,213	12.74	0.0785	223.5	941.9	1165.4	865.4 1088.9	0.3747 1.3179 1.6926	255
256	33.09	2.251	12,54	0.0797	224.6	941.2	1165.8	864.6 1089.1	0.3761 1.3151 1.6912	256
257	33.66	2,290	12.34	0.0810	225.6	940.5	1166.1	863.9 1089.4	0.3776 1.3122 1.6898	257
258	34.24	2,330	12,14	0.0824	226.6	939.8	1166.4	863.1 1089.6	0.3790 1.3094 1.6884	258
259	34.83	· 2.370	11.95	0.0837	227.6	939.1	1166.7	862.3 1089.8	0.3804 1.3067 1.6871	259
260°		2.410		0.0850			1167.0	861.5 1090.1	0.3818 1.3040 1.6858	260
261		2.451		0.0864		-	1167.4	860.8 1090.3	0.3833 1.3012 1.6845	261
262		2.493		0.0878			1167.7	860.0 1090.5	0.3847 1.2985 1.6832	262
263		2,535		0.0892			1168.0	859,2 1090.8	0.3861 1.2957 1.6818	263
264	37.89	2.578	11.04	0.0906	232.7	935.6	1168.3	858.4 1091.0	0,3874 1,2930 1,6804	264
OCEO	70 FA	0.601	10.07	0.0000	022 #	024.0	1160 6	007 (1001 0	0.2000 1.0002 1.6701	005
265°		2.621		0.0920			1168.6	857.6 1091.2	0.3888 1.2903 1.6791	265
266		2.665		0.0935			1168.9	856.9 1091.5	0.3902 1.2876 1.6778	266
267		2.710		0.0949			1169.3	856.1 1091.7	0.3916 1.2849 1.6765	267
268		2.755		0.0963			1169.6	855.3 1092.0	0.3930 1.2821 1.6751	268
269	41,16	2.801	10,22	0.0978	237.8	932,1	1169.9	854.5 1092.2	0.3944 1.2794 1.6738	269
270°	41 95	2,847	10.06	0.0994	238 8	031 4	1170.2	853 8 1002 4	0,3959 1,2766 1,6725	270
271		2.894		0.1010			1170.2	853.0 1092.7	0.3973 1.2738 1.6711	271
272		2.942		0.1010			1170.8	852.2 1092.9	0.3987 1.2711 1.6698	272
273		2.990		0.1023			1171.2	851.4 1093.2	0.4001 1.2683 1,6684	273
274		3.039		0.1057			1171.5	850,6 1093.4	0.4015 1.2656 1.6671	274
		,	20					200,0 2000.1		
275°		3.089		0.1073			1171.8	849.8 1093.6	0.4029 1.2629 1.6658	275
276	46.14	3.140		0.1090			1172.1	849.1 1093.9	0.4043 1.2602 1.6645	276
277		3.191		0.1106			1172,4	848.3 1094.1	0.4057 1.2575 1,6632	277
278		3.242		0.1123			1172.7	847.5 1094.3	0.4070 1.2549 1.6619	278
279	48.40	3,294	8.77	0.1140	248.0	925.0	1173,0	846.7 1094.5	0.4084 1,2523 1,6607	279
			_							

^{*1} atmo (standard atmosphere) = 760 mms. of Hg. by definition = 29.921 ins. of Hg. = 14.696 lbs. per sq. in. For water, at 246° (27.3 lbs.), sp. vol., v' or σ = 0.0170 cu. ft. per lb.; 1/v' = 59.0 lbs. per cu. ft.; 144 Apv' = 0.09 B.t.u.; at 270° (41.8 lbs.), v' or σ = 0.0172 | 1/v' = 58.3 | 144 Apv' = 0.13 ".

(12)

Table 1: Temperatures

I av	LC I.	I CIII	pera										
Temp.	Pre	ssure	Sp. Vol.	Density lbs. per cu. ft.	Heat	Latent	Total f heat of	internal E	nergy		Entropy		Temp.
Fahr.	lbs.	Atmos	ner ib.	cu. ft.	of the liquid	evap.		B. t. u. Evap. St	team	Water	Evap.	Steam	Fahr.
t	P		v or s		h or a	Lorr		l or p	E		L/Torr/T		t
	-	2 247			•								
280°		3.347		0.1157			1173.3	845.9 10			1.2496		280°
281		3.401	8.51				1173.6	845.1 10			1.2470		281
282	50.77			0.1192			1173.9	844,3 10			1.2443		282
283		3.510		0.1210			1174.2	843.5 10			1.2416		283
284	52.40	3.566	8.14	0.1228	253.1	921.3	1174.4	842.7 10	95.6	0.4154	1.2389	1.6543	284
•													
285°		3,623	8.02	0.1246	254.2		1174.7	841.9 10			1,2363		285°
286	54.08		7,90		255,2		1175.0	841.1 109			1,2337		286
287	54.93			0.1283			1175.3	840.3 109			1.2311		287
288		3.797		0.1302	257.2	918.4	1175.6	839.5 109	96.5	0.4209	1.2284	1.6493	288
289	56,67	3.856	7,57	0.1322	258,3	917.6	1175.9	838.6 109	96.7	0.4222	1.2258	1.6480	289
290 °	57.55	3.916	7.46	0.1341	259.3	916.9	1176.2	837.8 109	97.0	0.4235	1,2232	1.6467	290°
291	58.44	3,977	7.35	0.1360	260.3	916.2	1176.5	837.0 109	97.2	0.4249	1.2205	1.6454	291
292	59.34	4.038	7.24	0.1380	261.3	915.4	1176.8	836.2 109	97.4	0.4262	1.2179	1.6441	292
293	60,26	4.100	7.14	0.1400	262.4	914.7	1177.1	835.4 109	97.6	0,4276	1,2153	1,6429	293
294	61,19	4,163	7.04	0.1421	263,4	914.0	1177.4	834.6 109	97.8	0,4290	1,2127	1,6417	294
295°	62.13	4.227	6.94	0.1441	264.4	913.2	1177.6	833,8 109	98.0	0.4304	1.2101	1.6405	295°
296	63.08	4.292	6.84	0,1462	265.5	912.4	1177.9	833.0 109			1,2075		296
297		4.358		0.1483	266.5		1178.2	832.2 109			1.2049		297
298		4,424		0.1504			1178.5	831,4 109			1,2023		298
299		4.491		0.1525			1178.8	830.5 109			1.1997		299
												-,0000	
300°	67 00	4.559	6.46	0,1547	269 6	909.5	1179,1	829,7 109	99 1	0 4371	1,1972	6343	300°
301		4.628		0.1569			1179.3	828.9 109			1.1946		301
302	69.03			0.1591			1179.6	828,1 109			1.1921		302
303		4.767		0.1613			1179.9	827.3 109			1.1895		303
304		4.838	-	0.1636			1180.1	826.4 109			1.1869		304
001	,	.,	٠	0,2000	2.0.,	,,,,,	1100.1	020.1 203		0.1.20	1.1003		002
305°	72.17	4.911	6.03	0.1659	274.7	905.7	1180.4	825.6 110	00.1	0.4439	1.1844	6283	305°
306		4.984		0.1683			1180.7	824.8 110			1.1819		306
307		5,058		0.1707			1181.0	824.0 110			1,1793		307
308		5.133	5.78	0.1731			1181.2	823,2 110			1.1767		308
309		5,209		0.1755			1181.5	822.3 110			1.1742		309
000	70.55	5.205	3.70	0.2755	270.0	502.0	1101.5	022.5 110		0.7131	1.17 12 1	0250	000
310°	77 67	5,285	5.62	0.1779	279 9	901.9	1181.8	821.5 110	01.1	0 4507	1,1717	6224	310°
311		5.362		0.1804			1182.0	820.7 110			1.1692		311
312		5.441		0.1829			1182.3	819.9 110			1.1667		312
313		5.520	5.40	0.1854	283.0		1182.6	819.0 110			1.1642 1		313
314		5,600		0.1879			1182.8	818.2 110			1.1617		314
O4.2	02.50	3.000	5.55	0,1075	201.0	0.00	1102.0	010.2 110		0.1500	1017		OTE
315°	83 40	5.681	5 26	0.1904	285.0	898 n	1183.1	817.4 110	12.1	0 4573	1.1592 1	6165	315°
316		5.763		0.1930	286.1		1183.3	816.5 110			1.1567		316
317	85.90			0.1956			1183.6	815.7 110			1.1542		317
318		5.928		0.1982	288.1		1183.8	814.9 110			1.1517		318
319		6.013	-	0.2009			1184.1	814.0 110			1.1492		319
OLO	66.57	0.013	4.50	0.2009	209.2	054.5	1107,1	814.0 110	14.5	0,4027	1,1734 1		OTO
320°	80 62	6.099	4 91	0.2036	200.2	804 2	1184,4	813.2 110	12.1	0 4640	1.1468 1	6108	320°
321		6.185		0.2064			1184.6	812.4 110			1.1444 1		
322	92.19			0.2092			1184.9	811.5 110			1.1419		321 322
323	93.50			0.2092			1185.1	810.7 110			1.1394		
324							1185.4				1.1370 1		323
OCT.	94.82	0,434	+,00	0.2148	474.3	051.0	*******	809.8 110	J.7	U.TU72	1.13/0 1	.0002	324
325°	96.15	6 542	160	0.2176	295,4	900.2	1185 6	809.0 110	и 1	0 470E	1.1346 1	60ET	2054
326°							1185.9	808.2 110					325°
327	97.49			0.2205				807.3 110			1,1321 1		326
	98,85			0.2234			1186.1				1.1297 1		327
	100.23			0.2263			1186.4	806.5 110			1.1273 1		328
329	101.63	9,910	4,30	0.2293	299.0	00/.1	1186.6	805.6 110	rt.0	U.4/38	1.1249 1	1,000/	329
TO+0	1450.B	. X-77	7 K #+ 11	no non R +	n []aa	2 80 02	717. A-1	/T-1.286X	10-8.	144 A	A 1859 [1	ī 2A	7847

Table 1: Temperatures

Temp.	Pressur lbs. At	re tmos*	Sp. Yol. cu. ft. per lb.	Density ibs. per	Heat of the liquid	Latent heat of	Total heat of steam	Interna B. 1 Evap.	Energy L. u. Steam	Entrop Water Evap.		Temp. Fahr.
t	p		v or s	1/y	h or q	evap. Lorr	H	l or e	E	nore L/Torr		t t
330°		7.01	4 306	0.2322	•		1186.9	804.8	1105.0	0.4771 1.122	·	330°
331		7.11		0.2353			1187.1		1105.2	0.4784 1.120		331
332		7.21		0.2384			1187.4		1105.4	0.4797 1.117		332
333		7.31		0.2415			1187.6		1105.6	0.4810 1.115		333
334	108.8 7	7.40	4.088	0.2446	304.7	883.1	1187.8	801.4	1105.8	0.4824 1.112	7 1.5951	334
335°	110.3	7.50	4.035	0.2478	305.8	882 3	1188.1	800.5	1106.0	0.4837 1.110	3 1 5040	335°
336		7.61		0.2510			1188.3		1106.1	0.4850 1.107		336
337		7,72		0.2542			1188.6		1106.3	0,4863 1,105		337
338		7.82	3.884	0.2575			1188.8	798.0	1106.5	0.4876 1.103		338
339	116.4	7.92	3.835	0.2608	309.9	879.1	1189.0	797.2	1106.7	0.4889 1.100	8 1.5897	339
34 0°	118.0	8.03	3 787	0.2641	311.0	878 3	1189.3	796 3	1106.9	0,4902 1,098	4 1 5886	340°
341		8.14		0.2675			1189.5		1107.0	0.4915 1.096		341
342		8,25		0.2709			1189.7		1107.2	0.4928 1.093		342
343		8,36		0.2743			1190.0	793.7	1107.4	0.4941 1.091	3 1.5854	343
344	124.4	8.47	3.600	0.2778	315.1	875.1	1190.2	792.9	1107.6	0.4954 1.088	9 1.5843	344
345°	126,0 8	8.58	3.555	0.2813	316.2	874.2	1190.4	79 2 0	1107.8	0.4967 1.087	5 1.5832	345°
346		8.69		0.2848			1190.6		1108.0	0.4980 1.084		346
347		8.80	3,468	0.2884	318.3	872.6	1190.9	790.3	1108.1	0.4993 1.081	8 1.5811	347
348		8.92		0.2920			1191.1		1108.3	0.5006 1.079	4 1.5800	348
349	132.8	9.04	3,383	0.2956	320.3	871.0	1191.3	788.6	1108.5	0.5019 1.077	1 1.5790	349
350°	134.6	9.16	3,342	0.2992	321.4	870.1	1191,5	787.7	1108.6	0.5032 1.074	8 1 5780	350°
351		9.28		0.3029			1191.8		1108.8	0.5045 1.072		351 ·
352	138.1	9,40	3,261	0.3067	323.5	868.5	1192.0	786.0	1109.0	0.5058 1.070		352
353		9.52		0.3105			1192.2		1109.2	0.5071 1.067		353
354	141.7	9.64	3.182	0.3143	325.6	866.8	1192.4	784.2	1109.3	0.5084 1.065	3 1.5737	354
355°	143.5	9.76	3,143	0.3182	326,6	866.0	1192.6	783.4	1109.5	0.5097 1.063	0 1.5727	355°
356	145.4	9.89	3,105	0.3221	327.7	865.2	1192.9	782.5	1109.7	0.5110 1.060	7 1.5717	356
357	147.2 10			0.3261			1193,1		1109.8	0.5123 1.058	* .	357
358	149.1 10	-		0.3301			1193.3		1110.0	0.5136 1.056		358
-359	151.0 10	0,28	2.993	0.3341	330,8	802.7	1193.5	119.9	1110.2	0.5149 1.053	1,5080	359
360°	153.0 1	0.41	2,957	0.3382	331.9	861.8	1193.7	779.0	1110.4	0.5162 1.051	4 1.5676	360°
36T	154.9 1	0.54	2,922	0.3423	332.9	861.0	1193.9	778.1	1110.5	0.5174 1.049	1.5665	361
362	156.9 1		-	0.3464			1194.1		1110.7	0.5187 1.046		362
363	158.8 1			0.3505			1194.4		1110.8	0.5200 1.044		363
364	160.8 1	0.94	2.820	0.3546	330,1	6,50,5	1194.6	113.3	1111.0	0.5213 1.042	22 1,3033	364
365°	162,9 1	1.08	2.787	0,3588	337,1	857.7	1194.8	774.6	1111.1	0.5225 1.040	0 1.5625	365°
366	164.9 1			0.3631			1195.0		1111.3	0.5238 1.037		366
367	167.0 1			0.3674			1195.2		1111.4	0.5251 1.035		367
368 369	169.0 1 171.1 1		2,690 2,658	0.3717 0.3761			1195,4 1195,6		1111.6 1111.8	0.5263 1.033 0.5276 1.030		368 369
305	1/1.1 1	1.04	2.036	0.5701	341.3	034,2	1193,0	//1.0	1111.0	0.3270 1.030	79 1,3363	309
370°	173.3 1	1.79	2.627	0.3806			1195.8		1111.9	0.5289 1.028		370°
371	175,4 1			0.3851			1196.0		1112.1	0.5301 1.020		371
372	177.6 1			0.3896 0.3942			1196.2		1112.2 1112.4	0.5314 1.024 0.5327 1.023		372 373
373 374	179.7 1 181.9 1			0.3998			1196.4 1196.6		1112.4	0.5327 1.02.		374
375°				0.4034			1196.8		1112.7	0.5352 1.013		
376	186.4 1			0.4081			1197.0	764.8	1112.9	0.5364 1.015		376
377 378	188.7 1 190,9 1			0,4129 0,4177			1197.2 1197.4		1113.0 1113.2	0.5376 1.012 0.5389 1.010		377 378
379	190,9 1			0,4225			1197.4	762.1	1113.2	0.5369 1.010		
7.0			_,,									

^{*1} atmo (standard atmosphere) = 760 mms. of Hg. by definition = 29.921 ins. of Hg. = 14.696 lbs. per sq. in.

For water, at 345°(126 lbs.), sp. vol., v'or σ=0.0179 cu. ft. per lb.; \(\frac{1}{2}\psi = 55.8\) lbs. per cu. ft.; \(\frac{144 \text{ Apv'} = 0.42 \text{ B.t.u.}}{144 \text{ Apv'} = 0.42 \text{ B.t.u.}}\)

at 370°(173 lbs.), v'or σ=0.0183

(14)

Table 1: Temperatures

Temp.	Pres	EUFA	Sp. Vol.	Density	Heat	Latent	Total		i Energy		Entropy		Temp.
Fahr.	ibs.	Atmos	per lb.	lbs. per cu. ft.	of the liquid	evap.	heat of steam	Evap.	t. u. Steam	Water	Evap.	Steam	Fahr.
t	P	-	A 01 8	1/y	h or q	Lorr	Н	i or p	E	n or ø	L/T or r/	T N or φ	t
380°	195.6	13.31	2,340	0.427	352.9	844.8	1197.7	761.2	1113.5	0.5413	1.0060	1.5473	380 °
381	197.9	13.47		0.432			1197.9		1113.6			1.5464	381
382		13.63	2.287		355.0		1198.1		1113.8		1.0015		382
383		13.79		0.442			1198.3		1113.9		0.9993		383
384	205.1	13.96	2,236	0.447	357.2	841.5	1198.5	/5/.0	1114.1	0.5404	0.9971	1.5435	384
385°	207.6	14.13		0.452	358.2	840.5	1198.7		1114,2			1.5426	385°
386		14.30		0.457	359.3		1198.9		1114.4			1.5416	386
387		14.47		0.463	360.3		1199.0		1114.5		0.9906		387
388		14.64		0.468			1199.2		1114.6		0.9884		388 389
389	217.0	14.81	2.113	0.473	302.4	837,0	1199.4	/33.1	1114.8	0.5520	0.9862	1,3300	309
390 °	220.2	14.98	2.089	0.479	363.5	836.1	1199.6	752.2	1114.9		0.9840		390 °
391		15.16	2.066	0.484	364.6		1199.8		1115.1		0.9818		391
392		15.34	2.043	0.489			1199.9		1115.2		0.9796		392
393		15.52		0.495			1200.1		1115.3		0.9774		393
394	230.7	15.70	1.999	0.500	367.7	832.5	1200.3	748.5	1115.4	0.5590	0.9752	1,5342	394
395°		15.88		0.506			1200.4		1115.6		0.9730		395°
396		16.07		0.512			1200.6		1115.7		0.9708		396
397		16.25		0.517			1200.8		1115.9		0.9687		397
398		16.43		0.523			1201.0		1116.0		0.9665		398
399	244.3	16.62	1.892	0.529	3/3.0	828.1	1201.1	743,9	1116.1	0.5651	0.9644	1,3293	399
4 00°	247.1	16.81	1.872	0.534	374.1	827.2	1201.3	743.0	1116.3	0.5663	0.9623	1.5286	400°
410		18.80		0,596	384.7		1202.9		1117.6		0.9409		410
420		20.97		0.662			1204.4		1118.9	0.5908	0.9198		420
430		23.34		0.735	406.2		1205.8		1120.0		0.8990		430
440	380.8			0.814	417.0		1207.1		1121.1		0.8785		440
450°	422.	28.7	1.11	0.90	428.	780.	1208.	695.	1122.	0.627	0.858	1.485	450°
460	466.	31.7 35.0	1.00	1.00 1.10	439. 450.	770. 760.	1209.	685.	1123.	0.639	0.837	1.476	460
470	514. 565.	38.4	0.91 0.83	1.21	462.	749.	1210. 1211.	675. 664.	1124. 1124.	0.651 0.662	0.817 0.797	1.468 1.459	470
480	620.	42.2	0.75	1.32	473.	738.	1211.	654.	1125.	0.674	0.777	1.459	480
490	020.	72.2	0.75	1.52	4,5.	750.	1211.	054.	1125.	0.074	0.777	1.731	490
500°	679.	46.2	0.69	1.45	484.	727.	1211.	643.	1125.	0.686	0.757	1.443	500°
51 0	743.	50.5	0.63	1.59	496.	715.	1211.	632.	1125.	0.698	0.737	1.435	510
520	810.	55.1	0.57	1.74	507.	703.	1210.	620.	1125.	0.709	0.718	1.427	520
53 0	883.	60.1	0.52	1.91	519.	690.	1209.	608.	1124.	0.7	0.698	1.418	530
54 0	960.	65.3	0.48	2.08	531.	677.	1208.	596.	1123.	0.732	0.678	1.409	54 0
550 °	1043.	70.9	0.44	2.28	542.	664.	1206.	583.	1121.	0.743	0.657	1.400	550°
560	1130.	76.9	0.40	2.49	554.	650.	1204.	570.	1119.	0.754	0.637	1.391	560
570	1224.	83.3	0.37	2.71	566.	635.	1201.	556.	1117.	0.765	0.616	1.381	570
580	1323. 1428.	90.0	0.34	2.96	578.	619.	1197. 1193.	542.	1115.	0.776	0.595	1.371	580
59 0	1440.	97.2	0.31	3.23	591.	602.	1193.	527.	1112.	0.787	0.574	1.361	59 0
600°		104.8	0.28	3.53	604.	585.	1189.	511.	1108.	0.799	0.552	1.351	600°
		112.8	0.26	3.9		566.		494.			0.530		610
620 630	1783. 1916.	121.3 130.4	0.24 0.22	4.2 4.6		546. 525.		476. 457.			0.506 0.482		620
640	2056.	139.9	0.22	4.6 5.1		501.		436.			0.464		6 3 0 6 4 0
660	2204. 2361.	160.6	0.18 0.16	5.6 6.2		475. 4 4 6.		413. 387.		t'	0.428 0.398		850°
670	2526.	171 0	0.16	6.2 6.9		411.		357.			0.364		660
690	2883.	196.2	0.14	9.0		316.		274.			0.304		670 690
706.1		217.8		20.1		000.		000.		•	0.000		706.1
				-									

T°=t°+459.6; J=777.5 ft. lbs. per B.t.n. [log=2.89 071]; A=1/σ=1.286×10-1144 A=0.1852 [log=1.26764].

For water, at 400° (247 lbs.), sp. vol., v' or σ=0.019 cu. ft. per lb.; 1/v'=53.5 lbs. per ou. ft.; 144 Apv'=0.86 B.t.n.; at 600° (1574 lbs.), e v' or σ=0.024 " ; 144 Apv'=6.9 ".

(15)

Table 2. Saturated Steam: Pressure Table

Press.	Temp.	Press.	Sp. Vol.	Density	Heat of the	Latent heat of	Total	Internal B. 1	Energy		Entropy		Press
ibs.	Deg. F.	Atmos*	cu. ft. per lb.	lbs. per cu. ft.	of the liquid	evap.	steam		t. u. Steam	Water	Evap.	Steam	lbs.
p	t	_	v or s	1/ _V	h or q	Lorr	н	l or p	E		/T or r/T		P
1	101.83	0.068		0.00300		1034.6			1042.7	0.1327			1
2	126.15	0.136		0.00576		1021.0			1050.7	0.1749			2 3
3 4	141.52	0.204 0.272		0.00845 0.01107		1012.3 1005.7			1055.8 1059.5	0.2008			4
*	153.01	0.212	90.3	0.01107	120.9	1003.7	1120.5	330.0	1035.3	0,2190	1,0410	1.0014	₹ ,
5	162.28	0.340	73.33	0.01364	130.1	1000.3	1130.5	932.4	1062.5	0,2348	1.6084	1.8432	5
6	170.06	0.408	61.89	0.01616	137.9	995.8	1133.7	927.0	1064.9	0.2471	1.5814	1.8285	6
7	176.85	0.476		0.01867	144.7		1136.5		1067.1	0.2579			7
8	182.86	0.544		0.02115	150.8		1139.0		1069.0	0.2673			8
9	188.27	0.612	42.36	0.02361	156.2	985.0	1141.1	914.4	1070.5	0.2756	1.5202	1.7958	9
10	193.22	0.680	38.38	0.02606	161.1	982.0	1143.1	910.9	1072.0	0.2832	1.5042	1.7874	10
ii	197.75			0.02849	165.7		1144.9		1073.4	0.2902			11
12	201.96	0.816	32.36	0.03090	169.9	976.6	1146.5	904.8	1074.7	0.2967	1.4760	1.7727	12
13	205.87	0.885		0.03330	173.8		1148.0		1075.8	0.3025			13
14	209.55	0.953		0.03569	177.5		1149.4		1076.8	0.3081			14
14.7 15	212.00 213.0	1.000 1.021		0.03732 0.03806	180.0 181.0		1150.4 1150.7		1077.5 1077.8	0.3118 0.3133			14.7 15
16	216.3	1.089		0.03300	184.4		1152.0		1077.8	0.3183			16
17	219.4	1.157		0.04277	187.5		1153.1		1079.6	0.3229			17
18	222.4	1.225	22.16	0.04512	190.5	963.7	1154.2	889.9	1080.4	0,3273	1.4127	1.7400	18
19	225.2	1.293	21.07	0.04746	193.4	961.8	1155.2	887.8	1081.1	0.3315	1.4045	1.7360	19
20	228.0	1 261	20.08	0.04090	106 1	060.0	1156.0	0010	1001.0	0 2255	1 2065	1 7200	00
21	228.0 230.6	1.361 1.429		0.04980 0.05213	196.1 198.8		1156.2 1157.1		1081.9 1082.6	0.3355			20 21
22	233.1	1.423		0.05445	201.3		1158.0		1083.2	0.3430			22
23	235.5	1.565		0.05676	203.8		1158.8		1083.9	0.3465			23
24	237.8	1.633	16.93	0.05907	206.1	953.5	1159.6	878.5	1084.5	0.3499			24
	040.	7 501	16.00	0.067.4	000.4	050.0	77.50.4	075.0	2005 2				
25	240.1 242.2	1.701 1.769		0.0614 0.0636	208.4 210.6		1160.4 1161.2		1085.1 1085.6	0.3532			25 06
26 27	244.4	1.837		0.0659	210.0		1161.2		1085.0	0.3564			26 27
28	246.4	1.905	14.67		214.8		1162.6		1086.7	0.3623			28
29	248.4	1.973	14.19	0.0705	216.8		1163.2		1087.2	0.3652			29
		•											
30	250.3	2.041		0.0728	218.8		1163.9		1087.7	0.3680			30
31 32	252.2 254.1	2.109 2.178	12.93	0.0751 0.0773	220.7 222.6		1164.5 1165.1		1088.2 1088.6	0.3707 0.3733			31 32
33	255.8	2.246	12.57		224.4		1165.7		1089.1			1.6914	33
34	257.6	2.314	12.22		226.2		1166.3		1089.5			1.6891	34
35	259.3	2.382		0.0841	227.9		1166.8		1089.9			1.6868	35
36	261.0	2.450 2.518		0.0863 0.0886	229.6 231.3		1167.3 1167.8		1090.3 1090.7			1.6846 1.6824	36
37 38	262.6 264.2	2,586		0.0908	232.9		1168.4		1090.7			1.6802	37 38
39	265.8	2.654		0.0931	234.5		1168.9		1091.4			1.6781	
40	267.3	2.722		0.0953	236.1		1169.4		1091.8			1.6761	
41 42	268.7 270,2	2.790 2.858		0.0976 0.0998	237.6 239.1		1169.8 1170.3		1092.2			1.6741	41 42
43	271.7	2.926		0.1020	240.5		1170.3		1092.5 1092.8			1.6721 1.6702	
44	273.1	2.994		0.1043	242.0		1171.2		1092.3			1.6683	
-													
45	274.5	3.062		0.1065	243.4		1171.6		1093.5			1.6665	
46 47	275.8 277.2	3.130 3.198		0.1087 0.1109	244.8 246.1		1172.0 1172.4		1093.8 1094.1			1.6647 1.6630	
48	277.2 278.5	3.198		0.1109	240.1		1172.4 1172.8		1094.1			1.6613	
49	279.8	3.334		0.1151	248.8		1172.8		1094.7			1.6597	

*1 atmo (standard atmosphere) = 760 mms. of Hg. by def. = 29.921 ins. of Hg. = 14.696 lbs. per sq. in. For water, at 15 lbs., sp. vol., v' or σ = 0.0167 cu. ft. per lb.; 1/v' = 59.8 lbs. per cu. ft.; 144 Apv' = 0.05 B.tu.; at 40 lbs., v' or σ = 0.0171 "; 1/v' = 58.3 "; 144 Apv' = 0.13 ".

Table 2: Pressures

	_		Sp. Vol.	Density	Heat	Latent	Total	Interna	l Energy		Entropy		_
Press.	Temp. Deg. F.	Press. Atmos	cu. ft.	Density ibs. per cu. ft.	of the liquid	heat of evap.	heat of steam		t. u. Steam	Water	Evap.	Steam	Press.
p	t	-	8 10 V	1/y	h or q	Lorr	Н	l or p	E		L/T or r/1		p
50	281.0	3,402	8.51	0.1175	250.1	923.5	1173.6	845,0	1095.0	0,4113	1,2468	1.6581	50
51	282.3	3.470		0.1197		922.6		844.0	1095.3		1.2435		51
52	283.5	3.538		0.1219		921.7			1095.5		1.2402		52
53	284.7	3.606		0.1241		920.8			1095.8		1.2370		53
54	285.9	3.674	7.91	0.1263	233.1	919.9	11/5.0	041.1	1096.1	0.4160	1.2339	1.0319	54
55	287.1	3.742	7.78	0.1285	256.3	919.0	1175.4	840.2	1096.3	0,4196	1,2309	1,6505	55
56	288,2	3.810		0.1307		918.2			1096.6		1.2278		56
57	289.4	3.878		0.1329		917.4			1096.8		1.2248		57
58 59	290.5 291.6	3.947 4.015	7.40	0.1350 0.1372		916.5 915.7			1097.1 1097.3		1,2218 1,2189		58 59
00	271.0	4.013	1,20	0,1372	201.0	713.1	1170.7	000.5	1097.5	0.4231	1,2109	1.0110	03
60	292.7	4.083		0.1394		914.9			1097.6		1.2160		60
61	293.8	4.151		0.1416		914.1			1097.8		1.2132		61
62	294.9	4.219		0.1438		913.3			1098.0		1.2104		62
63 64	295.9 297.0	4,287 4,355		0.1460 0.1482		912.5 911.8			1098.2 1098.4		1,2077 1,2050		63 64
02	271.0	4,555	0.73	0.1402	200.4	311.0	1170.2	032.2	1090.4	0.4330	1.2050	1.0500	OZ.
65	298.0	4.423		0.1503		911.0			1098.7		1.2024		65
66	299.0	4.491		0.1525		910.2			1098.9		1.1998		66
67	300.0 301.0	4.559 4.627		0.1547 0.1569		909.5 908.7			1099.1		1.1972		67
68 69	302.0	4.695		0.1590		908.0			1099.3 1099.5		1.1921		68 69
00	502.0	1,055	0.23	0.2550	271.0	300.0	1175.0	020.1	1000.0	0.1550	1.1721	1.0017	00
70	302,9	4,763		0.1612		907.2			1099.7		1.1896		70
71	303.9	4.831		0.1634		906.5			1099.9		1.1872		71
72 73	304.8 305.8	4.899 4.967		0.1656 0.1678		905.8 905.1			1100.1 1100.3		1.1848 1.1825		72
7 4	306,7	5,035		0.1699		903.1			1100.5		1.1823		73 7 4
-			0.02	0033					1100.0	0.1102	2.2002	2.0200	
75	307.6	5.103		0.1721		903.7			1100.6		1.1778		75
76	308.5 309.4	5.171 5.239		0.1743 0.1764		903.0 902.3			1100.8		1.1755		76
77 78	310.3	5.307		0.1786		901.7			1101.0 1101.2		1.1732 1.1710		77 78
79	311.2	5.375		0.1808		901.0			1101.4		1.1687		79
											•		
80	312.0	5.444		0.1829		900.3			1101.6		1.1665		80
81 82	312.9 313.8	5.512 5.580		0.1851 0.1873		899.7 899.0			1101.7 1101.9		1.1623	1.6190	81 82
83	314.6	5.648		0.1894		898.4		-	1101.9		1.1602		83
84	315.4	5.716		0.1915		897.7			1162.2		1.1581		84
or	216.2	r 704		0.7025	000.0	0077	1102 4	016.5	1100.4	0.4500			07
85 86	316.3	5.784		0.1937 0.1959		897.1 896.4			1102.4		1.1561		85 96
86 87	317.1 317.9	5.852 5.920		0.1939		895.8			1102.6 1102.7		1.1540 1.1520		86 87
88	318.7	5.988		0.2001		895.2			1102.9		1.1500		88
89	319.5	6.056		0.2023		894.6			1103.0		1.1481		89
00	320.3	6 104	4 00	0.2044	200 5	902.0	1104 4	0120	1102.0	0.4644	1 1461	1 6105	00
90 91	320.3 321.1	6.124 6.192		0.2044 0.2065		893.9 893.3			1103.2 1103.3		1.1461 1.1442	-	90 91
92	321.8	6.260		0.2087		892.7			1103.5		1.1423		92
93	322.6	6.328		0.2109	292.9	892.1	1185.0	811.0	1103.6	0.4674	1.1404	1.6078	93
94	323.4	6.396	4.69	0.2130	293.7	891.5	1185.2	810.4	1103.8	0.4684	1.1385	1.6069	94
95	324.1	6.464	4 65	0.2151	294 5	890.9	1185 4	809 7	1103.9	0 4694	1.1367	1 6061	95
96	324.9	6.532		0.2172		890.3			1104.1		1.1348		96
97	325.6	6.600	4.56	0.2193	296.1	889.7	1185.8	808.5	1104.2		1.1330		97
98	326.4	6.668	-	0.2215		889.2			1104.4		1.1312		98
99	327.1	6.736	4.47	0.2237	297.6	888. 6	1186,2	807.2	1104.5	0.4733	1.1295	1.6028	99
To=t	°+459.6	3: J=777	.5 ft. 1b	s, per B.t.;	. Flor=	2.89 073	1: A=1/	J=1.286	×10-3; 1	44 A=0.	1852 []0	$\sigma = \overline{1.267}$	7647.

T°=t°+459.6; J=777.5 ft.1bs. per B.t.u. [log=2.89 071]; $A=1/J=1.286\times10^{-3}$; $144\ A=0.1852\ [log=\overline{1}.26764]$. For water, at 65 lbs., sp. vol., v' or $\sigma=0.0174\ cu.$ ft. per lb.; 1/v'=57.4 lbs. per cu. ft.; $144\ Apv'=0.21\ B.t.u.$; at 90 lbs., v' or $\sigma=0.0176$ " ; 1/v'=56.8 " ; $144\ Apv'=0.30$. (17)

Table 2: Pressures

I GOI				-	** *							
Press.	Temp.	Press Atmos*	Sp. Vol.	Density the ner	Heat of the	Latent best of	Total heat of	Interna	Energy t. u.		Entropy	Press
ibs.	Deg. F.	Atmos*	per ib.	cu. ft.	liquid	evap.		Evap.	Steam	Water	Evap. Steam	lbs.
p	t		A OL C	1/y	h or q	Lorr	H	l or p	E		L/Torr/T Norø	P
100	327.8	6.80		0.2258	•	888.0			1104.6		1,1277 1,6020	100
101	328.6	6.87		0.2279		887.4			1104.8		1.1260 1.6012	101
102	329.3	6.94		0.2300			1186.7		1104.8			102
	330.0	7.01		0.2322		-	1186.9		1104.9		1,1242 1,6004	
103 104	330.7	7.08		0.2343			1185.9		1105.0		1,1225 1,5996 1,1208 1,5988	103
703	330.7	7.00	4.200	0,2373	301.3	003.0	1107.0	004.4	1105.1	0.4700	1.1200 1.3900	104
105	331.4	7.14	4 230	0.2365	302.0	885.2	1187 2	803.6	1105.3	0.4780	1.1191 1.5980	105
106	332.0	7.21		0.2386			1187.4		1105.4		1.1174 1.5972	106
107	332.7	7.28		0.2408		884.1			1105.5		1.1158 1.5965	107
108	333.4	7.35		0.2429		883.6			1105.7		1.1141 1.5957	108
109	334.1	7.42		0.2450			1187.9		1105.8		1.1125 1.5950	109
400				0.2.00				002,0		0.1025	2.2200 2.0000	200
110	334.8	7.49	4.047	0.2472	305.5	882.5	1188.0	800.7	1105.9	0.4834	1.1108 1.5942	110
īii	335,4	7.55	4.012	0.2493			1188.2		1106.0		1.1092 1.5935	111
112	336.14	7.62	3.978	0.2514			1188.4		1106.2		1.1076 1.5928	112
113	336.8	7.69	3,945	0.2535		880.9			1106.3		1.1061 1.5921	113
114	337.4	7.76	3.912	0.2556	308.3	880.4	1188.7	798.5	1106.4	0.4869	1.1045 1.5914	114
115	338.1	7.83	3,880	0.2577	309.0	879.8	1188.8	797.9	1106.5	0.4877	1,1030 1,5907	115
116	338.7	7.89	3.848	0.2599	309.6	879.3	1189.0	797.4	1106.6	0,4886	1.1014 1.5900	116
117	339,4	7.96	3.817	0,2620	310.3	878.8	1189.1	796,8	1106.8	0.4894	1.0999 1.5893	117
118	340,0	8.03		0.2641	311.0	878.3	1189.3	796.3	1106.9	0.4903	1.0984 1.5887	118
119	340,6	8.10	3.756	0.2662	311.6	877.8	1189.4	795.7	1107.0	0.4911	1.0969 1.5880	119
120	341.3	8.17		0.2683		-	1189.6		1107.1		1.0954 1.5873	120
121	341.9	8.23		0.2705			1189.7		1107.2	-	1.0939 1.5866	121
122	342.5	8.30		0.2726			1189.8		1107.3		1.0924 1.5859	122
123	343.2	8.37		0.2748			1190.0		1107.4		1.0910 1.5853	123
124	343.8	8.44	3.611	0.2769	314.9	875.2	1190.1	793,1	1107.6	0.4951	1,0895 1,5846	124
105	244.4	0.50	2 502	0.0701	215 5	0747	1100 2	702.6	11077	0.4050	1 0000 1 5020	105
125	344.4	8.50		0.2791			1190.3		1107.7		1.0880 1.5839	125
126 127	345.0 345.6	8.57 8.64		0.2812 0.2833			1190.4 1190.5		1107.8		1.0865 1.5832	126 127
128	346.2	8.71		0.2854		873.3			1107.9 1108.0		1.0851 1.5825 1.0837 1.5819	128
129	346.8	8.78		0.2875			1190.8		1108.1		1.0823 1.5813	129
170	340.0	0.70	3.770	0.2073	310.0	0/4.0	1150.0	150.5	1100.1	0.4990	1.0023 1.3013	129
130	347.4	8.85	3 452	0.2897	3186	872.3	1191.0	790 O	1108.2	A 400R	1,0809 1,5807	130
131	348.0	8.91		0.2918		871.8			1108.3		1.0796 1.5801	131
132	348.5	8.98		0.2939			1191.2		1108.4		1,0782 1,5795	132
133	349.1	9.05	-	0.2960			1191.3		1108.5		1.0769 1.5789	133
134	349.7	9.12		0.2981		-	1191.5		1108.6		1,0755 1,5783	134
135	350.3	9.19	3.331	0.3002	321.7	869,9	1191,6	787.5	1108,7	0.5035	1.0742 1.5777	135
136	350.8	9,25	3.308	0.3023	322.3	869.4	1191.7	787.0	1108.8	0.5043	1.0728 1.5771	136
137	351.4	9.32	3.285	0.3044			1191.8	786.5	1108,9	0.5050	1.0715 1.5765	137
138	352.0	9.39	3.263	0.3065	323.4	868.5	1192.0	786.0	1109.0	0.5057	1.0702 1.5759	138
139	352.5	9.46	3.241	0.3086	324.0	868.1	1192.1	785.5	1109.1	0.5064	1.0689 1.5753	139
140	353.1	9.53		0.3107			1192.2		1109.2		1.0675 1.5747	
141	353.6	9.59		0.3129			1192.3		1109.3		1.0662 1.5741	141
142	354.2	9.66		0.3150		866.7			1109.4		1,0649 1.5735	142
143	354.7	9.73		0.3171			1192.6		1109.5		1.0637 1.5730	143
144	355.3	9.80	3.133	0.3192	<i>3</i> 26.9	865.8	1192.7	783.2	1109.6	0.5100	1.0624 1.5724	144
4			2 ***	0.2022	204 4	000	1100 0	#00 F	7700 -	0 510-	1 0010 1 77-0	44-
145	355.8	9.87		0.3213			1192.8		1109.6		1.0612 1.5719	145
146	356.3	9.93		0.3234			1192.9		1109.7		1.0599 1.5713	146
147 148	356.9 357.4			0.3255 0.3276			1193.0 1193.2		1109.8 1109.9		1.0587 1.5708	147 148
149	357. 4 357.9			0.3276			1193.2		1110.0		1.0574 1.5702 1.0562 1.5697	
TET	331.9	10,14	3.033									149
		4 3 3	-4		Λ	4 TT L.	- 3-6-141	00	007 (. e TT 1	4 000 lb	z

^{*1} atmo (standard atmosphere) = 760 mms. of Hg. by definition = 29.921 ins. of Hg. = 14.696 lbs. per sq. in. For water, at 115 lbs., sp. vol., v' or σ =0.0178 cu. ft. per lb.; 1/v'=56.0 lbs. per cu. ft.; 144 Apv'=0.38 B.t.u.; at 140 lbs., v' or σ =0.0180 "; 1/v'=55.4 "; 144 Apv'=0.47 ".

Table 2: Pressures

I au		A 1 C 3 3 1		0	114		T		_				
Press.	Temp.	Press.	op. voi.	Density lbs. per	Heat of the	heat of	Total heat of	Internal	Energy	,	Entropy		Press.
ibs.	Deg. F.	Atmos	cu. ft. per lb.	lbs. per cu. ft.	liquid	evap.		Evap.	Steam	Water	Evap.	Steam	lbs.
p	t		V OT 8	1/4	h or q	L or r	H	l or p	E	n or ø	L/Torr/T	N or ϕ	p
150	358.5	10.21	3.012	0.3320	330.2	863.2	1193.4	780.4	1110,1	0.5142	1.0550	1 5692	150
151	359.0	10.28		0.3341			1193.5		1110.2		1,0538		151
152	359.5	10.34		0.3362			1193.6		1110.3		1.0525		152
153	360.0	10.41	2,956	0.3383	331.9	861.8	1193.7	779.0	1110,4	0.5162	1.0513	1.5675	153
154	360.5	10.48	2,938	0.3404			1193.8		1110,4		1.0501		154
••													
155	361.0	10.55	2.920	0.3425	332.9	861.0	1194.0	778.1	1110.5	0.5175	1.0489	1,5664	155
156	361.6	10.61	2.902	0.3446	333.5	860.6	1194.1		1110.6	0.5182	1.0477	1.5659	156
157	362.1	10.68		0.3467			1194.2		1110.7		1.0466		157
158	362.6	10.75		0.3488			1194.3		1110.8		1.0454		158
159	363.1	10.82	2.851	0.3508	335.1	859.3	1194.4	776.3	1110.8	0.5201	1,0443	1.5644	159
400						~~~							
160	363.6	10.89		0.3529			1194.5		1110.9		1,0431		160
161	364.1	10.96		0.3549			1194.6		1111.0		1.0420		161
162 163	364.6	11.02		0.3570			1194.7		1111.1		1.0409		162
164	365.1 365.6	11.09		0.3591 0.3612			1194.8 1194.9	774.1	1111.2		1.0398 1.0387		163
104	305.0	11.16	2.709	0.3012	337.1	031.4	1194,9	//4,1	1111.2	0.3233	1,0307	1,3020	164
165	366.0	11.23	2 753	0.3633	338 2	856 B	1195.0	773 6	1111.3	0 5230	1.0376	1 5615	165
166	366.5	11.30		0.3654			1195.1		1111.4		1.0365		166
167	367.0	11.36		0.3675			1195.2		1111.4		1.0354		167
168	367.5	11.43		0.3696			1195.3		1111.5		1.0343		168
169	368.0	11.50		0.3717			1195,4	771.9			1.0332		169
					-								
170	368.5	11.57	2.675	0.3738	340.7	854.7	1195.4	771.5	1111,7	0.5269	1.0321	1.5590	170
171	368.9	11.64	2.660	0.3759	341.2	854.3	1195.5	771.1	1111.7	0.5275	1.0311	1.5586	171
172	369.4	11.70		0.3780			1195.6	770.7			1.0300		172
173	369.9	11.77		0.3801			1195.7		1111.9		1.0289		173
174	370.4	11.84	2.616	0.3822	342.7	853.1	1195.8	769.8	1112.0	0.5293	1.0278	1.5571	174
175	370.8	11.91		0.3843			1195.9	769.4			1.0268		175
176	371.3 371.7	11.97		0.3864			1196.0	769.0			1.0257		176
177 178	372,2	12,04 12,11		0.3885 0.3906	344.2		1196.1	768.6 768.2			1.0246 1.0235		177
179	372.7	12.11		0.3927			1196.2	767.8			1.0235		178 179
113	314.1	12.10	4,547	0.3921	373.4	031.2	1150.5	707.8	1112,4	0.3344	1.0223	1.3347	119
180	373.1	12,25	2.533	0.3948	345.6	850.8	1196.4	767.4	1112.4	0.5328	1.0215	1 5543	180
181	373.6	12,32	-	0.3969			1196.5	767.0	-		1,0205		181
182	374.0	12,38	2.507	0.3989	346.6	850.0	1196.6	766.6	1112.6		1.0195		182
183	374.5	12,45	2.494	0.4010	347.1	849.6	1196.7	766.2	1112.6	0.5345	1.0185	1.5530	183
184	374.9	12.81	2.481	0.4031	347.6	849.2	1196.8	765.8	1112.7	0.5%: 1	1.0174	1.5525	184
185	375.4	12.59		0.4052			1196.8	765.4			1.0164		185
186	375.8	12.66		0.4073			1196,9	765.0			1.0154		186
187	376.3	12.72		0.4094			1197.0	764.6			1.0144		187
188	376.7	12.79		0.4115			1197.1		1113.0		1,0134		188
189	377.2	12.86	2.418	0.4136	349.9	847.3	1197.2	763.8	1113.0	0.5378	1.0124	1.5502	189
190	377.6	12,93	2 406	0.4157	250.4	846 Q	1197.3	762 4	1113.1	O 5284	1.0114	1 5/09	190
191	378.0	13.00		0.4178	350. 1	846.5	1197.3	763.0			1.0105		191
192	378.5	13.06	2.333	0.4199			1197.4	762.6			1.0095		192
193	378.9	13,13		0.4220			1197.5	762.2			1,0085		193
194	379,3	13.20		0.4241			1197.6		1113.4		1.0076		194
					- "		-	•	-				
195	379.8	13.27		0.4262			1197.7		1113.4	0.5410	1.0066	1.5476	195
196	380.2	13,34	2,335	0.4283			1197.8		1113.5		1.0056		196
197	380.6	13,40		0.4304			1197.8		1113.6		1.0047		197
198	381.0	13.47		0.4325			1197.9		1113.6		1.0038		198
199	381.4	13.54	2.301	0.4346	354.4	843.6	1198.0	759.9	1113.7	0,5431	1.0029	1.5460	199
To=t	°+459.6	3: J=777	.5 ft. lbs	. per B.t.u.	llog=2	.89 071]; A=1/3	=1.286	3×10-*: 3	44 1=).1852 [le	g=1.26	6641.

Table 2: Pressures

Press.	Temp. Deg. F.	Press Atmos*	Sp. Vol. cu. ft. per lb.	Density ibs. per cu. ft.	Heat of the liquid	Latent heat of evap.	Total heat of steam	Internal B. 1 Evap.		Water	Evap. Steam	Press.
p	t	-	V OF 8	1/y	h or q	Lorr	H	l or p	E	n or #	L/Torr/T Norø	P
200	381.9	13.61	2.290	0.437	354.9	843,2	1198.1	759.5	1113.7	0.5437	1.0019 1.5456	200
201	382,3	13.68	2.279	0.439	355.3	842.8	1198.2	759.2	1113.8	0.5442	1.0010 1.5452	201
202	382.7	13.74	2.269				1198.2		1113.9		1.0001 1.5448	202
203	383.1	13.81	2.258				1198.3		1113.9		0.9992 1.5444	203
204	383.5	13.88	2.247	0.445	356.7	841.7	1198.4	758.0	1114.0	0.5458	0.9982 1.5440	204
205	384.0	13.95	2,237	0 447	257 1	941 A	1198.5	757 6	1114.0	0 5463	0.9973 1.5436	205 ີ
206	384.4	14.02	2,227				1198.5		1114.1		0.9964 1.5432	206
207	384.8	14.08	2,217				1198.6		1114.2		0.9955 1,5428	207
208	385.2	14.15	2.207				1198.7	756.5	1114.2	0.5478	0.9946 1.5424	208
209	385.6	14.22	2.197	0.455	358.8	839.9	1198.8	756.2	1114.3	0.5483	0.9937 1.5420	209
210	386.0	14.29	2.187	0.457	250.2	920.6	1198.8	755 0	1114,4	U E100	0.9928 1.5416	210
211	386.4	14.36	2.177				1198.9		1114.4		0.9920 1.5413	
212	386.8€	14,43	2.167				1199.0		1114.5		0.9911 1.5409	
213	387.2	14.49	2.158				1199.1		1114.5		0.9902 1.5405	
214	387.6	14.56	2.148	0.466	360.9	838.2	1199.1	754.4	1114.6	0.5508	0.9893 1.5401	214
215	388.0	14.63	2.138	0.468	361.4	927 Q	1199.2	754 O	1114.6	0 5512	0.9885 1.5398	215
216	388.4	14.70	2.128			-	1199.3		1114.7		0.9876 1,5394	
217	388.8	14.77	2.118				1199.4		1114.7		0.9867 1.5390	
218	389.1	14.83	2.109				1199.4		1114.8		0.9858 1.5386	
219	389.5	14.90	2.100	0.476	363.0	836.5	1199.5	752.6	1114.8	0.5533	0.9850 1.5383	219
220	389.9	14.97	2.091	0.478	363 4	836.2	1199,6	752.3	1114.9	0 5538	0.9841 1.5379	220
221	390.3	15.04	2.082				1199.6		1115.0		0.9833 1.5376	
222	390.7	15.11	2.073				1199.7		1115.0		0.9824 1.5372	
223	391.1	15.17	2.064				1199,8		1115.1		0.9816 1,5369	
224	391.5	15,24	2.055	0.487	365.0	834.8	1199.8	750.8	1115.1	0.5557	0.9808 1.5365	224
225	391.9	15.31	2.046	0.489	365.5	834 4	1199.9	750 5	1115.2	0.5562	0.9799 1.5361	225
226	392.2	15.38		0.491			1200.0		1115,2		0.9791 1.5358	
227	392.6	15.45		0.493			1200.0		1115.3		0.9783 1.5355	
228	393.0	15.51	2.021	0.495	366.7	833.4	1200.1	749.4	1115.3	0.5577	0.9774 1.5351	228
229	393.4	15.58	2.013	0.497	367.1	833.1	1200.2	749.1	1115.4	0.5582	0.9766 1.5348	229
230	393.8	15.65	2.004	0.499	367.5	832.8	1200.2	748.8	1115.4	0.5586	0.9758 1.5344	230
231	394.1	15.72		0.501			1200.3	748.4	1115.5	0.5591	0.9750 1.5341	
	~ 394.5	15.79		0.503			1200.4		1115.5		0.9741 1.5337	
233	394.9	15.86		0.505			1200.4		1115.6		0.9733 1.5334	
234	395.2	15.92	1.972	0.507	369.0	831.4	1200.5	747.4	1115.6	0.5605	0.9725 1.5330	234
235	395.6	15.99	1.964	0.509	369.4	831.1	1200.6	747.0	1115.7	0.5610	0.9717 1.5327	235
236	396,0	16.06		0.511			1200.6		1115.7		0.9708 1.5323	
237	396.4	16.13					1200.7		1115.8		0.9700 1.5319	
238	396.7	16.20		0.515			1200.7		1115.8		0.9692 1.5316	
239	397.1	16.26	1.932	0.518	3/1.0	829.8	1200.8	745.7	1115.9	0.5629	0.9684 1.5313	239
240	397.4	16.33	-	0.520			1200.9		1115.9		0.9676 1.5309	
241	397.8	16.40		0.522			1200.9	745.0	1116.0	0.5638	0.9668 1.5306	241
242	398,2	16.47		0.524			1201.0		1116.0		0.9661 1.5303	
243 244	398.5 398.9	16.53 16.60		0.526 0.528			1201.1 1201.1		1116.1 1116.1		0.9653 1.5300 0.9646 1.5297	
			001									
245	399.3	16.67		0.530			1201.2		1116.2		0.9638 1.5293	
246 247	399.6 400.0	16.74 16.81		0.532 0.534			1201.2 1201.3		1116.2		0.9630 1.5289 0.9623 1.5286	
248	400.0	16.88		0,534			1201.3		1116.3		0.9615 1.5283	
249	400.7	16.94		0.538			1201.4		1116.4		0.9607 1.5279	
											.696 lbs. per sq. i	

*1 atmo (standard atmosphere) = 760 mms. of Hg. by def. = 29.921 ins. of Hg. = 14.696 lbs. per sq. in. For water, at 215 lbs., sp. vol., \mathbf{v}' or $\sigma = 0.0185$ cu. ft. per lb.; $1/\mathbf{v}' = 54.0$ lbs. per ou. ft.; 144 Ap $\mathbf{v}' = 0.74$ B. t. u.; at 240 lbs., \mathbf{v}' or $\sigma = 0.0186$ "; $1/\mathbf{v}' = 53.6$ "; 144 Ap $\mathbf{v}' = 0.83$ ". (20)

Table 2: Pressures

Press.	Temp.	Press.	cu. ft.	Density lbs. per	Heat of the	heat of	Total heat of	_ B.	l Energy		Entropy		Press.
ibs.	Deg. F.	Atmos	per lb.	cu. Tt.	liquid h or q	evap. Lorr	steam H	Evap. i or ρ	Steam E	Water	Evap. L/T or r/	Steam F Nord	lbs.
P		17.01											P
250 252	401.1 401.8	17.01 17.15		0.541 0.545	375.2 376.0		1201.5 1201.6		1116.4		0.9600	1.5269	250 252
254	402.4	17.28	1.822	0.549			1201.7		1116.6			1.5263	254
256	403.1	17.42	1.809				1201.8		1116.7			1.5256	256
258	403.8	17.56		0.557	378.2	823.7	1201,9	739.5	1116.8			1.5250	258
260	404.5	17.69	1.782	0.561	378.9	823.1	1202.1	738.9	1116.9	0.5719	0.9525	1.5244	260
262	405.2	17.83	1.769	0.565			1202.2	738.2	1117.0	0.5727	0.9511	1.5238	262
264	405.9	17.96	1.756	0.569			1202.3		1117.1	0.5735		1.5232	264
266	406.6	18.10	1.743	0.574			1202.4		1117.2			1.5226	266
268	407.2	18.24	1.731	0.578	381.8	840.7	1202.5	730,4	1117.2	0.5752	U,9408	1.5220	268
270	407.9	18.37	1.718				1202.6		1117.3	0.5760	0.9454		270
272	408.6	18.51	1.705	0.587	383.2		1202.7		1117.4		0.9440		272
274	409.2	18.64		0.591			1202.8		1117.5	0.5776		1.5202	274
276	409.9 410.5	18.78 18.92	1.681				1202.9 1203.0		1117.6 1117.6		0.9412 0.9398		276 278
278	410.5	10.92	1.009	0.399	363,3	617.7	1203.0	133.3	1117.0	0.3794	0.5556	1.3190	210
280	411.2	19.05		0.603			1203.1		1117.7		0.9385		280
282	411.8	19.19		0.608			1203.2		1117.8		0.9371		282
284	412.4 413.1	19.32 19.46	1.635 1.624	0 612		-	1203.3		1117.9		0.9357		284
286 288	413.1	19.40	1.613				1203.4 1203.5		1118.0 1118.1		0.9344 0.9330		286 288
	713.7		1.015	0.020	300.1	011.0	1205.5	130.3	1110.1	0,3632	0.9330	1,5102	
290	414.4	19.73	1,602				1203,6		1118.1		0.9316		290
292	415.0	19.87	1.591				1203.7		1118.2		0.9302		292
294 296	415.6 416.2	20,01 20,14	1.571	0.633			1203.8 1203.9		1118.3 1118.4		0.9289 0.9276		294 296
298	416.8	20.28		0.641			1204.0		1118.4		0.9263		298
000	417.5	00.41	1 551	0.645	200.7	011 2	1004.1	7000	1110 €	0 5070	0.0007	1 5100	
300 310	417.5 420.5	20.41 21.09		0,645 0.666	392.7 395.9		1204.1 1204.5		1118.5 1118.9		0.9251 0.9187		300 310
320	423.4	21.78	-	0.687			1204.9		1119.2		0.9125		320
330	426.3	22,46		0.708	402.2		1205.3		1119.6		0.9065		330
34 0	429.1	23.14	1.372	0.729	405.3	800.4	1205.7	715.9	1119.9	0.6020	0.9006	1.5026	340
350	431,9	23.82	1,334	0.750	408.2	797.8	1206.1	713.3	1120.2	0.6053	0.8949	1.5002	350
360	434.6	24.50	-	0.770	411.2		1206.4		1120.5	0.6085			360
370	437.2	25.18		0.791	414.0		1206.8		1120.8		0.8840		370
380	439.8	25.86		0.812	416.8		1207.1		1121.1		0.8788		380
390	442.3	26.54	1.200	0.833	419.5		1207.4	703,3	1121.4	0.0178	0.8737	1.4915	390
400	444.7	27.22	1.17	0.86	422.	786.	1208.	701.	1122.	0.621	0.868	1.489	400
410	447.2	27.90	1.14	0.88	425.	783.	1208.	699.	1122.	0.624	0.863	1.487	410
420	449.6	28.58 29.26	1.11 1.09	0.90 0.92	427. 430.	780. 778.	1208. 1208.	696. 694.	1122. 1122.	0.627	0.858	1.485	420
430 440	451.9 454.2	29.20	1.06	0.92	433.	776.	1208.	692.	1122.	0.629 0.632	0.854 0.849	1.483	430
****	737.2	49.9 T	2.00	0.54	755.	770.	1200.	0,2.	1100.	0.032	0.049	1.481	440
450	456.5	30.62	1.04	0.96	435.	774.	1209.	690.	1123.	0.635		1.479	450
460	458.7	31.30	1.01	0.99	438.	771.	1209.	687.	1123.	0.637	0.840	1.477	460
470 480	460.9 463.0	31.98 32.66	0.99 0.97	1.01 1.03	440. 443.	769. 767.	1209. 1209.	685. 683.	1123. 1123.	0.640 0.643	0.835 0.831	1.475 1.474	470 480
490	465.1	33.34	0.95	1.05	445.	764.	1210.	680.	1123.	0.645	0.827	1.474	490
500 525	467.2	34.02	0.93	1.08	448.	762.	1210.	678.	1124.	0.648	0.823	1.471	500 505
550	472.3 477.2	35.72 37.42	0.89 0.85	1.12 1.18	453. 458.	757. 752.	1210. 1210.	673.	1124.	0.654	0.813	1.467	525 550
575	481.9	39.13	0.83	1.24	456. 464.	732. 747.	1210.	668. 663.	1125. 1125.	0.659 0.664	0.803 0.794	1.462 1.458	575
600	486.4	40.83	0.781		469.	742.	1211.	658.	1125.	0.670		1.454	600
							1]; A=1/;						

 $\begin{array}{l} \textbf{T}^{\circ} = \textbf{t}^{\circ} + \textbf{459.6}; \textbf{J} = 777.5 \, \text{ft. lbs. per B.t.u.} [\log = 2.89 \, 071]; \textbf{A} = 1/J = 1.286 \times 10^{-3}; \textbf{144 A} = 0.1852 \, [\log = \overline{\textbf{1}}.26 \, 764]. \\ \textbf{For water, at 280 lbs., sp. vol., v' or } \sigma = 0.0189 \, \text{cu. ft. per lb.}; \ 1/v' = 53.0 \, \text{lbs. per cu. ft.}; \ 144 \, \text{Apv'} = 0.98 \, \text{B.t.u.}; \\ \textbf{at 450 lbs.,} \qquad \textbf{v' or } \sigma = 0.0197 \qquad \text{"} \qquad ; \ 1/v' = 50.8 \qquad \text{"} \qquad ; \ 144 \, \text{Apv'} = .165 \qquad \text{"} \qquad . \end{array}$

Table 3: Saturated and Superheated Steam

	Degrees of Superheat													
Press. ibs.	Water	Sat. Steam	10°	20°	30°	40°	50°	60°	70°	80°	90°	100°	110°	120°
1 t	101			121.7			151.7	161.7	171.7	181.7	191.7	201.7	211.7	
Ţ	0.0	333.0	339.3 1108.9	345.5						381.9 1140.8		393.9 1149.9	399.9	
p	0.1327	1104.4	1.9836				2.0144					2.0503		
27	0.1321	L,7/J4	1.7000	X.772J	1.,,,,,	2.000	2.0117	2.0210	4.0471	2.0000	2.0131	2.0303	2.03/1	2.000
2 t	126	5.1		146.1			176.1	186.1	196.1	206.1	216.1	226.1	236.1	246.1
Ţ		173,5		179.8						198.2			207.2	
þ		1115.0	1119.5 1.9259				1137.8					1160.7		
n	0.1749	1.9180	1,9239	1.9330	1.9414	1.9400	1.9559	1.9030	1.9099	1.9/08	1.9830	1.9904	1.99/1	2.0036
3 t	14:	1.5	151.5	161.5	171.5	181.5	191.5	201.5	211.5	221.5	231.5	241.5	251.5	261.5
¥		118.5		122.8						135.1			141.1	
h		1121.6	1126.2							1158.2		1167.4		
n	0.2008	1.8848	1.8927	1.9002	1.9077	1.9130	1.9221	1.9289	1.9330	1.9423	1,9490	1.9557	1.9023	1,9687
4 t	153	3.0	163.0	173.0			203.0	213.0	223.0	233.0	243.0	253.0	263.0	273.0
٧		90.5		93.7		96.8				102.9			107.5	
h		1126.5	1131.1							1163.2		1172.4		
n	0.2198	1.8614	1.8690	1.8764	1.8838	1.8910	1.8980	1.9048	1.9115	1.9182	1.9249	1.9316	1.9382	1.9446
5 t	162	2.3	172.3	182.3	192.3	202.3	212.3	222,3	232.3	242,3	252.3	262.3	272.3	282.3
V		73.3		75.9		78.4	79.7	80.9	82.1	83.3	84.5	85.7	86.9	88.2
h		1130.5	1135.1							1167.2			1181.0	
n	0.2348	1.8432	1.8507	1.8581	1.8654	1.8725	1.8794	1.8861	1.8927	1.8993	1.9059	1.9125	1.9189	1,9252
6 t	170	0.0	180.0	190.0	200.0	210.0	220.0	230.0	240.0	250.0	260.0	270.0	280.0	290.0
٧		61.9			65.1	66.1	67.2	68.2	69.2	70.2	71.2	72.2	73.2	74.2
b		1133.7		1141.9						1170.5			1184.4	
13	0.2471	1.8285	1.8360	1.8432	1.8504	1.8575	1.8643	1.8709	1.8775	1.8841	1.8906	1.8970	1.9033	1.9095
7 t	170	6.9	186.9	196.9	206.9	216.9	226.9	236.9	246,9	256.9	266.9	276.9	286.9	296.9
7		53.6	54.5	55.4	56.3	57.2	58.1	58.9	59.8	60.7	61.6		63.3	
b		1136.5				1155.0					1178.0		1187.3	
I		1.8161	1.8235	1.8306	1.8377	1.8447	1.8515	1.8581	1.8647	1.8712	1.8776	1.8840	1.8902	1.8963
8 t		2.9	192.9	202.9	212.9	222.9	232.9	242,9	252,9	262.9	272.9	282.9	292.9	302.9
7		47.3	48.1	48.9	49.7	50.4	51.2	52.0	52.8	53.5			55.8	
t		1139.0				1157.5				1176.0			1189.8	
I	0.2673	1.8053	1.8126	1.8197	1.8267	1.8337	1.8404	1.8469	1.8534	1.8599	1.8663	1.8727	1.8788	1.8849
9 t	. 18	8.3	198.3	208.3	218.3	228.3	238.3	248.3	258.3	268.3	278.3	288.3	298.3	308.3
,		42.4	43.1			45.2		46.6		47.9			49.9	50.6
ł		1141.1				1159.7					1182.8			1196.7
I	0.2756	1.7958	1.8030	1.8100	1.8170	1.8239	1.8306	1.8371	1.8436	1.8500	1.8563	1.8626	1.8687	1.8748
10 1	: 19	3.2	203.2	213.2	223.2	233,2	243.2	253.2	263.2	273.2	283.2	293.2	303.2	313.2
			39.0	39.7	40,3	40.9	41.5	42.2	42.8	43.4	44.0	44.6		45.8
1		1143.1	1147.7	1152.4	1157.1	1161.7	1166.3	1171.0	1175.6	1180.3	1184.9	1189.5	1194,2	1198.8
1	1 0.2832	1.7874	1.7946	1.8015	1.8084	1.8153	1.8220	1.8285	1.8349	1.8413	1.8476	1.8538	1.8599	1,8659
11 1	19	7.8					247.8					297.8	307.8	317.8
	7 0.0	35.1				37.4				39,7		40.8	41.3	41.9
_		1144.9					1168.2	1172.8	1177.4	1182.1	1186.8	1191.4	1196.1	1200.7
1	1 0.2902	2 1.7797	1.7868	1.7937	1.8006	1.8075	1.8141	1.8205	1.8269	1.8333	1.8396	1.8458	1.8519	1.8579
12	20	2.0				242.0	252.0	262.0	272.0	282.0	292.0	302.0	312.0	322.0
1	7 0.0			33.4			35.0	35.5	36.0	36.5	37.0	37.5	38.0	38.6
	-	1146.5				1165.2	1169.9	1174.5	1179.1	1183.8	1188.5	1193.1	1197.8	1202.5
1	1 0.2967	7 1.7727	1.7797	T\000	1./935	1.8003		1.8133	1.0197	1.8260	1.8322	1.8384	1.8445	1.8505
						1	(22)							

t is the temperature, in Fahrenheit degrees; V is the specific volume, in cu. ft. per lb.; h is the total heat, in B. t. u., from water at 32°; n is the entropy, from water at 32°.

	- ··· <u>-</u>	•	•	•••	Da	grees of Superheat	
130° 140°	150° 160°	170° 180° 1	90° 200°	250° 300°	350° 400°	·	Press.
231.7 241.7	251.7 261.7	271.7 281.7 29	91.7 301.7	351.7 401.7		6Q1.7 701.7	t 1
411.8 417.8		435.7 441.7 4		483.5 513.4			▼
1163.6 1168.2 2.0704 2.0770		.182.0 1186.5 11 3.0962 2.1024 2.1		1218.5 1241.5 2.1426 2.1701		1334,1 1381,0 2,2679 2,3100	
2.0704 2.0770	2.0005 2.0055 2	U3U2 2.1U2T 2.1	2.1143	2.1720 2.1701	2.1307 2.2210	2.2019 2.3100	щ
256.1 266.1		296.1 306.1 31		376.1 426.1			t 2
213.2 216.2		225.2 228.2 23		249.1 264.1		323.8 353.6	Ā
1174.4 1179.0 2.0100 2.0162	2,0223 2.0284 2	1192.7 1197.2 12 10345 2.0406 2.0		1229.4 1252.4 2.0802 2.1071	2 1333 2 1586	1345.2 1392.2 2.2044 2.2459	h n
2,0100 2,0100				3.0002 2.1071	2,1000 2,1000	2.2011 2.2133	•
271.5 281.5		311.5 321.5 33		391.5 441.5		641.5 741.5	t 3
145.1 147.1 1181.1 1185.7	149.1 151.1 . 1190.3 1194.9 1	153.1 155.1 15		169.1 179.1 1236.2 1259.3		218.9 238.8 1352.4 1399.4	Þ h
1.9749 1.9809		9989 2.0049 2.0		2.0438 2.0703		2.1669 2.2081	
283.0 293.0		323.0 333.0 34		403.0 453.0		653.0 753.0	
110.5 112.0 1186.2 1190.8	113.5 115.0 1 1195.4 1200.0 1	110.5 118.0 11		1241.4 1264.5		165.9 180.8 1357.7 1404.8	
1.9505 1.9563		.9739 1.9898 1.9		2.0184 2.0445		2.1392 2.1803	
000 0 000 0	220 2 200 2		70.0 0.00	410.0 460.0	****		
292.3 302.3 8.94 9.06		332.3 342.3 35 94.2 95.4 9		412.3 462.3	512.3 562.3 115.8 121.8		t 5 v
1190.2 1194.9		1208.7 1213.3 12			1291.9 1315.2		ň
1.9311 1.9369	1.9428 1.9487 1	1.9546 1.9604 1.9		1.9987 2.0246		2.1179 2.1586	n
200.0 210.0	200 0 220 0	240.0 250.0 26		400 0 470 0	F20.0 F70.0	670 0 770 0	
300.0 310.0 75.2 76.2		340.0 350.0 36 79.3 80.3 8	370.0 31.3 82.3	420.0 470.0 87.3 92.3		670.0 770.0 112.2 122.2	t 6 V
1193.6 1198.2		1212.0 1216.6 12		1249.0 1272.2		1365.7 1413.0	
1.9154 1.9213	1.9272 1.9330 1	1.9388 1.9445 1.9	9503 1.9561	1.9827 2.0085	2.0331 2.0568	2.1006 2.1410	n
306.9 316.9	326 9 336 9	346.9 356.9 36	66 9 376 9	426.9 476.9	526.9 576.9	676.9 776.9	t 7
65.1 66.0	66.8 67.6	68.5 69.3 7	0.2 71.1	75.4 79.6	83.9 88.2	96.8 105.3	7
1196.5 1201.2		1215.0 1219.6 12				1368.9 1416.3	
1.9023 1.9082	1.9141 1.9199 1	1.9256 1.9313 1.9	9370 1.9427	1.9693 1.9947	2.0192 2.0426	2.0860 2,1261	n
312.9 322.9	332.9 342.9 3	352.9 362.9 37	72.9 382.9	432.9 482.9	532.9 582.9	682.9 782.9	t 8
57.3 58.1		60.3 61.1 6				85.1 92.6	V
1199.0 1203.7 1.8909 1,8968		217.6 1222.2 12 ,9140 1,9197 1,9		1254.7 1278.0		1371.6 1419.0 2,0734 2,1133	h
1.0505 1,0500	1,9020 1,9000 1	1.9140 1.9197 1.5	7434 1.7311	1.9370 1.9029	2.0071 2.0303	2.0734 2.1133	ш
318.3 328.3		358,3 368.3 37		438.3 488.3		688.3 788.3	t 9
51.3 52.0		54.0 54.7 5				76.0 82.7	¥
1201.4 1206.0 1.8808 1.8867		.219.9 1224.5 12 1.9039 1.9096 1.9		1257.1 1280.3 1.9473 1.9725			h n
-10000 210007	1.0723 1.0702 1		7151 1.7500	2,5110 1,5125	2,7,03 2,02,3	2.0020 2.12020	**
323.2 333.2		363.2 373.2 38		443.2 493.2			t 10
46.4 47.0 1203.4 1208.1		48.9 49.5 50 222.0 1226.7 12				68.7 74.7 1376.4 1424.0	v h
1.8719 1.8778	1.8836 1.8893 1	1.8950 1.9006 1.9	9062 1.9117	1.9381 1.9632	1.9871 2.0099	2.0526 2.0920	
327.8 337.8 42.4 43.0		367.8 377.8 38	87.8 397.8 5.8 46.3	447.8 497.8		697,8 797.8	t 11
1205.3 1210.0		44.6 45.2 4 1223.9 1228.6 12		49.0 51.8 1261.2 1284.5	54.5 57.2 1307.9 1331.4	62.7 68.2 1378.5 1426.1	V h
1.8638 1.8696		.8868 1.8924 1.8		1.9298 1.9547		2.0437 2.0829	
332,0 342,0	250 A 260 A	372.0 382.0 39	οο ο Δοο ο ο ο ο ο ο ο ο ο ο ο ο ο ο ο	452 N 502 A	550 0 Eno 0	702.0 802.0	+ 10
39.1 39.6			2.1 42.6		50.2 52.7	57.7 62.7	A 172
1207.1 1211.8	1216.4 1221.0 1	225.7 1230.4 12	35.1 1239.8	1263.0 1286.3	1309.8 1333.3	1380.4 1428.0	h
1.8564 1,8622	1.8680 1.8737 1	1.8793 1.8849 1.8			1,9707 1,9933	2.0356 2.0747	n
		₹	(23)	•			

Table 3: Superheated Steam

	",	Set Set	Degrees	of Superh	eat									
Press. lbs.		Set. Water Steam	10°	20°	30°	40°	50°	60°	70°	80 °	90°	100°	110°	120°
13		205.9		225.9					275.9			305.9		
		0.02 30.03		31.02 1157.4			<i>32.</i> 48 1171.4		33.43			34.83 1194.8	35,32	
	h n	173.8 1148.0 0.3025 1.7664		1.7803			1.8004						1.8379	
•		0.0000 1.700	2,,,,,,,	211000		11,700	2.000	2,0003	2.0202			210025	1.0077	2.0 .00
14	t	209.6		229.6					279.6				319.6	
₩,		0.02 28.02		28.94					31.18				32,94	
	h	177.5 1149.4 0.3081 1.7604		1158.8 1.7742			1172.9		1.8070				1200.9 1.8317	
	11	0.3061 1.7004	1.7074	1.7742	1.7610	1./0//	1./5-13	1.0007	1.0070	1.0132	1.0177	1.0230	1.0317	1.0370
15	t	213.0	223.0	233.0	243.0	253.0	263.0	273.0	283.0	293.0	303.0	313.0	323.0	333.0
	٧	0.02 26.27		27.13					29.23				30.87	
	h	181.0 1150.7		1160.1			1174.2						1202.3	
	n	0.3133 1.7549	1.7618	1.7686	1.7754	1.7821	1./880	1.7950	1.8013	1.80/5	1.8137	1.8199	1.8259	1.8318
16	ŧ.	216.3	226.3	236.3	246.3	256.3	266.3	276.3	286.3	296.3	306.3	316.3	326.3	336.3
	v	0.02 24.74		25.54					27.51				29.06	
	h	184.4 1152.0	1156.7	1161.4	1166.1	1170.8	1175.5					1198.9	1203.6	1208.3
	n	0.3183 1.7494	1.7563	1.7631	1.7698	1.7765	1.7830	1.7894	1.7957	1.8019	1.8080	1.8141	1.8201	1.8260
47		219.4	220.4	239.4	240.4	250.4	260.4	270 4	289.4	200.4	300.4	210 4	329.4	220.4
17	v	0.02 23.38		24.13					25.99				27.45	
	'n	187.5 1153.1		1162.5			1176.7						1204.9	
	n	0.3229 1.7444		1.7581					1.7906				1.8150	
		222.4	020.4	040.4	050.4	000.4	otto 4	000.4	000.4	200.4	210.4	700.4	222.4	040.4
18		222.4 0.02 22.16		242.4 22.88					292.4 24.64				332.4 26.02	
	V h	190.5 1154.2		1163.6					1187.2				1206.0	
	n	0.3273 1.7400		1.7536					1.7861				1.8104	
					•									
19	t	225.2		245.2					295.2				335.2	
	Ā	0.02 21.07		21.75					23.42				24.73	
	h n	193.4 1155.2 0.3315 1.7360		1164.7 1.7495					1188.3 1.7820				1207.2 1.8063	
	**	0.0010 1.7000	1.7 720	1.7773	1.7502	1.7020	1.7055	1.7757	1.7020	1.7001	1.7 374	1.0003	1.0000	1.0121
20	t	228.0		248.0			278.0	288.0	298.0	308.0	318.0	328.0	338.0	348.0
	V	0.02 20.08	20.41	20.73	21.05	21.37			22.32				23.56	
	h	196.1 1156.2		1165.7					1189.3				1208.3	
	n	0.3355 1.7320	1./388	1.7456	1./544	1./56/	1./032	1.//10	1.7779	1./640	1.7901	1./901	1.8021	1.8080
21	t	230.6	240.6	250.6	260,6	270.6	280.6	290.6	300.6	310.6	320.6	330.6	340.6	350.6
	v	0.02 19.18		19.80					21.32				22.51	
	h	198.8 1157.1				1176.1			1190.3					1214.0
	n	0.3393 1.7280	1.7348	3 1.7415	1,7481	1.7547	1.7612	1.7675	1.7737	1,7799	1.7860	1.7921	1.7980	1.8038
22	+	233.1	242 1	252.1	263 1	273.1	283 1	203 1	303.1	212 1	323 1	222 1	343.1	353 1
20	v	0.02 18.37		18.96					20.41				21.55	
	h	201.3 1158.0				1177.1	1181.8	1186.6	1191.3	1196.0	1200.8	1205.5	1210.3	1215.0
	\boldsymbol{a}	0.3430 1.7241	1.7309	1.7376	1.7442	1.7507	1.7571	1.7635	1.7698	1.7759	1.7820	1.7881	1.7940	1.7998
02		025 5	245 5	חבר ב	265 5	חשב ב	205 5	205 5	20E E	215 5	325.5	225 E	245 5	255 5
23	T V	235.5 0.02 17.62	443.3 17 01	18.19	403.3 18 47	275.5 18.75	203.3 19.03	493.3 19 30	305.5 19.58	313.3 10 85	20.12		20.66	355.5 20.93
	'n	203,8 1158,8				1178.0					1201.7			1215.9
	n	0.3465 1.7204				1.7470					1.7782			1.7960
		A== A	a		00-	085.0	00= 0	004.0	207 5	22 = 2	205.0	225 6	24~ ~	2500
24	t			257.8					307.8 18.81				347.8 19.85	
	v	0,02 16.93 206.1 1159.6		17.48 4 1169 2		10.02					1202.6			1216.8
		0.3499 1.7169									1.7747			1.7924
	_			4					•					

t = temperature in F. degs.

V=sp. vol. in on. ft. per lb.
h=total heat in B. t.u.

L=entropy.

To Fahr. absolute = to + 459.60.

J=777.5 ft. lbs. per B. t.u. [log=2.89 071].

A=1/J=1.286 × 10⁻³ B. t.u. per ft. lb. [3.10 929].

Values for saturated steam are given in Tables 1 and 2.

1 3 0° 140°	150° 160°	170° 180°	190°	200°	250°	300°	350°	Degrees of 400° 500°	Superheat 600°	Press. ibs.
335.9 345.9 36.26 36.73 1208.7 1213.4 1.8497 1.8556	37.20 37.67 1218.0 1222.7	375.9 385.9 38.14 38.61 1227.4 1232.0 1.8727 1.8782	39.07 1236.7	1241.4	455.9 41.87 1264.7 1.9154	44.19 1288.1	1311.5	605.9 705.9 48.82 53.43 1335.0 1382. 1.9862 2.028	3 58.04 2 1429.8	t 13 v h n
339.6 349.6 33.82 34.26 1210.2 1214.9 1.8435 1.8493	34.69 35.13 1219.6 1224.2	379.6 389.6 35.56 36.00 2 1228.9 1233.6 5 1.8662 1.8718	36.43 5 1238.3	36.86 1243.1		41.19 1289.6		609.6 709.6 45.49 49.78 1336.7 1383. 1.9795 2.021	54.06 9 1431.5	t 14 V h
343.0 353.0 31.69 32.10 1211.6 1216.3 1.8377 1.8435	32.50 32.91 1221.0 1225.6	383.0 393.0 33.32 33.73 5 1230.3 1235.0 3 1.8604 1.8659	34.13 1239.7	34.53 1244.4	463.0 36.56 1267.7 1.9029	38.58 1291.1	40.59 1314.7	613.0 713.0 42.59 46.59 1338.3 1385. 1.9733 2.015	50.59 5 1433.2	t 15 v h n
346.3 356.3 29.82 30.21 1213.0 1217.7 1.8319 1.8377	30.59 30.97 1222.4 1227.0	386.3 396.3 31.36 31.74 1231.7 1236.4 1.8546 1.8601	32.12 1241.1	32.50 1245.8		36.29 1292.6		616.3 716.3 40.05 43.83 1339.8 1387. 1.9672 2.008	47.55 0 1434.8	t 16 v h n
349.4 359.4 28.18 28.54 1214.2 1218.9 1.8267 1.8324	28.90 29.26 1223.6 1228.3	389.4 399.4 29.62 29.98 3 1233.0 1237.7 1.8493 1.8548	30.33 1242.4	30.69 1247.1	469.4 32.48 1270.5 1.8916	34.26 1294.0	36.04 1317.5	619.4 719.4 37.81 41.35 1341.1 1388. 1.9617 2.003	44.87 3 1436.1	t 17 v h n
352.4 362.4 26.70 27.04 1215.4 1220.1 1.8220 1.8278	27.39 27.73 1224.8 1229.5	392.4 402.4 28.07 28.41 5 1234.2 1238.9 1.8447 1.8502	28.74 1243.6	29.08 1248.3		32.46 1295.3		622.4 722.4 35.81 39.15 1342.4 1389. 1.9568 1.998	42.48 7 1437.5	t 18 v h n
355.2 365.2 25.38 25.70 1216.6 1221.3 1.8179 1.8236	26.03 26.35 1226.0 1230.7	395.2 405.2 26.67 26.99 7 1235.4 1240.1 0 1.8404 1.8459	27.32 1244.8	27.64 1249.5	475.2 29.24 1273.0 1.8825	30,84 1296.5	32.43 1320.0	625.2 725.2 34.01 37.18 1343.6 1391. 1.9523 1.993	3 40.34 0 1438.8	t 19 v h n
358.0 368.0 24.18 24.49 1217.7 1222.4 1.8137 1.8194	24.80 25.11 1227.1 1231.8	398.0 408.0 25.41 25.72 3 1236.5 1241.2 7 1.8362 1.8412	26.02 2 1245.9	26.33 1250.6	478.0 27.85 1274.1 1.8781	29.37 1297.6	30.88	628.0 728.0 32.39 35.40 1344.8 1392. 1.9479 1.989	38.40 2 1440.0	t 20 v h n
360.6 370.6 23.10 23.39 1218.7 1223.4 1.8096 1.8153	23.68 23.98 1228.1 1232.8	400.6 410.6 24.27 24.56 8 1237.5 1242.2 4 1.8319 1.8374	24.85 2 1246.9	25.15 1251.7		28.04 1298.7		630.6 730.6 30.92 33.79 1346.0 1393. 1.9434 1.984	36.65 3 1441.1	t 21 v h n
363.1 373.1 22.11 22.39 1219.7 1224.4 1.8055 1.8112	22.67 22.95 1229.1 1233.8	403.1 413.1 23.23 23.51 8 1238.5 1243.3 4 1.8279 1.8333	23.79 2 1249.0	24.06 1252.7	1276.3	26.83 1299.8	583.1 28.21 1323.4 1.9171	633.1 733.1 29.58 32.3 1347.0 1394. 1.9392 1.980	2 35.05 4 1442.2	t 22 v h n
365.5 375.5 21.20 21.47 1220.6 1225.3 1.8017 1.8074	21.74 22.01 1230.0 1234.8	5 405.5 415.5 22.28 22.54 8 1239.5 1244. 5 1.8240 1.829	22.81 2 1249.0	23.08 1253.7		25.72 1300.8		635.5 735.5 28.36 30.95 1348.1 1395. 1.9351 1.976	32.59 5 1443.3	t 23 v h n
367.8 377.8 20.37 20.63 1221.5 1226.2 1,7981 1.8037	20.89 21.14 1231.0 1235.7	3 407.8 417.8 4 21.40 21.66 7 1240.4 1245. 8 1.8203 1.825	21.91 1249.9	22.17 1254.7		24.71 1301.8		637.8 737.1 27.23 29.7 1349.1 1396 1.9313 1.972	4 32,25 5 1444,3	t 24 v h n

Conversion from Metric Units

1 kg. per sq. cm.=14.22 lbs. per sq. in. [log=1.15 300]. 1 cu. meter=35.31 cu. ft. [log=1.64 795].

To change degs. C. to degs. F., multiply by \$\frac{1}{2}\$, and add 32. To change mean kg. calories per kg. to mean B.t.u. per lb., multiply by \$\frac{1}{2}\$. Entropy same in both systems.

Table 3: Superheated Steam

,			Begrees of Superheat												
Props. Ibs.			Bat. team	10°	20°	30°	40°	50°	60°	70°	80°	90°	100°	110°	120°
	t V h n	240.1 0.02 1 208.4 11 0.3532 1	6.30 160.4	250.1 16.57 1165.2 1.7204	16.84 1170.0	1174.8	17.35 1179.6		1189.2	18.11 1193.9		18.61 1203.4		19.11 1213.0	1217.7
26		242.1 0.02 1 210.6 1 0.3564 1	2 15.72 161.2	252.2	262.2 16.24 1170.8	272.2 16.49 1175.6	282.2 16.73 1180:4	292.2 16.97 1185.2	302.2 17.21 1190.0	312.2 17.45 1194.7	322.2 17.69	332.2 17.93 1204.2	342.2 18.17 1209.0	352.2 18.41 1213.8 1.7801	362.2 18.65 1218.5
27	t v h n	244. 0.02 1 212.7 1 0.3594 1	15,18 161.9			15.91 1176.4	16.14 1181.2	16.37 1186.0	16.61 1190.7	16.84 1195.5	324.4 17.08 1200.3 1.7592	17.31 1205.1	17.54 1209.8	354.4 17.77 1214.6 1.7771	18.00 1219.3
28	t V h n	246. 0.02 1 214.8 1 0.3623 1	14.67 .162.6			15.38 1177.1	15.60 1181.9	15.82 1186.7	16.05 1191.5	16.28 1196.2	326.4 16.51 1201.0 1.7563	16.73 1205.8	16.95 1210.6	356.4 17.18 1215.4 1.7742	17.40 1220.1
29	t V h n	248. 0.02 3 216.8 1 0.3652 1	14.19 163.2			14.87 1177.8	15.09 1182.6	15.31 1187.4	15.53 1192.2	15.75 1197.0	328.4 15.97 1201.8 1.7533	16.19 1206.6	16.40 1211.4	358.4 16.62 1216.2 1.7712	16.83
30	t V h n	250. 0.02 1 218.8 1 0.3680 1	13.74 .163.9	13.97 1168.8	270.4 14.19 1173.6 1.7125	14.41 1178.5	14.62 1183.3	14.83 1188.1	15.05 1192.9	15.26 1197.7	330.4 15.47 1202.5 1.7505	15.68 1207.3	15.89 1212.1	360,4 16,10 1216,9 1,7684	16.31
31	V h	252. 0.02 2 220.7 1 0.3707 1	13.32 164.5	13.54 1169.4	272.3 13.76 1174.3 1.7098	13.97 1179.1	14.18 1184.0	14.38 1188.8	14.59 1193.6	14.79 1198.4	332.3 14.99 1203.2 1.7477	15.20 1208.0	15.40 1212.8	362.3 15.60 1217.6 1.7656	15.80 1222.4
32	t v h n	254. 0.02 222.6 1 0.3733	12.93 1165.1	13.15 1170 0	274.1 13.36 1174.9 1.7072	13.56 1179.8	13.76	13.96 1189.4	14.16 1194.3	14,35 1199.1	334.1 14.55 1203.9 1.7451	14.75 1208.7	14.95 1213.5	364.1 15.14 1218.3 1.7630	15.34
33	t v h n	255 0.02 224.4 1 0.3759 1	12.57 1165.7	12.78 1170.6	275.8 12.98 1175.5 1.7048	13.18 1180.4	13.37 1185.2	13.56 1190.1	13.76 1194.9	13.95 1199.7	335.8 14.14 1204.6 1.7427	14.33 1209.4	14.52 1214.2		
34	t V h	257, 0.02 226.2 1 0.3784 1	12,22 1166.3	12.42 1171.2		12.81 1181.0		13.19 1190.7	13,38 1195.5	13.57 1200.3	1205.2	347.6 13.94 1210.0 1.7462	14.12 1214.8		
35	t v h n	259. 0.02 227.9 1 0.3808 1	11.89 1166.8	12.09 1171.7		12.48 1181.5		12.85 1191.3	13.03 1196.1	13.21 1201.0			13.75 1215.4		14.11 1225.0
36	t v h n	261. 0.02 229.6 0.3832	11.58 L167.3	11.78 1172.3 1.6914	1.6980	12.15 1182.1 1.7046	12.33 1187.0 1.7110	12.51 1191.8	12.69 1196.7	12.86 1201.5		13.22	13.39 1216.0		
37	t v h n	262. 0.02 231.3 0.3855	11.29 1167.8	11.48 1172.8		11.85 1182.6		12,19 1192,4	12.37 1197.3	12.54 1202.1			13.05 1216.6	1221.4	13,40 1226.2

											Deg			
130°	140°	150°	160°	170°	180°	190°	200°	250°	300°	350°	400°	500°	•	Press. lbs.
370.1	380.1	390.1	400.1	410.1	420.1	430.1	440.1	490.1	540.1	590.1	640.1	740.1	840.1	t 25
19.61			20.35						23.77			28.61		¥
	1227.1 1.8004					1250.8 1.8277							1445.4 2.0078	
	382.2 19.13		402.2 19.61						542.2			742.2 27.56		t 26
	1228.0					1251.7	20.55 1256.5	1280.1	1303.7	1327.4			1446.3	v h
1.7916	1.7972	1.8028	1.8083	1.8138	1.8192	1.8246	1.8298				1.9244	1.9654	2.0034	n
374.4	384.4	394.4	404.4	414.4	424.4	434.4	444.4	494.4	544.4	594.4	644.4	744.4	844.4	t 27
18.24	18.47	18.70	18.93	19.16	19.38	19.61	19.84	20.97	22.10	23.23	24.35	26.59	28.81	v
	1228.8 1.7942					1252.5 1.8215				1328.3			1447.3 2.0001	
1.7000	1.7712	2.7 7 7 0	1.0055	1.0100	1.0102	1.0213	1.0200	1.0322	1.0705	1.0772	1.7212	1.7021	2.0001	ш
	3 8 6.4 17.84					436.4 18.95				596.4		746.4		t 28
	1229.6					1253.4						25.68 1400.3	1448.2	V h
1.7857	1.7913	1.7969	1.8024	1.8079	1.8133	1.8186	1.8239	1.8493	1.8734	1.8963	1.9183	1.9592	1.9972	n
378 4	388.4	398.4	408,4	418.4	428.4	438.4	448.4	498.4	548.4	598.4	648.4	748.4	848.4	t 29
17.05	17.26	17.48	17.69	17.91	18.12	18.33	18.55	19.61	20.66	21.70	22.75	24.83	26.91	▼
	1230.4 1.7883					1254.2 1.8155							1449.0 1.9936	
1,7027	1.7663	1.7330	1.7993	1.0070	1,0102	1.0133	1,0207	1.0100	1.0702	1.0930	1.7177	1,7337	1.9930	11
	390.4					440.4							850.4	
	16.73 1231.2					17.76 1255.0							26.05 1449.9	
	1.7854					1.8126							1.9904	
297 2	392,3	4023	412.3	422.3	432 3	442 3	452.3	502.3	552.3	602.3	652.3	752.3	852.3	t 31
	16.21	16.41	16.61	16.81	17.01	17.21	17.41	18.40	19.39	20.37	21.35	23.30	25.24	▼
	1231.9					1255.7							1450.7	
1.7770	1.7826	1./881	1.7930	1./991	1,8045	1.8098	1,8150	1.8402	1.8043	1.8871	1,9089	1.9490	1.9874	11
	394.1					444.1				604.1			854.1	t 32
	15.73 1232.6					16.70 1256.4				1332.3			24.48 1451.6	♥ h
	1.7799					1.8071				1.8843			1.9845	
385 R	395.8	4 05 8	415 8	425 8	435 Q	445.8	455 R	505.8	555.8	605.8	655.8	755.8	855.8	t 33
15.10	15.29					16.23	16.42	17.35	18.28	19.20	20.12	21.95	23.78	v ~
	1233.3					1257.2				1333.1			1452.3 1.9818	h
1.7719	1.7775	1.7830	1./884	1.7939	1./993	1.8046	1.8098	1.8349	1.8390	1.0017	1.9034	1.9441	1.9010	
	397.6	407.6	417.6	427.6	437.6	447.6	457.6	507.6	557.6	607.6			857.6	t 34
	14.87 1234.0					15.79 1257.8							23.12 1453.1	♥ h
	1.7751					1.8021				1.8791			1.9791	
380.3	399.3	400 3	410 2	420.3	430 3	449.3	459 3	509.3	559.3	609.3	659.3	759.3	859.3	t 35
14.29	14.47	14.65	14.83	15.01	15 18	15.26	15.54	16.42	17.30	18.17	19.04	20.76	22,49	V
1229.8	1234.6	1239.4	1244.2	1248.9	1253.7	1258.5	1263.3	1287.1	1310.8	1334.5	1358.3	1405.9	1453.8	h
1./0/2	1,7728										1.0707	1.7370	1.5700	
	401.0	411.0	421.0	431.0	441.0	451.0	461.0	511.0	561.0	611.0			861.0	t 36
	14.09 1235.2	14.27 1240.0	14.44 1244.8	14.61 1249.6	14./9 1254 3	14.96 1259.1	1263.9	1287.7	1311.5	1335.2	18.54 1359.0		1454.5	D h
1.7650	1.7705					1.7975	1.8027	1.8278	1.8518	1.8744			1.9741	
392.6	402.6	412.6	422.6	432.6	442.6	452.6	462.6	512.6	562.6	612.6	662.6	762.6	862.6	t 37
13.57	13 74	13 01	14 08	14 24	14 41	14 58	14 74	15.59	16.42	17.24	18.06	19.70	21.32	V
1231.0	1235.8 1.7683	1240.6	1245.4	1250.2	1255.0	1259.8	1264.6	1288.4	1312.2	1335,9	1359.7	1407.3	1455.3	h
1.7025	1./053	1.//38	1.7/93	1./597	1.7900	1./933	1,8005	4 .0434	*******	1,0120	T-0330	4,3J7L	T+2/TO	44

(27)

Table 3: Superheated Steam

	7	Degreés of Superheat													
Press. lbs.		Sat. Water Steam	10°	20°	30°	40°	50°	60°	7 0°	80°	90°	100°	110°	120°	
38	t	264.2	274.2	284.2	294.2	304.2	314.2		334.2			364.2	374.2	384.2	
	V	0.02 11.0		11.36					12.23				12.90		
	h n	232.9 1168. 0.3877 1.680		1178.2					1202.7 1.7254				1222.0 1.7491		
	11	0.30// 1.000	1.00/0	1.0937	1.7002	1,7000	1./129	1,/192	1.7434	1./314	1./3/4	1.7433	1.7491	1./340	
39	t	265.8	275.8	285.8	295.8	305.8	315.8	325.8	335.8	345.8	355.8	365.8	375.8	385.8	
	V	0.02 10.7		11.09					11.94				12.59		
	h	234.5 1168		1178.8					1203.3				1222.7		
	n	0.3899 1.678	1.0849	1.6915	1.0981	1.7045	1.7108	1.7171	1.7233	1.7293	1,7353	1.7412	1.7470	1,7527	
40	ŧ	267.3	277.3	287.3	297.3	307.3	317.3	327.3	337.3	347.3	357.3	367.3	377.3	387.3	
	٧	0.02 10.4	9 10.66	10.83	11.00	11.16	11.33	11.50	11.66	11.82	11.98		12,29		
	h	236.0 1169		1179.3					1203.8				1223.2		
	n	0.3920 1.676		1.6895	1.6961	1.7025	1.7089	1.7151	1.7212	1.7273	1.7333	1.7392	1.7450	1.7507	
41	t.	268.7	278.7	288.7	298.7	308.7	318.7	328.7	338.7	348.7	358.7	368.7	378.7	388.7	
	v	0.02 10.2		10.58					11.38				12.01		
	h	237.6 1169		1179.8					1204.3				1223.8		
	n	0.3941 1.674	1.6809	1.6875	1.6941	1.7005	1.7069	1.7131	1.7192	1.7253	1.7312	1.7371	1.7429	1.7486	
42	t	270.2	280.2	290.2	300.2	310.2	320.2	330.2	340.2	350.2	360.2	370.2	380,2	390.2	
	٧	0.02 10.0	_	10.34					11.13				11.74		
	h	239.1 1170		1180.2					1204.8				1224.4		
	n	0.3962 1.672	1.6789	1.6855	1.6921	1.6985	1.7049	1.7111	1.7172	1.7233	1.7292	1.7351	1.7409	1.7466	
43	t	271.7	281.7	291.7	301.7	311.7	321.7	331.7	341.7	351.7	361.7	371.7	381.7	391.7	
	V	0.02 9.80	9.96	10.12	10.28	10.43	10.58	10.74	10.89	11.04	11.19	11.34	11.49	11.64	
	h	240.5 1170		1180.7					1205.4				1224.9		
	n	0.3982 1.670	12 1,6770	1.6836	1.6902	1.6966	1.7030	1.7092	1.7153	1.7214	1.7273	1.7332	1.7390	1.7447	
44	t	273.1	283.1	293.1	303.1	313.1	323.1	333.1	343.1	353.1	363.1	373.1	383.1	393.1	
	٧	0.02 9.59		9.90		10.21			10.66				11.24		
	h	242.0 1171		1181.2					1205.9				1225.4		
	n	0.4002 1.668	33 1.6/51	1.6817	1.6883	1.6947	1.7011	1.7073	1.7134	1.7195	1.7254	1./313	1.7371	1.7427	
45	t	274.5	284.5	294.5	304.5	314.5	324.5	334.5	344.5	354.5	364.5	374.5	384.5	394.5	
	V	0.02 9.39			9.85	10.00			10.44				11.00		
	h	243.4 1171		1181.6					1206.4				1225.9		
	n	0.4021 1.666	5 1.6733	1.6799	1.0804	1.6929	1.6993	1./055	1.7116	1./1//	1.7236	1.7295	1.7353	1.7409	
46	t	275.8	285.8	295.8	305.8	315.8	325.8	335.8	345.8	355.8	365.8	375.8	385.8	395.8	
	V	0.02 9.20			9.65	9.79			10.22				10.78		
	h	244.8 1172		1182.1					1206.9				1226.4		
	n	0.4040 1.66	+/ 1.0/13	1.6781	1.0040	1.0911	1.09/3	1.7037	1.7098	1./139	1./218	1,/2//	1,7335	1./391	
47	t	277.2	287.2	297.2	307.2	317.2	327.2			357.2	367.2	377.2	387.2		
	V	0.02 9.02			9,45	9.60	9.74		10.02				10.57		
	h	246.1 1172 0.4059 1.66	-	1182.5					1207.3				1226.9 1.7318		
	n	0.4039 1.00	30 1.0090	1.6764	1.0829	1.0894	1,0938	1.7020	1.7081	1./142	1.7201	1.7200	1./318	1./3/4	
48	t	278.5	288.5	298.5	308.5	318.5	328.5	338.5	348.5				388.5		
	Ā	0.02 8.8		9.13			9.55	9.69			10.10		10,36		
	h n	247.5 1172 0.4077 1.66									1217.6 1.7184		1227.4 1.7301		
	11	0.TU11 1.00	T.000	1.0/4/	1,0014	1.00//	1,0771	1.7003	1.7004	1.1143	1./107	1.1473	1.7301	1.1331	
49	t	279.8		299.8			329.8						389.8		
	V	0.02 8.6		8.95	9.09	9.23	9.37	9.50	9.64	9.77	9.90	10.03	10.16	10.30	
	h	248.8 1173 0.4095 1.65	0.4 11/8.3 07 1 666	5 1 6737	1100.4	1193.4	1198.4	1,6087	1.7042	17100	1 7168	1.7227	1.7285	1.7341	
	*1	0,7033 1,03			4,07,70	1.0001			A., OTO	1., 103	2.7 200	1,,441	, <i></i> 003	2.,012	

t = temperature in F. degs.

T° Fahr. absolute = t° + 459.6°.

y = sp. vol. in cu. ft. per lb.

1=777.5 ft. lbs. per B. t. u. [log = 2.89 071].

h = total heat in B. t. u.

A = 1/J = 1.286 × 10⁻³ B. t. u. per ft. lb. [3.10 929].

Values for saturated steam

144 A = 0.1852 (log = 1.26 764).

CONTROL OF The results of the steam are given in Tables 1 and 2.

Degrees of Superheat	
130° 140° 150° 160° 170° 180° 190° 200° 250° 300° 350° 400° 500° 600°	Press. lbs.
394.2 404.2 414.2 424.2 434.2 444.2 454.2 464.2 514.2 564.2 614.2 664.2 764.2 864.2	t 38
13.23 13.40 13.57 13.73 13.89 14.05 14.22 14.38 15.20 16.01 16.81 17.61 19.21 20.79	¥ ~
	h
1.7604 1.7660 1.7715 1.7770 1.7824 1.7877 1.7930 1.7982 1.8232 1.8471 1.8696 1.8912 1.9317 1.9692	n
395.8 405.8 415.8 425.8 435.8 445.8 455.8 465.8 515.8 565.8 615.8 665.8 765.8 865.8	t 39
12.92 13.08 13.24 13.40 13.56 13.72 13.87 14.03 14.83 15.62 16.40 17.18 18.74 20.28	V 00
1232:5 1237.1 1241.9 1246.6 1251.4 1256.2 1261.0 1265.8 1289.7 1313.5 1337.2 1361.0 1408.6 1456.7	h
1.7584 1.7639 1.7694 1.7748 1.7802 1.7856 1.7909 1.7960 1.8210 1.8448 1.8674 1.8889 1.9293 1.9668	n
397.3 407.3 417.3 427.3 437.3 447.3 457.3 467.3 517.3 567.3 617.3 667.3 767.3 867.3	t 40
12.61 12.77 12.93 13.08 13.23 13.39 13.54 13.70 14.48 15.25 16.02 16.78 18.30 19.80	V
1232.9 1237.7 1242.4 1247.2 1252.0 1256.8 1261.6 1266.4 1290.3 1314.1 1337.8 1361.6 1409.3 1457.4	h
1.7564 1.7619 1.7674 1.7728 1.7782 1.7836 1.7888 1.7940 1.8189 1.8427 1.8652 1.8867 1.9271 1.9646	n
398.7 408.7 418.7 428.7 438.7 448.7 458.7 468.7 518.7 568.7 618.7 668.7 76 8. 7 868.7	t 41
12.32 12.48 12.63 12.79 12.93 13.08 13.23 13.38 14.15 14.90 15.65 16.39 17.87 19.34	Ÿ
1233.4 1238.2 1243.0 1247.8 1252.6 1257.4 1262.2 1267.0 1290.9 1314.7 1338.5 1362.3 1410.0 1458.0	h
1.7542 1.7598 1.7653 1.7707 1.7762 1.7815 1.7868 1.7919 1.8168 1.8406 1.8631 1.8845 1.9249 1.9624	n
400.2 410.2 420.2 430.2 440.2 450.2 460.2 470.2 520.2 570.2 620.2 670.2 770.2 870.2	t 42
12.04 12.19 12.34 12.49 12.64 12.79 12.94 13.09 13.83 14.56 15.29 16.02 17.46 18.90	v
1234.0 1238.8 1243.6 1248.4 1253.2 1258.0 1262.8 1267.6 1291.5 1315.3 1339.1 1362.9 1410.6 1458.6	h
1.7523 1.7578 1.7633 1.7687 1.7741 1.7795 1.7847 1.7899 1.8147 1.8385 1.8609 1.8823 1.9227 1.9601	n
401.7 411.7 421.7 431.7 441.7 451.7 461.7 471.7 521.7 571.7 621.7 671.7 771.7 871.7	t 43
11.78 11.93 12.08 12.22 12.37 12.52 12.66 12.80 13.53 14.25 14.96 15.67 17.08 18.48	v
1234.5 1239.3 1244.1 1249.0 1253.8 1258.6 1263.4 1268.2 1292.1 1315.9 1339.7 1363.5 1411.2 1459.2	h
1.7504 1.7559 1.7614 1.7668 1.7722 1.7775 1.7828 1.7879 1.8127 1.8364 1.8589 1.8803 1.9206 1.9580	n
403.1 413.1 423.1 433.1 443.1 453.1 463.1 473.1 523.1 573.1 623.1 673.1 773.1 873.1	t 44
11.53 11.67 11.82 11.96 12.10 12.25 12.39 12.53 13.24 13.94 14.64 15.33 16.70 18.08	٧
1235.1 1239.9 1244.7 1249.5 1254.3 1259.1 1263.9 1268.7 1292.6 1316.4 1340.2 1364.0 1411.8 1459.8	h
1.7483 1.7539 1.7595 1.7649 1.7703 1.7756 1.7808 1.7860 1.8108 1.8344 1.8568 1.8782 1.9185 1.9559	n
404.5 414.5 424.5 434.5 444.5 454.5 464.5 474.5 524.5 574.5 624.5 674.5 774.5 874.5	t 45
11.29 11.43 11.57 11.71 11.85 11.99 12.13 12.27 12.96 13.65 14.33 15.01 16.36 17.70	V
1235.6 1240.4 1245.2 1250.0 1254.8 1259.7 1264.5 1269.3 1293.2 1317.0 1340.8 1364.6 1412.4 1460.4 1.7465 1.7521 1.7576 1.7630 1.7684 1.7737 1.7790 1.7841 1.8089 1.8325 1.8549 1.8762 1.9165 1.9539	h n
1.7403 1.7321 1.7370 1.7030 1.7004 1.7737 1.7750 1.7041 1.0009 1.0323 1.0349 1.0702 1.7303 1.7339	11
405.8 415.8 425.8 435.8 445.8 455.8 465.8 475.8 525.8 575.8 625.8 675.8 775.8 875.8	t 46
11.06 11.20 11.34 11.47 11.60 11.74 11.88 12.02 12.69 13.36 14.03 14.70 16.02 17.33	V
1236.1 1240.9 1245.7 1250.6 1255.4 1260.2 1265.0 1269.8 1293.7 1317.5 1341.3 1365.2 1413.0 1461.0 1.7447 1.7503 1.7558 1.7612 1.7666 1.7719 1.7771 1.7823 1.8071 1.8306 1.8530 1.8743 1.9145 1.9519	h n
1.1705 1.1005 1.1012 1.1000 1.1115 1.1111 1.1025 1.0011 1.0500 1.0500 1.0715 1.5515 1.5525	-
407.2 417.2 427.2 437.2 447.2 457.2 467.2 477.2 527.2 577.2 627.2 677.2 777.2 877.2	t 47
10.84 10.98 11.11 11.24 11.38 11.51 11.64 11.78 12.44 13.10 13.75 14.40 15.69 16.98 1236.6 1241.4 1246.2 1251.0 1255.8 1260.7 1265.5 1270.3 1294.3 1318.1 1341.9 1365.7 1413.5 1461.6	V h
1236.6 1241.4 1246.2 1251.0 1255.8 1260.7 1265.5 1270.3 1294.3 1318.1 1341.9 1365.7 1413.5 1461.6 1.7430 1.7486 1.7541 1.7595 1.7648 1.7701 1.7753 1.7805 1.8053 1.8288 1.8511 1.8724 1.9126 1.9500	
408.5 418.5 428.5 438.5 448.5 458.5 468.5 478.5 528.5 578.5 628.5 678.5 778.5 878.5	t 48
10.62 10.75 10.89 11.02 11.15 11.28 11.41 11.54 12.19 12.84 13.48 14.12 15.38 16.64 1237,1 1241,9 1246,7 1251.6 1256,4 1261.2 1266.0 1270.8 1294.8 1318.6 1342.4 1366.3 1414.1 1462.2	V h
1.7413 1.7469 1.7524 1.7578 1.7631 1.7684 1.7736 1.7788 1.8035 1.8270 1.8493 1.8706 1.9107 1.9481	
409.8 419.8 429.8 439.8 449.8 459.8 469.8 479.8 529.8 579.8 629.8 679.8 779.8 879.8	t 49
10.43 10.55 10.68 10.81 10.94 11.07 11.19 11.32 11.96 12.59 13.22 13.85 15.09 16.32 1237.6 1242.4 1247.2 1252.0 1256.8 1261.7 1266.5 1271.4 1295.3 1319.1 1342.9 1366.8 1414.6 1462.7	V h
1.7397 1.7453 1.7507 1.7561 1.7615 1.7668 1.7720 1.7771 1.8019 1.8253 1.8476 1.8688 1.9090 1.9463	

Table 3: Superheated Steam

-		o. Dapoin		of Supert	aot									
Press.		ĈSat. Water Steam	10°	20°	30°	40°	50°	60°	70°	80°	90°	100°	110°	120°
50	-	281.0		301.0			331.0					381.0		401.0
	Ÿ L	0.02 8.51 250.1 1173.6	8,65	8.78 1183.7	8.92	9.06	9.19 1198.8	9,32			9.71	9.84 1223.4	9.97	10.10
	h n	0.4113 1.6581		1.6716			1.6909					1.7211		
		0.1220 2.0002	2.0017	1,0,10	2.0,02	2.0010	2.0505	1.05.1	1., 000	1.,050	1.7 1.50	2.,222	2., 205	2.7000
51	t	282.3		302.3					352.3				392.3	
	Ā	0.02 8.35			8.76	8.89		9.15	9.28		9.53	9.66		9.91
	h n	251,4 1174,0 0.4130 1.6565		1184.1 1.6700					1209.1 1.7016				1228.8 1.7253	
	4	0.4130 1,0303	1,0033	1.0700	1.0700	1.0030	1.0093	1.0933	1.7010	1.7070	1./130	1./193	1.7433	1.7310
52	t	283.5	293.5	303.5	313.5	323.5	333.5	343.5	353.5	363.5	373.5	383.5	393.5	403.5
	7	0.02 8.21			8.60	8.73			9.12	9.24		9.49	9.61	9.74
	h	252.6 1174.3		1184.5			1199.6					1224.3		
	n	0.4147 1.6549	1.0017	1.6684	1.6750	1.6814	1.6877	1.6939	1.7001	1.7061	1.7020	1.7179	1.7237	1.7294
53	t	284.7 ¢	294.7	304.7	314.7	324.7	334.7	344.7	354.7	364.7	374.7	384.7	394.7	404.7
	v	0.02 8.05	8.19	8.32	8.45	8.58	8.70	8.83	8.96	9.08	9.20	9.32		9.56
	h	253.9 1174.7		1184.9					1209.9				1229.6	
	n	0.4164 1.6534	1.6602	1.6669	1.6735	1.6799	1.6862	1 6924	1.6986	1.7046	1.7105	1.7164	1.7222	1.7279
54	÷	285.9	295 9	305.9	315 Q	325.9	335 Q	345 9	355.9	365 9	375 9	385 Q	395.9	405 9
UZ.	v	0.02 7.91			8.30	8.43	8.55	8.67	8 80		9.04	9.16	9.28	9.40
	h	255.1 1175.0		1185.2		1195.4			1210 4		1220.2	1225.1	1230.0	1234.9
	n	0.4180 1.6519	1.6587	1.6654	1.6720	1.6784	1.6847	1.6909	1.6971	1.7031	1.7090	1.7149	1 7207	1.7264
55		287.1	207 1	307.1	217 1	327 1	337 1	347 1	357.1	367 1	277 1	397 1	397.1	407 1
	7	0.02 7.78	7.91	8.03	8.16	8 28	8.40	8.52	8.64	8.76	8.88	9.00	9.12	9.24
	'n	256.3 1175.4		1185.6					1210 8				1230.5	
	n	0.4196 1.6505	1.6573	1.6640	1.6706	1.6770	1.6833	1.6895	1.6957	1.7017	1.7076	1.7135	1.7193	1.7250
£0		288.2	208.3	308.2	2187	228.2	229.2	2/8 2	358.2	269.0	279.0	299.0	398.2	408.3
56	7	0.02 7.65	7.78	7.90	8.02	8.14		8.38			8.74	8.85	8.96	9.08
	'n	257.5 1175.7		1185.9					1211.1				1230.9	
	n	0.4212 1.6490	1.6558	1.6625	1.6691	1.6755	1.6818	1.6880	1.6941	1.7002	1.7062	1.7120	1.7178	1.7235
En		000.4	000.4	200.4	210.4	200.4	220.4	240.4	250.4	260.4	270.4	200.4	399.4	400.4
57	T V	289.4 0.02 7.52	7.65	309.4 7.77	7.89	8.01		8.24	359.4 8.36	8.48			8.82	
	'n	258.7 1176.6		1186.3					1211.5				1231.3	
	n	0.4227 1.6475				1.6740	1.6803	1.6865	1.6926	1.6987	1.7047	1.7105	1.7163	1.7220
		200 5	200 5	210 5	200 5	220 5	240 5	250 5	260 5	250 5	200 F	200 5	400 5	430.5
58	Ţ	290.5 0.02 7.40	300.5 7.52	310.5 7.64	320.5 7.76	330.5 7.88	340.5 8.00	350.5 8.11	300.5 8.23	370.5 8.34	380.5 8.45	390.5 8.57	400,5 8,68	8.79
	'n	259.8 1176.4		1186.6					1211.9				1231.7	
	n	0.4242 1.6460		1.6595			1.6788	1.6850	1.6911	1.6972	1.7032	1.7090	1.7148	1.7205
		001.6	201.6	227.6	207.6	227.6	241.6	251 6	261.6	271 6	201 6	201.6	401.6	411.6
59		291.6 0.02 7.28	301.6 7.40	311.6 7.52	321.6 7.64	331.6 7.76	341.6 7.87	351.6 7.98	361.6 8.10		8.32	391.6 8.43	401.6 8 54	8.65
	V h	261.0 1176.7				1197.2			1212.3				1232.1	
	ñ	0.4257 1.6446				1.6712			1.6898			1.7076	1.7134	1.7191
				610 F	H	-	240.77	250 5	260 7	200 0	200 7	200 7	400 77	410.77
60		292.7 0.02 7.17		312.7 7.40					362.7 7.97		382.7 8.19	392.7 8.30	402,7 8.41	
	Þ	262.1 1177.0							1212.7				1232.5	
	n	0.4272 1.6432				1.6698			1.6884			1.7062	1.7120	1.7177
144.00		202.0	202.0	222.0	202.0	222.0	2/2 6	252 0	262 0	277 0	202 0	202 0	402 o	412 0
61	t	293.8 0.02 7.06	303.8 7.18	313.8 7.29	323.8 7.40	333.8 7.52	343.8 7.63	333.8 7.74	363.8 7.85	3/3.8 7.95		393.8 8.17	403,8 8,28	8.39
	h	263.2 1177.3		1187.6					1213.0				1232.9	
	n	0.4287 1.6419		1.6555					1.6871				1.7107	
-		204.0	204.0	314.9	204 0	22/10	244 0	25 <i>4</i> O	364.9	274.0	284 D	204.0	404.9	4140
62	¥	294.9 0,02 6.95	7.06					7.62	7.73	7.83		8.05		8.26
	ň	264.3 1177.6				1198.3						1228,4		
	n	0.4302 1.6406				1.6673			1.6858		1.6978	1.7037	1.7094	1.7150
			-				(20)							

(30)

											Deg	rees of S	uperheat	
130° 1	140°	150°	160°	170°	180°	190°	200°	250°	300°	350°	400°	500°	600°	Press.
411.0 4	21.0	431.0	441.0	451.0	461.0	471.0	481.0		581.0		681.0	781.0	881.0	t 50
10.23 1 1238.1 12	0.35			10.73 1257.3					12.36 1319.7			14.80	16.01 1463.3	V V
1.7382 1.				1.7599					1.8237				1.9445	h n
412.3 4	100.2	432.3	110 2	452.3	160 2	470.2	100.0	E20.2	500.3	620.2	con a	#00 A	000.0	. 24
10.04 1				10.54					582.3 12.13			782.3 14.52		t 51 v
1238.5 12				1257.8			1272.4	1296.3	1320.2	1344.0			1463.8	h
1.7366 1.	.7421	1.7475	1.7529	1.7583	1.7636	1.7688	1.7739	1.7986	1.8220	1.8442	1.8654	1.9054	1.9427	n
413.5 4				453.5					583.5			783.5		t 52
9.86 9 1239.0 12	9,98 243 R			10.35 1258.3			10.71 1272.8		11.91			14.26 1416.2		V h
1.7350 1.				1.7567			1.7721						1.9409	n
414.7 4	יל אכו	1217	1117	454.7	1617	171 7	1917	E21 7	584.7	6217	6017	◆ 784.7	0017	t 53
	9.81	9.93		10.16					11.70			14.01		v 03
1239.4 12				1258.7					1321.1				1464.8	h
1.7335 1.	.7390	1.7444	1.7498	1,7551	1.7604	1.7656	1.7707	1.7954	1.8187	1.8409	1.8620	1.9020	1.9392	n
415.9 4				455.9					585.9			785.9		t 54
9.52 9 1239.8 12	9.64 244 7	9.75	9.87 1254 3	9.99 1259,2	10.11				11.49 1321.6			13.76	14.88 1465.3	v h
1.7320 1.				1.7536					1.8172				1.9375	n
417.1 4	107.1	127 1	117 1	457.1	167 1	<i>177</i> 1	107 1	527 1	587.1	627 1	687 1	787.1	007 1	t 55
	9.47	9.59	9.70	9.82	9.94	10.05			11.30			13.52		v 50
1240.2 12				1259.6					1322.0				1465.8	h
1.7306 1.	./301	1./415	1./408	1.7521	1./5/4	1.7626	1./6//	1./924	1.8157	1.83/8	1.8589	1.8988	1.9359	n
418,2 4				458 2		478.2	488.2		588.2			788.2	888.2	t 5 6
9.20 9 1240.7 12	9.32 245.5	9.43 1250.4	9.54 1255.2	9,66 1260,1	9.77 1264.9	9.88 1269.8			11.10 1322.5	1346.4		13,29 1418.2	14.37	V h
1.7291 1.				1.7506					1.8141				1.9343	n
419,4 4	29.4	439,4	449.4	459.4	469.4	479.4	489.4	539.4	589.4	639.4	689.4	789.4	889.4	t 57
	9.16	9.27	9.38	9.50	9.61	9.72			10.92			15.07		V
1241.1 12 1.7276 1.		1250.8		1260.5 1.7491			1275.1 1.7647				1370.8		1466.7 1.9326	h n
420.5 4 8.90 9	130.5 9.01	440.5 9.12	450.5 9.23	460.5 9.34	470.5 9.45	480.5 9.56	490.5 9.67		590.5 10.74			790.5 12.86		t 58 V
1241.5 12		1251.2	1256.1	1260.9	1265.8	1270.6	1275.5	1299.5	1323.4	1347.3	1371.2	1419.1	1467.2	h
1.7261 1.	.7316	1.7370	1.7423	1.7476	1.7529	1.7581	1.7632	1.7878	1.8110	1.8330	1.8540	1.8939	1.9310	n
421.6 4				461.6					591.6			791.6		t 5 9
8.76 8 1241.9 12	8.87	8.98	9,09	9.19 1261.4		9.41			10.57	11.09 1347.8		12.65	13.68 1467.7	V h
1,7247 1.				1.7462			1.7618						1.9294	
422.7 4	122 7	1127	1507	462.7	ልንን ን	482 7	402.7	542.7	592.7	642.7	692.7	792.7	892.7	t 60
	8.73	8.84	8.94	9.05	9.15	9.26	9.36	9.89	10.41	10.92		12.45		¥
1242.3 12				1261.8			1276.4 1.7603				1372.2			h -
1.7233 1.	.7288	1.7342	1.7395	1.7448	1.7500	1./554	1.7003	1./049	1.0001	1.0301	1.8511	1.0900	1.94/9	n
423.8 4				463.8					593.8 10.25			793.8		t 61
8.50 8 1242.7 12		8.70 1252.5		8.91 1262.2	9.02 1267.0	9.12 1271.9	9.22 1276.8					12.26 1420.4		v h
1.7219 1.		1.7328	1.7382	1.7435	1.7487	1.7539	1.7590						1.9265	n
424.9 4	34,9	444.9	454.9	464.9	474.9	484.9	494.9	544.9	594.9	644.9	694.9	794.9	894.9	t 62
8.36	8.4 6	8.57	8.67	8.77	8.88	8.98			10.09			12.07		7
1243.1 1: 1.7206 1.		1252.9 1.7315		1262.6 1.7422			1277.2 1.7577			1.8273	1373.0 1.8483		1469.1 1.9250	h n
			41,503	ART 1866	-	_,, _,,	(31)							-

(31)

Table 3: Superheated Steam

Degrees of Superheat

			Degrees (of Superh	eat									
Press. lbs.	Water	Sat, Steam	10°	20°	30°	40°	50°	60°	70°	80°	90°	100°	110°	120°
63 t	295		305.9		325.9	335.9				375.9	385.9			415.9
V	0.02	6.85	6.96	7.07	7.18	7.29	7.40	7.51	7.61	7.72	7.82	7.93	8.03	8.14
h	265.4		1183.1						1213.8 1.6845			1228.7 1.7024		
n	0.4316	1.0393	1.6461	1.0329	1.0393	1.0039	1.0/44	1.0/04	1.0043	1.0903	4.0903	1.7024	1.7001	1./13/
64 t	29	7.0	307.0	317.0	327.0	337.0	347.0	357.0	367.0	377.0	387.0	397.0	407.0	417.0
V	0.02	6.75	6.86	6.97	7.08	7,19	7.29	7.40	7.50	7.60	7.71	7.81	7.91	
h		1178.2			1193.8				1214.1			1229.1		
n	0.4330	1.6380	1.6448	1.6516	1.6582	1.6646	1.6709	1.6771	1.6832	1.6892	1.6952	1.7011	1.7068	1.7124
65 t	29	8.0	308.0	318.0	328.0	338.0	348.0	358.0	368.0	378.0	388.0	398.0	408.0	418.0
▼	0.02	6.65	6.76	6.87	6.98	7.09	7.20	7.30	7.40	7.50	7.60	7.70	7.80	7.90
h		1178.5			1194.1				1214.5				1234.4	
n	0.4344	1.6368	1.6436	1.6504	1.6570	1.6635	1.6698	1.6760	1.6821	1.6881	1.6940	1.6999	1.7056	1.7112
66 t	29	9.0	309.0	319.0	329.0	339 N	349.0	359 N	369.0	379 n	389.0	399.0	409.0	419 N
Δ Δ	0.02	6.56	6.66	6.77	6.88	6.98	7.09	7.19	7.29	7.39	7.49	7.59	7.69	7.79
h		1178.8			1194.4	1199.5	1204.7	1209.8	1214.8	1219.8	1224.8	1229.8	1234.8	1239.7
n	0.4358	1.6355	1.6423	1.6491	1.6557	1.6622	1.6685	1.6747	1.6808	1.6868	1.6927	1.6986	1.7043	1.7099
67 t	20	0.0	310.0	220 O	330.0	240.0	350.0	360 0	370.0	290 A	390.0	400.0	410.0	420 O
V V	0.02	6.47	6.58	6.68	6.78	6.89	6.99	7.09	7.19	7.29	7.39	7.49	7.58	7.68
h		1179.0			1194.7				1215.1				1235.2	
n	0.4371	1.6343	1.6411	1.6479	1.6545	1.6610	1.6673	1.6735	1.6796	1.6856	1.6915	1.6974	1.7031	1.7087
68 t	30	1,0	211.0	221 A	331.0	241.0	351.0	261 N	371.0	291 A	391.0	401.0	411.0	421.0
	0.02	6.38	6.48	6.58	6.69	6.79	6.89	6.99	7.09	7.19	7.29	7.38	7.48	7.57
h		1179.3			1195.0				1215.5				1235.5	
n	0.4385	1.6331	1.6399	1.6467	1.6534	1.6598	1.6661	1.6723	1.6784	1.6844	1.6903	1.6961	1.7019	1.7075
69 t	20	2.0	312.0	202.0	332.0	242.0	352.0	262.0	372.0	202.0	392.0	402.0	412.0	400.0
09 r	0.02	6.29	5.39	6.49	6.60	6.70	6.80	6.90	6.99	7.09	7.19	7.28	7.38	7.47
ň		1179.6			1195.3				1215.8				1235.8	
n	0.4398	1.6319	1.6387	1.6455	1.6521	1.6586	1.6649	1.6711	1.6772	1.6832	1.6892	1.6950	1.7007	1.7063
70 ±	. 20	20	312.9	222.0	332.9	242.0	352.9	362,9	372.9	382.9	392.9	402.9	412,9	422.9
70 t	0.02	2.9 6.20*	6.30	6.40	6.51	6.61	6.71	6.81	6.90	7.00	7.09	7.18	7.28	7.37
'n		1179.8				1200.8			1216.1				1236.2	
n	0.4411	1.6307	1.6376	1.6444	1.6510	1.6574	1.6637	1.6699	1.6760	1.6820	1.6880	1.6939	1.6996	1.7052
771 4	20	20	313.9	202.0	333.9	343.9	353.9	363.9	272 0	383.9	393.9	403.9	413.9	423.9
71 t	0.02	3.9 6.12	6.22	6.32	6.42	6.52	6.62	6.72	6.81	6.90	7.00	7.09	7.18	7.27
'n		1180.1				1201.1			1216.4				1236.5	
n	0.4424	1.6296	1.6365	1.6433	1.6499	1.6563	1.6627	1.6689	1.6750	1.6810	1.6869	1.6928	1.6985	1.7041
72 t	30	14.8	314 8	324 R	334.8	344 R	354.8	364.8	374.8	384 R	394.8	404.8	414.8	424.8
v		6.04	6.14	6.24	6.34	6,44	6.54	6.63	6.72	6.81	6.90	6.99	7.08	7.17
h	274.5	1180.4	1185.7	1191.0	1196.2	1201.4	1206.6	1211.7	1216.8	1221.8	1226.8	1231.8	1236.8	1241.7
מ	0.4437	1.6285	1.6354	1.6422	1.6488	1.6553	1.6616	1.6678	1.6739	1.6799	1.6858	1.6917	1.6974	1.7030
73 t	31	05.8	315.8	325.8	335.8	345.8	355.8	365.8	375.8	385.8	395.8	405.8	415.8	425.8
10 1		5.96	6.06	6.15	6.25	6.35	6.45	6.54	6.63	6.73	6.82	6.91	7.00	7.09
h		1180.6	1185.9	1191.2	1196.5	1201.7			1217.1				1237.1	
r	0.4449	1.6274	1.6343	1.6411	1.6478	1.6543	1.6606	1.6667	1.6728	1.6788	1.6847	1.6906	1.6963	1.7019
74 t	. 20	06.7	316.7	326.7	336.7	346.7	356.7	366.7	376.7	386.7	396.7	406.7	416.7	426.7
V V		5.89	5.98	6.07	6,17	6.27	6.36	6.46	6.55	6,64	6.73	6.82	6.91	7.00
Ì	276.5	1180.9	1186.2			1202.0			1217.4					1242,4
I	0.4462	2 1.6263	1.6332	1.6400	1.6467	1.6532	1.6595	1.6656	1.6717	1.6777	1.6837	1.6895	1.6952	1.7008

t=temperature in F. degs. To Fahr. absolute = t° + 459.6°. Internal energy = total heat in B. t. u.
L=total heat in B. t. u.
L=1/J=1.286×10⁻³ B. t. u. per ft. lb. [$\bar{3}$.10 929]. Values for saturated steam 144 A=0.1852 [$\log = \bar{1}$.26 764].

											De	grees of S	Superheat	
130°	140°	150°	160°	170°	180°	190°	200°	250°	300°	350°	400°	500°	600°	Press. lbs.
425.9	435.9	445.9	455.9	465.9	475.9	485.9	495.9	545.9	595.9	645.9	695.9	795.9	895,9	t 63
8.24	8.34	8.44	8.54	8.64	8.74	8.84	8.94	9.44	9.94	10.43		11.89	12.85	V
1243.5 1.7193				1263.0 1.7409					1325.5			1421.2		h
1.7193	1.7440	1.7302	1.7330	1.7409	1.7401	1.7515	1.7304	1.7009	1.8040	1,8200	1.8469	1.8866	1.9236	n
427.0	437.0	447.0	457.0	467.0	477.0	487.0	497.0	547.0	597.0	647.0	697.0	797.0	897.0	t 64
8.12		8.32	8.42	8.52	8.62	8.72	8.81	9.31	9.80	10.28		11.71		▼
1243.9				1263.3					1326.0				1469.9	h
1.7180	1.7235	1.7290	1,7343	1.7396	1.7448	1.7500	1.7551	1.7796	1.8027	1.8246	1.8455	1.8852	1.9222	n
428.0	438.0	448.0	458.0	468.0	478.0	488.0	498.0	548 0	598.0	648.0	698.0	798.0	898.0	t 65
8.00	8.10	8.20	8.29	8.39	8.49	8.59	8.69	9.17	9.65	10.12		11.54	12.48	V 30
1244.2				1263.7					1326.4		1374.3	1422.1	1470.3	h
1.7168	1.7223	1.7277	1.7331	1.7384	1.7436	1.7488	1.7539	1.7784	1.8014	1.8233	1.8442	1.8839	1.9208	n
429.0	439.0	449.0	459.0	469 O	479.0	489.0	499 n	549.0	500 A	649.0	600 N	799.0	800 N	t 66
7.89	7.98	8.08	8.18	8.28	8.37	8.47	8.56	9.04	9.51	9.98		11.38	12.30	v
1244.6	1249.5		1259.2	1264.1	1269.0	1273.9			1326.8		1374.8	1422.6	1470.8	h
1.7155	1.7210	1.7264	1.7318	1.7371	1.7423	1.7474	1.7525	1.7771	1.8001	1.8220	1.8429	1.8825	1.9194	n
430.0	440.0	450.0	460 O	470.0	480.0	490.0	500,0	550.0	600 A	650.0	700.0	800 O	000.0	t 67
7.78	7.88	7.97	8.07	8.16	8.26	8.35	8.45	8.92	9.38	9.84		800.0 11.22	12.13	Δ 01
1245.0				1264.5					1327.2				1471.2	'n
1,7143	1.7198	1.7252	1.7306	1.7359	1.7411	1.7462	1.7513	1.7758	1.7988	1.8207	1.8416	1.8812	1.9181	n
421.0	443.0	451.0	461.0	471.0	401 A	401.0	501.0	551.0	601.0	651.0	701.0	901 O	001.0	+ co
431.0 7.67	7.77	451.0 7.86	461.0 7.96	4/1.0 8.05	481.0 8.14	491.0 8.23	8.33	551.0 8.79	601.0 9.25	9.70		801.0 11.06		t 68 V
1245.3				1264.8					1327.5				1471.6	h
1.7131	1.7186	1,7240	1.7294	1.7347	1.7399	1.7450	1,7501	1.7746	1.7976	1.8195	1.8403	1.8799	1.9168	n
420.0	440.0	450.0	460.0	470.0	400.0	400.0	F00.0	550.0	600.0	650.0	700.0	000.0	000.0	+ 60
432.0 7.56	442.0 7.66	452.0 7.75	462.0 7.85	472.0 7.94	482.0 8.03	492.0 8.12	502.0 8.22	552.0 8.67	602,0 9,12	652,0 9,57		802,0 10,91	902.0	t 69 V
1245.6				1265.2					1327.9				1472.0	'n
1.7119				1.7335					1.7963				1.9155	n
														. ==
432.9		452.9		472.9 7.83	482.9 7.92			552.9 8.56	602,9 9,01	652,9 9,45		802.9	902.9 11.63	t 70
7.46 1246.0	7.56 1250 9	7.65 1255 8	7.74 1260 7	1265.5		8.02 1275 3	8.11 1280 2		1328.3		9.89 1376 2		1472.4	v h
1,7107				1.7323					1,7951			1.8773		n
	443.9		463.9		483.9			553.9		653.9		803.9		t 71
7.36 1246,3	7.46	7.55	7.64	7.73 1265.9	7.82	7.91 1275 7	8.00 1280 6	8.44 1304.7	8.88 1328.7	9.32	9.76 1376.6	1424.6	11.48 1472 R	v h
1.7097				1.7312					1.7939			1.8761		n
	444.8	454.8	464.8		484.8				604.8 8.74	654.8 9.16		804.8 10.42		t 72
7.25 1246,7	7.34 1251 6	7.43 1256 5	7.52	7.61 1266.3	7.70	7.79 1276 1	7.88 1281 0	8.31 1305 0	1329.0		9.58 1377 0	1425.0		V h
1.7086				1.7301					1.7928				1.9117	
			•				404 0	·	505 5		707 C	007.0	001.0	
435.8				475.8					605.8			805.8		t 73
7.18 1247.0	7.27 1251 0	7.36 1256.8	7.45	7.54 1266.6	7.63	7.71 1276 4	7.80 1281 3	8.23 1305 4	8.66 1329.4	9.08 1353.3		103.4 1425.3		V h
1.7075				1.7290					1.7917				1.9105	n
					•						wa	2215		
436.7				476.7			506.7	556.7	606.7			806.7		t 74
7.08 1247.3	7.17	7,26	7,35	7.44 1266.9	7.52	7.61		8.13 1305.8	8.55 1329.8	8.97 1353 7	9.38 1377 7	10.20	1474.0	♥ h
1,7064		1.7173	1.7226	1,7279	1.7331	1.7382			1.7905				1,9093	-
			_,,	_,,,		_,								-

1 kg. per sq. om. = 14.22 lbs. per sq. in. [log=1.15 300]. 1 cm. meter=35.31 cm. ft. [log=1.54 795].

To change degs. C. to degs. F., multiply by \$\frac{1}{2}\$, and add 32. To change mean kg. calories per kg. to mean B.t.u. per lb., multiply by \$\frac{1}{2}\$. Entropy same in both systems.

Table 3: Superheated Steam

	å		Degrees o	of Superh	eat								*	
Press.	Water	Set. Steam	10°	20°	30°	40°	50°	60°	70°	80°	90°	100°	110°	120°
75 t	30° 0.02	7.6 5.81	5.91	327.6 6.00	6.10	6.19	357.6 6.28	6.37	6.46	6.55	397.6 6.64	407.6 6.73	6.82	427.6 6.91
h n	277.4 0.4474		1186.5 1.6321				1207.5 1.6584	1.6645	1.6706	1.6767	1.6825	1232.8 1.6883	1.6941	1.6998
76 t	30		318.5		338.5	348.5 6.12	358.5 6.21	368.5 6.30	378.5 6.39	388.5 6.48	398.5 6.56	408.5 6.65	418.5 6.74	428.5 6.82
V h		5.74 1181.4	5.83 1186.7	5.92 1192 0	6.02		1207.8					1233.1		
n		1.6242	1.6310	1.6378	1.6445	1.6509	1.6572	1.6634	1.6695	1.6756	1.6815	1.6873	1.6930	1.6986
77 t		9.4		329.4					379.4				419.4	
Ž	0.02	5.67 1181.6		5.85 1192.2	5.95	6.04	6.13 1208.0	6.22	6.31	6.40	6.49	6.57 1233,4	6.65	
h n		1.6231		1.6368			1.6562					1.6863		
78 t		0.3		330.3					380.3				420.3	
V h	0.02	5.60 1181.8		5.78 1192.6	5.87	5,97	6.06 1208.3	6.15	6.24	6.32	6.41	6.49 1233.7	6.57	6.66
n		1.6221		1.6358	1.6425	1.6490	1.6553					1.6854		
79 t		1.2	321.2		341.2			371.2		391.2			421.2	
V h	0.02	5,54 1182.1	5.63	5.72 1192.8	5.81	5.90	5.99 1208 6	6.07	6.16	6.25	6.33	6.41 1234.0	6.49	6.58
h n		1.6210		1.6347			1.6542					1.6843		
80 t	31	2.0	322,0	332.0	342.0	352.0	362.0	372.0	382.0	392.0	402.0	412.0	422.0	432.0
V	0.02	5.47	5.56	5.65	5.74	5.83	5.92	6.00	6.09	6.18	6.26	6.34	6.42	6.50
h n		1182.3 1,6200		1193.0 1.6338			1208.8 1.6532					1234.3 1.6833		
81 t	31	2.9	322.9	332.9	342.9	352.9	362.9	372.9	382.9	392.9	402.9	412.9	422.9	432.9
y	0.02	5.41	5.50	5.58	5.67	5.76	5.85	5.94	6.03		6.19	6.27	6.35	6.43
n n		1182.5 1.6190		1193.3 1.6328			1209.1 1.6523					1234.6 1.6823		
82 t	31	3.8	323.8	333.8	343.8	353.8	363 8	373.8	383.8	393.8	403.8	413.8	423.8	433.8
¥	0.02	5.34			5.61	5.70	5.78	5.86	5.95		6.11	6.19	6.27	6.35
n n		1182:8 1.6180		1193.6 1.6318			1209.4 1.6513		1.6636			1235.0 1.6813		
83 t	31	4.6	324.6	334.6	344.6	354.6	364.6	374.6	384.6	394.6	404.6	414.6	424.6	434.6
y		5.28	5.37	5.45	5.54	5.63	5.72	5.80	5.88	5.96	6.04	6.12		6.28
h n		1183.0 1.6170		1193.8 1.6308					1220.0 1.6626			1235.2 1.6804		
84 t		15.4 5.22	325.4 5.31	335.4 5.39	345.4 5.48	355.4 5.57	365.4 5.65	375.4 5.73	385.4 5.82	395.4 5.90	405.4 5.98	415.4 6.05	425.4 6.13	435.4 6.21
y h		1183.2		1194.0					1220.3			1235.5		
n		1.6160	1.6230	1.6298	1.6365	1.6430	1.6493	1.6555	1.6616	1.6677	1.6736	1.6794	1.6851	1.6907
85 t		16.3	326.3			356.3	366.3		386.3		406.3		426.3	,
∀		5.16 1183 A	5.25	5.33	5.42	5.51 1204.9	5.59 1210 2	5.67 1215 4	5.75 1220 6	5.83 1225 7	5.91 1230 7	5.99 1235 8	6.06	6.14 1245 8
		1.6151									1.6727			
86 t		17.1	327.1	337.1	347.1	357.1	367.1	377.1	387.1	397.1	407.1	417.1	427.1	437.1
Y			5.19								5.85			
h		1183.6 1.6141									1231.0 1.6717			
														•
87 t		17.9	327.9	337.9	347.9	357.9	367.9 5.47	377.9	387.9	397.9	407.9	417.9		
b		5.05 1183.8		5,22 1194.7			1210.7	1215.0	1221 1	3.71 1226.2	1231.3	5.86 1236.4	3.93 1241 4	1246.3
		1.6132					1.6466	1,6528	1.6589	1.6649	1.6708	1.6766	1.6823	1.6879
	*		•			•	(34)		•		•			

30°	140°	150°	160°	170°	180°	190°	200°	250°	300°	350°	400°	500°	uperheat 600°	Press lbs.
37.6		437.0 7.17	467.6 7.26	477,6 7.34	487.6	497.6 7.51	507.6			657.6	707.6			t 75
7.00	7.09			1267.3	7.43		7.60	8.02	8.44	8.86 1354.1	9.27	10.08	1474.4	V h
	1252.6 1.7108	1,7162							1.7894			1.8714		h n
29 5	448,5	458 5	468 5	478.5	488 5	408 5	508 5	558 5	608.5	658 5	708 5	808.5	one s	t 76
	7.00	7.08		· 7.25	7.34	7.42	7.51	7,93	8.34	8.75	9.15		10.76	
	1252.9	1257.8							1330.5				1474.8	
	1.7097			1.7256						1.8101			1,9069	
139.4	449.4	459.4	469,4	479.4	489.4	499.4	509.4	559.4	609.4	659.4	709.4	809,4	909.4	t 77
6.82	6.91	7.00	7.08	7.16	7.25	7.33	7.42	7.83	8.24	8.64	9.04	9.84	10.63	V
248.3	1253.2	1258.1	1263.0	1267.9	1272.8	1277.7	1282.6	1306.7	1330.8	1354.8	1378.7	1426.8	1475.1	h
.7033	1.7087	1,7141	1.7194	1.7246	1.7298	1.7349	1,7400	1.7643	1.7872	1.8090	1.8298	1.8691	1,9058	n
	450.3			480.3					610.3			810.3		t 78
	6.83	6.92	7.00	7.08	7.16	7.24	7.33	7.74		8.54	8.93	9.72	10.50	V
	1253.5					1278.0				1355.2			1475.5	h
.7023	1.7077	1.7131	1.7184	1.7236	1.7288	1.7339	1.7389	1.7633	1.7862	1.8080	1.8287	1.8081	1.9047	n
H 1.2	451.2	461.2	471.2	481.2	491.2	501.2	511.2	561.2	611.2	661.2	711.2	811.2	911.2	t 79
	6.95	6.83	6.91	6.99	7.08	7.16	7.24	7.64	8.04	8.43	8.82	9.60		7
	1253.8					1278.4				1355.5			1475.8	h
.7012	1,7066	1.7120	1.7173	1.7225	1,7277	1.7328	1.7378	1.7622	1.7851	1.8068	1.8276	1.8669	1.9036	n
142.0	452.0	462.0	472.0	482.0	492.0	502.0	512.0	562.0	612.0	662.0	712.0	812.0	912.0	t 80
6.58	6.67	6.75	6.83	6.91	7.00	7.08	7.17	7.56	7.95	8.34	8.72	9.49	10.24	V
249.2	1254.1					1278.7				1355.9	1379.8	1427.9	1476.2	h
.7001	1.7056	1.7110	1.7163	1.7215	1.7267	1.7318	1.7368	1.7612	1.7840	1.8058	1.8265	1.8658	1.9025	n
	452.9			482,9						662.9		812.9		t 81
	6.60	6.68	6.76	6.84	6.92	7.00	7.08	7.47	7.86	8.25		9.39		Ā
	1254,4 1,7046					1279.0 1.7308				1356.2			1476.6 1.9014	
1420	452.0													
6.43	453.8 6.52		6.68	483.8 6.76	493.8 6.84	6.92	7.00	7.39		663.8 8.15		813.8 9.27		t 82
	1254.8					1279.3				1356.5			1476.9	
	1.7036					1.7298				1.8037			1.9003	
144.5	454.6	464.6	474.6	484.6	494.6	504.6	514.6	564.6	614.6	664.6	714.6	814.6	914.6	t 83
6.36	6.44	6.52	6.60	6.68	6.76	6.84	6.92	7,30	7.68	8.05	8.42	9.17	9.90	7
250.2	1255.1	1260.0	1264.9	1269.8	1274.7	1279.7	1284.6	1308.8	1332.9	1356.9	1380.8	1428.9	1477.2	h
.6971	1.7026	1.7080	1.7133	1.7185	1.7237	1.7288	1.7338	1.7581	1.7810	1.8027	1.8234	1.8626	1.8992	n
145.4	455.4	465.4		485.4			515.4	565.4	615.4	665.4		815.4	915.4	t 84
	6.37	6.45		6.61			6.84	7.22	7.60			9.06	9.79	7
	1255.3					1279.9				1357.2			1477.6	
.6963	1,7017	1.7070	1.7123	1.7175	1,7227	1.7278	1.7328	1.7571	1.7799	1.8017	1.8224	1.8616	1,8981	n
	456.3			486.3					616.3			816.3		t 85
6.22 250 e	6.30	6.38	6.45	6.53	6.61	6.69	6.76	7.14	7.51	7.88	8.24		9.68	V
	1255,7 1,7008			1270.4 1.7166					1333.5 1.7790				1477.9 1.8971	
447 i	457.1	467 1	Δ77 1	487.1	<i>4</i> 07 1	507 1	5177	567 1	617.1	667 1	717 1	817.1	017 1	+ 00
	6.23	6.31	6,38	6.46	6.54	6.62			7.43			8,86	917.1	t 86
	1255.9			1270.7						1357.8			1478.2	h
	1.6998			1.7157						1.7997				n
447.9	457.9	467.9	477.9	487.9	497.9	507.9	517.9	567.9	617.9	667.9	717.9	817.9	917.9	t 87
6.09	6.16	6.24	6.32		6.48	6,56	6.63	7.00	7.37	7.73		8.81	9.52	7
	1256.2			1271:0	1275.9	1280.9				1358.1			1478.5	
.6934	1.6989	1.7043	1.7095	1.7147	1 7199	1.7250	1.7300	1.3542	1.7770	1.7988	1.8194	1.8586	1.8951	n

Table 3: Superheated Steam

			Degrees o	f Superhe	at									
Press.	Water	8at. Steam	10°	20°	30°	40°	50°	60°	70°	80°	90°	100°	110°	120°
88 t	31	8.7	3 28.7	338.7	348.7	358.7	368.7	378.7	388.7	398.7	408.7	418.7	428.7	438.7
y	0.02	5.00	5.08	5.16	5.24	5.33	5.41	5.49	5.57	5.65	5.72	5.80	5.87	5.95
h		1184.0	1189.5						1221.4			1236.6		
n	0,4023	1.6123	1.6193	1.0202	1.0329	1.0394	1.045/	1.0319	1.6580	1.0041	1,0/00	1.6758	1,0013	1,00/1
89 t	31	.9.5	329.5	339.5	349.5	359.5	369.5	379.5	389.5	399.5	409.5	419,5	429.5	439.5
y		4.94	5.02	5.10	5.19	5.27	5.35	5.43	5.51	5.59	5.66	5.74	5.81	5.88
h		1184.2		1195.2					1221.6			1236.9		
n	0.4033	1.6114	1.0184	1.6253	1.0320	1.0385	1.0448	1.0310	1.6572	1,0032	1.0091	1.6749	1.0000	1.0002
90 t	32	20,3	330.3	340.3	350.3	360.3	370.3	380.3	390,3	400.3	410.3	420,3	430.3	440.3
V		4.89	4.97	5.05	5.13	5.21	5.29	5.37	5.44	5.52	5.60	5.67	5.74	5.82
h		1184.4		1195.4					1221.9			1237.2		
n	0.4644	1.6105	1.6175	1.6244	1.6311	1.6376	1.6440	1.6502	1.6563	1.0023	1.6682	1.6740	1.6797	1,0853
91 t	32	21.1	331.1	341.1	351.1	361.1	371.1	381.1	391.1	401.1	411.1	421.1	431.1	441.1
V	0.02	4.84	4.92	5.00	5.08	5.16	5.24	5.31	5.39	5.47	5.54	5.61	5.69	5.76
h		1184.6		1195.7					1222.1				1242.4	
n	0.4654	1.6096	1.6166	1.6235	1.6302	1.6367	1.6431	1.6493	1.6554	1.0012	1.6674	1.6732	1,6788	1.0844
92 t	32	21.8	331.8	341.8	351.8	361.8	371.8	381.8	391.8	401.8	411.8	421.8	431,8	441.8
V		4.79	4.87	4.95	5.03	5.11	5.19	5.26	5.33	5.41	5.48	5.56	5.63	5.70
b		1184.8		1195.9					1222.4			1237.7		
n	0.4664	1.6087	1.6157	1.6226	1,6293	1.6359	1.6423	1.6485	1.6546	1.6606	1.6665	1.6723	1.6780	1.6836
93 t	32	22.6	332.6	342,6	352.6	362.6	372.6	382.6	392.6	402.6	412.6	422.6	432,6	442.6
V	0.02	4.74	4.82	4.90	4.98	5.06	5.14	5.21	5.28	5.36	5.43	5.50	5.57	5.64
h		1185.0		1196.1					1222.6					1248.0
r	0.4674	1,6078	1.6148	1.6217	1.6284	1.6350	1.6414	1.6476	1.6537	1.6597	1.6656	1.6714	1.6771	1.6827
94 t	32	23.4	333.4	343.4	353.4	363.4	373.4	383.4	393.4	403.4	413.4	423.4	433.4	443.4
V	0.02	4.69	4.77	4.85	4.93	5.01	5.09	5.16	5.23	5.30	5.37	5.45	5.52	5.59
h		1185.2		1196.3	-				1222.9					1248.2
1	U.4684	1.6069	1.6139	1.6208	1.62/6	1.6341	1.6405	1.0407	1.6528	1.0588	1.004/	1.6/05	1.6/62	1.6818
95 t	- 32	24.1	334.1	344,1	354,1	364,1	374.1	384,1	394,1	404.1	414.1	424.1	434.1	444.1
y	0.02	4.65 •	4.73	4.80	4.88	4.96	5.03	5.10	5.18	5.25	5.32	5.39	5.46	5.53
þ		1185.4		1196.5					1223.1					1248.5
r	0.4094	1,6061	1.0131	1.6200	1.0208	1,0333	1,6397	1.0459	1.6520	1.6581	1.0040	1.009/	1,0/54	1.6810
96 t	3	24,9	334.9	344.9	354.9	364.9	374.9	384.9	394.9	404.9	414.9	424.9	434.9	444.9
V		4.60	4.68	4.75	4.83	4.91	4.98	5.05	5.12	5.20	5.27	5.34	5.41	5.48
ľ		1185.6		1196.7					1223.3					1248.7
I	1 0,470	1.6052	1.0122	1.6191	1.0238	1.0324	1.0388	1,0451	1.6512	1.05/2	1.0031	1.0089	1.0/43	1.6801
97 1	t 3	25.6	335,6	345.6	355.6	365.6	375.6	385.6	395.6	405.6	415.6	425.6	43 5.6	445.6
7		4.56	4.64	4.71	4.78	4.86	4.94	5.01	5.08	5.15	5.22	5.29	5.36	5.43
ì		1185.8 4 1.6044		1196.9							1233,8 1,6623			1249.0 1.6793
1	1 0.4/1	1,0077	1.0113	1.6184	1.0231	1,0310	1.0360	1,0443	1,0304	1,0504	1,0023	1,0001	1.0/3/	1.0793
98 1	t 3	26.4	336.4	346.4	356.4	366.4	376.4			406.4			436.4	
			4.59	4.66	4.74	4.81	4.89	4.96	5.03	5.10	5.17	5.24	5.31	5.38
1		1186.0 4 1.6036		1197.1		1208.0			1223.8		1234.1			1249.2 1.6786
	L U.T/2'	T 1,0030	1.010/	1,01/0	1.0244	1.0009	1.03/3	1,0133	1.0170	T,0330	1,0013	1,0073	A,U/JU	1,0700
99 1		27.1		347.1	357.1				397.1		417.1	427.1	437.1	
, 3			4.55	4.62	4.69	4,77	4.84	4.91	4.98	5.05	5.12	5.19	5.26	5.32
		3 1.6028				1208.2					1234.3			1249.5 1.6778
	u U,7/3.	J 1,0020	1,0099	4.0100	1,0430	1,0001	1,0303	1,0720	, ±,0703	1.0379	4,0000	1,0000	1,0144	4,0//0

t = temperature in F. degs. To Fahr. absolute = to + 459.6°. Internal energy = total heat in B.t.u.
h = total heat in B.t.u.
h = total heat in B.t.u.
A = 1/J = 1.286 × 10^-8 B.t.u. per ft. lb. [3.10 929].
Values for saturated steam are given in Tables 1 and 2.

											Deg	rees of S	uperheat	_
130°	140°	150°	160°	170°	180°	190°	200°	250°	300°	350°	400°	500°	600°	Press. lbs.
448.7	458.7	468.7	478.7	488.7	498.7	508.7	518.7	568.7	618.7	668,7	718.7	818.7	918.7	t 88
6.02	6.10	6.17	6.25	6.32	6.40	6.47	6.54	6.91	7.27	7.63	7.98	8.68	9.36	v 00
1251.6	1256.5		1266.4						1334.4			1430.5		h
1.6926	1.6980	1.7034	1.7087	1.7139	1.7190	1.7241	1.7291	1.7533	1.7761	1,7978	1.8185	1.8577	1.8941	n
449.5	459.5	469.5	479.5	489.5	499.5	509.5	510 5	560 5	619.5	669.5	710 5	819.5	919.5	t 89
5.96	6.03	6.11	6.18	6.25	6.33	6.40	6.48	6.84	7.19	7.54	7.89	8,58	9.26	v 09
	1256.8		1266.7				1286.4	1310.6	1334.7	1358.7		1430.8		h
1.6918	1.6972	1.7025	1.7078	1.7130	1.7181	1.7232	1.7282	1.7524	1.7752	1.7969	1.8176	1.8567	1.8931	n
45D 2	460.3	470.3	480.3	490.3	500.3	510.3	520.3	570.2	620.3	670.2	720.2	820.3	920.3	t 90
5.90	5.97	6.04	6.12	6.19	6.26	6.34	6.40	6.76	7.11	7.45	7.80	8,49	9.16	ν Σ
	1257.1		1266.9						1334.9				1479.4	'n
1.6909	1.6963	1.7016	1.7069	1.7121	1.7172	1.7223	1.7273	1.7515	1.7743	1.7960	1.8166	1.8558	1.8921	n
451.1	461.1	A71 1	481.1	401.1	501.1	£11 1	E01 1	571 1	601.1	671.1	701.1	001.1	001.1	4 01
5.83	5.91	5.98	6.05	6.13	6.20	6.27	6.34	6.69	621.1 7.04	7.38	7.72	\$21.1 8.40	921,1	t 91 v
	1257.3		1267.2						1335.2				1479.8	ň
	1.6954		1.7060						1.7734				1.8912	n
451.0	461.0	4771 0	401.0	401.0	501.0	711.0	501.0	F71 0	601.0	671.0	701.0	001.0	001.0	
451.8 5.78	461.8 5.85	471.8 5.92	481.8 5.99	6.06	501.8 6.13	511.8 6.20	521.8 6.28	6.62	621.8 6.96	7.30	721.8	821.8 8,32	921.8 8.98	t 92 v
	1257.6		1267.5						1335.5				1480.1	h
1.6891	1.6945		1.7051						1.7725				1.8902	n
450.5	450.5	480.5	400.6	400.6	500.6	#10 ¢	500.5	r=0.c	coo c	cho c	500 F	000.5	000 6	
452.6 5.72	462,6 5,79	472.6 5.86	482.6 5.93	492.6 6.00	502.6 6.07	512.6 6.14	522.6 6.21	572.6 6.56	622.6 6.90	672.6 7.23	722.6	822.6 8.23	922.6 8.89	t 93 v
	1257.9		1267.8						1335.8				1480.4	h
	1.6936					1.7196				1.7932			1.8892	n
	463.4	473.4	483.4		503.4				623.4			823.4		t 94
5.66	5.73 1258.2	5.80	5.87 1268.1	5.94	6.01	6.08	6.15	6.49	6.83	7.16 1360.2	7.50	8.15	8.80 1480.7	V h
	1.6928		1.7033						1.7706				1.8882	n
					•				_,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,					
	464.1		484.1		504.1	514.1			624.1				924.1	t 95
5.60	5.67	5.74	5.81	5.88	5.95	6.02	6.09	6.43	6.76	7.09	7.42	8.06	8.72	V
	1258.4 1.6920					1283.1 1.7179			1.7698	1360.5			1481.0 1.8873	h n
1.0000	1.0720	1.0713	1.7025	1.7077	1.7120	1.717	1.1227	1.7170	1.7050	1.,,,1	1.0101	1.0011	1.0075	**
	464,9	474.9	-		504.9	514.9	524.9		621.9			824.9	924.9	t 96
5.55	5.62	5.69	5.76	5.82	5.89	5.96	6.03	6.37	6.70	7.03	7.35	7.99	8.63	V L
	1258.7 1.6911		1.7016			1283.4			1336.7 1,7688				1481.3	h n
1,0037	1,0911	1.090+	1,7010	1.7008	1./119	1./1/0	1.7220	1.7701	1.7000	1.7903	1.0112	1.0502	1.0007	11
455.6	465.6	475.6	485.6						625.6			825.6		t 97
5.50	5.56	5,63	5.70	5.77	5.84	5.90	5.97	6.30	6.63	6.95	7.28	7.91	8.55	Ÿ
	1258.9 1.6903		1268.9			1.7162			1337.0 1,7680				1481.6 1.8855	h n
1.0049	1.0903	1.0930	1.7008	1.7000	1./111	1.7102	1.7212	1.7733	1.7000	1.7090	1.0103	1,0193	1.0033	11
	466.4		486.4						626.4				926.4	t 98
	5.51	5.58	5.65		5.78	5.85		6.24		6.89		7.84		∇
	1259.2		1269.1			1.7154	1 7204	1313,1	1337.2 1.7672	1 7888			1481.9 1,8846	h n
1,0041	1.6895	T.0340	1.7000	1,7003	1,/104	1.1137	1.1204	2., 773	2,,012	2.7000	2.0073	2,0703	±,0010	
457.1	467.1	477.1	487.1	497.1	507.1				627.1			827.1		t 99
5.39		5,52	5.59	5.66	5.72	5.79		6.18	6.50	6.82	7.14	7.76	8.39	V
	1259.4	1264.4	1269.4	1274.3	1279.3	1284.2				1361.6			1482,2	
1.0833	1.6887	1.6940	1.0993	1.7045	1,/096	1.7146	1./190	1./430	1.7004	1.7880	1,000/	1.04/0	1.8838	**

1 kg. per sq. cm. = 14.22 lbs. per sq. in. [log = 1.15 300]. 1 cn. meter = 35.31 cn. ft. [log = 1.54 795].

To change degs. C. to degs. F., multiply by \$, and add 32. To change mean kg. calories per kg. to mean B.t.u. per lb., multiply by \$. Entropy same in both systems.

Table 3 perheated Steam

	-	Degrees of Superh	eat								
Press. ibs.		10° 20°	30° 40°	50°	60°	7 0°	80°	90°	100°	110°	120°
100 t	327,8 0,02 4,43	337.8 347.8 4.51 4.58	357.8 367.8 4.65 4.72		387.8 4.86	397.8 4,93	407.8 5.00	417.8 5.07	427.8 5.14	437.8 5.21	447.8 5.27
'n	298.3 1186.3		1203.0 1208.4	1213.8				-	1239.7		
n	0.4743 1,6020		1.6228 1.6294	1.6358					1.6658		
101 t	328.6		358.6 368.6	378.6						438.6	
Ā	0.02 4.39	4.47 4.54	4,61 4,68		4.82	4.89	4.96	5.02	5.09 1239.9		5.22
h n	299,1 1186.5 0.4752 1.6012		1203.2 1208.6 1.6220 1.6286	1214.0 1 1,6350 1					1.6650		
	.,										
102 t	329.3	339.3 349.3		379.3						439.3	
Ā	0.02 4.35	4.42 4.49	4.56 4.64 1203.4 1208 8	4.71	4.78	4.84	4.91	4.98	5.04 1240.1	5.11	5.18
h	299.8 1186.7		1,6212 1.6278	1214,2 1 1.6343 1					1.6643		
n	0.4762 1.6004	1.0070 1.0145	1.0212 1.0278	1,0545	1.0400	1.0407	1.0520	1.0303	1.0043	1.0099	1.0755
103 t	330.0 €	340.0 350.0		380.0						440.0	
y	0.02 4.31	4.38 4.45	4.52 4.59		4.73	4.80	4.87	4.93	5,00	5.06	5.13
h	300.6 1186.9		1203.6 1209.1	1214.5						1245.5	
n	0.4771 1.5996	1.6068 1.6137	1.6204 1.6270	1.6334	1.6397	1.0458	1.0518	1.6577	1.0035	1.6691	1.6/4/
104 t	330.7	340.7 350.7	360.7 370.7	380.7	390.7	400.7	410.7	420.7	430.7	440.7	450.7
7	0.02 4.27	4.34 4.41	4.48 4.55	4.62	4.69	4.75	4.82	4.89	4.95	5.02	5.09
h	301.3 1187.0		1203.8 1209.2	12146					1240.6		
n	0.4780 1.5988	1.6060 1.6129	1.6197 1.6262	1.6326	1.6389	1.6450	1.6510	1.6569	1.6627	1.6683	1.6739
105 t	331,4	341.4 351.4	361,4 371,4	381.4	391.4	401.4	411.4	421.4	431.4	441.4	451.4
▼	0.02 4.23	4.30 4.37	4.44 4.51	4.58	4.65	4.71		4.84	4.91	4.97	5.04
h	302.0 1187.2	1192.9 1198.5	1204.0 1209.5	1214 9	1220.2	1225.4	1230.6	1235.7	1240.8	1245.9	1250.9
n	0.4789 1.5980	1.6052 1.6121	1.6189 1.6255	1,6319	1,6381	1.6442	1.6502	1.6561	1.6619	1.6676	1.6732
106 t	332.0	342.0 352.0	362.0 372.0	382 0	392.0	402.0	412.0	422.0	432.0	442,0	452.0
V	0.02 4.19	4.26 4.33	4.40 4.47	4.54	4.60	4 67	4.74	4.80	4.86	4.93	4,99
h	302.7 1187.4		1204.2 1209.7	1215.1							1251.2
n	0.4798 1.5972	1.6044 1.6113	1.6181 1.6247	1.6311	1,6374	1.6435	1.6495	1.6554	1.6612	1.6668	1.6724
107 t	332.7	342,7 352,7	362,7 372,7	382 7	392.7	402.7	412.7	422.7	432.7	442.7	452.7
	0.02 4.16	4,23 4.29	4,36 4,43	4 50	4 57	4.63	4.70	4.76	4.82	4.89	4.95
h	303.4 1187.5	1193.2 1198.8	1204 3 1209.8	1215,2							1251.4
n	0.4807 1.5965	1.6037 1.6107	1,6175 1,6240	1.6304	1.6367	1.6428	1.6488	1.6547	1.6605	1.6661	1.6717
108 t	333.4	343.4 353.4	363.4 373.4	383.4	393,4	403,4	413.4	423.4	433.4	443.4	453.4
	0.02 4.12	4.19 4.25	4.32 4.39	4.46	4.53	4.59	4.66	4.72	4,78	4.85	4.91
h	304.1 1187.7		1204.6 1210 1			1226.1					1251.6
n	0.4816 1.5957	1,6029 1,6099	1,6167 1,6233	1,6297	1.6359	1.6420	1,6480	1.6539	1,6597	1.6654	1.6709
109 t	334.1	344.1 354.1	364.1 374.1	384.1	394,1	404.1	414.1	424.1	434,1	444.1	454.1
	0.02 4.08	4.15 4.22	4.29 4.35	4.42	4.49	4.55	4.62	4.68	4.74	4.80	4.87
h	304.8 1187.9		2 1204.8 1210 3			1226.3					1251.9
n	0.4825 1.5950	1,6022 1,6092	2 1.6160 1.6226	1.6290	1.6353	1.6414	1.6474	1,6533	1.6591	1.6647	1.6703
110 t	334,8	344.8 354.8	364.8 374.8			404,8			434,8	444.8	454.8
7	0,02 4.05	4,12 4,18	4.25 4.32	4.38		4.51			4.70		
h		1193.8 1199.4				1226,5					1252,1
n	0.4834 1.5942	1.6014 1.6084	1.6152 1.6218	1,6282	1.6345	1,6406	1,6466	1.6525	1.6583	1,6640	1,6695
111 t	335,4	345,4 355.4	365.4 375.4	385.4	395.4	405.4	415.4	425.4	435.4	445,4	455.4
▼	0.02 4.01	4.08 4.14	4.21 4.28	4.35	4.41	4.47	4.54	4.60		4.72	
h	306.2 1188.2	1194.0 1199	5 1205.2 1210.7								1252,3
n	0.4843 1.5935	1,6007 1,607	7 1.6145 1.6212	1.6276	1.6339	1.6400	1.6459	1.6518	1.6576	1,6633	1.6688
112 t	336,1	346,1 356.1	366.1 376.1	386.1	396.1	406.1	416.1	426.1	436.1	446.1	456.1
▼	0.02 3.98	4.05 4.11	4.18 4.24	4.31	4.37	4.43	4.50	4.56	4,62	4,68	4.75
h		1194,1 1199,	8 1205.4 1210.9	1216.3	1221.7	1227.0	1232.2	1237.4	1242.5	1247.6	1252.6
n	0.4852 1.5928	1.6000 1.607	0 1.6138 1.6205		1.6332	1.6393	1,6453	1.6512	1.6570	1,6620	1,6682
				(29)							

(38)

		4										rees of S	uperheat	Press.
130°	140°	150°	160°	170°	180°	190°	200°	250°	300°	350°	400°	500°	600°	lbs.
457.8	467.8 5.41	477.8 5.47	487.8 5.54	497.8 5.61	507.8 5.67	517.8 5.74	527.8 5.80	577.8 6.12	627.8 6.44	677.8 6.75	727.8	827.8	927.8	t 100
5.34 1254.7		1264.7							1337.8		7.07 1385.9	7.69 1434.1	8.31 1482,5	v h
1.6826	1.6880	1.6933	1.6985	1.7037	1.7088	1.7138	1.7188	1.7428	1.7656	1.7872	1.8079	1.8468	1.8829	n
458.6	468.6		488.6	498.6		518.6		578.6		678.6		828.6	928.6	t 101
3.29	5.36	5,42 1264.9	5,49	5.56	5.62	5.68	5.75	6.07	6.38 1338.1	6.69	7.01	7.62 1434.4	8.24	V.
1255.0 1.6818			1.6977						1.7647				1.8820	h n
459,3	469.3	479.3	489.3	499.3	509.3	519.3	529.3	579.3	629.3	679.3	729.3	829.3	929,3	t 102
5.24	5.31	5.37	5.44	5.50	5.57	5.63	5.70	6.02	6.33	6.63	6.94	7.55	8.16	v
1255.2	1260.2 1.6864		1270.2 1.6969						1338.3 1.7639			1434.7 1.8451		h n
												_		
460.0 5.19	470.0 5.26	480.0 5.32	490.0 5.39	500.0 5.45	510.0 5.52	520.0 5.58	530.0 5.64	580.0 5.96	630.0 6.27	680.0 6.57	730.0 6.88	830.0 7.48	930.0 8.08	t 103
	1260.4	1265.4	1270.4	1275.3	1280.3	1285.2	1290.1	1314.4	1338,6	1362,7			1483.4	h
1.6802	1.6856	1. 6 909	1.6961	1.7013	1.7064	1.7114	1.7164	1.7404	1.7631	1.7847	1:8054	1.8442	1.8803	n
460.7		480.7		500.7		520.7	530.7		630.7			830.7		t 104
5.15	5.21 1260.7	5.28 1265 6	5,34 1270,6	5.40 1275.6	5,47 1280 5	5,53 1285 5	5.59 1200 4	5.90 1314 6	6.21 1338.8	6.51	6.82	7.41 1435.2	8.01 1483 6	v h
	1.6848		1.6954						1.7623			1.8434		n
461.4	471.4	481.4	491.4	501.4	511.4	521.4	531.4	581.4	631,4	681.4	731.4	831.4	931.4	t 105
5.10	5.17	5.23	5.29	5.36	5.42	5.48	5.54	5.85	6.15	6.45	6.76	7.35	7.94	V
	1260.9 1.6841		1270.9 1.6946						1339.1 1.7614			1435.5 1.8426		h n
462.0 5.06	472.0 5.12	482.0 5.18	492.0 5.25	502.0 5.31	512.0 5.37	522.0 5.43	532.0 5.49	582.0 5.80	632.0 6.10	682.0 6.40	732.0 6.70	832.0 7.29	932.0 7.87	t 106
	1261.2		1271.1						1339.4			1435.8		h
1.6779	1.6833	1.6886	1.6938	1.6990	1.7041	1.7091	1.7140	1.7380	1.7606	1.7822	1.8029	1.8417	1.8777	n
462.7	472.7		492.7				532.7		632.7			832.7		t 107
5.02 1256.4	5.08 1261.4	5.14 1266.4	5.21 1271 4	5.27 1276 3	5.33	5.39 1286 2	5.45 1201 1	5.75 1315 4	6.05 1339.6	6.34 1363 7	6.6 4	7.22 1436.0	7.80 1484 4	v h
	1.6826	1.6879	1.6931	1.6983	1.7034	1.7084			1.7599			1.8410		n
463.4	473.4	483.4	493.4	503.4	513,4	523.4	533.4	583.4	633.4	683.4	733.4	833.4	933.4	t 108
4.98	5.04	5.10	5.16	5.22	5.28	5.34	5.40	5.70	6 00	6.29	6.58	7.16	7.73	V
	1261,6 1,6818		1271.6 1.6923						1339.9 1.7591			1436,3 1.8401		h n
	474.1			504.1					634.1			834.1		t 109
	4.99	5.05	5.12	5.18	5.24	5.29	5.35	5.65	5.95	6.24	6.53	7.10	7.66	¥ 103
	1261.9		1271.8						1340.1			1436.6		h
1.6758	1.6812		1.6916				1./118	1.7358	1.7584	1.7799	1.8006	1,8393	1.8753	n
	474.8 4.95		494.8 5.07	504.8 5.13	514.8 5.19	524.8 5.25			634.8 5.90		734,8 6.47	834.8 7.03	934.8 7.59	t 110
4.89 1257.1	1262,1	5,01 1267.1	1272,1						1340.4			1436.8		h
	1.6804	1.6857	1.6909	1.6960	1.7011	1.7061	1.7110	1.7350	1.7576	1.7791	1.7997	1.8384	1.8744	n
	475.4		495.4						635.4			835.4		t 111
4.85 1257 3	4.91 1262.3	4.97 1267 3	5.03 1272.3	5.09 1277 3	5.15 1282 2	5,20 1287 2	5.26 1292 1	5.56 1316 4	5,85 1340.6	6,14 1364,8	6,42 1388 9	6.97 1437 1	7.53 1485.5	v h
	1.6797		1.6902							1.7783			1.8736	n
466.1	476.1	486.1	496.1	506.1	516.1	526.1	536.1	586.1	636,1	686.1	736.1	836.1	936.1	t 112
4.81	4.87	4.93	4.99	5.05	5.10	5.16	5.22	5.51	5.80	6.08	6.36	6.92	7.46	V
	1262.6 1.6790					1287.4 1.7047				1365.0 1.7776				
				•			(39)	·		-				•

Table 3: Superheated Steam

_	_	Degrees of Super	heat								
Press. ibs.	Sat. Water Steam	10° 20°	30° 40°	50°	60°	70°	80°	90°	100°	110°	120°
113 t	336.8	346.8 356.8		386.8	396.8	406.8	416.8	426.8	436.8	446.8	456.8
v h	0.02 3.95 307.6 1188.5	4.01 4.07	4.14 4.21 1205.6 1211.1	4.27	4.34	4.40 1227.2	4.46	4.52	4.58	4.64 1247.7	4.71
n	0.4860 1.5921		1.6131 1.6198			1.6387				1.6619	
444 1		245 4 255 4	2004 2004						4277.4	4457.4	4577.4
114 t	337.4 0.02 3.91	347.4 357.4 3.98 4.04	367.4 377.4 4.11 4.17	387.4 4.24	397.4 4.30	407.4 4.36	4.42	427.4 4.49	437.4 4.55	447.4 4.61	457,4
ň	308.3 1188.7		1205.7 1211.2			1227.4				1248.0	
n	0.4869 1.5914	1.5986 1.6057	1.6125 1.6191			1.6380				1.6613	
115 t	338.1	348.1 358.1	368.1 378.1	388 1	398.1	408 1	418.1	428 1	438.1	448.1	458 1
T	0.02 3.88	3.95 4.01	4.08 4.14	4.20	4.27	4.33	4.39	4.45	4.51	4.57	4.63
h	309.0 1188.8		1205.9 1211.4			1227.6				1248.2	
n	0.4877 1.5907	1.5979 1.6050	1.6118 1.6185	1.6249	1.6312	1.6373	1.6433	1.6492	1.6549	1.6606	1.6661
116 t	338.7	348.7 358.7	368.7 378.7	388.7	398.7	408.7	418.7	428.7	438.7	448.7	458.7
7	0.02 3.85	3.92 3.98	4.04 4.10	4.17	4.23	4.29	4.35	4.41	4.47	4.53	4.59
h	309.6 1189.0		1206.1 1211.6			1227.8				1248.4	
n	0.4886 1.5900	1.5972 1.0043	1.6111 1.6178	1.0242	1.0303	1.6366	1.0420	1.0465	1.0343	1.0399	1.6654
117 t	339.4		369.4 379.4			409.4				449.4	
V	0.02 3.82	3.88 3.94	4.01 4.07	4.14	4.20	4.26	4.32	4.38	4.44	4.50	4.56
h n	310,3 1189,1 0,4894 1,5893		1206.3 1211.8 1,6104 1,6171			1228.0 1.6360				1.6592	1253.6
											• • • •
118 t	340.0		370.0 380.0				420.0			450.0	
v h	0.02 3.79 311.0 1189.3	3.85 3.91	3.98 4.04 1206,4 1212,0	4.10	4.16	4.22 1228,2	4.28	4.34	4.40 1243 7	4.46	4.52 1253.8
'n	0.4903 1.5887		1.6097 1.6164			1.6353					1.6641
440 .	240.6	240 5 250 5	ar a	200.6	400.5	470.5	400 6	400.6	440.5	440.0	450.5
119 t	340.6 0.02 3.76	350.6 360.6 3.82 3.88	370.6 380.6 3.95 4.01	390.6 4.07	400.6	410.6 4.19	420.6 4.25	430.6 4.31	440.6 4.37	450.6 4.42	460.6 4.48
'n	311.6 1189.4		1206.7 1212.2			1228.4					1254.0
n	0.4911 1.5880	1.5953 1.6023	1.6092 1.6159	1.6223	1.6286	1.6347	1.6407	1.6466	1.6523	1.6580	1.6635
120 t	341.3	351.3 361.3	371.3 381.3	391.3	401.3	411.3	421 3	431.3	441.3	451 3	461.3
TZO U	0.02 3.73	3,79 3,85	3,92 3,98	4,04	4.10	4.16	4,22	4.28	4.33	4.39	4.45
h	312.3 1189.6		1206.8 1212.4					1238.9			1254.2
n	0.4919 1.5873	1.5946 1.6016	5 1.6085 1.6152	1.6216	1.6279	1,6340	1,6400	1.6459	1.6517	1.6573	1.6628
121 t	341.9	351.9 361.9	371.9 381.9	391.9	401.9	411.9	421.9	431.9	441.9	451.9	461.9
V	0.02 3.70	3.76 3.82	3.88 3.94	4.00	4.06	4.12	4.18	4.24	4.30	4.36	4,41
h n	313.0 1189.7 0.4927 1.5866		1207.0 1212.5 1.6078 1.6145					1239,1 1.6452			1254.4 1.6621
11	0.4927 1.3600	1,3939 1,0010	1,0076 1,0145	1,0209	1.0272	1.0554	1,0595	1,0432	1.0510	1.0300	1.0021
122 t	342.5	352.5 362.5		392.5	402.5		422.5	432.5	442.5		462.5
v h	0.02 3.67 313.6 1189.8	3.73 3.79	3.85 3.91 5 1207.2 1212.7	3.97	4.03	4.09 1228 0	4.15	4.21 1239.3	4.27		4.38 1254.6
n	0.4935 1.5859		3 1.6071 1.6138					1.6446			1.6614
123 t	343,2	353.2 363.2	373.2 383.2	393.2	403.2	413.2	423.2	433.2	443.2	453.2	463.2
123 t	0.02 3.64	3.70 3.76	3.82 3.88	3,94		4.06	4,12	4.18	4.23	4.29	4.35
'n	314.3 1190.0	1195.9 1201.	7 1207.4 1212.9	1218.4	1223.8	1229.1	1234.3	1239.5	1244.7	1249.8	1254.8
n	0,4943 1,5853	1,5926 1,599	7 1.6066 1.6133	1.6197	1.6260	1.6321	1.6381	1.6440	1.6497	1.6554	1.6609
124 t	343.8	353.8 363.8	373.8 383.8	393.8	403.8	413.8	423,8	433,8	443.8	453.8	463.8
V	0.02 3.61	3.67 3.73	3.79 3.85	3.91	3.97	4.03	4.09	4.14	4.20	4.26	4.31
h			8 1207.5 1213.1					1239.7			1255.0
n	0.4951 1.5846	1.5919 1.599	0 1.6059 1.6126	1,6190	1,6253	1.0315	1,6374	1.6433	1.0491	1.0547	1.6602

t = temperature in F. degs. To Fahr, absolute = to + 459.60. Internal energy y=sp. vol. in ou. ft. per lb. J = 777.5 ft. lbs. per B. t. u. [log = 2.89 071]. J = 777.5 ft. lbs. per B. t. u. [log = 2.89 071]. $J = 1.286 \times 10^{-3}$ B. t. u. per ft. lb. [3.10 929]. Values for saturated steam $J = 1.286 \times 10^{-3}$ B. t. u. per ft. lb. [3.10 929]. Values for saturated steam are entropy.

											De	grees of	Superheat	_
130°	140°	150°	160°	17 9°	180°	190°	200°	250°	300°	350°	400°	500°	600°	Press. lbs.
466.8	476.8	486.8	496.8	506.8	516.8	526.8	536.8	586.8	636.8	686.8	736.8	836.8	936.8	t 113
4.77	4.82	4.88	4.94	5.00	5.06	5.12	5.18	5.48	5.76	6.04	6.31	6.86	7.40	V
1257.8				1277.7				1316.9					1486.0	h
1.6730	1.6783	1.6836	1.6888	1.6939	1,6990	1,7040	1.7089	1.7329	1.7554	1.7769	1,7975	1.8362	1.8721	n
467.4	477.4	487.4	497,4	507.4	517,4	527.4	537.4	587.4	637.4	687.4	737.4	837,4	937.4	t 114
4.73	4.78	4.84	4.90	4.96	5.02	5.07	5.13	5.42	5.70	5.98	6.25	6.80	7.34	v
1258.0				1278.0				1317.1					1486.3	h
1.6723	1.6777	1.6829	1.6881	1.6932	1.6983	1.7033	1.7082	1.7322	1.7547	1.7761	1.7967	1.8354	1.8713	n
468.1	478.1	488.1	498.1	508.1	518.1	528.1	538.1	588.1	638 1	688 1	738.1	838.1	938 1	t 115
4.69	4.75	4.81	4.87	4.92	4.98	5.03	5.09	5.38	5.66	5.93	6.20	6.75	7.28	V
1258.2				1278.2				1317.3					1486.5	h
1.6716	1.6770	1.6822	1.6874	1.6925	1.6976	1.7026	1.7075	1.7314	1.7540	1.7754	1.7960	1.8347	1.8706	n
468.7	478 7	488.7	498 7	508.7	518.7	528 7	538.7	588 7	638.7	688 7	738 7	838.7	938 7	t 116
4.65	4.71	4.77	4.83	4.88	4.94	4.99	5.05	5.33	5.61	5.88	6.15		7.22	V
1258.4				1278.4				1317.6					1486.8	h
1.6709	1.6763	1.6815	1.6867	1.6918	1.6969	1.7019	1.7068	1.7307	1.7533	1.7747	1.7953	1.8340	1.8698	n
469.4	479 4	489 4	400 4	509.4	5194	529.4	539 4	589.4	639.4	689.4	739 4	839.4	939.4	t 117
4.61	4.67	4.73	4.79	4.84	4.90	4.95	5.01	5.29	5.56	5.83	6.10	6.63	7.16	V
1258.6				1278.6				1317.8				1438.6		h
1.6702	1.6756	1,6809	1.6861	1.6912	1.6962	1.7012	1.7061	1.7300	1.7526	1.7740	1.7945	1.8332	1.8691	n
470.0	480 O	490.0	500 O	510.0	520.0	530.0	540.0	590.0	640 O	690.0	740.0	840.0	940 0	t 118
4.57	4.63	4.69	4.75	4.80	4.86	4.91	4.97	5.25	5.52	5.79	6.06	6.58	7.11	v
1258.9				1278.8			1293.7					1438.9		h
1.6696	1,6749	1.6802	1,6854	1,6905	1,6955	1.7005	1.7054	1,7293	1.7518	1.7732	1.7938	1.8325	1.8683	n
470.6	480 6	490 6	500.6	510 6	520.6	530 6	540.6	590.6	640.6	690.6	740.6	840.6	940.6	t 119
4.54	4.60	4.66	4.71	4.77	4.82	4.87	4.93	5.21	5.48	5.74	6.01	6.53	7.05	V
1259.1				1279.0				1318.2				1439.1		h
1.6690	1.6743	1,6796	1.6848	1,6899	1.6949	1.6999	1.7048	1.7287	1,7512	1.7726	1.7932	1.8318	1.8677	n
471.3	481.3	491.3	501.3	511.3	521.3	531.3	541.3	591.3	641.3	691.3	741.3	841.3	941.3	t 120
4.50	4.56	4.62	4.68	4.73	4.78	4.83	4.89	5.17	5.44	5.70	5.96	6.48	6.99	7
1259.3				1279.2			1294.1				1391-0			h
1.6683	1.6736	1.6789	1.6841	1.6893	1.6943	1.6992	1.7041	1.7280	1.7505	1.7719	1.7924	1.8311	1.8009	n
471.9	481.9	491,9	501.9	511.9	521,9	531.9	541.9	591.9	641.9	69)	741.9	841.9	941.9	t 121
4.47	4.53	4.58	4.64	4.69	4.75	4.80	4.86	5.13	5.40	5.66	5.92	6.43	6.94	V
1259.5				1279.4				1318,7			1391.3			h
1.6676	1,6730	1,6782	1.0834	1.6886	1.6936	1.6985	1.7034	1,72/3	1.7498	1.7712	1.7917	1,8303	1.8002	n
472.5	482.5	492.5	502.5	512.5	522.5	532.5	542.5	592.5	642.5	692.5	742.5	842.5	942.5	t 122
4.43	4.49	4.55	4.60	4.66	4.71	4.76	4.82	5.09	5.35	5.61	5.87	6.38	6.88	V
1259.7				1279.6			1294.6				1391.5		1488.3 1.8655	h
1,6669	1,0/23	1,0//5	1,0827	1,6879	1,6929	1,6978	1.7027	1,7200	1.7491	1.7703	1.7910	1.0290	1.6033	11
473.2		493.2		513.2		533.2		593.2				843.2		t 123
4.40	4.46	4.51	4.57	4.62	4.67	4.72	4.78	5.05	5.31	5.57	5.83	6.33	6.83	7
1259,9 1,6663				12 7 9.9 1.6 8 73			1294.8 1.7021	1319,1 1 7250	1545,4 1 7484	1.50/,0 1.7608	1391.8 1.7903			h n
1,000	1,0/1/	1.0709	1,0041	1.00/3	1,0943	1.07/4	1.7021	1.14JJ	4.1 TOT	2,7030	1,1903	A,U4U9	2.0010	
473.8				513.8				593.8				843.8		t 124
4.36	4.42	4.48	4.53	4.58	4.64	4.69			5.27	5.53	5.78	6.28	6.78	Ā
1260.1 1 1.6657		1270.1		1.6865			1295.0 1,7015						1488.7 1.8640	h n
1,000/	1,0/10	1.0702	1.0014	T.0003	1.0310	1,0500	1,7013	-,1454	4.1 ₹11	~.14.74	4,1090	0404	2,0010	

Table 3: Superheated Steam

		o.,oupern	Degrees	at Camanh	1									
Press.		Sat				400	=00		700		000	1000	4400	4000
be.		Water Steam	10°	20°	30°	40°	50°	60°	70°	8 0°	90°	100°	110°	120°
125	ŧ	344.4	354.4	364.4	374.4	384.4	394.4	404.4	414.4	424.4	434.4	444.4	454.4	464.4
	٧	0.02 3.58		3.70	3.76	3.82	3.88	3.94	4.00	4.06	4.11	4.17	4.22	4.28
	h	315.5 1190.3		1202.0			1218.8					1245.1		
	n	0.4959 1,5839	1,5913	1.5983	1,6052	1.6119	1.6183	1.6246	1.6307	1.6367	1.6426	1.6484	1.6540	1,6595
400		245.0	2550	265.0	275 0	20° 0	205.0	40° 0	4150	40° 0	4250	44° 0	455.0	465.0
126	7	345.0 0.02 3.56		365.0 3.68	3.74	3.80	3.86	3.91	415.0 3.97		4.08			4.25
	'n	316.2 1190.4		1202,1					1229.7				1250.4	
		0,4967 1.5832		1.5976					1.6301				1,6533	
	**	0.1501 2.5002	2.0300	2.55.0	2.0015					_,,,,,,	-,00	_,,,,,,	_,,,,,,	_,,,,,,,
127	t	345.6	355.6	365.6	375.6	385.6	395.6	405.6	415.6			445.6	455.6	465.6
	V	0.02 3.53	3.59	3.65	3.71	3.77	3,83	3.88	3.94		4.05	4.11		4.22
	h	316.8 1190.5		1202.3					1229.9				1250.6	
	n	0.4974 1.5825	1.5899	1.5970	1,6038	1,6105	1.6170	1.6233	1.6295	1.6355	1.6413	1.6470	1.6526	1.6581
128		346.2 *	256.2	366.2	376.2	286.2	306.2	406.2	416.2	426.2	436.2	446.2	456.2	466.2
120	7	0.02 3.50			3,68	3.74		3,86	3.91		4.02			4.19
	'n	317.4 1190.7		1202.5					1230 1				1250.8	
		0.4982 1.5819		1.5964					1,6289			-	1.6520	
		-,												
129	t	346,8		366.8					416.8			446.8	456.8	
	V	0.02 3.48			3.65	3.71	3.77		3.88		3.99	4.05	4.10	
	h	318 0 1190.9		1202.6					1230 3				1251.0	
	n	0.4990 1.5813	1.5887	1.5958	1.6027	1.6094	1,6158	1.6221	1.6283	1.6343	1.6402	1.6459	1.6515	1,6570
130	ŧ	347.4	357 A	367,4	377 A	387 4	307 A	407.4	417.4	427 4	437 4	447 4	457.4	467 4
200	V	0 02 3,45	3.51		3,63	3.69	3.74		3.85	3.91	3.96	4.02		4.13
	h	318.6 1191.0		1202.8					1230.4				1251.2	
	n	0.4998 1.5807	1.5881	1.5952	1.6021	1,6088	1.6153	1.6216	1 6277	1.6337	1.6396	1.6453	1.6509	1.6564
404		140.0	250.0	200.0	250.0	200.0	200 #	400.0	410.0	400.0	120.0	440.0	450.0	460.0
131	-	348.0 0.02 3.43	358.0 3.49	368.0 3.54			398. 0 3.72	408.0 3.77	418 0 3.83	428.0 3.88	438.0 3,94	448.0 3.99	458.0 4.05	468.0 4.10
	V h	0.02 3.43 319.3 1191.1		1203,0	3,60 1208 7	3.66			1230 6				1251.4	
	'n	0.5005 1.5801		1.5946					1.6271				1,6503	
	_	-,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	-,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	_,,,,	_,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,		-10-17						-,0000	_,,,,,,
132	t	348.5	358,5	368.5	378.5	388.5	398.5		418 5			448 5	458.5	468.5
	Ā	0.02 3.40	3.46		3.58	3 63	3.69		3 80	3.85		3.96	4.02	T
	h	319.9 1191.2							1230.8				1251.6	
	n	0.5013 1.5795	1,5009	1,5940	1,0009	1.6077	1.0141	1.0204	1.6265	1.0323	1.0384	1.0441	1.6498	1.0353
133	t	349.1	359.1	369.1	379.1	389.1	399.1	409.1	419.1	429.1	439.1	449.1	459.1	469.1
	v	0.02 3.38	3.44		3.55	3.61	3.66	3.72	3.77	3.83		3.94	3.99	
	h	320.5 1191.3	1197.4	1203.3	1209.0	1214.6			1231.0			1246.7	1251.8	1256.8
	n	0.5020 1.5789	1.5863	1.5935	1,6004	1.6071	1.6136	1.6199	1.6260	1.6320	1.6379	1.6436	1,6492	1.6547
404		240.7	250.7	200 7	270 7	200 7	200 7	400.7	410 7	400 7	420 7	440.7	450.7	460.77
134	¥ 6	349.7 0.02 3.35	3.41	3,47	3.53	389.7 3.58	399.7 3.64	3.69	419.7 3.74	3.80	3.85	3.91	459.7	4.01
	'n	321,1 1191,5				1214.9			1231.2					1257.0
	'n	0,5028 1,5783				1.6065			1.6254					1.6541
136		350.3	360,3	370.3	380.3	390.3	400.3	410.3	420.3	430.3	440.3	450.3	460.3	470.3
	Ā			3.44			3.61	3.67	3.72	3.77	3.83		3.93	
	h	321.7 1191.6 0,5035 1,5777				1215.0						1247.0		
	n	0,3033 1,3777	1.3632	1.3943	1.3532	1,6059	1.0124	1.010/	1.0246	1.0308	1.6367	1.6424	T.0490	1.0333
136	i t	350.8	360.8	370.8	380.8	390.8	400.8	410.8	420.8	430.8	440.8	450.8	460.8	470.8
		0.02 3.31		3.42		3,53	3,59	3.64	3.70	3.75	3.80	3,85	3,90	3.96
	h	322.3 1191.7	1197.8			1215.1	1220.7	1226.2	1231.5	1236.8	1242.0			1257.4
	n	0.5043 1.5771	1.5846	5 1.5917	1,5986	1.6053	1.6118	1.6181	1.6243	1.6303	1.6361	1.6418	1.6474	1,6529
13.00	7 4	361 4	261 4	271 4	201 4	201 4	401.4	A11 A	421,4	A21 A	AA7 A	AET A	461.4	A771 A
110	7 t V	351.4 0.02 3.29		371,4 3,40					3.67				3.88	
	h	322,8 1191,8					1220.9					1247.4		
	ñ	0.5050 1.5765				1,6047					1,6355			1.6524
							(42)			(,				

t (42)

									Deg	rees of Sc	perheat	, 1 *
130° 140°	150° 16	0° 170°	180°	190°	200°	250°	300°	350°	400°	500°	600°	Press.
474.4 484.4	494.4 504	1.4 514.4	524.4	534.4	544.4	594.4	644.4	694.4	744.4	844.4	944,4	t 125
4,33 4.39 1260,4 1265,4	4.45 4.5 1270.4 127		4.60	4.65	4.71	4.97	5,23	5.49	5.74	6.24	6.73	▼
1.6650 1.6703	1.6755 1.68						1343.8 1.7470	1.7684		1440.6 1.8275		h n
457.0 407.0	405 0 50		TOT O	7070								
475.0 485.0 4.30 4.36	495.0 505 4,41 4,4		525.0 4.57	535.0 4.62	545.0 4.68	595.0 4.94	645.0 5.20	695.0 5.45	745.0 5.70	845.0 6.19	945.0 6.68	t 126
1260.6 1265.6	1270.6 127						1344.0			1440.8		h
1.6643 1.6696	1,6748 1.68	300 1.6851	1.6902	1.6952	1.7000	1.7238	1.7463	1.7677	1.7881	1.8267	1.8625	n
475.6 485.6	495,6 50	5.6 515.6	525.6	535.6	545.6	595.6	645.6	695.6	745.6	845.6	945.6	t 127
4.27 4.32	4.38 4.4		4.54	4.59	4.64	4.90	5.16	5.41	5.66	6.15	6.63	7
1260.8 1265.8 1,6636 1,6690	1270.8 127 1,6742 1,6						1344.2 1,7456		1392.6 1,7874		1489.4	h, n
2.0000 2.0050	1.07 12 1.0	77 2,0013	1.0055	1.0513	1,0555	1.7201	1.7 130	1.7070	2,7071	9	1,010	**
476.2 486.2 4.24 4.29	496.2 500			536.2			646.2			846.2		t 128
4.24 4.29 1261.0 1266.0	4.35 4.4 1271,0 127		4.50 1285.9	4.55 1290.9	4.61 1295.8	4.86 1320.1	5.12 1344,4	5.37 1368.6	5.62 1392.8	6.10 1441.2	6,58 1489.7	y h
1.6630 1.6684	1,6736 1,6						1.7450			1.8253		n
476.8 486.8	496,8 50	6.8 516.8	526.8	536,8	546.8	596 R	646,8	696 S	746 2	846.8	946 2	t 129
4.21 4.26	4.32 4.3		4.47	4.52	4.57	4.83	5.08	5.33	5.57	6.05	6.53	V 125
1261.2 1266.2	1271.2 127				1296.0					1441.4		h
1,6624 1.6677	1,6730 1.6	/82 1,6833	1.6883	1,6933	1.6982	1.7219	1.7444	1.7657	1.7861	1.8247	1.8605	n
477.4 487.4		7.4 517.4					647.4			847.4		t 130
4.18 4.23 1261.4 1266.4	4.28 4. 1271,4 127	34 4.39	4,44	4.49	4.54	4.80	5.05 1344,9	5,29	5,53	6.01 1441.7	6.49	v h
1.6619 1.6672	1.6724 1.6							1.7651		1.8241		n
1500 1000				#					740.0	040.0	040.0	
478.0 488.0 4.15 4.20	498.0 50 4.25 4.	8.0 518.0 31 4.36	528.0 4.41	538.0 4.46	548.0 4.51	598.0 4.76	648.0 5.01	698.0 5.25	748.0 5.49	848.0 5.97	948.0 6.44	t 131
1261.6 1266.6	1271.6 127						1345.1			1441,9		h
1.6613 1.6666	1.6718 1.6	770 1.6821	1.6871	1.6921	1.6970	1.7207	1.7431	1.7645	1.7849	1.8234	1.8591	n
478.5 488.5	498.5 50	8.5 518.5	528.5	538.5	548.5	598.5	648.5	698.5	748.5	848.5	948.5	t 132
4.12 4.17	4,22 4.		4.38	4.43	4.48	4.73	4.98	5.22	5.45		6.40	V
1261.8 1266.8 1.6607 1.6660	1271.8 127 1,6712 1,6						1345.3	1.7639		1442.1 1.8228		h n
479.1 489.1 4.09 4.14		9.1 519.1 25 4.30	529.1 4.35	539.1 4.40	549.1 4.45	599.1 4.70	649.1 4.94	699,1 5,18	749.1 5.42	849.1 5.89	949.1 6.36	t 133 v
1261.9 1266.9	1271.9 127			-			1345.5			1442.3		h
1.6601 1.6654	1.6706 1.6				1.6958	1.7195	1.7419	1.7632	1.7836	1.8221	1.8578	n
479.7 489.7	499.7 50	9.7 519.7	529.7	539.7	549.7	599.7	649.7	699.7	749.7	849.7	949.7	t 134
4.06 4.11		22 4.27	4.32	4.37	4.42	4.66	4.90	5.14	5.38	5.84	6.31	V
1262.1 1267.1	1272.1 127							1369.9 1.7626		1442.5 1.8215		h n
1.6595 1.6649	1.0701 1.0	752 1.6803	1.0055	1.0903					1.7000	1.0213	1.0312	
480.3 490.3		0.3 520.3					650.3			850.3		t 135
4,03 4.08 1262,3 1267,3	4,14 4. 1272,3 127	19 4.24 73 1282 3	4.29	4.33	4.38	4,63 1321 6	4.87 1345 9	5.11 1370.2	5.34 1394 4	5.80 1442.8	6.27	v h
1.6589 1.6643	1,6695 1.6							1.7620		1.8209		n
480.8 490,8	500.8 51	0.8 520.8	530 B	540 R	550 8	600.8	650.8	700 8	750.8	850.8	950 R	t 136
4,01 4.06		16 4,21	4.26	4.30	4.35	4.60	4.84	5.08	5.31	5.76	6.22	V
1262.5 1267.5		7.5 1282.5						1370.4 1.7614		1443.0	1491.5 1.8559	h
1.6584 1.6637	1.0089 1,6	741 1,6792	1.0842	1.0891	1,0940	1./1//	1./401					n
481.4 491.4		1.4 521.4							751.4			t 137
3.98 4.03 1262.7 1267.7	4.08 4. 1272,7 127	13 4.18 77 1282 7	4.23 1287 7	4,27 1292.7	4.32 1297.6		4.81 1346.3	5,04 1370.6	5.27 1394.8		6.18 1491.8	v h
1.6578 1.6631	1.6683 1.6							1,7608	1.7811		1.8552	
					(43)				• '.			

Table 3: Superheated Steam

Labic	5. Duperne										
Press.	Sat.	Degrees of Superheat	400	FOO	000	700	000	000	1000	4400	4000
lbs.	Water Steam	10° 20° 30°	40°	50°	60°	70°	80°	90°	100°	110°	120°
138 t	352.0	362,0 372.0 382.0	392.0	402,0	412.0	422,0	432.0	442.0	452.0	462.0	472.0
▼ ▼	0.02 3.26	3,32 3,37 3,43	3.48	3.54	3,59	3.64	3.70	3.75	3.80	3.85	3.90
h	323.4 1192.0	1198.1 1204.0 1209.8	1215.5	1221.1	1226.5		1237.2		1247.6	1252.7	1257.8
n	0.5057 1.5759	1.5834 1.5906 1.5975	1.6042	1.6107	1.6170	1.6232	1.6292	1,6350	1,6407	1.6463	1.6518
**											
139 t	352.5	362.5 372.5 382.5		402.5				-		462.5	
7	0.02 3.24	3.30 3.35 3.41	3,46	3.52		3.62	3.67	3.72	3.78	3.83	
h'	324.0 1192.1	1198.2 1204.1 1210.0		1221.2						1252.9	
n	0.5064 1.5753	1.5828 1.5900 1.5969	1.6036	1.6101	1.6164	1.6224	1,6285	1.6344	1.6401	1.6457	1.6512
140 ±	252 1	363.1 373.1 383.1	202 1	402.1	<i>4</i> 12 1	423.1	122 1	112 1	152 1	463.1	172 1
140 t	353,1	3,27 3,32 3,38	3,44	3.49	3.54	3.60	3,65	3.70	3.75		3.85
7	0.02 3.22 * 324.6 1192.2	1198.3 1204.3 1210.1		1221.4						1253.1	
_	0.5072 1.5747	1.5822 1.5894 1.5964		1.6096						1.6451	
	0,5072 1,5747 C	1.3022 1.3037 1,3301	1.0001	1.0050	2.0255	2.0220	1.0200	1.0000	1.0075	1.0151	1.0300
141 t	353.6	363.6 373.6 383.6	393.6	403.6	413.6	423.6	433.6	443.6	453.6	463.6	473.6
w.V	0.02 3.20	3,25 3,30 3,36	3.41	3.47	3.52	3.57	3.62	3.67	3.72	3.77	
'n	325.2 1192.3	1198.4 1204.4 1210.2	1215.9	1221.5	1227.0	1232.4	1237.7	1242.9	1248.1	1253.3	1258.4
n	0.5079 1.5741	1,5816 1,5888 1,5958	1.6025	1.6090	1.6153	1.6214	1.6274	1.6332	1.6389	1.6445	1.6500
/w'	w					٥					
142 t		364.2 374.2 384.2				424.2				464.2	
K	0.02 3.18	3.23 3.28 3.34	3,39	3.44	3.50	3.55	3.60	3.65	3.70	3.75	3.80
		1198.6 1204.6 1210.4		1221.7						1253.5	
n	0.5086 1.5735	1.5810 1.5882 1.5952	1.6019	1.6084	1.6147	1.6209	1.6269	1.6327	1.0384	1.6440	1,0495
143 t	354.7	364.7 374.7 384.7	304.7	404.7	4147	424.7	4347	444 7	454 7	464.7	A7A 7
γ ₂ 950 Γ		3.21 3.26 3.32	3.37	3,42	3,48	3.53	3.58	3.63	3.68	3.73	3.77
ň		1198.7 1204.7 1210.6		1221.9						1253.6	
	0.5093 1.5730	1.5805 1.5877 1.5947		1.6079						1,6435	
									,,,		
144 t	355.3	365.3 375.3 385.3	395.3	405.3	415.3	425.3	435.3	445.3	455.3	465.3	475.3
V	0.02 3.13	3.19 3.24 3.29	3.35	3.40	3.45		3,55	3.60	3,65		3.75
h		1198.8 1204.8 1210.7		1222.0						1253.8	
n	0.5100 1.5724	1.5799 1.5872 1.5942	1,6009	1.6074	1,6137	1.6199	1.6258	1,6316	1,6373	1.6429	1.6484
442 4	255.0	265 0 275 0 205 0	205.0	405.0	4150	40E 0	125 0	1150	155.0	46E 0	47E 0
145 t		365.8 375.8 385.8 3.17 3.22 3.27	3,32	3,38	3,43	425.8 3.48	3,53	3.58	3.63	465.8	
V h		3.17 3.22 3.27 1199.0 1205.0 1210.8						1243.6		3.68 1254.0	
h n		1.5794 1.5867 1.5937				1.6194				1,6424	
**	0,5107 1,5717	1,5/54 1,500/ 1,555/	1,0007	1,000	1.0102	1.0171	1,0255	1.0011	1.0500	1.0121	1.07/3
146 t	356.3	366.3 376.3 386.3	396.3	406.3	416.3	426.3	436.3	446.3	456.3	466.3	476.3
V		3.14 3.19 3.25	3.30	3.35	3.40	3.45	3.50	3.55	3.60	3.65	3.70
h	328.0 1192.9	1199.1 1205.1 1211.0	1216.7	1222.3	1227.8	1233.2	1238.5	1243.8	1249.0	1254.2	1259.3
n	0.5114 1.5713	1.5789 1.5861 1.5931	1.5999	1,6063	1.6126	1.6188	1.6248	1.6306	1.6363	1.6419	1.6473
	955.0	200 200 200	206.0	400.0	416.0	400.0	1200	446.0	4000	4000	Atric o
147 t			396.9			426.9				466.9	
7		3.12 3.17 3.23	3.28	3,33	3,38	3,43	3.48	3.53	3.58	3.63	
h		1199,2 1205,3 1211,2 1,5784 1,5856 1,5926						1244.0 1.6301			1259.4 1.6468
10	0.5121 1.5708	1,3704 1,3630 1,3920	1.3994	1,0056	1.0121	1,0103	1.0243	1,0301	1.0556	1,0111	1,0100
148 t	357.4	367.4 377.4 387.4	397.4	407.4	417.4	427.4	437.4	447.4	457.4	467.4	477.4
v		3.10 3.15 3.21				3.41				3,61	
Ì		1199.4 1205.4 1211.3						1244.1			1259.6
r		1.5778 1.5850 1.5920						1.6295			1.6463
				4555							Almin -
149		367.9 377.9 387.9				427.9				467.9	
		3.08 3.13 3.19				3,39				3.58	
į								1244.3			1259.8
I	i 0.5135 1.5097	1.5773 1.5845 1.5915	1.3983	1,0048	1.0111	1.01/2	1.0232	1.0291	1,054	1,040 ⁴	1.6458 •
	t = temperature	in F. degs. To Fahr, abs	olute=t°	+459.6°		0011		Intern	al energ	y .	

t = temperature in F. degs. T° Fahr. absolute = t° + 459.6°. Internal energy y = sp. vol. in on. ft. per lb. J = 777.5 ft. lbs. per B. t. n. [log = 2.89 071]. h = total heat in B. t. n. $A = \frac{1}{3}J = 1.286 \times 10^{-3}$ B. t. n. per ft. lb. [$\bar{3}$.10 929]. Values for saturated steam are given in Tables 1 and 2.

											Deg	rees of S	uperheat	_
130° 1	40°	150°	160°	170°	180°	190°	200°	250°	300°	350°	400°	500°	600°	Press. lbs.
482.0 49	92.0	502.0	512.0	522.0	532.0	542.0	552.0	602.0	652.0	702.0	752.0	852.0	952.0	t 138
3,95 4	.00	4.05	4.10	4.15	4.20	4.24	4.29	4.54	4,78	5.01	5.23	5.68	6.13	▼
1262.9 12			1277.9						1346.5				1492.0	h
1.6572 1.6	6625	1,00//	1,6729	1,0/80	1.0830	1.08/9	1.0928	1./104	1.7389	1.7601	1.7805	1.8190	1.8546	n
482.5 4	92.5	502.5	512.5	522.5	532.5	542.5	552.5	602.5	652,5	702.5	752.5	852.5	952.5	t 139
3,93	3,97	4.02	4.07	4.12	4.17	4.22	4.27	4.51	4.74	4.97	5.20		6.10	▼
1263.1 12			1278.1						1346.7					h
1.6566 1.	9919	1.00/1	1.6723	1.0//4	1.0824	1.08/3	1.6922	1.7158	1.7382	1.7595	1.7799	1.8183	1.8540	n d
483.1 4	93.1		513.1	523.1	533.1	543.1	553.1	603.1	653.1	703.1	753.1	853.1	953.1*	t 140
	3.95	4.00	4.05	4.09	4.14	4.19	4.24	4.48	4.71	4.94	5.16	5.61	6.06	v *
1263.3 12 1.6560 1.			1278.3 1.6717						1346.9 1,7376			1443.8 1,8177	1492.4	
1.0300 1.	0014	1.0000	1.0/1/	1.0700	1.0010	1,0007	1.0510	1./134	1.7370	1.7309	1,7792	1,01//	1,0000	n
483.6 4			513.6					603.6	653.6	703.6	753.6	853.6	953.6	t 141
	3.92	3.97	4.02	4.07	4.12	4.16	4.21	4.45	4.68	4.91	5.13	5.57	6.02	V
1263.5 12 1.6554 1.4			1278.5 1,6711				1.6911		1347.1		1395.6		1.8527	Щ
1.0551 1.	0000	1.0000	1,0711	1.0702	le Case	1,0002	1.0711	1,7110	1.7570	1.7505	1,7700	1,0170		
484.2 4			514.2		,	544.2		604.2		704.2	754.2			4 142 ′
	3.90	3.94		4.04	4.09	4.13	4.18	4.42	4.65 1347.3	4.88	5.10 1395.8	5.54	5.98	V
1263.7 12 1,6549 1,			1278.7 1.6705						1.7364		1.7780			h* n
							0200	_,, _ ,,						_
484.7 4			514.7						654.7			854.7		t 143
3,82 3 1263,8 12	3.87 269 9	3.92	3.97 1278.8	4.01	4.06	4.11	4.16	4.39	4.62 1347.5	4.84	5.06 1396.0	5.50	5.94	V h
1.6544 1.			1.6700				1,6900				1,7775			n
		_,,,,,												
485.3 4		505.3	515 3		535.3	545.3		605.3		705.3		855.3		t 144
3.80 3 1264,0 12	3.84 260 A	3.89 1274 0	3,94 1279,0	3.99 1284 0	4.03	4.08 1294 0	4.13 1298 9	4.36	4,59 1347.7	4,81 1372.0	5.03 1396.2	5.46 1444 7	5.90 1493 3	v h
1.6538 1.			1.6695						1.7353		1.7768			n
485.8 4 3.77 3	95.8 3.82	505.8 3.87	515.8 3.92	525.8 3.96	535.8 4.01	545.8 4.05	555.8 4.10	605.8 4.33	655.8 4.56	705.8 4.78	755.8 5.00	855.8 5.43	955.8 5.86	t 145 V
1264.2 12			1279.2						1347.9		1396,4			h
1.6533 1.			1.6690				1.6889				1.7763			n
406.2 4	06.3	roc 2	F1.C 2	roc a	F2C 2	E4C 2	556.2	606.2	6/6 2	706.2	756 2	056.2	056.2	A 140
486.3 4 3.75 3	96. <i>3</i> 3.80	506.3 3.84	516.3 3,89	526,3 3,93	536.3 3.98	546,3 4.02	550.5 4.07	606,3 4,30	4.53	706.3 4.75	756.3 4.97	5.39	956.3 5.82	t 146
1264,4 12			1279.4						1348.1		1396.6			h
1.6527 1.			1.6684				1.6883	1.7118	1.7342	1.7554	1.7757	1.8141	1.8498	n
486.9 4	06.0	506.9	5160	526.9	526 Q	546 0	556.9	606.9	656.9	706.9	756.9	856.9	956.9	t 147
	3.77	3,82	3.86	3.91	3.96	4.00	4.05	4,27	4.50	4.72	4.94	5.36	5.78	Δ
1264.5 12			1279.6						1348.2		1396.8			h
1.6522 1.	6576	1.6628	1.6679	1.6730	1.6780	1.6829	1.6878	1.7113	1,7336	1.7549	1.7752	1.8135	1,8492	n
487.4 4	97.4	507.4	517.4	527.4	537.4	547.4	557.4	607.4	657.4	707.4	757.4	857.4	957.4	t 148
3.70	3.75	3.79		3.88	3.93	3.97	4.02	4.25	4.47	4.69	4.90	5.32	5,75	y
1264.7 12			1279.8						1348.4			1445.5		h
1.6517 1.	0570	1.6622	1.6673	1,6724	1.6774	1.6823	1.0872	1./10/	1.7330	1.7542	1.//40	1.0129	1.8486	n
487.9 4	97.9	507.9	517.9	527.9	537.9	547.9	557.9		657.9		757.9	857.9	957.9	t 149
	3.72	3.77	3.82	3.86	3.91	3.95	4.00	4.22	4.44	4.66	4.87	5.29	5.71	V
1264.9 12	269.9	1274,9	1280.0	1285.0	1290.0	1294.9			1348.6 1.7325				1494,4	
1.6512 1.	0202	1.0017	1.6668	1.6/19	1.0/09	1.0819	1.0007	1,/102	1,/343	1./33/	1.7740	1.5124	1.8480	п

1 kg. per sq. cm.=14.22 lbs. per sq. in. [log=1.15 300]. 1 cn. meter=35.31 cn. ft. [log=1.54 795].

To change degs. C. to degs. F., multiply by ?, and add 32. To change mean kg. calories per kg. to mean B.t.u. per lb., multiply by ?. Entropy same in both systems.

Table 3: Superheated Steam

		Dagrees of Superh	eat				
Press. Ibs.	* Sat. Water Steam	100 000	30° 40°	50°	60° 70°	80° 90°	100° 110° 120°
150 t		368.5 378.5	388.5 398.5		18.5 428.5	438.5 448.5	
Ţ	0.02 3.01 330.2 1193.4	3.06 3.11 1199,6 1205,7	3.17 3.22		3,32 3.37 228,5 1233,9	3.42 3.46	
h n					.6106 1.6168		
						•	
151 t		369.0 379.0			119.0 429.0		
ď		3.04 3.09 5 1199.8 1205.8	3.15 3.20 1211 7 1217 5		3.30 3.35 228,7 1234,1	3.40 3.44 1239 4 1244	
<u> </u>					.6100 1.6162		
152 t		369.5 379.5 3,02 3.07	389.5 399.5 3.13 3.18		119.5 429 5 3.28 3.33	439.5 449.5 3.38 3.42	
Ď					228.8 1234.2		
n			1.5899 1.5967	1,6032 1,	.6095 1.6157	1.6216 1.627	
150 4	360.0°	370.0 380.0	200.0 400.0	4100 4	20.0 430.0	440.0 450.0	1600 1700 1000
153 t	0.00 0.00	3.01 3.06	3,11 3,16		3.26 3.31	3 35 3.40	
Ď					228 9 1234.4		
13	* 0.5162 1.567	1.5751 1.5824	1.5894 1.5962	1.6027 1.	.6090 1.6152	1.6211 1.626	9 1.6326 1.6383 1.6437
154 t	360.5	370.5 380.5	390,5 400,5	4105 4	20,5 430 5	440 5 450 9	460.5 470.5 480.5
~~~ v		2,99 3.04	3.09 3.14		3.24 3 29	3.33 3.38	
h					229 1 1234 5		
n	0.5169 1.5670	1.5746 1.5819	1.5889 1.5958	1.6023 1.	.6085 1.6147	1.6207 1.626	5 1.6322 1.6378 1.6432
155 t	361,0	371.0 381.0	391.0 401.0	411.0 4	21.0 4310	441.0 451.0	461.0 471.0 481.0
7	0.02 2.92	2.97 3.02	3.07 3.12		3 22 3.27	3.31 3.36	
þ					229 2 1234.7		
n	0.5175 1.5665	1.5741 1.5814	1,5884 1,5953	1 6018 1.	.6080 1.6142	1.6202 1.626	0 1.6317 1.6373 1.6427
156 t		371.6 381.6			21.6 431.6		
Ā		2.95 3 00	3 05 3 10		3.20 3.25	3.29 3.34	
h n					229 4 1234.8 .6075 1.6137		
		2,0,00 2,000	2,00,7 2,07	2.0022 2.	.0070 2.0207	2,025, 2,025	2,0022 2,000, 2,0122
157 t		372.1 382.1			22 1 432.1		
y h		2.93 2.98 1200,5 1206,6	3.03 3.08 1212 6 1218 4		3,18 3 23 229 6 1235.0	3.27 3.32	
n					,6070 1,6132		
				4000	100 5 100 5		
158 t		372.6 382.6 2.92 2.97	392 6 402.6 3.02 3.07		122 6 432 6 3.16 3.21	442.6 452.6 3,25 3,30	
'n					229.7 1235.2		
n	0.5195 1.5649	1.5725 1.5798	1.5869 1.5937	1,6002 1,	.6065 1.6127	1,6187 1,624	5 1.6301 1.6357 1.6411
159 t	363.1	373,1 383,1	202 1 403 1	413 1 4	23.1 433.1	443 1 453 1	. 463.1 473.1 483.1
705 U			3.00 3.05		3.14 3.19	3.23 3.28	
h					229.8 1235.3		
n	0.5201 1.564	1.5721 1.5794	1.5865 1.5933	1.5998 1.	.6061 1.6122	1.6182 1.624	0 1.6297 1.6353 1.6407
160 t	363.6	373.6 383.6	393.6 403.6	413.6 4	123.6 433.6	443,6 453,6	463.6 473.6 483.6
y	0,00	2.88 2.93			3.12 3.17		
b			1213.0 1218.8		230.0 1235.5		
I	0,5208 1.5639	9 1.5716 1.5789	1.5860 1.5928	1.5993 1.	.6056 1.6118	1.01// 1.023	5 1,6292 1,6348 1,6402
161 t		374.1 384.1			124.1 434.1		
• 3		2.87 2.91	2.96 3.01	3.06		3,20 3,24	
1	336.2 1194.0 0.5214 1.563		1213.1 1218.9 1.5855 1.5923		230.1 1235.6 .6052 1.6113		
							6
162	364.6	374.6 384.6			124.6 434.6		
1			2.95 3.00 1213.2 1219.0		3.09 3,13 230,3 1235,8	3.18 3.22 1241 1 1246	
		9 1.5706 1.5780			.6047 1.6108		

(46)

			4000	4800	4200	4040					•	rees of Sc	•	Press.
130°	140°	150°	160°	170°	180°	190°	200°	250°	300°	350°	400°	500°	600°	iba.
3,66	498.5 3.70	508.5 3.75	518.5 3.79	528.5 3.84	538.5 3.88	548.5 3.92	558.5 3.97	608.5 4.19	658.5 4.41	708.5 4.63	758.5 4.84	858.5 5.25	958.5 5.67	t 150 y
1265.0 1 1.6507			1280,1 1,6663				1300.0 1.6862					1445,9 1,8118		h n
	499.0	509.0	519.0	529 0	539 0	549 0	559 O	609.0	659.0	709.0		859,0		t 151
3.63	3.68	3.72	3.77	3.81	3.86	3.90	3.95	4.17	4.38	4.60	4.81	5.22	5.64	V
1265,2 1 1.6501			1280.3 1.6657				1300.2 1.6856	1.7091				1446,1 1,8112		h n
489.5	499.5	509.5	519.5	529.5	539.5	549.5	559.5	609.5	659.5	709.5	759.5	859.5	959.5	t 152
3.61 1265.4	3.66	3.70	3.75 1280.5	3.79	3.84	3.88	3.92 1300.3	4.14	4.36	4.57	4.78	5.19	5,60	7
1.6496			1.6652					1.7085				1446,3 1.8106		h n
490.0	500.0	510.0	520.0	530.0	540.0	550,0	560.0	610.0	660.0	710.0	760.0	860.0	960.0	t 153
3.59 1265.5	3.63 1270.6	3.68 1275.6	3.72 1280.6	3.77 1285 6	3.81	3.85 1295 5	3.90 1300 5	4.12 1325.0	4.33 1340 4	4.54 1373.7	4.75 1308 0	5.16	5.57 1495.2•	V h
1.6491			1.6647				1.6845						1.8457	
490.5		510.5				550.5		610.5		710.5	760.5		960.5	t 154
3,57 1265.7	3.61 1270.8	3.66 1275.8	3.70 1280.8	3.74 1285.8	3.79 1290.8	3.83 1295.7	3.88 1300.7	4.09 1325.2	4.30 1349.6	4.51 1373.8	4.72 1398.2	5.13 1446.7	5.54 1495.4	V h
1.6486			1.6642							1.7509	1.7712	1.8095	1.8451	n
491.0			521.0					611.0				861.0		t 155
3,55 1265,9	3.59 1271.0	3.63 1276.0	3.68 1281.0	3.72 1286.0	3.76 1291.0	3.81 1295.9	3.85 1300 8	4.06 1325.3	4,28 1349.7	4,49 1374.0	4.70 1398.4	5.10 1446.9	5.50 1495.6	v h
1,6481	1.6534	1,6586	1.6637	1.6688	1.6737	1,6786	1.6835	1.7070	1.7293	1.7504	1.7707	1.8090	1.8445	n
491.6 3.52			521.6 3.66	531.6 3.70	541.6 3.74	551.6 3.79	561.6 3.83	611.6 4.04	661.9 4.25	711.6 4.46	761.6 4,67	861.6 5.07	961.6 5.47	t 156
1266.0	3.57 1271.4	3.61 1276.1	1281.2				1301.0	1325.5	1349.9	1374.2		1447.1		y h
1.6475	1.6528	1.6580	1.6631	1.6682	1.6731	1.6781	1.6830	1.7064	1.7287	1.7498	1.7701	1.8084	1.8439	n
492.1 3.50	502.1 3.55	512.1 3.59	522.1 3.63	532.1 3.68	542.1 3.72	552,1 3,76	562,1 3,81	612.1 4.02	662.1 4.23	712.1 4.44	762.1 4.64	862.1	962.1 5.44	t 157
1266.2	1271.3	1276.3	1281.3	1286.3	1291,3	1296.2	1301.2	1325.7	1350.1	1374.4	1398.7	1447.3	1496.0	v h
1.6470	1.6523		1.6626				1.6825	1.7059	1.7282	1.7493	1,7696	1,8078	1.8434	n
492,6 3,48	502.6 3.52	512.6 3.57	522.6 3.61	532.6 3.66	542.6 3.70	552.6 3.74	562.6 3.78	612.6 3.99	662.6 4,20	712.6 4.41	762.6 4.62	862.6 5.01	962.6 5.40	t 158 v
1266.3	1271.4	1276,4	1281.5	1286.5	1291.5	1296.4	1301.3	1325.9	1350.3	1374.6	1398.9	1447.5	1496.2	ĥ
1.6464	1.6517		1.6620							1,7487		1.8072		n
493.1 3.46	503.1 3.50	513.1 3.55	523.1 3.59	533,1 3,63	543. <b>1</b> 3.68	553.1 3.72	563.1 3.76	613.1 3.97	663.1 4.18	713.1 4.39	763.1 4.59	863.1 4.98	963.1 5.37	t 159 V
1266.5	1271.6	1276.6	1281.6	1286.6	1291.6	1296.6	1301.5	1326.0	1350.4	1374.8	1399.1	1447,7	1496.4	ĥ
1,6460			1.6616							1,7483			1.8423	n
493.6 3.44		513.6 3.53	523.6 3.57		543.6 3.66	553.6 3.70	563.6 3.74	613.6 3.95	663.6 4.15	713,6 4,36		863.6 4.95	963,6 5.34	t 160 v
1266.7	1271.8	1276.8	1281.8	1286.8	1291.8	1296.8	1301.7	1326.2	1350.6	1375.0	1399,3	1447.9	1496.6	h
1,6456						1.6761				1.7477			1,8418	
494.1 3.42	504,1 3,46	514.1 3.51	524.1 3.55	534.1 3.59	544.1 3.63	554.1 3.67	564.1 3.72	614.1 3.92	664,1 4,13	714.1 4.34	764.1 4.54	864.1 4.92	964.1 5.31	t 161 v
1266.8 1.6451	1271.9	1276.9	1282.0	1287.0	1292.0	1296.9	1301.8	1326.4	1350.8	1375.1 1.7472	1399.4	1448.1	1496.8 1.8413	h
-						1.6756								n 
494,6 3,40	3.44	3,49	524.6 3.53	3,57	3,61	3,65		3.90		714.6 4,31	4.51	864.6 4,89	5,28	t 162 V
1267.0	1272.1	1277.1	1282.2	1287.2	1292.2	1297.1 1.6751				1375,3	1399.6	1448.3	1497.0 1.8407	h
THE WITTER	-14-17-3	A.C.U.A	1.000	1,4032		1,0/31	(47)	~		4,5 TO 5	4./0/0		4.070/	44

(47)

Table 3: Superheated Steam

D	-	Degrees of Superheat		
Press. Ibs.	Sat. Water Steam	10° 20° 30° 40°	50° 60° 70° 80°	90° 100° 110° 120°
163 t	365.1	375.1 385.1 395.1 405.1	415.1 425.1 435.1 445.1	
v h	0.02 2.78 337.2 1194.8	2.83 2.88 2.93 2.98 1201.2 1207.4 1213.4 1219.2	3.02 3.07 3.11 3.16 1224.9 1230.4 1235.8 1241.2	3.20 3.25 3.29 3.34 2 1246,5 1251,7 1256,9 1262,0
n	0.5226 1.5624	1.5701 1.5775 1.5846 1.5914	1.5979 1.6042 1.6104 1.6163	
164 t	365,6	375,6 385.6 395.6 405.6	415.6 425.6 435.6 445.6	455,6 465,6 475,6 485,6
v	0.02 2.77	2.82 2.87 2.91 2.96	3.01 3.05 3.10 3.14	
h	337.7 1194.9	1201.3 1207.5 1213.5 12 <b>1</b> 9.3 1,5697 1,5771 1,5842 1,5910	1225.1 1230.6 1236.0 1241.4 1,5975 1.6038 1.6100 1.6160	
n	0.5233 1.5620	1,509/ 1,5//1 1,5042 1,5910	1,010,1 0010,1 6766,1	0 1.6218
165 t	366.0	376.0 386.0 396.0 406.0	416.0 426.0 436.0 446.0	
v h	0.02 2.75 338.2 1195.0	2.80 2.85 2.90 2.94 1201.4 1207.6 1213.6 1219.5	2.99 3.04 3.08 3.12 1225.2 1230.7 1236.1 1241.5	3.17 3.21 3.26 3.30 5 1246.8 1252.0 1257.2 1262.3
n	0.5239 1.5615	1.5692 1.5766 1.5837 1.5905	1.5970 1.6033 1.6095 1.615	
166 t	366,5	376.5 386.5 396.5 406.5	416.5 426.5 436.5 446.5	456.5 466.5 476.5 486.5
V	0.02 2.74	2.79 2.84 2.88 2.93	2.97 3.02 3.06 3.11	3.15 3.19 3.24 3.28
	* 338.7 1195.1	1201.5 1207.8 1213.8 1219.6	1225.3 1230.9 1236.4 1241.	
n	0.5245 1.5610	1.5688 1.5762 1.5832 1.5901	1.5966 1.6029 1.6091 1.6150	1.6208 1.6265 1.6321 1.6375
167 t	367.0	377.0 387.0 397.0 407.0	417.0 427.0 437.0 447.0	
V	0.02 2.72	2.77 2.81 2.86 2.91	2.96 3.00 3.04 3.09	3.13 3.18 3.22 3.26
h n	339.2 1195.2 0.5251 1.5605	1201,6 1207,9 1213,9 1219,7 1,5683 1,5757 1,5828 1,5896	1225.5 1231.0 1236.5 1241.8 1.5962 1.6025 1.6086 1.6140	
168 t	367.5 0.02 2.71	377.5 387.5 397.5 407.5 2,76 2.81 2,85 2,89	417.5 427.5 437.5 447.5 2.94 2.98 3.03 3.07	3 457.5 467.5 477.5 487.5 3.12 3.16 3.20 3.24
v h	0.02 2.71 339.7 1195.3	1201.7 1208.0 1214.0 1219.9	1225.6 1231.2 1236.7 1242.0	
n	0.5257 1.5600	1.5678 1.5752 1.5823 1.5891	1.5957 1.6020 1.6081 1.614	
169 t	368.0	378,0 388.0 398.0 408.0	418.0 428.0 438.0 448.0	458.0 468.0 478.0 488.0
V	0.02 2.69	2.74 2.78 2.83 2.88	2.92 2.97 3.01 3.06	
h n	340.2 1195.4 0.5263 1.5595	1201.8 1208.1 1214.1 1220.0 1.5673 1.5747 1.5818 1.5887	1225.7 1231.3 1236.8 1242. 1,5952 1,6015 1,6076 1,613	
170 t	368.5 0.02 2.68	378.5 388.5 398.5 408.5 2.73 2.78 2.82 2.86	418.5 428.5 438.5 448.5 2.91 2.95 3.00 3.04	
h	340.7 1195.4	1202.0 1208.2 1214.3 1220.2	1225.9 1231.5 1237.0 1242.	
n	0.5269 1.5590	1,5668 1,5742 1,5814 1,5882	1.5947 1.6010 1.6071 1.613	1 1.6189 1.6246 1.6302 1.6356
171 t	368.9	378.9 388.9 398.9 408.9	418.9 428.9 438.9 448.9	458.9 468.9 478.9 488.9
y	0.02 2.66	2.71 2.76 2.80 2.84	2.89 2.93 2.98 3.02	
h n	341,2 1195,5 0.5275 1.5586	1202.1 1208.3 1214.4 1220.3 1.5664 1.5739 1.5810 1.5878	1226.0 1231.6 1237.1 1242. 1,5944 1,6007 1,6068 1,612	
п	0.5275 1.5580	1,300+ 1,3735 1,3610 1,3676		7 1.0163 1.0242 1.0238 1.0332
172 t	369.4	379.4 389.4 399.4 409.4	419.4 429.4 439.4 449.4	
v h	0.02 2.64 341.7 1195.6	2.69 2.74 2.78 2.83 1202.2 1208.5 1214.5 1220.4	2.88 2.92 2.96 3.00 1226,2 1231,8 1237,2 1242,	
n	0.5281 1.5581	1.5659 1.5734 1.5805 1.5873	1.5939 1.6002 1.6063 1.612	
173 t	369.9	379.9 389.9 399.9 409.9	419.9 429.9 439.9 449.9	9 459 9   469 9   479 9   489 9
7.0 0	0.02 2.63	2.68 2.72 2.77 2.82	2.86 2.90 2.95 2.99	
h	342.2 1195.7	1202.3 1208.6 1214.6 1220.5	1226.3 1231.9 1237.4 1242.	7 1248.0 1253.3 1258.5 1263.6
n	0.5287 1.5576	1,5655 1,5729 1,5800 1,5869	1.5934 1.5997 1.6059 1.611	8 1.6176 1.6233 1.6288 1.6342
174 t	370.4	380.4 390.4 400.4 410.4	420.4 430.4 440.4 450.4	
V	0.02 2.62	2.67 2.72 2.76 2.80	2.84 2.89 2.93 2.97	
h n	342.7 1195.8 0.5293 1.5571	1202,4 1208,7 1214,8 1220,7 1,5650 1,5724 1,5795 1,5864	1226,4 1232,0 1237,5 1242, 1,5930 1,5993 1,6054 1,611	
**				
	V - remperature	in F. degs. To Fahr, absolute = to	+ n. []or - 2 80 0717	Internal energy

y = sp. vol. in ou. ft. per lb. y = y vol. in ou. ft. per lb. y = y vol. in ou. ft. per lb. y = y vol. in ou. ft. per lb. y = y = y vol. in ou. ft. per lb. y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y = y

											Deg	rees of S	uperheat	_
130°	140°	150°	160°	170°	180°	190°	<b>200°</b>	<b>250°</b>	300°	350°	<b>400°</b>	500°	600°	Press. ibs.
495.1	505.1	515.1	525.1	535.1	545.1	555.1	565.1	615.1	665.1	715.1	765.1	865.1	965,1	t 163
	3.42	3.47	3.51	3.55	3.59	3.63	3.68	3.88	4.08	4.29	4.49	4.86	5.25	V
1267.1 1 1.6441 1				1287.3 1.6647				1326.8 1.7028					1497.2 1.8402	h n
2.0112	.,	_,,,,			-,	_,,,,	2.0770	2,7020	,	2.7 102	2.7005	1.00 17	1.0102	**
	505.6	515.6		535.6	545.6			615.6		715.6		865.6		t 164
3,36 1267,3 1	3.41	3.45 1277 4	3.49 1282.4	3.53 1287.4	3.57 1292.4	3.61 1297 4	3.66 1302 4	3.86 1327.0	4.06	4.26 1375 7	4.46	4.83	5.22 1497.4	v h
1.6437 1				1.6643				1.7024					1.8398	n
106.0	<b>506.0</b>	<b>5160</b>	<b>506.0</b>	r2C 0	T4C 0	TTC 0	566.0	(1( 0	<i>(((</i> 0	77.60	<b>T</b> CC 0	066.0	066.0	
	506,0 3.39	516.0 3.43	3.47	536.0 3.51	3.55	3.59	3.64	616,0 3,84	4.04	716.0 4.24	766.0 4.44	866.0 4.81	966.0 5.19	t 165 v
1267.4 1				1287.6	-			1327.1				1448.8		h
1.6433 1	1.6486	1.6537	1.6588	1.6638	1.6688	1.6737	1.6786	1.7019	1.7242	1.7453	1.7655	1.8037	1.8393	n
496.5	506.5	516.5	526.5	536.5	546.5	556.5	566.5	616.5	666.5	716.5	766.5	866.5	966.5	t 166
	3.37	3.41	3.45	3.49	3.53	3.57	3.62	3.81	4.01	4.21	4.41	4.78	5.16	V TOÓ
1267.6 1				1287.8				1327.3			1400.3			h
1.6428 1	L.6 <del>48</del> 0	1.6532	1.6583	1.6634	1.6684	1.6733	1.6782	1.7014	1.7237	1.7448	1.7650	1.8032	1.8387	n
497.0	507.0	517.0	527.0	537.0	547.0	557.0	567.0	617.0	667.0	717.0	767.0	867.0	967.0	t 167
	3.35	3.39	3.43	3.47	3.51	3.55	3.60	3.79	3.99	4.19	4.39	4.75	5.13	v
1267.8 1 1.6423 1				1288.0 1,6629				1327.4 1.7009			1400.5 1.7645			h
1.0725 1		1.0326	1.0319	1.0023	1.0075	1.0720	1.0777	1.7009	1.7232	1.7773	1.70-13	1.0027	1.0302	n
	507.5	517.5		537.5	547.5	557.5		617.5		717.5			967.5	t 168
3,29 1267,9 1	3.33	3.37	3.41	3.45 1288.1	3.49	3.53	3.58	3,77 1327.6	3.97	4.17	4.36 1400.7	4.73	5,10	V h
1.6419 1				1.6624				1.7004			1.7640			h n
	508.0	518.0	528.0	538.0	548.0	558.0		618.0		718.0 4.15		868.0	968.0	t 169
3,27 1268.1 1	3.31 273 2	3.35 1278 2	3.39 1283 2	3.43 1288.2	3.47 1293 2	3.51 1298 2	3.56 1303 2	3.75 1327.8	3,95 1352 2		4.34 1400.8	4.70 1499 5	5.07 1498 4	v h
1.6414 1				1.6619				1.6999			1.7635			n
400 "	۲00 F	<b>510 5</b>	בסט ב	<b>520 5</b>	T 40 T	558.5	568.5	618.5	668.5	718.5	מבס ל	868.5	069 5	1 170
	508.5 3.29	518.5 3.34	528.5 3.38	538.5 3.42	548.5 3.46	3,50	3.54	3,73	3,92	4.12	768.5 4.31	4.67	968,5 5.04	t 170 v
1268.2 1				1288.4				1327.9			1401.0			'n
1.6409 1	.6461	1.6513	1.6564	1.6614	1.6664	1.6713	1.6762	1.6994	1.7217	1.7427	1.7630	1.8011	1.8366	n
498,9	508.9	518,9	528.9	538.9	548.9	558.9	568.9	618.9	668.9	718.^	768.9	868.9	968.9	t 171
3.23	3.27	3.32	3.36	3.40	3.44	3.48	3.52	3.71	3.90	4.10	4.29	4.65	5.02	v
1268.4 1				1288.6				1328.1			1401.2			h
1.6405 1	1.6457	1.6509	1.6560	1.6610	1.6660	1.6709	1.0/58	1.6990	1.7213	1.7423	1.7625	1.8007	1.8362	n
499.4	509.4	519.4	529.4	539.4	549.4			619.4		719.4		869.4	969.4	t 172
	3.26	3.30	3,34	3.38	3.42	3.46	3.50	3.69 1328.2	3.88	4.08	4.26	4.62	4.99	V.
1268.5 1 1.6400 1				1288.7 1.6605				1.6985			1401.4 1.7620			h n
499.9				539.9 3.36			569.9 3.48	619.9 3.67	669.9 3.86	719.9 4.05	769.9 4.24	869.9		t 173
3.20 1268.7 1	3,24 273 8	3,28 1278.8	3.32 1283 9	1288.9	3.40 1293 9	3.44 1298 8		1328.4			1401.6	4.60 1450 2	4,96 1499 1	v h
1.6395 1				1.6601				1.6980					1.8351	n
500.4	510 4	520.4	520 4	540.4	550 4	560 4	570.4	620.4	670.4	720.4	770 4	870.4	<b>07</b> 0 4	t 174
	3,22	3.26	3.30	3.34	3,38	3.42	3.46	3.65	3.84	4.03	4.22	4.58	4.93	τ 1/4 V
1268.8 1		1279.0	1284.0	1289.0	1294.0	1299.0	1303.9	1328.6	1353.0	1377.3			1499.3	'n
1.6390 1	.6443	1.6495	1.6546	1.6596	1.6645	1.6694	1.6743	1.6975	1.7197	1.7408	1.7610	1.7991	1.8346	n

## Table 3. Superheated Steam

* .	•		Degrees (	of Superh	eat									
Press.		Sat. team	10°	20°	30°	40°	50°	60°	70°	80°	90°	100°	110°	120°
175 t	370.8		380.8		400.8	410.8	420.8	430.8	440.8	450.8	460.8	470.8	480.8	490.8
v h	0.02 2 343.2 11	2.60 195 9	2.65 1202 5	2.69 1208 8	2.74 1214.9	2.78	2.83	2.87	2.91 1237.7	2.96	3.00	3.04	3.08 1258.8	3.12
n	0.5299 1.				1.5792				1.6051				1.6280	
176 t	371.3	2	381.3	391 3	401.3	411 3	421.3	431.3	441.3	451 2	461.3	A71 2	481.3	401.2
v	0.02	2.59	2.64	2.68	2.72	2.77	2.81	2.86	2.90	2.94	2.98	3.02	3.07	3,11
h n	343.7 11 0.5305 1.				1215.0 1.5787				1237.8				1258.9	
11	0.3303 1.	.3302	1,3041	1.5715	1.3707	1,3630	1,5921	1.3904	1.6046	1.0103	1.0103	1.6220	1.6275	1,0329
177 t	371.7 0.02 2	7 2.57	381.7 2.62		401.7				441.7		461.7		481.7	
v h	344.2 1			2.66 1209.0	2.71 1215.2	2.75 1221.1	2.80 1226.8	2.84 1232.4	2.88 1237.9	2,92 1243.3	2.97 1248 6	3.01 1253 9	3.05 1259.1	3.09 1264 2
n	0.5311 1.	.5557	1.5636	1.5711	1.5782	1.5851			1.6041				1.6270	
178 t	372.2	2 •	382.2	392.2	402.2	412.2	422.2	432.2	442.2	452.2	462.2	472,2	482.2	492.2
V		2.56	2.61	2.65	2.69	2.74	2.78	2.83	2.87	2.91	2.95	2.99	3.03	3.07
h n	344,7 11 0,5317 1.				1215.3 1.5778				1238.1 1.6037				1259.2 1.6266	
												1.0211	1.0200	
179 t V	372.7 0.02 2	7 2.55	382.7 2.59	392.7 2.63	402.7 2.68	412.7 2.72	422,7 2,77	432.7 2.81	442. <b>7</b> 2.85	452.7 2.89	462.7 2.94		482.7	
'n	345.2 11				1215.4				1238.2			2.98 1254.2	3.02 1259.4	3.06 1264.5
n	0.5322 1.	5547	1.5626	1.5701	1.5773	1.5841	1.5907	1.5970	1.6032	1.6091	1.6149	1.6206	1.6261	1.6315
180 t	373.1	l	383.1	393.1	403,1	413.1	423.1	433.1	443.1	453.1	463.1	473.1	483,1	493.1
v h	0.02 2 345.6 11	2.53	2.58	2.62	2.67 1215.5	2.71	2.75	2.80	2.84	2.88	2.92	2.96	3.00	3.04
n	0.5328 1.				1.5769				1238.4 1.6028				1259.5 1.6257	
181 t	373.6		282 6	202 6	403.6	1126			443.6					
TOT		2.52	2.57	2.61	2.65	2,70	2,74	2.78	2.82	2.86	463.6 2.91	2,95	483.6 2.99	493.6 3.03
h	346,1 11				1215.6				1238.5			1254.5	1259.7	1264.8
n	0.5334 1.	5539	1.5619	1.5693	1.5765	1.5834	1.5900	1.5963	1.6025	1.6084	1.6141	1.6198	1.6253	1.6307
182 t	374.0				404.0				444.0				484.0	
v h	0.02 2 346.6 11	2,51 196 <b>6</b>	2,55 1203 2	2.59 1209.6	2.64 1215.8	2.68	2.72 1227 5	2.77	2.81 1238.6	2.85	2.89	2,93 1254.6	2.97	3.01
n	0.5339 1.				1.5761				1.6020			1.6194		
183 t	374,5	5	384.5	394.5	404.5	414.5	424.5	434.5	444.5	454.5	464.5	474.5	484.5	494 5
V		2,49	2.54	2.58	2.63	2.67	2.71	2.75	2.79	2.84	2.88	2.92	2.96	2.99
h n	347,1 11 0.5345 1.				1215.9 1.5757		1227.7 1.5892					1254.7 1.6189		
184 t	374.9 0.02 2	) 2.48	384.9 2.52	394.9 2.56	404.9 2.61	414.9 2.66	424.9 2.70	434.9 2.74	444.9 2.78	454.9 2.82	464.9 2.86	474.9 2.90	484.9 2.94	494.9 2.98
'n	347.6 1				1216.0				1238.9			1254.9		
n	0.5351 1.	.5525	1.5605	1.5680	1.5752	1.5821	1.5887	<b>1.</b> 5950	1.6011	1.6071	1.6129	1.6185	1.6240	1.6294
185 t	375.4		385.4	395.4	405.4	415.4					465.4	475.4	485.4	495.4
v h	0.02 2 348.0 1				2,60		2.68 1227.9		2.76			2.89 1255.0	2.93	
n	0.5356 1.				1.5748		1.5882					1.6180		
186 t	375.8	3	385.8	395.8	405.8	415.8	425.8	435 8	445.8	455.8	465.8	475 8	485.8	495 8
7	0.02	2.46	2.50	2.54	2.58	2.63	2.67	2.71	2.75	2.79	2.83	2.87	2.91	2.95
h n	348.5 13 0.5362 1.				1216.3 1.5744		1228.0 1.5879		1239.2			1255.2		
_												1.6176		
187 t	376,3 0,02 2		386.3 2.49		406.3 2.57			436,3 2,70	446.3 2.74	456.3 2.78			486.3	
h	349.0 1	197.0	1203.7	1210.2	1216.4	1222.3	1228.1	1233.8	1239.3	1244.7	2.82 1250.0	2.86 1255.3		2.93 1265.6
'n	0.5367 1.					1,5808		1.5937	1.5998		1.6116			

			4000								-	rees of S	•	Posse.
130°	140°	150°	160°	170°	180°	190°	200°	250°	300°	350°	400°	500°	600°	lba.
500.8 3.16 1269.0 1.6387	510.8 3.20 1274.1 1.6439		530.8 3.28 1284.2 1.6542						670.8 3.82 1353.2 1.7193			870.8 4.55 1450.5 1.798 <b>7</b>	4.91 1499.5	t 175 v h n
3.15 1269.1	511,3 3,19 1274,2 1,6434		531.3 3.27 1284.3 1.6537		3.35 1294.3		3.42 1304.2		671.3 3,80 1353.3 1.7188		4.17 1402.1	871,3 4.53 1450.7 1.7982	4.88	t 176 v h
3.13 1269.3	511.7 3.17 1274.4 1.6429	3.21 1279.4	531.7 3.25 1284.5 1.6532	3.29 1289.5	3,33 1294.5	3.37 1299.4	3.41 1304.4		3.78		4.15 1402.2	871.7 4.51 1450.9 1.7977	4.86 1499.8	t 177 v h n
3.11 1269.4	512.2 3.15 1274.5 1.6425		532.2 3.23 1284.6 1.6527				572,2 3,39 1304,5 1,6725	3.58 1329.2	672.2 3.76 1353.6 1.7178			872.2 4.48 1451.0 1.7971		t 178 v h n
	512.7 3.14 1274.7 1.6420		532.7 3.22 1284.8 1.6523				572.7 3.37 1304.7 1,6720		3.74 1353.8			872.7 4.46 1451.2 1.7966		t 179 v h n
3.08 1269.7	513.1 3.12 1274.8 1.6416		533.1 3.20 1284.9 1.6519		3.28 1294.9		573.1 3.35 1304.8 1.6716		3,72 1353.9		4.09 1402.7	873.1 4.44 1451.4 1.7962	4.78 1500.3	t 180 v h n
3.07 1269,9	513.6 3.11 1275.0 1.6412	3.14 1280.0	533.6 3.18 1285.1 1.6515	3,22 1290,1			573.6 3.34 1305.0 1.6712		3.71 1354.1		4.07 1402.9	873.6 4.42 1451.6 1.7958	4.76 1500.5	t 181 v h n
3.05 1270.0	514.0 3.09 1275.1 1.6408		534.0 3.17 1285.2 1.6510		3.24 1295.2		574.0 3.32 1305.1 1.6707	3.51 1329.8		3.87 1378.6	4.04 1403.0	874.0 4.40 1451.7 1.7953	4.74 1500. <b>7</b>	t 182 v h n
3,03 1270.2	514.5 3.07 1275.3 1.6404	3.11 1280.3	534.5 3.15 1285.4 1.6506		3,23 1295,4		574.5 3.30 1305.3 1.6703		3.67 1354.4			874.5 4.37 1451.9 1.7948		t 183 v h n
3.02 1270.3	514.9 3.06 1275.4 1.6400		534.9 3.13 1285.5 1.6501		3.21 1295.5		3.29 1305.4 1.6699	3.47 1330.0 1.6930	1.7151	3.83 1379.0 1.7361	1.7563	4.35 1452.1 1.7943	4.69 1501.1 1.8297	t 184 v h n
3.01 1270.5	515.4 3.04 1275.6 1.6394	3,08 1280.6 1.6446	535.4 3.12 1285.7 1.6497	3.16 1290.7 1.6547	3,19 1295,7 1,6596	3.23 1300.6 1.6645	3.27 1305.6	3.45 1330.2	675.4 3.63 1354.7 1.7146	3.81 1379.1	3.98 1403.5	875.4 4.33 1452.2 1.7938	4.67 1501.2	t 185 v h n
2,99 1270.6	515.8 3.03 1275.7 1.6391	3.07 1280.7	535.8 3.10 1285.8 1.6493	3.14 1290.8	3.18 1295.8	3,22 1300.8	3.25	3,44 1330.3	675.8 3.62 1354.9 1.7142	3.79 1379.3	3.96 1403.7	875.8 4.31 1452.4 1.7934	4.64 1501.4	t 186 v h n
2.97 1270.7	516,3 3,01 1275,8 1,6386	3.05 1280.9	536.3 3.09 1286.0 1.6488	3.13 1291.0	3.16 1296.0	3,20 1300.9	3.24 1305.8	3.42 1330.5		726.3 3.77 1379.4 1.7347	3.94 1403.8	876.3 4.29 1452.6 1.7929	4.62 1501.6	t 187 v h n

(51)

Table 3: Superheated Steam

_		-	Degrees o	f Superho	at						1			
Press. lbs.	Water	Sat. Steam	10°	20°	<b>30°</b>	40°	50°	60°	<b>70°</b>	80°	<b>9</b> 0°	100°	110°	120°
188 t	37	6.7	385.7	396.7	406.7	416.7	426.7	436.7	446.7	456.7	466.7	476,7	486.7	496.7
٧	0.02	2.43	2.47	2.51	2.56	2.60	2.64	2.68	2.72		2.80	2.84		2.92
h n	0.5373	1197.1 1 5507	1203.8	1.5663		-			1239.5 1.5995				1260.7. 1,6223	
· · · · · · · · · · · · · · · · · · ·					1.5705	1,5001	1.5070				•			
189 t		7.2		397.2	407.2		427.2	437.2,		457.2		477.2	487.2	<b>497.</b> 2
v h	0.02 349 9	2.42 1197.2	2.46	2.50 1210.4	2.55 1216.6		2.63 1228 4	2.67	2.71 1239.6	2.75 1245 0	2.79 12 <b>5</b> 0 3	2.83 1255.6	2.87 1260.8	2.91 1265 9
n		1.5502		1.5658					1.5990				1.6218	
400 .			<b>205</b> 5		105.5	115.0	405.6	407.6	445.6		465.6	488.6	405.6	
190 t	0.02	77.6 2,41	387.6 2.45	397.6 2.49	407.6 2 <b>.5</b> 3	2.58	427.6 2.62	437.6 2.66	2.70	457.6 2.74	467.6 2.78	2.81	487.6 2.85	497.6 2.89
ň		1197.3		1210.5					1239.8				1260.9	
n	0.5384	1.5498	1.5579	1.5654	1.5727	1.5796	1.5862	1.5925	1.5986	1.6046	1.6103	1.6159	1,6214	1.6268
191 t	37	78.0€	388 O	398.0	408 O	418.0	428 O	438.0	448,0	458 N	468.0	478.0	488.0	498 O
V	0.02	2.39	2.43	2.48	2.52	2.56	2.60	2.64	2.68	2.72	2.76	2.80	2.84	2.88
h		1197.3		1210.6					1239.9		1250.6		1261.0	
n	0,5389	1.5494	1.5575	1.5650	1.5723	1.5792	1.5858	1.5921	1.5983	1.6042	1.6100	1.6156	1.6211	1.6265
192 t	37	78.5	388.5	398.5	408,5	418.5	428.5	438.5	448.5	458.5	468.5	478.5	488.5	498.5
V	0.02	2.38	2.42	2,46	2.51	2.55	2.59	2.63	2.67	2.71	2.75	2.79	2.83	2.86
h		1197.4		1210.7					1240.0		-		1261.2	
n	0.3393	1.5490	1.5571	1,3040	1.3/19	1.5769	1.5655	1.3910	1.5979	1.0036	1,0090	1,0132	1.6207	1,0201
193 t	37	78.9	388.9	398.9	408.9	418.9	428.9	438.9	448.9	458.9	468.9	478.9	488.9	
V	0.02	2.37	2.41	2.45	2.49	2.54	2.58	2.62	2.66	2.70	2.73	2.77	2.81	2.85
h n		1197.5 1.5485		1210.8 1.5642					1240.2 1.5974				1261.3 1.6203	
	0,5100	1,5 105	2.5000	2.5015	1.07.10	2.570	2,0000	2.0020	2.00.	2,000 .	2.0052		_,0_00	2,0200
194 t		79.3		399.3	409.3		429.3	439.3	449.3	459.3	469.3	479.3 2.76	489.3 2.80	
v h	0.02 352.2	2.36 1197.6	2.40 1204 4	2.44 1211.0	2.48 1217 2	2,52 1223 2	2,56 1229 0	2.60 1234 7	2.64 1240.3	2.68 1245.7	2.72 1251.0		1261.5	
n		1.5481		1.5638					1.5971				1.6199	
195 t	. 25	79.8	389.8	399.8	409.8	419.8	429.8	439.8	449.8	459.8	469.8	479.8	489.8	499.8
<b>100 t</b>	0.02	2.35	2,39	2,43	2.47	2.51	2.55	2.59	2.63	2.67	2.71	2.75	2.78	2.82
h		1197.7		1211.1					1240.4				1261.6	
n	0.5410	1.5476	1.5557	1.5633	1,5706	1.5776	1.5842	1.5905	1.5966	1,6025	1,6083	1.6139	1.6194	1.6248
196 t	38	30.2	390.2	400.2	410.2	420.2	430.2	440.2	450.2	460,2	470.2	480.2	490.2	500.2
v	0.02	2.34	2.38	2.42	2.46	2.50	2.54	2.58	2.62	2.66	2.70	2.73	2.77	2.81
h		1197.8 1.5472		1211.2 1.5629					1240.6 1,5962				1261.7 1.6190	
n	0,5710	, I,J714	1,3333	1,3023	1.5102	1.3114	1,5050	1,5501	1,5504	1.0022	1.0015	1.0133		
197 t		80.6		400.6	410.6		430.6	440.6		460,6	470.6	480.6	490.6	
V	0.02	2.32 1197.8	2.36	2.40 1211,3	2.45	2.49	2,53	2.57	2.61 1240.7	2.64	2.68	2,72	2.76 1261.9	2,79
h n		1.5468		1.5626					1.5958				1.6187	
198 t	0.02	81.0 2.31	391.0 2.35	401.0	411.0 2.44		431.0 2.52		451.0 2.59				491.0 2.74	4
v h		1197.9		1211.4					1240.8				1262.0	
n		5 1.5464		1.5622					1.5955				1.6183	
199 t	2	81.4	301 <i>A</i>	401,4	411 4	421 A	437 A	441 A	451.4	461 4	471 4	481 4	491.4	501 4
133 £	0.02		2.34		2,42	2.46	2.50	2.54	2.58	2.62	2,66	2.69	2,73	2.77
h		1198.0	1204,9	1211.5	1217.7	1223.8	1229,7		1240.9	1246.3	1251.6	1256.9	1262.1	1267.2
n	0.543	1 1.5460	1.5542	1.5618	1.5691	1.5761	1.5827	1.5890	1.5951	1.6011	1.6068	1.6124	1.6179	1.6233
	$\mathbf{t} = \mathbf{ter}$	mperature :	in F. degr	в. <b>Т</b> ° Fа	hr. abso	late=t°-	- <b>4</b> 59.6°				Intern	al energy		

t = temperature in F. degs. To Fahr. absolute = to + 459.60. Internal energy = total heat in B. t. u. J = 777.5 ft. lbs. per B. t. u.  $[\log = 2.89 \ 071]$ . A=1/J=1.286×10-3 B. t. u. per ft. lb. [3.10 929]. Values for saturated steam n = entropy. 144 A=0.1852  $[\log = \overline{1}.26\ 764]$ .

											Deg	rees of S	uperheat	
130°	140°	150°	160°	170°	180°	190°	200°	250°	300°	350°	400°	500°	600°	Press. ibs.
	516.7	·526.7		546.7	556.7	566,7	576.7	626.7	676,7	726.7	<b>~776.7</b>	876.7	976.7	t 188
2.96	3.00	3.04	3.07	3,11	3.15	3.18	3.22	3.40	3,58	3.75	3.92	4.26	4.60	Δ,
1270.9		1281.0					1306.0		1355.1	1379.6		1452.7		'n
1.6330	1.6382	1.6433	1.6484	1.6534	1.6583	1.6632	1.6681	1.6912	1.7133	1.7343	1.7544	1.7924	1.8278	n
507.2	517.2	527.2	537.2	547.2	557.2	567.2	577.2	627.2	677.2	727.2	ר דדד	פ ללפ	077.0	± 100
2.95	2.98	3.02	3.06	3.10		3.17	3.20	3.38	3.56	3.73	777,2 3.91	4.24	977.2 4.58	t 189 v
1271.0				1291.2					1355.3			1452.9		'n
1.6325	1.6378	1.6429	1.6479	1.6529	1.6578	1.6627	1.6676	1.6907	1.7128	1.7338		1.7919		n
507.6	£176	527.6	537.6	5176	557.6	567.6	5776	607.6	677 6	ממד ב	777 6	סמים	022.6	4 400
507.6 2.93	517.6 2.97	3.00	3.04	3.08	3,12	3.15	3.19	627,6 3,37	3.55	727.6 3.72	3.89	877.6 4.22	977.6 4.55	t 190 v
1271.2				1291.4					1355.5			1453.1		h
1.6322	1.6374			1.6525					1,7124			1.7915		n
'00 O	710 A	500 A	F20 A	T40.0	rron		r#0.0	600.0	C70.0	<b>T</b> 00.0	<b>5</b> 50 0	0000	050.0	
i08.0 2.92	2.95	528.0 2.99	3.03	548.0 3.06	3,10	3.14	3/8.0 3,17	628.0 3.35	3.53	728.0 3.70	778.0 3.87	8 <b>2</b> 8.0 4.20	978.0 4.53	t 191
1271.3				1291,5			1306.4					1453,2		v h
1.6318				1.6522			1.6668					1.7911		n
T00 F	<b>510 5</b>	<b>500 5</b>	<b>530 5</b>	5.40 f	##O #	# c 0 #	***	500 <b>m</b>						
508.5	518.5 2,94	528.5 2.98	538.5 3.01	548.5 3.05	558.5	568.5 3.12		628.5		728.5	778.5		978.5	t 192
2.90 1271.5				1291.7	3.09 1296.7		3.16 1306.6	3.34	3.51 1355.8	3.68 1380.2	3.85 1404 6	4.18 1453.4	4.51 1502 4	v h
1.6314				1.6518			1.6665					1.7907		n
508.9			538.9		558.9	568.9		628.9		728.9		878.9		t 193
2,89 1271,6	2 <b>.92</b> 1276 7	2.96 1281 7	3.00 1286.8	3.04 1291.8	3.07 1296.8	3.11 1301.8	3.14 1306.7	3.32 1331 4	3.49 1355 9	3.66 1380 3	3.83 1404.8	4.16 1453.6	4.49 1502 6	V h
1.6309		1.6412					1.6660				1.7522			n
	519.3	529.3		549.3	559.3	569.3		629.3		729.3		879.3	979.3	t 194
2,88 1271.7	2.91 1276.8	2.95 1281 8	2.98	3.02 1291.9	3.06 1296.9	3.09	3.13 1306.8	3.31	3,48 1356 1	3,64	3.81	4.14 1453.7	4,47	v h
1.6306				1.6509			1,6656					1.7897		n
509.8				549.8		569.8		629.8		729.8		879.8		t 195
2.86 1271.9	2.90	2.93	2.97	3.01 1292.1	3.04	3.08	3.11 1307.0	3.29	3,46	3.63	3.80 1415.1	4.12	4.44	v h
1,6301				1,6504			1,6652					1.7892		n
	520.2		540.2	550.2	560.2	570.2			680.2	730.2	780.2	880.2	980.2	t 196
2.85 1272.0	2.88	2.92	2.95	2.99 1292.2	3.03	3.06	3.10 1307.1	3.28	3.45	3.61	3.78 1405.2	4.11	4.42	v h
1,6297				1.6500			1.6647					1.7888		n
-10-27	-,00 13	2.0100	2,0,50	2.0500	2,00	2,0030	2.00 17	,	-1,, 0,, 0					
	520.6			550.6				630.6		730.6		880.6		t 197
2. <b>83</b> 1272.1	2.87	2.90	2.94	2.98 1292.4	3.01	3.05	3.08 1307.2	3.26	3.43	3.59	3.76	4.09 1454,2	4.40	V L
1,6293		1.6396					1.6643					1.7884		h n
. کردهای	2.0015		-											**
511.0				551.0					681.0			881.0		t 198
2.82	2.85	2.89	2.93	2.96	3,00	3,03	3.07	3,24	3,41	3,58	3.74	4.07	4,38	<b>V</b>
1272.3 1 1.6290 1		1282.4		1.6493			1307.3 1,6640					1454.4 1.7880		h n
		1,0093	±.0113	Z,UT93	2.0574	2.000								**
511.4				551.4					681.4			881.4		t 199
2.81 1272.4	2.84	2,88	2.91		2.98	3.02	3,06 1307.5	3.23	3.40	3.56	3.72	4.05 1454.5	4.36	<b>V</b>
1.6286		1282.5		1.6489					1.7086				1.8229	h n
,		_,,,,,,,,,												

1 kg. per sq. cm. = 14.22 lbs. per sq. in. [log=1.15 300]. 1 cu. meter=35.31 cu. ft. [log=1.54 795].

To change degs. C. to degs. F., multiply by \$, and add 32. To change mean kg.
calories per kg. to mean B.t.u. per lb., multiply by \$. Entropy same in both systems.

Table 3: Superheated Steam

I AUIC	J. Dupern	Cated Steam									
Press.	Sat.	Degrees of Superheat	400	<b>20</b> 0	***	700		000	4000	4400	4000
ibs.	Water Steam	10° 20° 30°	40°	50°	<b>6</b> 0°	70°	<b>80°</b>	90°	100°	110°	120°
200 t	381.9	391.9 401.9 411.9	421.9	431.9	441.9	451.9	461.9	471.9	481.9	491.9	501.9
V	0.02 2.29	2.33 2.37 2.41	2.45	2.49	2.53	2.57	2.61	2.64	2.68	2.72	2.76
þ	354.9 1198.1	1205.0 1211.6 1217.8				1241.1				1262.3	
n	0.5437 1.5456	1.5538 1.5614 1.5687	1.5/57	1.5823	1.5886	1.5947	1.6007	1.6064	1.6120	1.6175	1.6229
201 t	382.3	392.3 402.3 412.3	422.3	432.3	442.3	452.3	462.3	472.3	482.3	492.3	502.3
v	0.02 2.28	2,32 2,36 2.40	2.44	2.48	2.52	2.56	2.59	2.63	2.67	2.71	2.74
h	355.3 1198.2	1205.1 1211.7 1218.0	1224.0	1229.9	1235.6	1241,2	1246.6	1251.9		1262.4	
n	0.5442 1.5452	1.5534 1.5610 1.5683	1.5753	1.5820	1.5883	1.5944	1.6003	1.6061	1.6117	1.6172	1.6225
000 +	200 7	200 7 400 7 410 7	122 7	120 7	1107	452.7	160 7	470 T	190 7	400 7	E00 7
202 t ▼	382,7 0.02 2,27	392.7 402.7 412.7 2,31 2,35 2,39	2.43	2,47	2.51	2.55	2.58	2.62	482.7 2.66	492,7 2,70	2.73
h	355.8 1198.2	1205.2 1211.8 1218.1				1241.3				1262.5	
ñ	0.5447 1.5448	1,5530 1,5607 1,5680				1.5940				1.6168	
203 t	383.1	393.1 403.1 413.1				453.1				493.1	
V	0.02 2.26	2.30 2.34 2.38	2.42	2,46	2.50	2.53	2.57	2.61	2.64	2.68	2.72
h n	356.2 1198.3 0.5452 1.5444	1205.3 1211.9 1218.2 1,5526 1,5603 1,5676		1230.1 1.5812						1262.7 1.6164	
ш	0,5452 1,5444	1,5520 1,5005 1,5070	1,5740	1.5012	1.5075	1.5550	1.5550	1.0055	1.0109	1.010+	1,0210
204 t	383.5	393.5 403.5 413.5	423.5	433.5	443.5	453.5	463.5	473.5	483.5	493.5	503.5
V	0.02 2.25	2,29 2,33 2,37	2,41	2.45	2.48	2.52	2.56	2.60	2.63	2,67	2.70
h	356.7 1198.4	1205.4 1212.0 1218.3		1230.3						1262.8	
n	0.5458 1.5440	1.5522 1.5599 1.5672	1.5742	1.5809	1.5872	1.5933	1.5992	1.6050	1.6106	1.6161	1.6214
205 t	384.0	394.0 404.0 414.0	424 n	434 N	444 N	454.0	464 N	474 N	484 N	494.0	504.0
<b>200 t</b> ∇	0.02 2.24	2.28 2.32 2.36	2.40	2.44	2.47	2.51	2.55	2.58	2.62	2.66	2.69
'n	357.1 1198.5	1205.4 1212.1 1218.4		1230.4						1262,9	
n	0.5463 1.5436	1.5518 1.5595 1.5669	1.5739	1.5805	1.5868	1.5929	1.5988	1.6046	1.6102	1.6157	1,6210
		0011 1011 1711	40.4.4	10.1.1				454.4	404.4		
206 t	384.4 0.02 2,23	394.4 404.4 414.4 2,27 2.31 2.35	424.4 2.38	434.4 2.42	444.4 2.46	454.4 2.50	464.4 2.54	4/4.4 2.57		494.4	
v h	0.02 2.23 357.5 1198.5	1205.5 1212.2 1218.5				1241.8			2.61 1257.8	2.64 1263.0	2.68 1268 2
n	0.5468 1.5432	1,5514 1,5591 1,5665				1.5925				1.6153	
							-	-			
207 t	384.8	394.8 404.8 414.8		434.8		454.8				494.8	
<b>∀</b>	0.02 2.22	2.26 2.29 2.33	2.37	2.41	2.45	2.49	2.52	2.56	2.60	2.63	2.67
h n	358.0 1198.5 0.5473 1.5428	1205.6 1212.3 1218.6 1.5511 1.5588 1.5662				1241.9 1.5922				1263,2 1,6150	
п	0,3473 1,3426	1,5511 1,5500 1,5002	1.3131	1.51 90	1.5001	1,3944	1,3301	1,0030	1.007	1.0130	1,0203
208 t	385.2	395.2 405.2 415.2	425.2	435.2	445.2	455.2	465.2	475.2	485.2	495.2	505,2
7	0.02 2.21	2.25 2.28 2.32	2.36	2.40	2.44	2.48	2.51	2.55	2.58	2.62	2.66
h	358.4 1198.7	1205.7 1212.4 1218.7				1242.0				1263.3	-
n	0.5478 1.5424	1.5507 1.5584 1.5658	1.5728	1,5794	1,5857	1.5918	1.5977	1.6035	1.6091	1.6146	1.6199
209 t	385.6	395.6 405.6 415.6	425 6	435.6	445 6	455,6	465.6	475.6	485.6	495.6	505 6
<b>2</b> 03 €	0.02 2.20	2,24 2,27 2,31	2.35	2.39	2,43	2.46	2.50	2.54	2.57	2.61	2.64
'n	358.8 1198.8	1205.8 1212.5 1218.8	1224.9	1230.9	1236.6	1242.2				1263.4	
n	0.5483 1.5420	1,5503 1,5580 1,5654	1.5724	1.5790	1.5853	1.5914	1.5974	1.6031	1.6087	1.6142	1.6195
040.4	206.0	206.0 406.0 416.0	426 O	426 N	1160	156.0	166.0	476 O	106 N	406 O	506 O
210 t	386.0 0.02 2.19	396.0 406.0 416.0 2.23 2.26 2.30				456.0 2.45				496.0 2.60	
h	359.2 1198.8	1205.9 1212.6 1219.0	1225.1					1253.1			
n	0.5488 1.5416	1.5499 1.5576 1.5650		1.5787					1,6084		
211 t	386.4	396.4 406.4 416.4				456.4				496.4	
V.	0.02 2.18	2,22 2,25 2,29				2.44				2.59	
h n	359.6 1198.9 0.5493 1.5413	1206.0 1212.7 1219.1 1,5496 1,5573 1,5647				1242,4 1.5908				1263.7 1.6136	
п	CLPC,I CEPC,O	1,3750 1,3373 1,3047	2.5710	1,5704	1,507/	1,0700	1.3501	1,0043	1.0001	±.01.70	A.UAU3
212 t	386,8	396.8 406.8 416.8				456.8				496.8	
V	0.02 2.17	2.21 2.24 2.28				2.43					2.61
h	360.1 1199.0	1206.1 1212.8 1219.2							1258.6		
n	0.5498 1.5409	1.5492 1.5570 1.5644	1.5714		1,5843	1.5904	1.5964	1.6021	1.6077	1.6132	1.0182
				(54)		-					

								•			De	grees of 8	Superheat	
130°	140°	150°	160°	170°	180°	190°	<b>200°</b>	250°	300°	350°	400°	500°	600°	Press. lbs.
511.9	521.9	531.9	541.9	551.9	561.9	571.9	581.9	631.9	681.9	731.9	781.9	881.9	981.9	t 200
2.79	2.83	2.86	2.90	2.94	2.97	3.00	3.04	3.21	3.38	3.54	3.71	4.03	4.34	V L
1272.5 1.6282				1292.8 1.6485					1357.0 1.7082				1503.7 1.8225	h n
1.0202	1,000										1,7 1,50			
512.3	522.3			552.3	562.3		582.3		682.3		782.3	882.3		t 201
2.78 1272.6	2.81 1277 7	2.85 1282.8	2.88 1287 8	2.92 1292.9	2.96 1297 9	2.99 1302.8	3.03 1307 8	3.20 1332.5	3.37 1357.1	3.53 1381.6	3.69 1406.0	4.01 1454 8	4.32 1503.9	⊽ h
1.6278				1.6481					1.7078				1.8221	n
F10.7	roo #	£20 7	E 40 7	בבט ב	5607	570 7	E00 7	620 7	690 h	720 7	700 7	000 7	000 7	+ 000
2,77	522. <b>7</b> 2.80	2.84	542.7 2.87	552.7 2.91	562,7 2,94	572.7 2.98	3,01	632.7 3.18	3.35	732.7 3.51	782.7 3.67	882.7 3.99	982.7 4.30	t 202 v
1272.8		1282.9							1357.2				1504.0	'n
1.6274	1,6326	1.6377	1.6427	1.6477	1.6526	1.6575	1.6624	1.6854	1.7074	1.7283	1.7484	1.7863	1.8216	n
513.1	523.1	533 1	543 1	553.1	563 1	573 1	583 1	633.1	683 1	733.1	783 1	883.1	983.1	t 203
2.76	2.79	2.82	2.86	2.90	2.93	2.96	3.00	3.17	3.34	3.50	3.66	3.97	4.28	v
	1278.0			1293.2					1357.4			1455.2		h
1,6271	1.6323	1.6374	1.6424	1.6474	1.6523	1.6571	1.6620	1.6850	1.7070	1,7279	1.7480	1.7859	1.8212	n
513.5	523.5	533.5	543.5	553.5	563.5	573.5	583.5	633.5	683.5	733.5	783.5	883.5	983.5	t 204
2.74	2.78	2.81	2.85	2.88	2.92	2.95	2.98	3.15	3.32	3.48	3.64	3.95	4.26	v
1273.0 1.6267		1283.2		1,6470					1357.5 1.7066			1455.3 1.7855		h n
1,020,	1.0017			1,0770	1.0020	2.050.	2.0020	1.0010	1,7000	1.12/5	2.7 170	1.,000	1,0200	
514.0				554.0					684.0			884.0		t 205
2.73	2.76 1278.3	2.80	2.83	2.87 1293.4	2.90	2.94	2.97	3.14	3.30 1357.7	3.46 1382 1	3.62 1406.6	3.93 1455.5	4.24	v h
1.6263				1.6466					1.7062				1.8204	n
	<b>504</b>	<b></b>	~			554.4	504.4	ca4 4	co.4.4	7244	<b>~</b> 0.4.4	004.4	0044	
514.4 2. <b>7</b> 2	524,4 2,75	534.4 2.79	544.4 2.82	554.4 2.86	2.89	5/4,4 2,92	584.4 2.96	3.13	684.4 3.29	734,4 3,45	784.4 3.61	884.4 3.92	984.4 4.22	t 206 v
1273.3			-	1293.6			1308.5					1455,6		h
1.6259	1.6311	1.6362	1.6412	1.6462	1.6511	1.6560	1.6609	1.6838	1.7058	1.7267	1,7468	1.7847	1.8200	n
514.8	524,8	534.8	544.8	554.8	564.8	574.8	584.8	634.8	684.8	734.8	784 8	884,8	984 8	t 207
2.70	2.74	2.77	2.81	2.84	2.88	2.91	2.94	3.11	3.27	3.43	3.59	3.90	4.21	v
	1278.5			1293.7					1358.0			1455,8		h
1,6255	1.6307	1.6358	1.6408	1.6458	1.6507	1.6556	1.6605	1.6835	1.7054	1.7263	1.7464	1.7843	1.8196	n
515.2	525.2			555.2	565.2			635.2		735.2		885.2	985.2	t 208
2.69	2.73	2.76	2.80	2.83	2.86	2.90	2.93	3.10	3.26	3.42	3.58	3.89	4.19	Ā
	1278.7 1.6304			1293.8 1.6455			1308.8		1.7050			1455.9 1.7839		h n
	525.6			555.6					685.6 3.25			885.6		t 209
2.68 1273 7	2.71 1278.8	2.75 1283 8	2.78 1288 9	2.81 1293.9	2.85 1298 9	2.88	2.92 1308 9	3.09 1333.6	1358.2	3,40 1382.7	3.56 1407 2	3.87 1456.1	4.17	v h
	1.6300			1.6451					1.7046					n
516.0	526.0	526 O	546.0	556.0	566 O	576.0	586 O	636.0	686.0	736.0	786 O	996 N	006 N	+ 010
	2.70	2,74		2,80			2.91		3,23	3.39	3.54	886.0 3.85	4.15	t 210 v
	1278.9	1284.0	1289.0	1294.0	1299.0	1304.0		1333.7	1358.4	1382.8	1407.3	1456.2	1505.3	h
1.6244	1.6296	1.6347	1.6397	1.6447	1.6496	1.6544	1.6593	1.6823	1.7042	1.7251	1.7452	1.7830	1.8183	n
516.4	526.4	536.4	546.4	556.4	566.4	576.4	586.4	636.4	686.4	736.4	786.4	886.4	986.4	t 211
	2.69	2.72	2.76	2.79	2.83	2.86	2.89		3.22	3.37	3.53	3.84	4.13	V
	1278.1 1.6293			1294.2 1.6444					1358.5 1.7039				1505.5 1,8180	
		±.WTT	A.0037	*******	¥.U773	1.0571					A.1777	1.1041	1.0100	м
	526.8			556.8					686.8			886.8		t 212
2,64 1274 1	2.68 1278.2	2,71 1284 3		2.78 1294.3	2,82	2.85		3.04 1334 0		3.36 1383,1	3.51	3,82 1456 5	<b>4.</b> 12 1505,6	V h
	1.6289									1.7244				
					•		(55)	-		,				

Table 3: Superheated Steam

_		1	Degrees o	f Superhe	at									
Press. lbs.		Sat. Iteam	10°	<b>20°</b>	30°	40°	50°	60°	70°	<b>8</b> 0°	<b>90°</b>	100°	110°	120°
213 t	387.2					427.2	437.2	447.2			477.2	487.2	497.2	507.2
V	0.02 2 360.5 1	2.16	2,20 1206,2	2.23	2.27	2.31	2,35 1231,3	2.38	2,42	2.46	2.49	2,53 1258,7	2.56	2.60
h n	0.5503 1		1.5488						1.5901			1,6073		
214 t	387.			407.6			437.6		457.6		477.6	487.6		507.6
V h	0.02 360.1 1	2,15	2.19 1206.2	2,22 1213 0	2.26	2,30	2,34 1231,5	2.37	2.41	2.45	2.48	2,52 1258.8	2,55	2.59
h n	0.5508 1		1,5484						1.5897			1,6070		
	-		_,					_,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	_,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	_,		,		,
215 t	388.			408.0					458.0		478.0		498.0	
Ā		2.14	2.18	2.21	2,25	2.29	2.33	2.36	2.40 1242.9	2.43	2.47	2.51	2.54	2.57
h n	361.4 1 0.5513 1		1206.3 1.5481						1.5894				1264.2 1.6121	
			1,5 101	1.0000	1,5000	2.3700	2,5770	1,5000	1.5051	1.5755	1.0011	1.0007	1.0121	1,0174
216 t	388.			408.4					458.4			488.4		508.4
V		2.13	2.17	2.20	2.24	2.28	2.32	2.35	2.39	2.42	2.46	2.49	2.53	2.56
h n	361,8 1 0.5518 1		1206.4 1.5478						1243.0 1.5891				1264.3 1.6118	
	0.5510 1		1.5170	1.5550	1.5000	1.5700	1.5707	1.5050	1.3071	1.5550	1.0007	1.0005	1.0110	1.01/2
217 t	388.	.8	398.8	408.8	418.8	428.8	438.8	448.8	458.8	468.8	478.8	488.8		508.8
v	0.02	2.12	2.16	2.19	2.23	2.27	2.31	2.34	2.38	2.41	2.45	2.48	2.52	2.55
h n	362,2 1 0.5523 1		1206.5 1,5474						1243.2 1.5887				1264.4 1.6113	
ш	0,3323 1	1.3330	1.5777	1.3332	1,3020	1,5050	1,5705	1.3020	1,5007	1.5570	1,000+	1.0039	1,0113	1.0107
218 t	389.	.1	399.1	409.1	419.1	429.1	439.1	449.1	459.1	469.1	479.1	489.1	499.1	509.1
V	0.02	2.11	2.15	2.18	2.22	2.26	2.30	2.33	2.37	2.40	2.44	2.47	2.51	2.54
h n	362.6 I 0.5528 I		1206.6	1.5548					1243.3 1.5883				1264.5	
п	0.3320	1.5500	1.5470	1.3340	1,3024	1,3033	1.3739	1,3022	1,3003	1,3543	1,0000	1.0033	1.6110	1.0104
219 t	389	.5	399.5	409.5	419.5	429.5	439.5	449.5	459.5	469.5	479.5	489.5	499.5	509.5
v	0.02	2.10	2.14	2.17	2.21	2.25	2.29	2.32	2.36	2.39	2.43	2.46	2.50	2.53
h	363.0 I 0.5533 I			1213.5					1243.4		-		1264.6	
n	0.5555	1,3303	1,5407	1.5545	1.3019	1,3090	1,3730	1,3019	1.5880	1.3940	1,3997	1.0052	1.6107	1.0101
220 t	389	.9	399.9	409.9	419.9	429.9	439.9	449.9	459.9	469.9	479.9	489.9	499.9	509.9
V	0.02	2.09	2.13	2.16	2.20	2.24	2.28	2.31	2.35	2.38	2.42	2.45	2.49	2.52
h	363.4			1213.6					1243.5				1264.8	
n	0.5538	1.5579	1.5403	1.5541	1,3010	1,3000	1.5755	1.5610	1.5877	1.5930	1,3993	1.0049	1.6104	1.0157
221 t	390	).3	400.3	410.3	420.3	430.3	440.3	450.3	460.3	470.3	480.3	490.3	500.3	510.3
y	0.02	2.08	2.12	2.15	2.19	2.23	2.27	2.30	2.34	2.37	2.41	2.44	2.48	2.51
h	363.8			1213.7					1243.6					1270.0
n	0.5543	1.5370	1.5400	1.5538	1.5013	1,5005	1.5750	1.5813	1.5874	1.5933	1.5990	1.0040	1.0101	1.6154
222 t	390	0.7	400.7	410.7	420.7	430.7	440,7	450.7	460.7	470.7	480.7	490.7	500.7	510.7
y		2.07	2.11	2.14	2.18	2.22	2.26	2.29	2.33	2.36	2.40	2.43	2.47	2.50
h	364.2					1226.4			1243.8 1.5871					1270,2
n	0.5548	1,5572	1.5450	1,5555	1,3009	1,5680	1.5747	1.3610	1.36/1	1.5950	1,5907	1,0043	1.0090	1.6151
223 t	391	1.1		411.1			441.1	451.1	461.1	471.1		491.1	501,1	511.1
<u>v</u>	0.02	2.06	2.10	2.13	2.17	2.21	2.25	2.28	2.32	2.35	2.39	2.42	2.46	2.49
h		1199.8				1226.5					1254.6 1.5984			1270,3
n	0.5553	1.3309	1.5453	1,5552	T.3000	1.5677	1,3744	1.3607	1.3008	1.3941	1.3904	1,0040	1,0093	1,6148
224 t	39:	1.5	401.5	411.5	421.5	431.5	441,5	451.5	461.5	471.5	481.5	491.5	501.5	511.5
V				2.13					2.31			2.41		
h	365.0 0.5557					1226.6 1.5674					1254.8 1.5980			
п	0.3337	1.5305	1.3430	1,3320	1.3003	1.5074	1,3/4	, 1,3003	1,3004	1,3943	1.3900	1,0030	1.0091	T.0143
	<b>4</b> 4		in P das	- Mor	-LL-	-1-440	1.450 R	•			T-4	1		

									Dej	grees of S	Superheat	_
130° 140°	150° 160	170°	180°	190°	200°	250°	300°	350°	400°	500°	600°	Press. lbs.
517.2 527.2	537.2 547.	2 557.2	567.2	577.2	587.2	637,2	687,2	737.2	787.2	887.2	987.2	t 213
2.63 2.67	2.70 2.74		2.80	2.83	2.87	3.03	3.19	3.34	3.50	3.80	4.10	V
1274.2 1279.3							1358.7 1.7031			1456.7 1.7819	1505.8	h
1,6234 1.6286	1.0337 1.036	1,0437	1.0700	1.0554	1.0363	1,0012	1.7031	1.7240	1,/441	1,/619	1.61/2	n
517.6 527.6			567.6	577.6	587.6	637.6		737.6	787.6		987.6	t 214
2.62 2.66	2,69 2.72 1284.5 1289		2.79	2.82	2.86	3,02	3.18	3.33	3.48	3.79	4.08	V
1274.3 1279.4 1.6230 1.6282							1358.9 1.7027			1456.8 1,7815		h n
518.0 528.0 2.61 2.64	538.0 548. 2.68 2.71		568.0 2.78	578.0 2.81	588.0 2.84	638.0 3.00		738.0	788.0		988.0	t 215
2.61 2.64 1274.5 1279.6					1309.7		3.16 1359 1	3.31 1383 6	3.47 1408.0	3.78 1457.0	4.06 1506 1	v h
1.6227 1.6279					1.6576	-				1.7812		n
518.4 528.4	538.4 548.	4 558.4	569 A	570 /	E00 1	620 1	600 1	720 1	700 1	000_1	000 4	+ 010
2.60 2.63	2.66 2.70		2.77	2,80	588.4 2.83	2.99	688.4 3.15	738.4 3.30	788.4 3.45	888 <b>-4</b> 3.76	4.04	t 216
1274.6 1279.	1284.8 1289	8 1294.8	1299.8	1304.8	1309.8				1408.2			h
1.6224 1.6275	1.6326 1.637	6 1.6426	1.6475	1.6523	1.6572	1.6802	1.7020	1.7229	1.7430	1.7808	1.8160	n
518.8 528.8	538.8 548.	8 558.8	568.8	578.8	588.8	638.8	688.8	738.8	788.8	888.8	988.8	t 217
2.59 2.62	2.65 2.69	2.72	2.75	2.78	2.82	2.98	3.14	3.29	3.44	3.74	4.03	₹
1274.7 1279.8					1309.9					1457.3		h
1.6220 1.6272	2 1,6322 1,637	2 1,0422 .	1.04/1	1.6519	1.6568	1.6/98	1.7016	1.7225	1.7426	1.7804	1.8156	n
519.1 529.1			569.1	579.1	589.1	639.1	689.1	739.1	789.1	889.1	989.1	t 218
2.58 2.61	2.64 2.68		2.74	2.77	2.80	2.96	3.12	3.27	3.42	3.72	4.01	V
1274.8 1279.9 1,6216 1,626					1310.1 1.6565				1408.5 1.7422			h n
1,0220	2,0010 1,000	.0 1.0 (1)	2,0 .00	1.0510	1.0000	2.077	1,,,,,,,,	2.7002	-,, ,	2,,,,,,,,	1.0201	
519.5 529.5			569.5	579.5	589.5	639.5	689.5	739.5	789.5	889.5	989.5	t 219
2.56 2.60 1274.9 1280.0	2.63 2.66 1285,1 1290		2.73 1300 2	2.76 1305.2	2. <b>79</b> 1310.2	2.95 1335 0	3.11 1359.6	3.26 1384 1	3.41 1408.6	3.71 1457 6	3.99 1506.7	V h
1,6213 1,626					1.6562				1.7419			n
r10.0 r00.0	F20.0 F40	0 5500	T(0.0	570 O	T00.0	C20.0	C00.0	720.0	700.0	000.0	000 0	+ 000
519.9 529.9 2.55 2.59	539.9 549. 2.62 2.65		569.9 2.72	579.9 2.75	589.9 2.78	639.9 2.94	3.10	739.9 3.25	3,40	889.9 3.69	3.98	t 220
1275.1 1280.3				-	1310.3				1408.8			'n
1,6209 1,626	1,6312 1,636	2 1.6412	1.6461	1.6509	1.6558	1.6787	1.7005	1.7214	1.7415	1.7792	1.8145	n
520,3 530,3	540,3 550.	3 560.3	570.3	580.3	590.3	640,3	690 3	740.3	790.3	890,3	990.3	t 221
2.54 2.58	2.61 2.64		2.71	2.74	2.77	2.93	3 08	3.23	3.38	3.68	3.96	v
1275.2 1280.					1310.4				1408.9			h
1.6206 1.625	3 1.6 <b>30</b> 9 1.635	9 1.6409	1.6458	1,6506	1.6555	1.6784	1.7002	1.7211	1.7412	1.7789	1.8141	n
520.7 530.7	540.7 550.	7 560.7	570.7	580.7	590.7	640.7	690,7	740.7	790.7	890,7	990 7	t 222
2.53 2.56	2.60 2.63		2.70	2.73	2.76	2.92	3.07	3.22	3.37	3.66	3.94	V
1275.3 1280.4 1,6203 1.625					1310.6 1.6551				1409.0 1.7408			h n
1.0203 1.023.	1,0300 1,033	0 1,0403 .	1,0434	1.0302	1.0331	1.0700	1,0000	1.7207	1.7700	1.7703	1.0137	11
521.1 531.1							691.1			891.1		t 223
2.52 2.55 1275.4 1280.5	2.59 2.62 1285.6 1290		2,68	2.71 1305.7	2,75 1310,7	2.91	3.06 1360.2	3.21 1384 7	3.35 1409.2	3,64	3.92	y h
1.6200 1.6252					1.6548				1.7405			n
E01 E					503 F	617 5	601.5	741 -	701 "	907.5	001 =	. 004
521.5 531.5 2.51 2.54	541.5 551. 2.58 2.61		571.5 2.67	581.5 2.70	591.5 2.74	2,89	691.5 3.04	741.5 3.19	791.5 3.34	891.5 3.63	991.5 3.91	t 224 V
1275.6 1280.7					1310.8						1507.4	h
1.6197 1.6248					1.6545						1.8130	

Table 3: Superheated Steam

1 40	16	o. Superne	ateu Steam									
Press.	1	Sat.	Degrees of Superhe		=00	000	700	***	000	4000	4400	4000
lbs.		Water Steam	10° 20°	30° 40°	50°	60°	70°	80°	90°	100°	110°	120°
225	t	391.9	401.9 411.9			451.9		471.9		491.9	501.9	511.9
	<b>V</b>	0.02 2.05	2.09 2.12	2.15 2.19		2.26	2.30	2.33	2.37	2.40		2,47
		365.5 1199.9	1207.2 1214.1				1244.1			1260.2		
•	n	0.5562 1.5361	1,5447 1,5525	1,3000 1,307	1 1,3/30	1.3800	1.5861	1,5920	1,39//	1.6033	1.0000	1.0141
226	t	392,2	402.2 412.2	422,2 432,2	442,2	452,2	462,2	472.2	482,2	492,2	502,2	512,2
	٧	0.02 2.04	2.08 2.11	2.14 2.18	2.22	2.25	2.29	2.32	2.36	2.39	2.42	2.46
	h	365.9 1200.0	1207.3 1214.2				1244.2			1260.3		
	n	0.5567 1.5358	1.5443 1.5522	1.5596 1:566	7 1.5734	1.5797	1.5858	1.5917	1.5974	1.6030	1.6085	1.6138
227	ŧ	392.6	402.6 412.6	422.6 432.0	442.6	452.6	462,6	472.6	482.6	492.6	502.6	512.6
	v	0.02 2.03	2.07 2.10	2.14 2.17		2,24	2.28	2.31	2.35	2.38		2.45
	h	366.3 1200.0	1207.3 1214.2		0 1232,9		1244.3			1260.4		
	n	0.5572 1.5355	1.5440 1.5519	1.5593 1.566	4 1.5731	1.5794	1.5855	1.5914	1.5971	1,6027	1.6082	1.6135
000		202.0	403.0 413.0	1020 1220	1/20	452 O	462 O	472 A	402 A	402 O	E02 0	E12 0
228	τ V	393. <b>Q</b> 0.02 2.02	2.06 2.09	2.13 2.16		2.23	463.0 2.27	2.30	2.34	493.0 2.37		2.44
	'n	366.7 1200.1	1207.4 1214.3				1244.4			1260.5		
		0.5577 1.5351	1.5436 1.5515				1.5852			1,6023		
-				100 1 100			150.4		100.1		<b></b>	
229		393.4	403.4 413.4				463.4				503,4	
	V h	0.02 2.01 367.1 1200.2	2.05 2.08 1207.5 1214.4	2.12 2.16		2,23	2.26 1244.6	2.29	2,33	2.36 1260.6		2.43
		0.5582 1.5348	1.5433 1.5512				1.5849	-		1,6020		
										_,		
230	t	393,8	403.8 413.8				463.8				503.8	
	V	0.02 2.00	2.04 2.07	2.11 2.15		2,22	2.25	2.28	2.32	2.35	2.38	2.42
	h n	367.5 1200.2 0,5586 1,5344	1207.6 1214.5 1,5430 1,5509				1244.7 1,5845			1260.7 1.6017		
		0,5500 1,5511	1,5 (50 1,550)	1.5501 1.500	3 1,3121	1.5701	1.5015	1.5501	1,5501	1,0017	1.0072	1.0123
231	t	394.1	404.1 414.1	424.1 434.	L 444.1	454.1	464.1	474.1	484.1	494.1	504.1	514.1
	V	0.02 1.99	2.03 2.06	2.10 2.14		2.21	2,24	2.28	2.31	2.34	2.38	2.41
	h	367.9 1200.3 0,5591 1,5341	1207.7 1214.6 1,5427 1,5506				1244.8 1.5842			1260.9 1,6014		-
	n	0,3391 1,3341	1,5427 1,5500	1.5561 1.500	2 1,3/10	1.3761	1,3042	1,3501	1.3930	1,0014	1,0003	1.0122
232	t	394.5	404.5 414.5	424.5 434.	5 444.5	454.5	464.5		484.5	494.5	504.5	514.5
	V	0.02 1.99	2.03 2.06	2.09 2.13		2.20	2.23	2.27	2.30	2.33	2.37	2,40
	h	368.3 1200.4	1207.8 1214.7				1244.9			1261.0		
	n	0.5596 1.5337	1.5423 1.5502	1,3377 1,304	0 1.5/15	1,5//6	1.5839	1.2090	1,3933	1.6011	1.0003	1.0110
233	t	394,9	404.9 414.9	424.9 434.	9 444.9	454.9	464.9	474.9	484.9	494.9	504.9	514.9
	٧	0.02 1.98	2.02 2.05	2.08 2.12	2.16	2.19	2.22	2.26	2.29	2.32	2.36	2.39
	h	368.7 1200.4	1207.8 1214.8				1245.0				1266.4	
	n	0.5601 1.5334	1.5420 1.5499	1.5574 1.564	5 1.5712	1.5775	1.5836	1.5895	1.5952	1.6008	1.6062	1.6115
234	t.	395.2	405.2 415.2	425.2 435.	2 445.2	455.2	465.2	475.2	485.2	495,2	505.2	515.2
	V	0.02 1.97	2.01 2.04	2.07 2.13		2.18	2.22	2.25	2.28	2,31	2.35	2.38
	h	369.0 1200.5	1207.9 1214.9				1245.1				1266.5	
	n	0.5605 1,5330	1.5416 1.5496	1.5571 1.56	2 1.5709	1.5772	1.5833	1.5891	1.5948	1.6004	1.6059	1.6112
235	ŧ.	395.6	405.6 415.6	425 6 435	6 445.6	455.6	465.6	475 6	485 6	4956	505.6	515.6
200	v	0.02 1.96	2.00 2.03	2.07 2.10				2.24			2.34	
	h	369.4 1200.6	1208.0 1215.0		.8 1233.8		1245.2			1261.4	1266.6	1271.7
	n	0,5610 1,5327	1.5413 1.5493	1,5568 1,563	39 1.5706	1.5769	1.5830	1,5888	1.5945	1.6001	1.6056	1,6109
236	t.	396,0	406.0 416.0	426.0 436	0 446.0	456 O	466.0	476 O	486 O	496.0	506.0	516.0
	7	0.02 1.96		2.06 2.0		2.16		2,23	2,26	2.30		2,36
	p	369.8 1200.6	1208.0 1215.0	1221.6 1227	.9 1233.	9 1239.7	1245.3	1250.8	1256.2	1261.5	1266.7	1271.8
	D.	0.5615 1.5323	1.5409 1.5489	1.5564 1.56	35 1.570	2 1.5765	1,5826	1.5885	1.5942	1.5998	1.6052	1.6105
23	7 t.	396,4	406.4 416.4	426.4 436	.4 446 4	456.4	466,4	476.4	486.4	496.4	506.4	516.4
	. A	0.02 1.95		2.05 2.0				2,22	2.25	2.29	2.32	2,35
	h	370.2 1200.7	1208,1 1215,1	1221.7 122	3.0 1234.	0 1239.	3 1245.4	1250.9	1256.3	1261.6	1266.8	1271.9
	n	0.5619 1.5319	1.5405 1.5485	1.5561 1.56	32 1.569	9 1.5762	2 1,5823	1.5882	1.5939	1,5994	1,6049	1.6102

(58)

								Deg	rees of S	uperheat	_
130° 140°	150° 160°	170° 180	° 190°	<b>200°</b>	250°	<b>300°</b>	350°	400°	500°	600°	Press. lbs.
521.9 531.9	541.9 551.9			591.9	641.9		741.9	791.9	891.9		t 225
2.50 2.53 1275.7 1280.8	2,57 2.60 1285,9 1290,9	2.63 2.6 1296.0 1301		2.72 1310.9	2.88 1335.7	3.03 1360.3	3.18 1384.9	3.33 1409.4	3.62 1458,4	3,89 1507.6	V h
1.6194 1.6245	1.6296 1.6346								1.7775		n
522.2 532.2	542,2 552,2	562,2 572	.2 582.2	592.2	642.2	692.2	742,2	792,2	892,2	992,2	t 226
2.49 2.52	2.56 2.59	2.62 2.6		2.71	2.87	3.02	3.17	3.31	3.60	3.88	<b>V</b>
1275,8 1280,9 1,6190 1,6242	1286.0 1291.0 1.6293 1.6343			1311.1 1,6538			-		1458.6 1.7771		h n
522.6 532.6	542.6 552.6	562,6 572	.6 582.6	502.6	642.6	692.6	710 6	792.6	892.6	002.6	t 227
2.48 2.51	2.55 2.58	2.61 2.6		2.70	2.86	3.01	3.15	3.30	3.59	3.86	V 441
1275.9 1281.0		1 1296.2 1303		1311.2					1458.7		h
1.6187 1.6239	1.6290 1.6340	U 1.0369 1.0 <del>4</del>	36 1,0460	1.6535	1,0/04	1.0904	1.7190	1.7391	1,7708	1.8119	n
523.0 533.0 2.47 2.50	543.0 553.0 2,54 2,57	563.0 573 2.60 2.6			643.0 2.84	693.0 2.99	743.0 3.14	793.0 3.29	893.0 3.57	993.0 3.84	t 228
2.47 2.50 1276.0 1281.1		2.60 2.6 2 1296,3 1301		2.69 1311,3					1458.8		v h
1,6184 1,6235		5 1.6386 1.64		1.6531					1.7764		n
523.4 533.4	543.4 553.4	563.4 573	4 583.4	593.4	643.4	693.4	743.4	793.4	893.4	993.4	t 229
2,46 2,49	2.52 2.56	2.59 2.6		2.68	2.83	2.98	3.13	3.28	3.56	3.83	<b>V</b>
1276.2 1281.3 1.6181 1.6233		3 1296,4 1301 3 1,6383 1,64		1311.4 1.6528					1459.0 1.7761		h n
				<b>503.0</b>	C 42 0	co2 o	742.0				
523,8 533,8 2,45 2,48	543.8 553.8 2.51 2.55	5 563.8 573 2.58 2.6		593.8 2.67	2,82	2.97	743.8 3.12	793.8 3.26	893.8 3.54	993.8 3.82	t 230
1276.3 1281.4	1286.5 1291.5	5 1296.5 1301	.5 1306.5	1311,6	1336,3	1361.0	1385.6	1410.1	1459.1	1508.3	h
1.6177 1.6229	1.6280 1.6330	0 1.6379 1.64	28 1.6476	1.6525	1.6753	1.6971	1.7179	1.7379	1.7757	1.8108	n
524.1 534.1	544.1 554.1		1 584.1	594.1					894.1		t 231
2.44 2.47 1276.4 1281.5	2.50 2.54 1286,6 1291,6	2.57 2.66 5 1206 7 1301		2.66 1311.7	2.81 1336.4	2.96	3.10	3.25 1410 3	3.53 1459.3	3.80	v h
1.6174 1.6226	1,6277 1.6327			1.6522					1.7754		n
524.5 534.5	544.5 554.5	564.5 574.	5 584,5	594.5	644.5	694.5	744.5	794.5	894,5	994.5	t 232
2.43 2.46	2.49 2.52	2.56 2.59	2.62	2.65	2.80	2.95	3.09	3.23	3.51	3.78	y
1276.5 1281.6 1.6170 1.6222	1286.7 1291.7 1,6273 1,6323			1311.8 1,6518					1459.4 1.7749		h n
524.9 534.9 2.42 2.45	544.9 554.9 2.48 2.51	564.9 574 2.55 2.5		594.9 2.64	644.9 2,79	694.9 2.93	744.9 3.08	794.9 3.22	894.9 3.50	994.9 3.77	t 233 v
1276.6 1281.7	1286.8 1291.9	1296,9 1301	.9 1306.9	1311.9	1336.7	1361.4	1386.0	1410.6	1459.6	1508.8	h
1.6167 1.6219	1.6270 1.6320	0 1.6369 1.64	18 1,6466	1.6515	1.6744	1.6961	1.7169	1.7369	1.7746	1.8098	n
525.2 535.2	545.2 555.2				645.2	695.2	745.2	795.2	895.2		t 234
2.41 2.44	2.47 2.50	2.54 2.5		2.63	2.78	2.92	3,07	3.21	3.49	3.76	V b
1276.8 1281.9 1.6164 1.6216	1287.0 1292.0 1.6267 1.6317			1312.0 1.6512					1459.7 1.7742	1.8094	h n
525.6 535.6	545 6 555 6	565.6 575	6 585 6	595.6	645.6	695.6	745.6	795.6	895.6	995.6	t 235
2.40 2.43	2.46 2.50			2.62	2.77	2.91	3.06	3.20	3.47	3.74	v
1276.9 1282.0	1287.1 1292.1 1,6264 1,6314			1312.2 1.6509					1459.8 1.7739	1509,0	h n
1.6161 1.6213											
526.0 536.0 2.39 2.42	546.0 556.0 2.45 2.49	566.0 576 2.52 2.53		596.0 2.61	646.0 2.76	696.0 2.90	746.0 3.04	796.0 3.18	896.0 3.46	996.0 3.73	t 236 v
1277.0 1282.1	1287.2 1292.2	2 1297.2 1302	.2 1307.2	1312.3 1	337.1	1361,8	1386.4	1411.0	1460.0	1509.2	h
1.6157 1.6209	1.6260 1.6310	1.6359 1.64	08 1.6456	1.6505 1	1.6733	1.6951	1.7158	1.7358	1,7735	1.8087	n .
526.4 536.4		566.4 576.		596.4					896.4		t 237
2.38 2.41 1277.1 1282.2	2.44 2.48 1287.3 1292.3	2.51 2.54		2.60 1312.4 1	2.75 337.2	2.89 1361.9	3.03 1386 5	3.17 1411.1	3,44 1460 1	3.71 1509 3	v h
1.6154 1.6206	1.6256 1.6306			1.6501				1.7354			
		•		(59)							

(59)

Table 3: Superheated Steam

_		٠.	Degrees	of Superh	eat									
Press. Ibs.	Water	Sat. Steam	10°	20°	30°	40°	50°	60°	70°	80°	90°	100°	110°	120°
238 t v h	396 0.02 370.6	1.94	406.7 1.98	416.7 2.01 1215.2	2.04	436.7 2.08	446.7 2.11	2.15	466.7 2.18 1245,5	476.7 2.21	2.24	496.7 2.28 1261.7	506.7 2.31	516.7 2.34
n	0.5624			1.5482					1.5820			1.5991		
239 t	397			417.1		437.1			467.1				507.1	
v h	0.02 371.0	1.93 1200.8	1.97 1208.3	2,00 1215,3	2.03 1221.9	2,07 1228.2	2.10 1234.2	2.14 1240.0	2.17 1245.7	2.20 1251.2	2,24 1256.5	2,27 1261,8	2.30 1267.1	2,33 1272.3
n	0.5629			1.5479					1.5817			1.5988		
<b>24</b> 0 t	39			417.4					467.4				507.4	
v h	0.02 371.4	1.92	1.96	1.99 1215.4	2.02	2.06	2.09	2.13	2.16 1245.8	2.20	2,23	2.26	2.29 1267.1	2,32
n	0.5633			1,5476					1.5814			1.5985		
241 t	39	. <b>€</b> 7.8	407.8	417.8	427 8	437.8	447.8	457 8	467.8	477 R	487 8	497.8	507.8	517.8
V V	0.02	1.92	1.95	1.98	2.02	2.05	2.09	2.12	2.16	2.19	2.22	2.25	2.28	2.31
h	371.8			1215.5					1245.9				1267.2	
n	0.5638	1.5306	1.5393	1.5473	1.5549	1.5620	1,5687	1.5750	1.5811	1.5870	1.5927	1.5982	1.6037	1.6090
242 t	398			418.2		438.2	448.2		468.2		488.2	498.2	508.2	
V h	0.02 372.2	1.91	1.94	1.97 1215.6	2.01	2.04	2.08	2.11	2.15 1246.0	2.18	2.21	2.24	2.27 1267.4	2.30
h n	0.5642			1.5470					1.5808				1.6034	
243 t	0.02	3.5 1.90	408.5 1.93	418.5 1.96	428.5 2.00	438,5 2.04	448.5 2.07	458.5 2.10	468.5 2.14	478,5 2.17	488,5 2,20	498,5 2,23	508.5 2.26	518.5 2.30
h	372.6			1215.7					1246.1				1267.5	
n	0.5647			1.5467					1.5805				1,6031	
244 t	398	8.9	408.9	418.9	428.9	438.9	448.9	458.9	468.9	478.9	488.9	498.9	508.9	518.9
v	0.02	1.89	1.93	1.96	1.99	2.03	2.06	2.10	2.13	2.16	2.19	2.22	2.26	2.29
h	372.9			1215.8					1246.2				1267.6	
n	0.5651	1.5297	1.5384	1.5464	1.5540	1.5611	1.56/8	1.5741	1.5802	1.5861	1.5918	1.5973	1.6028	1.6081
245 t	39	9.3	409.3	419.3	429.3	439.3	449.3	459.3	469.3	479.3	489.3	499.3	509.3	519.3
٧ 1	0.02	1.89 °	1.92	1.95 1215.9	1.99	2.02	2.05	2.09	2.12 1246.3	2.15	2.18	2.22	2.25	2.28
h n	373,3 0,5655			1,5461					1.5799					1272.8 1.6078
_														
246 t	0.02	9.6 1.88	409.6 1.91	419.6 1.94	1.98	439.6 2.01	449.6 2.05	459.6 2.08	469,6 2,11	479.6 2.14	489.6 2.18	499.6 2.21	509.6 2,24	2,27
'n		1201.2		1215.9					1246,4	-				1272.9
n	0.5659	1.5289	1.5377	1.5458	1,5533	1.5605	1.5672	1.5735	1.5796	1.5855	1.5912	1.5967	1.6022	1.6075
247 t	40	0.0	410.0	420.0	430.0	440.0	450.0	460.0	470.0	480.0	490.0	500.0	510.0	520.0
٧	0.02	1.87	1.90	1.93	1.97	2.00	2.04	2.07	2.10	2.14	2.17	2.20	2.23	2.26
h n		1201.3 1.5286		1216.0 1.5455					1246.6 1.5793		1257.4			1273,0 1,6072
	0.5005	1.5200	1,3374	1.5755	1,3350	1.5002	1,5005	1.5152	1,57,50	1,5052	1,5505			
248 t		0.3		420.3					470.3				510.3	
V	0.02	1.86		1.93	1.96	2.00 1229.1	2.03			2.13	2.16 1257.5		2.22	2.25
h n		1201.4 1.5283				1.5599					1.5906			1273,2 1.6069
040 ·														
249 t	0.02	0.7 1.86		420.7 1.92		440.7 1.99	450.7 2.03		470.7 2.09		490.7 2,15	500.7 2.18	510.7 2.21	
ň		1201.4									1257.6			
	0.5672					1,5596					1.5903			1.6065
	<b>.</b>		in Tr do-	m.a.m.	.hh.	1	L 450 ea	,			T., 4.,	.1	_	

t=temperature in F. degs. To Fahr. absolute = to + 459.60. Internal energy y=sp, vol. in on. ft. per lb. J=777.5 ft. lbs. per B. t. u. [log=2.89 071]. J=777.5 ft. lbs. per B. t. u. [log=2.89 071]. J=777.5 ft. lbs. per B. t. u. [log=2.89 071].  $J=1.286\times10^{-3}$  B. t. u. per ft. lb. [3.10 929]. Values for saturated steam are given in Tables 1 and 2.

, •										Deg	rees of S	uperheat	
130° 14	0° 150	)° 160°	170°	180°	190°	200°	250°	300°	350°	400°	500°	600°	Press. Ibs.
	6.7 546		566.7	576.7	586 7	596.7	646.7	696,7	746.7	796.7	896.7		t 238
2.37 2. 1277.2 128	40 2.4 82.3 128	4     2,47 7,4  1292,4	2,50 1297.5	2,53 1302.5	2.56 1307.5	2,59 1312,5	2,74 1337.3	2.88 1362 0	3.02 1386 6	3.16 1411.2	3,44 1460 2	3.70 1509 5	V h
1.6151 1.6		253 1,6302				1.6498					1.7728		n
527.1 53	7.1 547	7.1 557.1	567.1	577.1	587.1	597.1	647.1	697.1	747.1	797 1	897.1	997 1	t 239
2.36 2.	40 2.4	3 2.46	2.49	2.52	2.55	2.58	2.73	2.87	3.01	3.15	3.42	3.68	V
1277.4 128 1.6148 1.6		7.5 1292,6 250 1,6299				1312.6 1.6495				1411.4 1.7348			h n
	NI.												
527.4 53 2.35 2.	37.4 547 39 2.4	7.4 557.4 12 2.45	567.4 2.48	577.4 2.51	587.4 2.54	597.4 2.57	647.4 2.71	697.4 2.85	747,4 2,99	797.4 3.13	897.4 3.40	997,4 3.67	t 240
1277.5 128		7.6 1292.7				1312.8					1460.5		h
1.6145 1.6	196 1.62	246 1,6296	1.6346	1.6395	1.6443	1.6492	1.6720	1.6937	1.7144	1.7344	1.7721	1.8072	n
527.8 53	7.8 547	7.8 557.8	567.8	577.8	587.8	597.8	647.8	697.8	747.8	797.8	897.8	997.8	t 241
	38 2.4		2.47	2.50	2.53	2.56	2.70	2.84	2.98	3.12	3.39	3.65	<b>V</b>
1277,6 128 1.6142 1.6		7,8 1292,8 243 1,6293				1312.9 1,6489				1411.6 1.7341		1.8069	h n
528,2 53 2,34 2,	88.2 548 .37 2.4		568.2 2.46	578,2 2,49	588.2 2.52	598.2 2.55	648.2 2.69	698.2 2.83	748.2 2.97	798.2 3.11	898,2 3,38	998,2 3.64	t 242 v
1277.7 128		7.9 1292.9				1313.0					1460.8		h
1,6139 1,6	5190 1.62	240 1,6290	1,6340	1.6389	1.6437	1.6486	1.6714	1.6931	1.7138	1.7338	1.7715	1.8066	n
528,5 53	88.5 548	3.5 558.5	568.5		588.5	598.5	648.5	698.5		798.5	898.5	998.5	t 243
	.36 2.3	39 2,42 8.0 1293.0	2,45	2.48	2.51	2.54 1313.1	2.68	2.82	2.96	3.10	3.36 1460.9	3.63	V.
1277.8 128 1.6136 1.6		0.0 1293.0 237 1.6287				1,6483				1,7335			h n
E00 0 E2	000 546	ם דרפה	#60 N	E70 O	588.9	£00 0	6400	600.0	7400	7000	000 0	000 0	+ 044
528.9 53 2.32 2	38.9 548 .35 2.3		568.9 2.44	578.9 2.47	2.50	2.53	2.67	698.9 2.81	2.95	798.9 3.09	898.9 3.35	3.61	t 244 V
1277.9 12	83.0 128	8.1 1293.1				1313.2			-	1412.0	1461.0	1510.3	h
1.6133 1.6	5184 1.62	234 1,6284	1,6334	1,6383	1,6431	1.6479	1,6707	1.6924	1.7132	1,7331	1,7708	1.8059	n .
529.3 53			569.3					699.3			899,3		t 245
2,31 2, 1278.0 12	,34 2.3 83 1 128	37 2.40 8,2 1293,2	2.43	2.46	2.49 1308 3	2.52	2,66 1338 2	2.80 1362.9	2.94 1387 5	3.08 1412 1	3.34 1461,2	3.60 1510 5	V h
1,6130 1,6		231 1.628							1.7129		1.7705		n
529,6 53	30 6 540	9.6 559.6	569.6	579 6	589.6	599.6	649,6	699 6	749.6	799,6	899.6	999 6	t 246
2.30 2.	.33 2.3		2.42	2.45	2.48	2.51	2.65	2.79	2.93	3.06	3,32	3.58	V 220
1278.1 12		8.3 1293.3				1313.4					1461.3		h
1.6127 1.6	01/8 1.0	228 1.6278	3 1,0327	1,0370	1,0424	1.6473	1.0701	1.0917	1./125	1.7324	1.7701	1.8051	n
530.0 54		0.0 560.0						700.0				1000.0	
2,29 2, 1278.2 12	.32 2 83.3 128	35 2,38 8,4 1293,4	2,41   1298 5	2,44 1303.6	2,47 1308.6	2,50 1313.6	2,64 1338.4	2,78 1363.2	2,92 1387,8	3.05 1412.3	3.31 1461 4	3,57 1510.7	V h
1.6124 1.6		225 1.627							1.7122			1.8048	
530.3 54	10.3 550	0.3 560.3	570.3	580.3	590.3	600.3	650.3		750.3	800.3	900,3	1000.3	t 248
	.31 2.	34 2.37	2.40	2.43	2.46	2.49	2.63	2.77	2.91	3.04	3.30	3.56	V
1278,4 12 1,6121 1,6		88.6 1293.6 222 1.627							1387.9 1.7119			1510. <del>9</del> 1.8045	h n
		•											
530.7 54 2.27 2		0,7 560,7 33 2,36		580.7 2.42	590.7 2.45	600.7 2.48	650.7 2.62	700,7 2,76	750.7 2.90	800.7 3.03		1000.7 3.54	t 249 v
1278.5 12		8.7 1293.1				1313.8	1338.7	1363,4	1388.0			1511,0	
1.6117 1.6	5168 1.6	219 1.626	1.6318	1.6367	1.6415	1.6463	1.6691	1.6908	1.7115			1.8041	

Table 3: Superheated Steam

Press.	Sat.	Degrees of Superheat				
ibs.	Water Steam	10° 20° 30°	40° 50°	60° 70°	80° 90°	100° 110° 120°
250 t v h n	401.0 0.02 1.85 375.2 1201.5 0.5676 1.5276		1.98 2.02 229.3 1235.4	461.0 471.0 2.05 2.08 1241.3 1246.9 1.5723 1.5784		501.0 511.0 521.0 2.17 2.21 2.24 1263.0 1268.2 1273.4 1.5956 1.6010 1.6062
255 t v h n	402,8 0,02 1,81 377,1 1201,8 0,5698 1,5260		1.94 1.98 229.8 1235.9	462.8 472.8 2.01 2.04 1241.8 1247.4 1.5709 1.5770	2.07 2.11 1252.9 1258.3	502.8 512.8 522.8 2.14 2.17 2.20 1263.6 1268.8 1273.9 1.5942 1.5996 1.6048
260 t v h n	404.5 0.02 1.78 378.9 1202.1 0.5719 1.5244	414.5 424.5 434.5 4 1.81 1.84 1.87 1 1209.9 1217.1 1223.9 12 1.5334 1.5416 1.5492 1.	1.91 1.94 230.3 1236.4	464.5 474.5 1.97 2.00 1242.3 1247.9 1.5695 1.5756	2.04 2.07 1253.4 1258.8	504.5 514.5 524.5 2.10 2.13 2.16 1264.1 1269.3 1274.5 1.5926 1.5980 1.6033
265 t v h n	406.2 0.02 1.75 380.7 1202.3 0.5739 1.5229		1.88 1.91 230.8 1236.9	466.2 476.2 1.94 1.97 1242.8 1248.4 1.5682 1.5742		506.2 516.2 526.2 2.06 2.09 2.12 1264.6 1269.8 1275.0 1.5914 1.5968 1.6020
270 t v h n	407.9 0.02 1.72 382.5 1202.6 0.5760 1.5214	417.9 427.9 437.9 4 1.75 1.78 1.81 1 1210.6 1217.9 1224.8 12 1.5305 1.5388 1.5466 1.	1.84 1.87 231.3 1237,4	467.9 477.9 1.90 1.93 1243.3 1248.9 1.5669 1.5729	1.96 1.99 1254.4 <b>1</b> 259.8	507.9 517.9 527.9 2.02 2.05 2.08 1265.2 1270.4 1275.6 1.5900 1.5954 1.6006
275 t v h n	409,6 0.02 1.69 384,3 1202,9 0.5780 1.5199	419.6 429.6 439.6 4 1.72 1.75 1.78 1 1210.9 1218.3 1225.3 1 1.5291 1.5375 1.5452 1	1.81 1.84 231.8 1237.9	469.6 479.6 1.87 1.90 1243.8 1249.4 1.5656 1.5716	1.93 1.96 1254.9 1260.3	509.6 519.6 529.6 1.99 2.02 2.04 1265.7 1271.0 1276.1 1.5886 1.5940 1.5993
280 t v h n	411,2 0,02 1,66 386,0 1203,1 0,5800 1,5185	421.2 431.2 441.2 4 1.69 1.72 1.75 1 1211.3 1218.7 1225.7 1 1.5278 1.5362 1.5440 1	1.78 1.81 232.2 1238.4	471.2 481.2 1.84 1.87 1244.3 1250.0 1.5643 1.5704	1.90 1.93 1255.5 1260.9	511.2 521.2 531.2 1.95 1.98 2.01 1266.2 1271.4 1276.6 1.5873 1.5927 1.5980
285 t v h n	412.8 0.02 1.63 387.7 1205.4 0.5820 1.5171		1.75 1.78 232.7 1238.9	472,8 482,8 1.81 1.84 1244,8 1250,5 1,5631 1,5692	1.87 1.90 1256.0 1261.4	512.8 522.8 532.8 1.92 1.95 1.98 1266.7 1271.9 1277.1 1.5861 1.5915 1.5968
290 t v h n	414.4 0.02 1.60 389.4 1203.6 0.5840 1.5156	424.4 434.4 444.4 4 1.63 1.66 1.69 1211.9 1219.4 1226.6 1 1.5251 1.5336 1.5414 1	1.72 1.75 233,2 1239,3	474.4 484.4 1.78 1.81 1245.2 1250.9 1.5618 1.5679	1.83 1.86 1256.4 1261.8	514.4 524.4 534.4 1.89 1.92 1.94 1267.1 1272.4 1277.6 1.5848 1.5902 1.5954
295 t v h n	415.9 0.02 1.57 391.1 1203.8 0.5859 1.5142	425.9 435.9 445.9 4 1.60 1.63 1.66 1212.3 1219.8 1227.0 1 1.5237 1.5323 1.5402 1	1.69 1.72 233.6 1239.8	475.9 485.9 1.75 1.78 1245.7 1251.4 1.5606 1.5667	1.80 1.83 1256.9 1262.3	515.9 525.9 535.9 1.86 1.89 1.91 1267.7 1272.9 1278. 1.5835 1.5889 1.5942
300 t v h n	417.5 0.02 1.55 392,7 1204.1 0.5878 1.5129	427.5 437.5 447.5 4 1.58 1.60 1.63 1212.6 1220.2 1227.4 1 1.5224 1.5310 1.5389 1	1.66 1.69 234.1 1240.3	477.5 487.5 1.72 1.75 1246.2 1251.9 1.5594 1.5655	1.78 1.80 1257.4 1262.8	517.5 527.5 537.5 1.83 1.86 1.88 1268.2 1273.4 1278.6 1.5824 1.5878 1.5930
305 t v h n	419.0 0.02 1.53 394.4 1204.3 0.5897 1.5115	429.0 439.0 449.0 4 1.56 1.58 1.61 1212.9 1220.6 1227.8 1 1.5212 1.5299 1.5378 1	1.64 1.67 .234.5 1240.7	479.0 489.0 1.69 1.72 1246.6 1252.3 1.5583 1.5644	1.75 1.78 1257.9 1263.3	519.0 529.0 539.0 1.80 1.83 1.85 1268.6 1273.8 1279.0 1.5812 1.5866 1.5918
310 t v h n		430.5 440.5 450.5 1.53 1.55 1.58 1213.2 1221.0 1228.2 1 1.5200 1.5987 1.5366	1,61 1.64 1234,9 1241,1	480.5 490.5 1.67 1.69 1247.0 1252.7 1.5572 1.5632	1.72 1.75 1258.3 1263.8	520,5 530,5 540,5 1,78 1,81 1,83 1269,1 1274,3 1279,5 1,5801 1,5855 1,5907

(62)

								Deg	rees of S	uperheat	_
130° 140°	150° 160°	170° 180°	190°	<b>200°</b>	<b>250°</b>	300°	350°	400°	500°	600°	Press. lbs.
531.0 541.0	551.0 561.0				651.0	701.0	751.0	801.0	901.0	1001.0	t 250
2.27 2.30 1278.6 1283.7	2,33 2,36 1288 8 1293 8	2,38 2,41 3 1298,9 1303		2.47 1313 q	2.61 1338,8	2.75	2.88	3.02 1412.7	3,28	3.53	v h
1.6114 1.6165		5 1.6315 1.636			1.6688			1.7311			n
F20 9 F40 9	552.8 562.8	E70 0 E00	P E00 9	602.0	650 O	ס כמל	750 0	000.0	000 0	1000 0	+ OFF
532.8 542.8 2.23 2.26	2,28 2,31	572.8 582. 2.34 2.37		2.43	652.8 2.56	702.8 2.70	752.8 2.83	2.96	902.8 3.22	3.47	t 255 v
1279.1 1284.2		1299,4 1304			1339.3				1462.5		h
1.6100 1.6151	1.6201 1.6251	l 1.6300 1.634	9 1.6397	1,6445	1.6673	1.6890	1.7096	1.7296	1.7671	1.8021	n
534.5 544.5	554.5 564.5				654.5	704.5	754.5		904.5		t 260
2.19 2.22 1279.6 1284.8	2.24 2.2 <b>7</b> 1289 9 1294 9	2.30 2.33 1300.0 1305.		2,39 1315 1	2.52 1340.0	2.65 1364 7	2.78 1389 4	2.91 1414 0	3.16 1463.2	3.41 1512.5	v h
1.6085 1.6136		5 1.6285 1.633			1.6658	-	-		1.7655		n
536.2 546.2	556,2 566,2	576.2 586.3	2 596.2	606.2	656.2	706.2	756.2	806.2	906.2	1006.2	t 265
2.15 2.18	2.20 2.23	2.26 2.29	2.32	2.35	2.48	2.61	2.74	2.86	3.11	3.35	v
1280.2 1285.3 1.6072 1.6123		5 1300.5 1305. 2 1.6271 1.632			1340.5 1.6644		1390,0		1463.8 1.7640		h n
1.0072 1.0123	1.01/3 1.0242	1.02/1 1.032	0 1,0306	1,0410	1,0044	1.0000	1.7000	1.7203	1,7040	1.7990	ш
537.9 547.9	557.9 567.9			607.9		707.9			907.9		t 270
2.11 2.14 1280,7 1285,8	2,16 2,19 1290,9 1296,0	2,22 2,25 1301,0 1306,		2,30 1316.2	2.43 1341.1	2.56 1365.9	2,69 1390.6	2,81 1415.2	3.05 1464.5	3,29 1513.8	V h
1.6058 1.6109		1.6258 1.630			1.6630			1.7251	1.7625	1.7975	n
539.6 549.6	559.6 569.6	579.6 589.	5 599.6	609.6	659.6	709.6	759.6	809.6	909.6	1009.6	t 275
2.07 2.10	2.13 2.16	2.18 2.21	2.24	2.26	2.39	2.52	2.64	2.77	3.00	3.24	V
1281,2 1286,3 1,6044 1,6095		5 1301.6 1306. 5 1.6244 1.629			1341.6 1.6616				1465.1 1.7611		h n
									- "		
541,2 551,2 2,04 2,07	561.2 571.2 2.09 2.12	581,2 591,3 2,15 2,17		611.2 $2.22$	661,2 2,35	711,2 2,48	761,2 2,60	811,2 2,72	911,2 2,95	1011.2 3.19	t 280 v
1281.7 1286.8		1302.1 1307.			1342.2				1465.7		h
1.6032 1.6083	1.6133 1.6182	2 1.6231 1.627	9 1.6327	1.6375	1.6603	1.6818	1.7024	1.7223	1.7597	1.7945	n
542.8 552.8	562,8 572.8	582.8 592.	8 602.8	612.8	662,8	712.8	762.8	812.8	912.8	1012,8	t 285
2.00 2.03	2.06 2.09	2.11 2.14		2.19	2.31	2,44	2.56		2.90	3.13	<b>V</b>
1282.2 1287.4 1,6020 1,6071		5 1302.6 1307. 0 1.6219 1.626					1392,3 1,7011		1466.3 1.7583	1.7931	h n
<b>5</b> 44.4 554.4	564.4 574.4	584.4 594.	4 604.4	614.4	664.4	714.4	764.4	21 <i>1 1</i>	914.4	1014.4	t 290
1.97 2.00	2.02 2.05	2.08 2.10		2.15	2.28	2,40	2.52	2,63	2.86	3.08	V 250
1282.7 1287.9		1 1303.1 1308					1392.8			1516.4	h
1.6006 1.6057	1.6107 1.6156	5 1.6205 1.625	3 1,6301	1.6349	1,6576	1,6791	1.6996	1,7195	1,7568	1.7916	n
545.9 555.9	565.9 575.9		9 605.9			715.9	765.9			1015.9	t 295
1.94 1.97 1283.2 1288.4	1.99 2.02	2.04 2.07 5 1303.6 1308		2.12 1318.8	2.24 1343 8	2,36 1368 7	2.48 1393.4	2.59 1418 1	2,82 1467 5	3.04 1517.0	v h
1.5994 1.6045		4 1.6192 1.624					1,6983			1,7902	
547.5 557.5	567.5 577.5	587.5 597.	5 607.5	617.5	667.5	717.5	767.5	817.5	917.5	1017.5	t. 300
1.91 1.94	1.96 1.99	2.01 2.04	2.06	2.09	2.21	2.33	2.44	2.55	2.77	2.99	<b>v</b>
1283.7 1288.9 1.5981 1.6032		1 1304,1 1309 1 1,6180 1,622					1393.9 1.6970			1517.6 1,7889	h
								1.7100	1./371	1,7007	
549.0 559.0 1.88 1.01		) 589.0 599.		619.0 2.05	669.0 2.17					1019.0	
1,88 1.91 1284,2 1289,3	1.93 1.96 1294,4 1299.	1.98 2.03 5 1304.6 1309				2,29 1369,7	2,41 1394,5	2,52 1419,2	2,73 1468.6	2.95 1518.2	♥ h
1.5970 1.6021		9 1,6168 1,621					1.6958			1.7876	n
550.5 560.5	570.5 580.5	590.5 600.	5 610.5	620.5	670.5	720.5	770.5	820.5	920.5	1020.5	t 310
1.85 1.88	1.90 1.93	1.95 1.98	3 2.00	2.02	2.14	2.26	2.37	2.48	2.69	2.90	<b>V</b>
1284.7 1289.8 1.5958 1.6009		0 1305,1 1310 8 1,6156 <b>1</b> 1,620		1.6299	1,8526	1.6741	1395,0 1,6946			1518.8 1.7863	
2.000				(53)			_,,	+ · ·	_,		_

(63)

Table 3: Superheated Steam

	-	Dagrees	of Superho	at									
Press. Ibs.	Sa Water Ste	t eac	20°	30°	40°	50°	60°	70°	80°	90°	100°	110°	120°
320 t v h n	423.4 0.02 1,4 399.1 120 0.5951 1.56	16 1,49 4.9 1213,8	443,4 1,51 1221,7 1,5264	1.53 1229.0		1.59 1242,0		493.4 1.64 1253.7 1.5610	1.67 1259.3		523.4 1.72 1270.0 1.5778		1.77 1280.4
330 t v h n	426,3 0,02 1, 402,2 120 0,5986 1,5	41 1.44 5.3 1214.4	446.3 1.46 1222.5 1.5242	1,49 1229,8	1.52 1236.6		1.57 1248.9	496.3 1.60 1254.6 1.5588	1.62 1260,2	1.65 1265.6	1.67 1270.9	536,3 1,70 1276,2 1,5809	1.72 1281.4
340 t v h n	429,1 0,02 1, 405,3 120 0,6020 1,5	37 1.40 5.7 1215.0	449.1 1.42 1223.2 1.5220	1.44 1230.6	1.47 1237.4	1.50 1243.8	1,53 1249,8	499.1 1.55 1255.5 1.5568	1.57 1261.1	1.60 1266.5	1.63 1271.8	539.1 1.65 1277.1 1.5789	1.67 1282.3
350 t v h n	431.9 0.02 1. 408.3 120 0.6053 1.5	33 1.36 6.1 1215.6	451.9 1.38 1223.9 1.5199	1.40 1231.4	1.43 1238.2		1.48 1250.6	501.9 1.51 1256.3 1.5547	1.54 1261.9	1.56 1267.3		541.9 1.61 1278.0 1.5768	1.63 1283.2
360 t v h n	434.6 0.02 1. 411.2 120 0.6085 1.4	30 1.32 6.4 1216.1	454.6 1.34 1224.5 1.5179	1.37 1232.2	1.40 1239.0	1.42 1245.4	1.44 1251.4	504.6 1.46 1257.2 1.5528	1.48 1262.8	1.52 1268.2	1.54 1273.6	544.6 1.56 1278.9 1.5749	1,59 1284.1
370 t v h n	437.2 0.02 1. 414.0 120 0.6116 1.4		457.2 1.31 1225.2 1.5160				1.41 1252.3	507.2 1.43 1258.0 1.5510	1.46 1263.6		1.50 1274.4	547.2 1.52 1279.7 1.5730	1.55 1284.9
380 t v h n	439.8 0.02 1. 416.8 120 0.6147 1.4	23 1.25 )7,1 1217,2	459.8 1.27 1225.9 1.5142	1.30 1233.6	1.32 1240.6	1.35 1247.0	1.37 1253.1	509.8 1.40 1258.9 1.5493	1.42 1264.5	1.44 1269.9	1.47 1275.3	549.8 1.49 1280.6 1.5713	1.51 1285.8
390 t v h n	442.3 0.02 1 419.5 120 0.6178 1.4	20 1.22 07.4 1217.8	462.3 1.24 1226.6 1.5124	1,26 1234,4	1.29 1241.4		1.34 1253.9	512,3 1,36 1259,7 1,5476	1,38 1265.3		1.43 1276.1	552.3 1.45 1281.4 1.5695	
400 t v h n	422.2 120	.17 1.19 )7.7 1218.3	464.7 1.21 1227.2 1.5107	1.23 1235.1			1.31 1254.7	514.7 1.33 1260.5 1.5459				554.7 1.42 1282.2 1.5678	1.44 1287.5
450 t v h n	0.02 1 435. 1	466.5 .04 1.06 209. 1221 .479 1.492	1.08 1231.		1.12 1246.	506.5 1.14 1252, 1.526	1.16 1258.		536.5 1.21 1270. 1.544	1.23	556.5 1.25 1281. 1.554	566.5 1.27 1286. 1.560	576.5 1.29 1291, 1.565
500 t V h n		0.93 0.95 10. 1223.	0.97 1233. 1.497	0.99 1242.	1.01 1249.	1.03 1256.	1.05 1262.	537.2 1.07 1268. 1.532	1.09 1274.	1279.	1.13 1285.	577.2 1.15 1290. 1.554	1295.
550 t v h n	0.02 0 458. 1	.85 0.87 210. 1225.	497.2 0.89 1236. 1.491	0.91 1245.	517.2 0.93 1253. 1.509	0.94 1260.	0.96 1266.		1.00 1277.	1.01 1283.		587.2 1.05 1293. 1.549	1.07 1299.
600 t v h n	0.02 0 %69. 1	.78 0.79 211. 1228.	506.4 0.81 1240. 1.486	0.83 1250.	0.85 12 <u>5</u> 7.	0.86 1264.	0.88 1270.	556.4 0.90 1276. 1.522	0.92 1282. 1.528	0.93 1288.	0.95 1293.	596.4 0.97 1298, 1,543	0.98 1304.

											Dec	rrann of G	iuperheat	
130°	140°	150°	160°	170°	180°	190°	<b>200°</b>	250°	300°	350°	400°	500°	600°	Press. lbs.
553.4	563.4	573.4	583.4	593.4		613.4	623.4	673.4	723.4	773.4		923.4		t 320
1.80 1285.6	1.82	1.85 1295 9	1.87 1301.0	1.90	1.92	1,94 1316.2	1.96 1321.3	2.08	2.19	2.30	2.41	2.61 1470.3	2,81	v h
1,5935			1.6085						1.6717				1.7898	n
rrc 2	566.3	576.3	586.3	506 2	606,3	616.3	626.3	676 2	726,3	775.3	906.2	006.2	1006.2	+ 000
556.3 1.75	1.77	1.80	1.82	1.84	1.86	1.89	1.91	2.02	2.13	2,24	826.3 2,34	926,3 2,54	2,74	t 330 V
1286.5	1291.7	1296,8	1301.9	1307.0	1312.1	1317.2	1322,2	1347.3	1372.3	1397.1		1471.5		'n
1.5913	1.5964	1.6014	1.6063	1.6111	1.6159	1.6206	1.6253	1.6480	1.6694	1.6899	1.7097	1.7467	1.7814	n
559.1	569.1	579.1	589.1	599.1	609.1	619.1	629,1	679.1	729.1	779,1	829.1	929.1	1029,1	t 340
1.70	1.72	1.75	1.77	1.79	1.81	1.84	1.86	1.97	2.08	2.18	2.28	2.47	2.67	<b>y</b>
1287.4 1.5892			1302.9 1.6041						1373.3 1.6671	-		1472.6	1,7790	h n
561.9 1.65	571.9 1.68	581.9 1.70	591.9 1.72	601.9 1.74	611.9 1.77	621.9 1.79	631.9 1.81	681.9 1.92	731.9 2.02	781.9 2.12	831.9 2.22	931.9 2.41		t 350
1288.3			1303.8				1324,1			-		1473.7	2,60 1523.5	v h
1,5871	1.5921	1.5971	1.6020	1.6068	1.6116	1.6163			1.6650		1.7052			n
564 6	574.6	584.6	594 6	604 6	614.6	624 6	634.6	684 6	734.6	784.6	834 6	934.6	1034 6	t 360
1.61	1,63	1.65	1.68	1.70	1.72	1.74	1.76	1.87	1.97	2.07	2.16	2.35	2.53	₹ 500
	1294.4		1304.7				1325.0			-			1524.6	h
1,5852	1.5902	1.5951	1.6000	1,0048	1,0090	1.6143	1.6190	1,0415	1.0029	1.0833	1.7031	1.7400	1.7745	n
567.2	577.2	587.2		607.2		627.2	637.2		737.2	787.2		937.2	1037.2	t 370
1.57	1.59 1295.3	1.61	1.64 1305.6	1.66	1.68	1.70	1.72	1.82	1.92 1376.2	2,02	2.11	2.30	2,47	V
	1.5883		1,5982						1.6610				1525.7 1.7725	h n
569.8 1.53	579.8 1.55	589.8 1.58	599.8 1.60	609,8 1,62	619.8 1.64	629,8 1,66	639,8 1,68	689.8 1.78	739.8 1.88	789.8 1.97	839,8 2.06	939.8 2.24	1039.8 2.41	t 380 v
	1296.1		1306.5							1402.1			1526.8	h 🖟
1,5816	1.5866	1.5915	1.5964	1,6012	1,6059	1.6106	1.6153	1.6378	1,6591	1.6795	1.6992	1.7361	1,7705	n
572,3	582,3	592.3	602.3	612.3	622.3	632.3	642.3	692.3	742.3	792.3	842.3	942.3	1042.3	t 390
1.50	1.52	1.54	1.56	1.58	1.60	1.62	1.64	1.74	1.83	1.92	2.01	2.19	2.35	<b>V</b>
	1297.0 1.5848		1307.3 1,5946							1403.1 1,6777			1527.9 1.7685	h n
								694.7		794. <b>7</b>				
574.7 1.46	584.7 1.48	594.7 1.50	1.52	1.54	1.56	634.7 1.58	1.60	1.70	1.79	1.88	1.97	2.14	1044.7 2.30	t 400
	1297.9	1303.0	1308.2	1313.3	1318.4	1323.5				1404.1	1429.0	1478.9	1528.9	h
1.5781	1.5821	1.5880	1.5929	1.5977	1.6024	1.6070	1.6117	1.6342	1.6554	1.6758	1.6955	1.7323	1.7666	n
586.5	596.5	606.5	616.5	626.5	636.5	646.5	656.5	706.5	756.5	806.5	856.5	956.5	1056.5	t 450
1.31	1.33	1.35	1.36	1.38	1.40	1.42	1.44	1.53	1.61	1.69	1.77	1.93	2.07	,
1297.	1302. 1.575	1307. 1.580	1312. 1.585	1317. 1.589	1323. 1.594	1328. 1.599	1333. 1.603	1358. 1.626	1383. 1 647	1409. 1.667	1434. 1 687	1484. 1.723	1534.	h n
1.570	1.373						1.000							
597.2			627.2	637.2	647.2 1.27	657.2 1.29	667.2 1.31	717.2 1.39	767.2 1.47	817.2 1.54	867.2 1.62	967.2 1.76	1067.2 1.89	t 500 V
1.19 1300.	1.20 1306.	1.22 1311.	1.24 1316.	1.26 1321.	1327.	1332.	1337.			1413.			1539.	h
1.564		1.574		1.584		1.594	1.598	1.620	1.641	1.661	1.680		1.751	n
607.2	617.2	627.2	637.2	647.2	657.2	667.2	677.2	727.2	777.2	827.2	877.2	977.2	1077.2	t 550
1.08	1.10	1.11	1.13	1.15	1.16	1.18	1.20	1.27	1.34	1.42	1.49	1.62	1.74	V
1304.	1309.	1315.	1320.	1325.	1330.	1336.		1366.		1417.	1442.		1543.	h
1.559	1.564	1.569	1.574	1.579	1.583	1.588	1.592	1.015	1.636	1.656	1.675		1.746	n
	626.4	636.4	646.4	656.4	666.4	676.4				836.4	886.4		1086.4	
1.00	1.02	1.03	1.05	1.06	1.08	1.09	1.11 1346.	1.18	1.25 1397.	1.31	1.38	1.50 1499.	1.62	V h
	1314. 1.558	1319.	1325. 1.568	1.573	1,577	1.582			1.629				1.739	
200		*****	2.500				(65)	•		~ *-	•			4

Table 4. Increase in Total Heat and in Entropy for Steam Superheated above 600°

Press.		From 6	00° Fah	r. superho	eat to												ress.
lbs.		700°	<b>8</b> 00°	900°	1000°	1100°	1200°	1300°	1400°	1500°	1600°	1700°	1800°	1900°	<b>2000°</b>	•	lbs.
1	Δħ Δn	47. 0.039		143. 0.110	192. 0.142			343. 0.230				554. 0.333			726. 0.404	Δh Δn	1
15		48. 0.036	-		194. 0.133			347. 0.216				564. 0.316			741. 0.387	Δh Δn	15
25	Δh Δn	48. 0.036	96. 0.069		195. 0.131			349. 0.214				566. 0.313			745. 0.384	Δh Δn	<b>2</b> 5
50		48. 0.035		146. 0.099	196. 0.128			351. 0.210				571. 0.308			752. 0.378		50
75		48. 0.035			197. 0.127			353. 0.208				574. 0.306			756. 0.376	Δh Δn	75
100		48. 0.034						354. 0.207				577. 0.304			759. 0.374		100
<b>15</b> 0			99. 0.065	149. 0.095				356. 0.204			-	582. 0.301			765. 0.370	Δh Δn	150
<b>20</b> 0	∆h ∆n	49. 0.033		150. 0.094				358. 0.203				586. 0.300		708. 0.346	771. 0.369	Δh Δn	200
<b>25</b> 0		50. 0.033		151. 0.094				360. 0.202		-		589. 0.298			776. 0.368		260
<b>30</b> 0	Δh Δn			151. 0.093				362. 0.201				591. 0.297		715. 0.344	780. 0.367		<b>30</b> 0
400	Δh Δn			152. 0.092				365. 0.199	421. 0.223			597. 0.295		722. 0.341	787. 0.364		400
500				154. 0.092				368. 0.198	424. 0.222			602. 0,294		728. 0,340	794. 0,363	Δh Δn	<b>5</b> 00
600	Δh Δn			155. 0.091				371. 0.197	427. 0.222					734. 0.340	800. 0.363		600

This table gives, either directly or by interpolation, the excess of the total heat or entropy at any given pressure and superheat above that at the same pressure and 600° superheat. The actual total heat or entropy is obtained by adding this increment to the corresponding value in the 600° column of Table 3.

# Table 5. Boiling Points For Thermometer Calibrations

# English Units

Press.	Temp.	Press.	Temp.	Press.	Temp.	Press.	Temp.	Press.	Temp.
in, of Hg.	Fahr.	in. of Hg.	Fahr.	in. of Hg.	Fahr.		Fahr.	in. of Hg	. Fahr.
22.0	196.95	25.0	203.10	28.0	208.67	29.5	211.27	31.0	213.80
.2	197.37	.2	203.48	.1	208.85	.6	211.44	.1	213.96
.4	197.79	.4	203.86	.2	209.03	.7	211.62	.2	214.13
.6	198.21	.6	204.24	.3	209.20	.8	211.79	.3	214.29
.8	198.63	.8	204.62	.4	209.37	.9	211.96	.4	214.46
23.0	199.05	26.0	205.00	28.5	209.55	30.0	212.13	31.5	214.62•
.2	199.47	.2	205.38	.6	209.73	.1	212.30	.6	214.79
.4	199.89	.4	205.75	.7	209.91	.2	212.47	.7	214.95
.6	200.31	.6	206.12	.8	210.08	.3	212.64	.8	215.11
.8	200.72	.8	206.49	.9	210.25	.4	212.81	.9	215.27
24.0 .2 .4 .6 .8	201.13 201.54 201.94 202.33 202.72	27.0 .2 .4 .6 .8	206.86 207.23 207.59 207.95 208.31	29.0 .1 .2 .3 .4	210.42 210.59 210.76 210.93 211.10	30.5 .6 .7 .8	212.97 213.13 213.30 213.46 213.63	32.0 .2 .4 .6 .8	215.43 215.75 216.08 216.40 216.72

# Metric Units

11100		, III CO							
Press.	Temp. Cent.	Press. mm. of Hg.	Temp. Cent.	Press. mm. of Hg	Temp. . Cent.	Press. mm. of H	Temp. Ig. Cent.	Press. mm. of H	Temp. g. Gent.
FF0	01.10	<b>700</b>	05 51			FFO	00.00		100 55
<b>55</b> 0	91.19	700	97.71	725	98.68	750	99.63	775	100.55
60	91.67	1	97.75	<u>6</u>	98.72	1	99.66	<u>6</u>	100.59
70	92.14	2 3	97.79	7	98.76	2	99.70	7	100.62
80	92.60	3	97.83	8	98.80	3	99.74	8	100.66
90	93.06	4	97.87	9	98.84	4	99.78	9	100.69
600	93.51	705	97.91	730	98.87	755	99.81	780	100.73
05	93.73	6	97.95	1	98.91	6	99.85	1	100.77
10	93.96	7	97.99	2	98.95	7	99.89	2	100.80
15	94.18	8	98.03	3	98.99	8	99.92	3	100.84
20	94.40	9	98.07	4	99.03	9	99.96	4	100.87
625	94.61	710	98.10	735	99.06	760	100.00	785	100.91
30	94.83	1	98.14	6	99.10	1	100.04	6	100.95
35	95.04	<b>2</b>	98.18	7	99.14	2	100.07	7	100.98
40	95.25	2 3	98.22	8	99.18	3	100.11	8	101.02
45	95.47	4	98.26	9	99.21	4	100.15	9	101.05
650	95.68	715	98.30	<b>74</b> 0	99,25	765	100.18	790	101.09
55	95.89	6	98.34	1	99.29	6	100.22	1	101.12
60	96.10	7	98.38	2	99.33	7	100.26	$ar{2}$	101.16
65	96.30	ė	98.41	3	99.36	Ř	100.29	3	101.20
70	96.51	9	98.45	4	99.40	9	100.33	4	101.23
675	96,71	720	98,49	745	99,44	770	100.37	795	101.27
80	96.91	1	98.53	6	99.48		100.40	6	101.30
85	97.12	2	98.57	7	99.51	$\hat{2}$	100.44	7	101.34
90	97.32	2 3	98.61	ė	99.55	3	100.48	8	101.37
95	97.52	4	98.65	9	99.59	4	100.51	ğ	101.41
30				_				_	

Table 6. Thermal Properties of Water At Saturation Pressure

Temp. Fahr.	Press. ibs.	Specific V ft.3/lb.	olume cm.³/gr.	Den: lbs./ft. ^a	sity grs./cm. ^s	144 Apv' B. t. u.	Specific Heat	Temp. Fahr.
<b>20°</b>	0.06	0.01603	1.00101	62.37	0.99899	0.000	1.0168	<b>20°</b>
`30	0.08	0.01602	1.00022	62.42	0.99978	0.000	1.0098	30
<b>4</b> 0	0.12	0.01602	1.00000	62.43	1.00000	0.000	1.0045	<b>4</b> 0
<b>50°</b>	0.18	0.01602	1.00027	62.42	0.99973	0.001	1.0012	<b>50°</b>
€0	0.26	0.01603	1.00096	62.37	0.99904	0.001	0.9990	60
70	0.36	0.01605	1.00201	62.30	0.99799	0.001	0.9977	70
80	0.51	0.01607	1.00338	62.22	0.99663	0.002	0.9970	80
90	0.70	0.01610	1.00504	62.11	0.99498	0.002	0.9967	90
<b>100°</b>	0.95	0.01613	1.00698	62.00	0.99307	0.003	0.9967	100°
110	1.27	0.01616	1.00915	61.86	0.99093	0.004	0.9970	110
120	1.69	0.01620	1.01157	61.71	0.98857	0.005	0.9974	<b>120</b>
130	2.22	0.01625	1.01420	61.55	0.98600	0.007	0.9979	130
140	2.89	0.01629	1.01705	61.38	0.98324	0.009	0.9986	<b>14</b> 0
<b>150</b> °	3.71	0.01634	1.02011	61.20	0.98029	0.011	0.9994	<b>150°</b>
160	4.74	0.01639	1.02337	61.00	0.97717	0.014	1.0002	160
170	5.99	0.01645	1.02682	60.80	0.97388	0.018	1.0010	170
180	7.51	0.01651	1.03047	60.58	0.97043	0.023	1.0019	180
190	9.34	0.01657	1.03431	60.36	0.96683	0.029	1.0029	190
<b>200</b> °	11.52	0.01663	1.03835	60.12	0.96307	0.036	1.0039	<b>200°</b>
210	14.13	0.01670	1.04256	59.88	0.95917	0.044	1.0050	210
<b>220</b>	17.19	0.01677	1.0469	59.63	0.9552	0.054	1.007*	220
230	20.77	0.01684	1.0515	59.37	0.9510	0.065	1.009*	230
<b>24</b> 0	24.97	0.01692	1.0562	59.11	0.9468	0.078	1.012*	240
<b>250°</b>	29.82	0.01700	1.0611	58.83	0.9425	0.094	1.015*	<b>250°</b>
260	35.42	0.01708	1.0662	58.55	0.9379	0.112	1.018	260
270	41.85	0.01716	1.0715	58.26	0.9332	0.133	1.021	270
280	49.18	0.01725	1.0771	57.96	0.9284	0.157	1.023	280
290	57.55	0.01735	1.0830	57.65	0.9234	0.185	1.026	290
<b>300</b> °	67.00	0.01744	1.0890	57.33	0.9183	0.217	1.029	<b>300</b> °
310	77.67	0.01754	1.0953	57.00	0.9130	0.254	1.032	310
<b>320</b>	89.63	0.01765	1.1019	56.66	0.9075	0.295	1.035	<b>320</b>
<b>33</b> 0	103.0	0.01776	1.1088	56.30	0.9019	0.340	1.038	330
340	118.0	0.01788	1.1160	55.94	0.8961	0.391	1.041	340

^{*} Values below  $220^{\circ}$  from mean ourve described on page 89. Values above  $250^{\circ}$  from Dieterioi's formula. The four values indicated are selected so as to give a smooth transition.

Table 6: Water

Temp. Fahr.	Press. !bs.	Specific ft.³/lb.	Volume cm.3/gr.	Der lbs./ft.³	nsity grs./cm.*	144 Apv' B. t. u.	Specific Heat	Temp. Fahr.
350°	135.	0.01800	1.1235	55.57	0.8902	0.448	1.045	350°
360	153.	0.01812	1.1313	55.18	0.8840	0.513	1.043	360
370	173.	0.01812	1.1313	-	°0.8776	0.515	1.048	370
380	196.	0.01823	1.1390	54.36	0.8778			
390						0.666	1.056	380
390	220.	0.01854	1.1573	53.94	0.8642	0.756	1.060	390
<b>400°</b>	247.	0.0187	1.167	53.5	0.857	0.86	1.064	<b>400°</b>
<b>41</b> 0	276.	0.0189	1.177	53.0	0.850	0.96	1.068	410
420	308.	0.0190	1.187	52.6	0.843	1.09	1.072	<b>\$</b> 20
<b>4</b> 30	343.	0.0192	1.197	52.2	0.835	1.22	1.077	430
<b>44</b> 0	381.	0.0194	1.208	51.7	0.828	1.36	1.082	<b>44</b> 0
<b>450°</b>	422.	0.0195	1.220	51.2	0.820	1.52	1.086	450°
<b>460</b>	466.	0.0197	1.232	50 <b>.7</b>	0.812	1.70	1.091	460
<b>47</b> 0	514.	0.0199	1.244	50.2	0.804	1.89	1.096	470
<b>480</b>	565.	0.0201	1.256	49.7	0.796	2.10	1.101	480
490	620.	0.0203	1.269	49.2	0.787	2.33	1.106	490
<b>E00</b> 0	670	0.0206	1.002	40 7	0.770	0.59	1 110	5000
<b>500°</b>	679.	0.0206	1.283	48.7	0.779	2.58	1.112	500°
<b>510</b>	743.	0.0208	1.297	48.1	0.771	2.86	1.117	510
<b>520</b>	810.	0.0210	1.312	47.6	0.763	3.15	1.123	520
<b>53</b> 0	883.	0.0213	1.329	47.0	0.755	3.48	1.128	530
<b>54</b> 0	960.	0.0216	1.35	46.3	0.74	3.8	1.134	<b>54</b> 0
<b>550°</b>	1043.	0.0219	1.37	45.6	0.73	4.2	1.140	550°
<b>56</b> 0	1130.	0.0223	1.39	44.9	0.71	4.7	1.146	560
<b>57</b> 0	1224.	0.0227	1.42	44.1	0.70	5.2	1.152	570
<b>580</b>	1323.	0.0231	1.44	43.3	0.69	5.7	1.158	580
<b>59</b> 0	1428.	0.0235	1.46	42.6	0.68	6.2	1.165	<b>590</b>
600°	1540.	0.024	1.49	41.8	0.67	6.8	1.172	600°
610	1658.	0.024*	1.52*	41.0*	0.66*	7.5*		610
620	1783.	0.025	1.55	40.2	0.65	8.2		620
630	1916.	0.025	1.59	39.4	0.64	9.0		630
<b>64</b> 0	2056.	0.026	1.63	38.5	0.62	9.9		640
<b>J2</b> 0								
650°	2204.	0.027	1.67	37.5	0.60	10.9		650°
660	2361.	0.027	1.72	36.4	0.58	12.0		660
670	2526.	0.028	1.78	35.2	0.56	13.3		670
690	2883.	0.031	1.95	32.1	0.51	16.6		690
706.1	3200.	0.050	3.11	20.1	0.32	29.5		706.1

^{*}The specific volumes and densities below 600° were taken from the 3rd (1905) edition of Landolt and Börnstein's "Physikalische Tabellen." These and the following values were obtained by the method described on page 103.

# **Conversion Tables**

# Temperature

#### TABLE OF EQUIVALENT TEMPERATURES

Cent.	Fahr.	Cent.	Fahr.	Cent.	Fahr.	Cent.	Fahr.	Cent.	Fahr.	Cent.	Fahr.	Cent.	Fahr.
25° -	– 13°	50°	122°	125°	257°	200°	392°	275°	527°	350°	662°	425°	797°
-20 -	- 4	55	131	130	266	205	401	280	536	355	671	430	806
15 -	+ 5	60	140	135	275	210	410	285	545	360	680	435	815
-10	14	65	149	140	284	215	419	290	554	365	689	440	824
<b></b> ·5	23	70	158	145	293	220	428	295	563	370	698	<b>4</b> 45	833
0°	32°	75°	167°	150°	302°	225°	437°	300°	572°	375°	70 <b>7</b> °	450°	842°
5	41	80	176	155	311	230	446	305	581	380	716	455	851
10	50	85	185	160	320	235	455	310	590	385	725	460	860
15	59	90	194	165	329	240	464	315	599	390	734	465	869
20	68	95	203	170	338	245	473	320	608	395	743	470	878
25°	77°	100%	212°	175°	347°	250°	482°	325°	617°	400°	752°	475°	887°
30	86	105	221	180	356	255	491	330	626	405	761	480	896
35	95	110	230	185	365	260	500	335	635	410	770	485	905
40	104	115	239	190	374	265	509	340	644	415	779	490	914
45	113	120	248	195	383	270	518	345	653	420	788	495	923

#### TABLE OF VALUES FOR INTERPOLATION IN ABOVE

$1^{\circ}C = 1.8^{\circ}F$	$4^{\circ}C = 7.2^{\circ}F$	$7^{\circ}$ C = 12.6°F	$1^{\circ}$ F = $0.55^{\circ}$ C	$4^{\circ}F = 2.22^{\circ}C$	$7^{\circ}F = 3.88^{\circ}C$
2 = 3.6	5 = 9.0	8 = 14.4	2 = 1.11	5 = 2.77	8 = 4.44
3 = 5.4	6 = 10.8	9 = 16.2	3 = 1.66	6 = 3.33	9 = 5.00

All decimals are exact.

All decimals are repeating decimals.

# Length area and volume

1 cm.	□ 0.3937*	inches,	$\log = 1.59517$	1 inch	-	2.54001 cm.,	$\log = 0.40483$
1 meter	= 3.28083	ft.,	0.51 598	1 ft.	===	0.30480 m.,	I.48 402
1 sq. cm.	<b>□</b> 0.15500	sq. in.,	1.19 033	1 sq. in.	===	6.4516 sq. cm.,	0.80 967
1 sq. meter	<b>= 10.7639</b>	sq. ft.,	1.03 197	1 sq. ft.	===	0.092903 sq. m.,	2.96 803
1 cu. cm.	= 0.061028	3 cu. in.,	2.78 550	1 cu. in.	522	16.387 cu. cm.,	1.21 450
1 cu. meter	= 35.3145 _c	cu. ft.,	1.54 795	1 cu. ft.	-	0.028317 cu. m.,	2.45 205
1 liter	— 0.26417	gals.,	<b>I.4</b> 2 188	1 gal.	==	3.7854 liters,	0.57 812

# Mass and density

1 kg.	===	2-204622	lbs., l	og = 0.34 333	1 lb.	==	0.453592	kg.,	log=	I-65 667
1 gr./cm.3,	***	62-4283	lbs./ft.3,	1.79 538	1 lb./ft. ³	=	0.016018	gr./cm.³,		2.20 462
Density of Hg.	253	0.491170	lbs./in.3 (at 32°)	), I.69 123	Den. of Hg.	-	13.59545	gr./cm.3 (at 0° C	J.),	1.83 839
g (standard)		32-1740	ft. sec2,	1.50 750	g (standard)	) == 9	80-665*	cm. sec2,		2.99 152

# Pressure

1 kg./cm. ² =	= 14·228	lbs./in.2, log	=1.15 300	1 lb./in.2	- 0.07030	7 kg./cm.²,	log == 2.84 700
("metric =	= 28.958	in. of Hg.,	1.46 177		= 2.0360	in. of Hg.,	0.30 877
atmosphere")=	= 735·5 <b>4</b>	mm. of Hg.,	2.86 661		= 51.718	mm. of Hg.,	1.71 360
-	= 32.84	ft. of H2O(at 60°),	1.51 640	•	= 27.71	ins. of H ₂ O (at	60°), 1.44 258
	<b>=</b> 0.9678	atmos,	I.98 579		= 0.06804	4 atmos,	2.83 279
	- 0.980665	megabars,†	I.99 152		- 0.06894	7 megabars,†	2.83 852
1000 mm. of Hg.	= 1.3158	atmos, log	= 0.11 919	1 atmo	= 780.*	mm. of Hg.,	$\log = 2.88081$
=	= 39.37*	in. of Hg.,	1.59 517		= 29.921	in. of Hg.,	1-47 598
-	= 44.65	ft. of H ₂ O (at 60°),	1.64.979		= 33.93	ft. of H2O (at 6	0°), 1.53 061
*	= 19.837	lbs./in.2,	1.28 640		= 14.696	lbs/in.2,	1.16 721
	- 1.3595	kg./cm.³	0.13 339		= 1.0333	kg./cm.2,	0.01 421
-	= 1.3333	megabars,†	0.12 491		= 1.0133	megabars,†	0.00 573

^{*} Exact value, by definition.

## Conversion Table

# Energy

		# moundals loss-		250		ft manuadal		0.1001.\/.10-9	ft lba	low 5 40	050
1 ft. lb. =		ft. poundals, log=			_	-		3.1081×10-2	16. 108.,	$\log = 2.49$	
2002	0.13826	kg. meters,	I.14		_	kg. meter	122	7.2330	. ,		982
200	1.3558	Joules,†	0.13		_	Joule †	==	0.73756	•		780
=		mean B. t. u.,	3.10			mean B. t. u.			,		071
66	0.3241	gr. calories,	I.51			gr. calorie	11111	3.086	•		982
atta	7.145 ×10-4		4.85		_	lb. °C. cal.	====	1.3996×10³	., '		598
-	1.3381×10 ⁻²		2.12		_	liter atmo		74.735	,		353
100		cu. ft. atmos,	4.67		-	cu. ft. atmo		2·1163×10 ³	•		557
ema .		H. P. hours,	7.70			•	==	1.98* ×10 ⁶	,,		667
First		chev. vap. hrs.,	7.70		_	chev. vap. hr.		1.9529×10 ⁶	,,		068
<del></del>	8.7662×10-4	watt nours	4.57	590	1	watt hour	===	$2.6552 \times 10^{3}$	•	8.42	410
1 Joulet =	0.10197	kg. meters, log=	T.nn	848	1	kg. meter	==	9-80665*	Joules.t	$\log = 0.99$	152
1.000001	0.73756	ft. lbs.,	1.86		_	ft. lb.	10021	1.3558	"	0.13	
	23.730	ft. poundals,	1.37			ft. poundal		4.2140×10-2			470
*=		mean B. t. u.,	4.97			mean B. t. u.		1.0542×10 ³	"		291
100	0.2390	gr. calories,	I.37		-		===	4.1834	""		153
=	5.270 ×10-4		4.72		_	lb. °C. cal.	===	1 8976×10 ³	"		818
200	9.8690×10-3		3.99		-	liter atmo	22	$1.0133 \times 10^{2}$	" '		573
-		cu. ft. atmos,	4.54			cu. ft. atmo		2.8693×10 ³	, "		777
===		H. P. hours,	7.57		-			2.6845×10 ⁶	" .		887
-		chev. vap. hrs.,	7.57		_	chev. vap. hr.		2.6478×10 ⁶	"		288
144	2.7778×10-4		4.44			watt hour		3.6* ×10 ³	"		630
	2.7710/120	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,		5,0	•				•		
1 B. t. u. =	$2.5200 \times 10^{2}$	gr. calories, log=	2.40	139	1	gr. calorie	1000	3.9683×10-3	B. t. u.,	$\log = \overline{3}.59$	861
-	0.5556	lb. °C. cal.,	1.74	473	1	lb. °C. cal.	222	1.8*	",	0.25	527
===	777.5+	ft. lbs.,	2.89	071	1	ft. lb.	===	1.2861×10-8	",	3.10	929
-	2.5016×104	ft. poundals,	4.39	822	1	ft. poundal	===	3.997 ×10.5	٠٠,	5.60	178
=	$1.0750 \times 10^{2}$	kg. meters,	2.03	139	1	kg. meter	===	9.302 ×10-3	٠٠,	3.96	861
-	$1.0542 \times 10^{3}$	Joules,†	3.02	291	1	Joule†	=	9.486 ×10-4	",	4.97	709
	10.404	liter atmos,	1.01	719	1	liter atmo	===	9.612 ×10-2		2.98	281
==	0.3674	cu. ft. atmos,	<b>1</b> .56	514	1	cu. ft. atmo	E5:	2.722	" .	0.43	486
=	3.927 ×10-4	H. P. hours,	4.59	405	1	H. P. hour	:102	$2.547 \times 10^{3}$	٠٠,	8.40	595
===	3.981 ×10-4	chev. vap. hrs.,	4.60	003	1	chev. vap. hr	.=	$2.512 \times 10^{3}$	";	8.39	996
=	0.2928	watt hours.	I.46	661	1	watt hour		3.415	"•	0.53	889
		D. 1. 1	¥			mean B. t. u.	_	2.5200×10 ²	er sol	log=2.40	100
1 gr. cal. =		mean B.t.u., log=			_		==		gr. car.,	_	
				333		lb. °C. cal.		4.5359×10 ²	"		667
=	3.086	ft. lbs.,		932	_	ft. lb.	==	0.3241	., ,		068
gazzari gazzari	99.27	ft. poundals,		682		ft. poundal	230	1.0073×10-2	'		318
==	0.4266	kg. meters,		000	_	kg. meter	2000	2.8441	'		000
2005		Joules,†		153		Joule†		0.2390	"		848
نظير				579	_	liter atmo		24.22	.,		421
		cu. ft. atmos,		374	_	cu. ft. atmo H. P. hour	1200	6.859 ×10 ² 6.417 ×10 ⁵	'		626
-		H. P. hours,		265	_	chev. vap. hr		6.329 ×10 ⁵	"		785 135
-		chev. vap. hrs.,		864	_	watt hour	. =	8.605 × 10 ²	*		478
****	1.1621×10-3	watt nours,	3.08	522	1	watt Hour	_	0.000 × 10-	•	BO	#/0

#### Power

1 horse power (H. P.) is 550 ft. lbs. per second. 1 watt is 1 Joule per second or 10⁷ ergs per second. 1 kilowatt (K. W.) is 1000 watts. 1 cheval-vapeur, or pferdekraft, or "continental horse power," is 75 kg. meters per second. 1 poncelet is 100 kg. meters per second.

```
1 K. W. = 1.3410
                                      \log = 0.12743
                                                         1 H. P.
                                                                            0.7457
                                                                                       K. W.,
                                                                                                  log=1.87 257
                          H. P.,
                          chev. vap.,
                                           0.13 343
                                                                            1.0139
                                                                                       chev. vap.,
                                                                                                       0.00 599
             1.3597
                                           0.00 849
                                                                            0.7604
                                                                                       poncelets,
                                                                                                       I.88 105
         = 1.0197
                          poncelets,
                                           2.86 780
                                                                        = 550.*
                                                                                       ft. lbs./sec.,
                                                                                                       2.74 036
         =737.56
                          ft. lbs./sec.,
                          kg. m./sec.,
                                           2.00 848
                                                                        76.040
                                                                                       kg. m./sec.,
                                                                                                       1.88 104
         =101.97
                                                                        = 0.7074
                                           I.97 709
                                                                                       B. t. u./sec.,
                                                                                                       I.84 965
                          B. t. u./sec.,
              .9486
                                                                     = 178.25
                                                                                       gr. cal./sec.,
                                                                                                       2.25 104
         = 239.04
                          gr. cals./sec.,
                                           2.37 848
```

^{*} Exact value, by definition.

^{† 1} Joule = 107 ergs.

# Logarithms to the Base 10

	0	1	2 *	3	4	5	6	7	8	9	10
1.00	0.0000	0004	0009	0013	0017	0022	0026	0030	0035	0039	0043
1.01	0043	0048	0052	0056	0060	0065	0069	0073	0077	0082	0086
1.02	0086	0090	0095	0099	0103	0107	0111	0116	0120	0124	0128
1.03 1.04	0128 0170	0133 0175	0137 0179	0141 0183	0145 0187	0149 019 <b>1</b>	0154 0195	0158 0199	0162 0204	0166 0208	0170 0212
1.05 1.06	0212 0253	0216 025 <b>7</b>	0220 0261	0224 0265	0228 0269	023 <b>3</b> 02 <b>73</b>	0237 0278	0241 0282	0245 0286	0249 0290	0253 0294
1.07	0294	0298	0302	0306	0310	0314	0318	0322	0326	0330	0334
1.08	0334	0338	0342	0346	0350	0354	0358	0362	0366	0370	0374
1.09	0374	0378	0382	0386	0390	0394	0398	0402	0406	0410	0414
1.10	0.0414	0418	0422	0426	0430	0434	0438	0441	0445	0449	045 <b>3</b>
1.11	^e 0453	0457	0461	0465	0469	0473	0477	0481	0484	0488	0492
1.12	0492	0496	0500	0504	0508	0512	0515	0519		0527	0531
1.13	0531	0535	0538	0542	0546	0550	0554	0558	0561	0565	0569
1.14	0569	0573	0577	0580	0584	0588	0592	0596	0599	0603	060 <b>7</b>
1.15	0607	0611	0615	0618	0622	0626	0630	0633	0637	0641	0645
1.16 1.17	0645	0648	0652	0656	0660	0663	0667	0671	0674	0678	0682
1.17	0682 0719	0686 0722	0689 0726	0693 0730	0697 0734	0700 0737	0704 0741	0708 0745	0711 0748	0715 0752	0719 075 <b>5</b>
1.19	0719	0759	0763	0766	0770	0737	0777	0743	0785	0732	0792
1.20	0.0792	0795	0799	0803	0806	0810	0813	0817	0821	0824	0828
1.21	0.0792	0831	0835	0839	0842	0846	0849	0853	0856	0860	0864
1.22	0864	0867	0871	0874	0878	0881	0885	0888	0892	0896	0899
1.23	0899	0903	0906	0910	0913	0917	0920	0924	0927	0931	0934
1.24	0934	0938	0941	0945	0948	0952	0955	0959	0962	0966	096 <b>9</b>
1.25	0969	0973	0976	0980	0983	0986	0990	0993	0997	1000	1004
1.26	1004	1007	1011	1014	1017	1021	1024	1028	1031	1035	1038
1.27	1038	1041	1045	1048	1052	1055	1059	1062	1065	1069	1072
1.28 1.29	1072	1075	1079 1113	1082 1116	1086	1089	1092	1096	1099	1103	1106
1.30	1106	1109			1119	1123	1126	1129	1133	1136	1139
1.31	0.1139 1173	1143 1176	1146 1179	1149 1183	1153 1186	1156 1189	1159 1193	1163 1196	1166	1169 1202	11 <b>73</b> 120 <b>6</b>
1.32	1206	1209	1212	1216	1219	1222	1225	1229	1199 1232	1235	1239
1.33	1239	1242	1245	1248	1252	1255	1258	1261	1265	1268	1271
1.34	1271	1274	1278	1281	1284	1287	1290	1294	1297	1300	1303
1.35	1303	1307	1310	1313	1316	1319	1323	1326	1329	1332	1335
1.36	1335	1339	1342	1345	1348	1351	1355	1358	1361	1364	1367
1.37	1367	1370	1374	1377		1383	1386	1389	1392	1396	1399
1.38	1399	1402	1405	1408	1411	1414	1418	1421	1424	1427	1430
1.39	1430	1433	1436	1440	1443	1446	1449	1452	1455	1458	1461
1.40	0.1461	1464	1467		1474	1477	1480	1483	1486	1489	1492
1.41 1.42	1492 1523	1495	1498		1504 1535	1508 1538	1511 1541				1523
1.42	1553	1556			1565	1569	1572	1575	1578		1553 1584
1.44	1584	1587				1599	1602	1605	1608	1611	1614
1.45	1614	1617				1629	1632	1635	1638	1641	1644
1.46	1644	1647			1655	1658	1661	1664			1673
1.47	1673	1676			1685	1688	1691	1694			1703
1.48	1703	1706	1708			1717	1720	1723	1726	1729	1732
1.49	1732	1735	1738	1741		1746 2)	1749	1752	1755	1758	1761
					1/	4 I					

(72)

	0	1.	2	3	4	5	6	7	8	9	10
1.50	0.1761	1764	1767	1770	1772	1775	1778	1781	1784	1787	1790
1.51	1790	1793	1796	1798	1801	1804	1807	1810	1813	1816	1818
1.52	1818	1821	1824	1827	1830	1833	1836	1838	1841	1844	1847
1.53	1847	1850	1853	1855	1858	1861	1864	1867	1870	1872	1875
1.54	1875	1878	1881	1884	1886	1889	1892	1895	1898	1901	1903
1.55	1903	1906	1909	1912	1915	1917	1920	1923	1926	1928	1931
1.56	1931	1934	1937	1940	1942	1945	1948	1951	1953	1956	1959
1.57	1959	1962	1965	1967	1970	1973	1976	1978	1981	1984	1987
1.58 1.59	1987 2014	1989 2017	1992 2019	1995 2022	1998 2025	2000 2028	2003 2030	2006 2033	2009 2036	2011 2038	2014 2041
1.60	0.2041										
1.61	2068	2044 2071	204 <b>7</b> 2074	2049 2076	2052 2079	2055 2082	2057	2060 2087	2063 2090	2066 • 2092	2068 2095
1.62	2008	2071	2101	2103	2106	2109	2084 2111	2114	2117		2122
1.63	2122	2125	2127	2130	2133	2135	2138	2140	2143		2148
1.64	2148	2151	2154	2156	2159	2162	2164		2170	2172	2175
1.65	2175	2177	2180	2183	2185	2188	2191	2193	2196		2201
1.66	2201	2204	2206	2209		2214	2217		2222		2227
1.67	2227	2230	2232	2235		2240	2243	2245	2248	2251	2253
1.68	2253	2256	2258	2261	2263	2266	2269	2271	2274	2276	2279
1.69	2279	2281	2284	2287	2289	2292	2294	2297	2299	2302	2304
1.70	0.2304	2307	2310	2312	2315	2317	2320	2322	2325	2327	2330
1.71	2330	2333	2335	2338	2340	2343	2345	2348	2350	2353	235 <b>5</b>
1.72	2355	2358	2360	2363	2365	2368	2370	2373	2375	2378	2380
1.73	2380	2383	2385	2388		2393	<b>2</b> 39 <b>5</b>	2398	2400		2405
1.74	2405	2408	2410	2413	2415	2418	2420	2423	2425	2428	2430
1.75	2430	2433	2435		2440	2443	2445	2448	2450	2453	245 <b>5</b>
1.76	2455			2463		2467		2472	2475		2480
1.77	2480	2482	2485	2487		2492	2494	2497			2504
1.78	2504 2529	2507 2531	2509 2533	2512 2536	2514 2538	2516 2541	2519 2543	2521 254 <b>5</b>	2524 2548	25 <i>2</i> 6 2550	2529 2553
1.79											
1.80	0.2553	2555	2558		2562	2565	2567	2570	2572		2577
1.81 1.82	2577 2601	2603	2582 2605	2584 2608	2610	2589 2613	2591 2615	2594 2617	2596 2620	2598 2622	260 <b>1</b> 262 <b>5</b>
1.83	2625	2627	2629	2632	2634	2636	2639	2641	2643	2646	2648
1.84	2648	2651	2653	2655	2658	2660	2662	2665	2667	2669	2672
1.85	2672	2674	2676	2679	2681	2683	2686	2688	2690	2693	2695
1.86	2695		2700	2702	2704	2707		2711		2716	2718
1.87	2718	2721	2723	2725	2728	2730	2732	2735	2737	2739	2742
1.88	2742	2744	2746	2749	2751	2753	2755	2758	2760	2762	2765
1.89	2765	2767	2769	2772	2774	2776	2778	2781	2783	2785	2788
1.90	0.2788	2790	2792	2794	2797	279 <b>9</b>	2801	2804	2806	2808	2810
1.91	2810	2813	2815	281 <b>7</b>	2819	2822	2824	2826	2828	2831	2833
1.92	2833			2840		2844		2849			2856
1.93	2856			2862		2867		2871		2876	2878
1.94	2878			2885		2889		2894			2900
1.95	2900	2903	2905	2907	2909	2911		2916			2923
1.96	2923			2929		2934		2938			2945
1.97		2947				2956		2960			2967
1.98 1.99	2967 2989	2969			2975 <b>2997</b>	2978 299 <b>9</b>		2982			2989
<b>4.77</b>	4707	<b>ム</b> フフエ	4333	ムフフジ	(73)		3002	3004	3000	-00VO	3010
					<b>1</b> - • 4	-					

# Logarithms to the Base 10

These two pages give the common logarithms of numbers between 1 and 10, correct to four places. Moving the decimal point n places to the right (or left) in the number is equivalent to adding n (or -n) to the logarithm. Thus,  $\log 0.017453 = 0.2419 - 2$  [ $= \overline{2}.2419$ ].

To facilitate interpolation, the tenths of the tabular differences are given at the end of each line, so that the differences themselves need not be considered. In using these aids, first find the nearest tabular entry, and then add (to move to the right) or subtract (to move to the left), as the case may require.

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Tabular Difference   Tabular		Place Tables."													is of		
1.1 0414 0453 0492 0531 0569 0607 0645 0682 0719 0755 0792 1.2 0792 0828 0864 0899 0934 0969 1004 1038 1072 1106 1139 1173 1139 1173 1206 1239 1271 1303 1335 1367 1399 1430 1461 1641 1492 1523 1553 1584 1614 1644 1673 1703 1732 1761 lation in the first 1.6 1461 1492 1523 1553 1584 1614 1644 1673 1703 1732 1761 lation in the first 1.6 2041 2668 2095 2122 2148 2175 2201 2227 2253 2279 2304 specialtable in the preceding page. 1.7 2304 2330 2355 2380 2405 2430 2455 2480 2504 2529 2553 1.8 2553 2577 2601 2625 2648 2672 2695 2718 2742 2765 2788 1.9 2788 2810 2833 2856 2878 2900 2923 2945 2967 2989 3010 2.0 0.3010 3032 3054 3075 3096 3118 3339 3160 3181 3201 3222 2 4 6 8 10 2.1 3222 3243 3263 3284 3304 3324 3345 3365 3385 3404 3424 2 4 6 8 10 2.2 3424 3444 3464 3483 3502 3522 3541 3560 3599 3598 3617 2 4 6 8 10 2.3 3617 3636 3655 3674 3692 3711 3729 3747 3766 3784 3802 2 4 5 7 9 2 2.4 3802 3820 3838 3856 3874 3892 3909 3927 3945 3962 3979 2 4 5 7 7 9 2 2.6 4150 4166 4183 4200 4216 4232 4249 4265 4281 4298 4314 2 3 5 7 8 2 2 4 4 6 8 10 2 3 5 6 8 4 472 4487 4502 4518 4533 4548 4564 4579 4594 4609 4624 2 3 5 6 8 2 2 9 4624 4639 4654 4669 4683 4698 4713 4728 4742 4757 4771 1 3 4 6 7 3 3 4 5 6 3 4 5 4 5 8 4 5 8 4 5 8 5 8 5 8 5 8 5 8 5		0	1	2	3	4	5	6	7	8	9	10					
1.1 0414	1.0	0.0000	0043	0086	0128	0170	0212	0253	0294	0334	0374	0414					
1.2   0792   0828   0864   0899   0934   0969   1004   1038   1072   1106   1139   1.3   1139   1173   1206   1239   1271   1303   1335   1367   1399   1430   1461   1492   1461   1492   1523   1553   1584   1614   1644   1673   1703   1732   1761   lation in the first incident in the incident in the first	1.1	0414	0453				0607	0645	0682		0755	0792					
1.4   1461   1492   1523   1553   1584   1614   1644   1673   1703   1732   1761   18tion in the first into into into into into into into int			0828					1004	1038	1072	1106	1139					
1.5 1761 1790 1818 1847 1875 1903 1931 1959 1987 2014 2041 tlm lines, use the special table on the preceding page.  1.7 2304 2330 2355 2380 2405 2430 2455 2480 2504 2529 2553 1.8 2553 2577 2601 2625 2648 2672 2695 2718 2742 2765 2788 2810 2833 2856 2878 2900 2923 2945 2967 2989 3010  2.0 0.3010 3032 3054 3075 3096 3118 3139 3160 3181 3201 3222 2 4 6 8 10 2.2 3424 3444 3464 3483 3502 3522 3541 3560 3579 3598 3617 2 4 6 8 10 2.2 3424 3444 3464 3483 3502 3522 3541 3560 3579 3598 3617 2 4 6 8 10 2.2 343 3263 388 3856 3874 3892 3909 3927 3945 3962 3979 2 4 5 7 9 2.4 3802 3820 3838 3856 3874 3892 3909 3927 3945 3962 3979 2 4 5 7 9 2.4 3802 3820 3838 3856 3874 3892 3909 3927 3945 3962 3979 2 4 5 7 9 2.5 3979 3997 4014 4031 4048 4065 4082 4099 4116 4133 4150 2 3 5 7 8 2.7 4314 4330 4346 4362 4378 4393 4409 4425 4440 4456 4472 2 3 5 6 8 2.8 4472 4487 4502 4518 4533 4548 4564 4579 4594 4609 4624 2 3 5 6 6 8 2.9 4624 4639 4654 4669 4683 4698 4713 4728 4745 4757 4771 1 3 4 6 7 3 3.0 0.4771 4786 4800 4814 4829 4843 4857 4871 4886 4900 4914 1 3 4 6 7 3 3.1 4914 4928 4942 4955 4969 4983 4997 5011 5024 5038 5011 3 4 5 6 7 3 3.2 5051 5065 5079 5092 5105 5119 5132 5145 5159 5172 5185 1 3 4 5 6 6 3 5594 5705 5797 5092 5105 5119 5132 5145 5159 5172 5185 1 3 4 5 6 6 3 3.5 5594 5705 5717 5729 5740 5752 5763 5775 5886 5899 5911 1 2 3 3 4 6 6 7 3 6 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	1.3	1139	1173	1206	1239	1271	1303	1335	1367	1399	1430	1461	1	0 a	oid l	inter	po-
1.6   2041   2068   2095   2122   2148   2175   2201   2227   2253   2279   2304   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   2014   201	1.4	1461	1492	1523	1553	1584	1614	1644	1673	1703	1732	1761					
1.7 2304 2330 2355 2380 2405 2430 2455 2480 2504 2529 2553 Preceding page.  1.8 2553 2577 2601 2625 2648 2672 2695 2718 2742 2765 2788   1.9 2788 2810 2833 2856 2878 2900 2923 2945 2967 2989 3010    2.0 0.3010 3032 3054 3075 3096 3118 3139 3160 3181 3201 3222 2 4 6 8 11   2.1 3222 3243 3263 3284 3304 3324 3345 3365 3385 3404 3424 2 4 6 8 10   2.2 3424 3444 3464 3483 3502 3522 3541 3560 3579 3598 3617 2 4 6 8 10   2.3 3617 3636 3655 3674 3692 3711 3729 3747 3766 3784 3802 2 4 5 7 9   2.4 3802 3820 3838 3856 3874 3892 3909 3927 3945 3962 3979 2 4 5 7 9   2.5 3979 3997 4014 4031 4048 4065 4082 4099 4116 4133 4150 2 3 5 7 9   2.6 4150 4166 4183 4200 4216 4232 4499 4265 4281 4298 4314 2 3 5 7 8   2.7 4314 4330 4346 4362 4378 4393 4409 4425 4440 4456 4472 2 3 5 6 8   2.8 4472 4487 4502 4518 4533 4548 4564 4579 4594 4609 4624 2 3 5 6 8   2.9 4624 4639 4654 4669 4683 4698 4713 4728 4742 4757 4771 1 3 4 6 7   3.0 0.4771 4786 4800 4814 4829 4843 4857 4871 4886 4900 4914 1 3 4 6 7   3.1 4914 4928 4942 4955 4969 4983 4997 5011 5024 5038 5051 1 3 4 6 7   3.1 4914 4928 4942 4955 4969 4983 4997 5011 5024 5038 5051 1 3 4 6 7   3.1 4914 4928 4942 4955 5969 4983 4997 5011 5024 5038 5051 1 3 4 6 7   3.1 4914 4928 3942 4955 5969 5105 5119 5132 5145 5159 5172 5185 1 3 4 5 6   3.4 5315 5328 5340 5353 5366 5378 5391 5403 5416 5428 5411 1 3 4 5 6   3.5 5441 5453 5465 5478 5490 5502 5514 5527 5539 5575 5586 5798 1 2 4 5 6   3.6 5553 5575 5587 5599 5611 5623 5635 5647 5658 5670 5682 1 2 4 5 6   3.7 5682 5694 5705 5717 5729 5740 5752 5763 5775 5786 5798 1 2 3 5 6   3.8 5798 5809 5821 5832 5843 5855 5866 5877 5888 5899 5911 1 2 3 3 4 5 6   3.9 5911 5922 5933 5944 5955 5966 5977 5988 5999 6010 6011 1 2 3 4 5 6   3.9 5911 5922 5933 5944 5955 5966 5977 5988 5999 6010 6021 1 2 3 4 5 6   3.9 5911 5922 5933 5944 5955 5966 5977 5988 5999 6010 6021 1 2 3 4 5 6   3.9 5911 5922 5933 5944 5955 5966 5977 5988 5999 6010 6021 1 2 3 4 5 6   3.9 5911 5922 5933 5944 5955 5966 6996 6096 6107 6117 6128 1 2 3 4 5 6   3.9 5911 5922 5933 5944 5955 5966 6996 60	1.5	1761	1790	1818	1847	1875	1903	1931	1959	1987	2014	2041			•		
1.8	1.6	2041	2068	2095	2122	2148	2175	2201		2253	2279		•				
2.0         0.3010         3032         3054         3075         3096         3118         3139         3160         3181         3201         3222         2         4         6         8 11           2.1         3222         3243         3263         3284         3304         3324         3345         3365         3385         3404         3424         2         4         6         8 10           2.2         3424         3444         3464         3483         3502         3522         3541         3560         3579         3598         3617         2         4         6         8 10           2.3         3617         3636         3655         3674         3692         3711         3729         3745         3662         3979         2         4         5         7         9           2.5         3979         3997         4014         4031         4048         4065         4082         4099         4116         4133         4150         2         3         5         7         9           2.5         3979         3997         4014         4031         4048         4065         4082         4099         4116						2405							hre	ucui	ng h	age.	•
2.0         0.3010         3032         3054         3075         3096         3118         3139         3160         3181         3201         3222         2         4         6         8 10           2.1         3222         3243         3263         3284         3304         3324         3345         3365         3385         3404         3424         2         4         6         8 10           2.2         3424         3444         3464         3483         3502         3522         3541         3560         3579         3598         3617         2         4         6         8 10           2.3         3617         3636         3655         3674         3692         3711         3729         3747         3766         3784         3802         2         4         5         7         9           2.5         3979         3997         4014         4031         4048         4065         4082         4099         4116         4133         4150         2         3         5         7         9           2.6         4150         4166         4183         4200         4216         4232         4249         4165																	
2.1 3222 3243 3263 3284 3304 3324 3345 3365 3385 3404 3424 2 4 6 8 10   2.2 3424 3444 3464 3483 3502 3522 3541 3560 3579 3598 3617 2 4 6 8 10   2.3 3617 3636 3655 3674 3692 3711 3729 3747 3766 3784 3802 2 4 5 7 9   2.4 3802 3820 3838 3856 3874 3892 3909 3927 3945 3962 3979 2 4 5 7 9   2.5 3979 3997 4014 4031 4048 4065 4082 4099 4116 4133 4150 2 3 5 7 9   2.6 4150 4166 4183 4200 4216 4232 4249 4265 4281 4298 4314 2 3 5 7 8   2.7 4314 4330 4346 4362 4378 4393 4409 4425 4440 4456 4472 2 3 5 6 8   2.8 4472 4487 4502 4518 4533 4548 4564 4579 4594 4609 4624 2 3 5 6 8   2.9 4624 4639 4654 4669 4683 4698 4713 4728 4742 4757 4771 1 3 4 6 7   3.0 0.4771 4786 4800 4814 4829 4843 4857 4871 4886 4900 4914 1 3 4 6 7   3.1 4914 4928 4942 4955 4969 4983 4997 5011 5024 5038 5051 1 3 4 6 7   3.2 5051 5065 5079 5092 5105 5119 5132 5145 5159 5172 5185 1 3 4 5 7   3.3 5185 5198 5211 5224 5237 5250 5263 5276 5289 5302 5315 1 3 4 5 6   3.5 5441 5433 5465 5478 5490 5502 5514 5517 5539 5551 5563 1 2 4 5 6   3.6 5563 5575 5587 5599 5611 5623 5635 5647 5658 5670 5682 1 2 4 5 6   3.7 5682 5694 5705 5717 5729 5740 5752 5763 5775 5786 5798 1 2 3 5 6   3.8 5798 5809 5821 5832 5843 5855 5866 5877 5888 5899 5911 1 2 3 3 4 5    4.1 6128 6138 6149 6160 6170 6180 6191 6201 6212 6222 6232 1 2 3 4 5    4.1 6128 6138 6149 6160 6170 6180 6191 6201 6212 6222 6232 1 2 3 4 5   4.2 6232 6243 6253 6263 6274 6284 6694 6605 6605 6665 6665 6665 6665 6665 666	1.9	2788	2810	2833	2856	2878	2900	<b>2923</b>	2945	2967	2989	3010					
2.2       3424       3444       3464       3483       3502       3522       3541       3560       3579       3598       3617       2 4 6 8 10         2.3       3617       3636       3655       3674       3692       3711       3729       3747       3766       5784       3802       2 4 5 7 9         2.4       3802       3820       3838       3856       3874       3892       3909       3927       3945       3962       3979       2 4 5 7 9         2.5       3979       3997       4014       4031       4048       4065       4082       4099       4116       4133       4150       2 3 5 7 8         2.6       4150       4166       4183       4200       4216       4232       4249       4265       4281       4298       4314       2 3 5 6 8         2.7       4314       4330       4346       4362       4378       4393       4409       4425       4440       4456       4472       2 3 5 6 8         2.9       4624       4639       4654       4669       4683       4698       4713       4728       4724       4757       4771       1 3 4 6 7         3.0       0.4771	2.0		3032	3054	3075	3096	3118	3139	3160	3181	3201		2	4	6	8 1	1
2.3 3617 3636 3655 3674 3692 3711 3729 3747 3766 3784 3802 2 4 5 7 9 2 4 5 7 9 2 4 5 7 9 2 4 5 7 9 2 4 5 7 9 2 4 5 7 9 2 4 5 7 9 2 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	2.1	3222	3243	3263	3284	3304	3324	3345	3365	3385	3404	3424	2	4	6	8 1	LO
2.4 3802 3820 3838 3856 3874 3892 3909 3927 3945 3962 3979 2 4 5 7 9 9   2.5 3979 3997 4014 4031 4048 4065 4082 4099 4116 4133 4150 2 3 5 7 9   2.6 4150 4166 4183 4200 4216 4232 4249 4265 4281 4298 4314 2 3 5 7 8   2.7 4314 4330 4346 4362 4378 4393 4409 4425 4440 4456 4472 2 3 5 6 8   2.8 4472 4487 4502 4518 4533 4548 4564 4579 4594 4609 4624 2 3 5 6 8   2.9 4624 4639 4654 4669 4683 4698 4713 4728 4742 4757 4771 1 3 4 6 7 7   3.0 0.4771 4786 4800 4814 4829 4843 4857 4871 4886 4900 4914 1 3 4 6 7 7   3.1 4914 4928 4942 4955 4969 4983 4997 5011 5024 5038 5051 1 3 4 6 7   3.2 5051 5065 5079 5092 5105 5119 5132 5145 5159 5172 5185 1 3 4 5 7   3.3 5185 5198 5211 5224 5237 5250 5263 5276 5289 5302 5315 1 3 4 5 6   3.4 5315 5328 5340 5353 5366 5378 5391 5403 5416 5428 5441 1 3 4 5 6   3.5 5441 5453 5465 5478 5490 5502 5514 5527 5539 5551 5563 1 2 4 5 6   3.6 5563 5575 5587 5599 5611 5623 5635 5647 5658 5670 5682 1 2 4 5 6   3.7 5682 5694 5705 5717 5729 5740 5752 5763 5775 5786 5798 1 2 3 5 6   3.8 5798 5809 5821 5832 5843 5855 5866 5877 5888 5899 5911 1 2 3 3 5 6   3.8 5798 5809 5821 5832 5843 5855 5866 5877 5888 5899 5911 1 2 3 3 5 6   3.9 5911 5922 5933 5944 5955 5966 5977 5988 5999 6010 6021 1 2 3 4 5    4.0 0.6021 6031 6042 6053 6064 6075 6085 6096 6107 6117 6128 1 2 3 4 5    4.1 6128 6138 6149 6160 6170 6180 6191 6201 6212 6222 6232 1 2 3 4 5    4.2 6232 6243 6253 6263 6274 6284 6294 6304 6314 6325 6335 1 2 3 4 5    4.3 6335 6345 6355 6365 6375 6385 6395 6405 6415 6425 6435 1 2 3 4 5    4.4 6435 6444 6454 6464 6474 6484 6493 6503 6513 6522 6532 1 2 3 4 5    4.5 6638 6637 6646 6656 6665 6665 6675 6684 6693 6702 6712 6721 1 2 3 4 5    4.6 6628 6637 6646 6656 6665 6665 6675 6684 6693 6702 6712 6721 1 2 3 4 5    4.6 6628 6637 6646 6656 6665 6665 6675 6684 6693 6702 6712 6721 1 2 3 4 5    4.6 6628 6637 6646 6656 6665 6665 6675 6684 6693 6702 6712 6721 1 2 3 4 5    4.6 6628 6637 6646 6656 6665 6665 6675 6684 6693 6702 6712 6712 1 2 3 4 5    4.6 6628 6637 6646 6656 6665 6665 6675 6684 6693 6702 6712 6712 1 2 3 4 5    4.	2.2	3424	3444	3464	3483	3502	3522	3541	3560	3579	3598	3617	2	4	6	8 1	10
2.5															-	-	-
2.6	2.4	3802	3820	3838	3856	3874	3892	3909	3927	3945	3962	3979	2	4	5	7	9
2.7	2.5	3979	3997	4014	4031	4048	4065	4082	4099	4116	4133	4150	2	3	5	7	9
2.8       4472       ,4487       4502       4518       4533       4548       4564       4579       4594       4609       4624       2       3       5       6       8         2.9       4624       4639       4654       4669       4683       4698       4713       4728       4742       4757       4771       1       3       4       6       7         3.0       0.4771       4786       4800       4814       4829       4843       4857       4871       4886       4900       4914       1       3       4       6        7         3.1       4914       4928       4942       4955       4969       4983       4997       5011       5024       5038       5051       1       3       4       6       7         3.2       5051       5065       5079       5092       5105       5119       5132       5145       5159       5172       5185       1       3       4       5       7         3.3       5185       5198       5211       5224       5237       5250       5263       5276       5289       5302       5315       1       3       4       5	2.6	4150	4166	4183	4200	4216	4232	4249	4265	4281	4298	4314	2	3	5	7	8
2.9       4624       4639       4654       4669       4683       4698       4713       4728       4724       4757       4771       1       3       4       6       7         3.0       0.4771       4786       4800       4814       4829       4843       4857       4871       4886       4900       4914       1       3       4       6       7         3.1       4914       4928       4942       4955       4969       4983       4997       5011       5024       5038       5051       1       3       4       6       7         3.2       5051       5065       5079       5092       5105       5119       5132       5145       5159       5172       5185       1       3       4       6       7         3.3       5185       5198       5211       5224       5237       5250       5263       5276       5289       5302       5315       1       3       4       5       6         3.4       5315       5328       5340       5353       5366       5378       5391       5403       5416       5428       5441       1       3       4       5											4456		2			6	8
3.0       0.4771       4786       4800       4814       4829       4843       4857       4871       4886       4900       4914       1       3       4       6       7         3.1       4914       4928       4942       4955       4969       4983       4997       5011       5024       5038       5051       1       3       4       6       7         3.2       5051       5065       5079       5092       5105       5119       5132       5145       5159       5172       5185       1       3       4       5       7         3.3       5185       5198       5211       5224       5237       5250       5263       5276       5289       5302       5315       1       3       4       5       6         3.4       5315       5328       5340       5353       5366       5378       5391       5403       5416       5428       5441       1       3       4       5       6         3.5       5441       5453       5465       5478       5490       5502       5514       5527       5539       5551       5563       1       2       4       5													_		5	_	_
3.1       4914       4928       4942       4955       4969       4983       4997       5011       5024       5038       5051       1       3       4       6       7         3.2       5051       5065       5079       5092       5105       5119       5132       5145       5159       5172       5185       1       3       4       5       7         3.3       5185       5198       5211       5224       5237       5250       5263       5276       5289       5302       5315       1       3       4       5       6         3.4       5315       5328       5340       5353       5366       5378       5391       5403       5416       5428       5441       1       3       4       5       6         3.5       5441       5453       5465       5478       5490       5502       5514       5527       5539       5551       5563       1       2       4       5       6         3.6       5563       5575       5587       5599       5611       5623       5635       5647       5658       5670       5682       1       2       4       5		4624	4639	4654	4669	4683	4698	4713	4728	4742	4757	4771	1	3	4	6	7
3.2       5051       5065       5079       5092       5105       5119       5132       5145       5159       5172       5185       1       3       4       5       7         3.3       5185       5198       5211       5224       5237       5250       5263       5276       5289       5302       5315       1       3       4       5       6         3.4       5315       5328       5340       5353       5366       5378       5391       5403       5416       5428       5441       1       3       4       5       6         3.5       5441       5453       5465       5478       5490       5502       5514       5527       5539       5551       5563       1       2       4       5       6         3.6       5563       5575       5587       5599       5611       5623       5635       5647       5658       5670       5682       1       2       4       5       6         3.7       5682       5694       5705       5717       5729       5740       5752       5763       5775       5786       5798       1       2       3       5															4		
3.3       5185       5198       5211       5224       5237       5250       5263       5276       5289       5302       5315       1       3       4       5       6         3.4       5315       5328       5340       5353       5366       5378       5391       5403       5416       5428       5441       1       3       4       5       6         3.5       5441       5453       5465       5478       5490       5502       5514       5527       5539       5551       5563       1       2       4       5       6         3.6       5563       5575       5587       5599       5611       5623       5635       5647       5658       5670       5682       1       2       4       5       6         3.7       5682       5694       5705       5717       5729       5740       5752       5763       5775       5786       5798       1       2       3       5       6         3.8       5798       5809       5821       5832       5843       5855       5866       5877       5888       5899       5911       1       2       3       4																	7
3.4 5315 5328 5340 5353 5366 5378 5391 5403 5416 5428 5441 1 3 4 5 6 3.5 5441 5453 5465 5478 5490 5502 5514 5527 5539 5551 5563 1 2 4 5 6 3.6 5563 5575 5587 5599 5611 5623 5635 5647 5658 5670 5682 1 2 4 5 6 3.7 5682 5694 5705 5717 5729 5740 5752 5763 5775 5786 5798 1 2 3 5 6 3.8 5798 5809 5821 5832 5843 5855 5866 5877 5888 5899 5911 1 2 3 5 6 3.9 5911 5922 5933 5944 5955 5966 5977 5988 5999 6010 6021 1 2 3 4 6 4.0 0.6021 6031 6042 6053 6064 6075 6085 6096 6107 6117 6128 1 2 3 4 5 4.1 6128 6138 6149 6160 6170 6180 6191 6201 6212 6222 6232 1 2 3 4 5 4.2 6232 6243 6253 6263 6274 6284 6294 6304 6314 6325 6335 1 2 3 4 5 4.3 6335 6345 6355 6365 6375 6385 6395 6405 6415 6425 6435 1 2 3 4 5 4.4 6435 6444 6454 6464 6474 6484 6493 6503 6513 6522 6532 1 2 3 4 5 4.5 6532 6542 6551 6561 6571 6580 6590 6599 6609 6618 6628 1 2 3 4 5 4.6 6628 6637 6646 6656 6665 6675 6684 6693 6702 6712 6721 1 2 3 4 5													-		4		7
3.5 5441 5453 5465 5478 5490 5502 5514 5527 5539 5551 5563 1 2 4 5 6 3.6 5563 5575 5587 5599 5611 5623 5635 5647 5658 5670 5682 1 2 4 5 6 3.7 5682 5694 5705 5717 5729 5740 5752 5763 5775 5786 5798 1 2 3 5 6 3.8 5798 5809 5821 5832 5843 5855 5866 5877 5888 5899 5911 1 2 3 5 6 3.9 5911 5922 5933 5944 5955 5966 5977 5988 5999 6010 6021 1 2 3 4 6 4.0 0.6021 6031 6042 6053 6064 6075 6085 6096 6107 6117 6128 1 2 3 4 5 4.1 6128 6138 6149 6160 6170 6180 6191 6201 6212 6222 6232 1 2 3 4 5 4.2 6232 6243 6253 6263 6274 6284 6294 6304 6314 6325 6335 1 2 3 4 5 4.3 6335 6345 6355 6365 6375 6385 6395 6405 6415 6425 6435 1 2 3 4 5 4.4 6435 6444 6454 6464 6474 6484 6493 6503 6513 6522 6532 1 2 3 4 5 4.5 6532 6542 6551 6561 6571 6580 6590 6599 6609 6618 6628 1 2 3 4 5 4.6 6628 6637 6646 6656 6665 6665 6675 6684 6693 6702 6712 6721 1 2 3 4 5					-	-							-	_	-	-	-
3.6 5563 5575 5587 5599 5611 5623 5635 5647 5658 5670 5682 1 2 4 5 6 3.7 5682 5694 5705 5717 5729 5740 5752 5763 5775 5786 5798 1 2 3 5 6 3.8 5798 5809 5821 5832 5843 5855 5866 5877 5888 5899 5911 1 2 3 5 6 3.9 5911 5922 5933 5944 5955 5966 5977 5988 5999 6010 6021 1 2 3 4 6 4.0 0.6021 6031 6042 6053 6064 6075 6085 6096 6107 6117 6128 1 2 3 4 5 4.1 6128 6138 6149 6160 6170 6180 6191 6201 6212 6222 6232 1 2 3 4 5 4.2 6232 6243 6253 6263 6274 6284 6294 6304 6314 6325 6335 1 2 3 4 5 4.3 6335 6345 6355 6365 6375 6385 6395 6405 6415 6425 6435 1 2 3 4 5 4.4 6435 6444 6454 6464 6474 6484 6493 6503 6513 6522 6532 1 2 3 4 5 4.5 6532 6542 6551 6561 6571 6580 6590 6599 6609 6618 6628 1 2 3 4 5 4.6 6628 6637 6646 6656 6665 6665 6675 6684 6693 6702 6712 6721 1 2 3 4 5		5315	5328	5340				5391	5403	5416	5428	5441	1	3	4	5	6
3.7       5682       5694       5705       5717       5729       5740       5752       5763       5775       5786       5798       1       2       3       5       6         3.8       5798       5809       5821       5832       5843       5855       5866       5877       5888       5899       5911       1       2       3       5       6         3.9       5911       5922       5933       5944       5955       5966       5977       5988       5999       6010       6021       1       2       3       4       6         4.0       0.6021       6031       6042       6053       6064       6075       6085       6096       6107       6117       6128       1       2       3       4       5         4.1       6128       6138       6149       6160       6170       6180       6191       6201       6212       6222       6232       1       2       3       4       5         4.2       6232       6243       6253       6263       6274       6284       6294       6304       6314       6325       6335       1       2       3       4													_				
3.8       5798       5809       5821       5832       5843       5855       5866       5877       5888       5899       5911       1       2       3       5       6         3.9       5911       5922       5933       5944       5955       5966       5977       5988       5999       6010       6021       1       2       3       4       6         4.0       0.6021       6031       6042       6053       6064       6075       6085       6096       6107       6117       6128       1       2       3       4       5         4.1       6128       6138       6149       6160       6170       6180       6191       6201       6212       6232       1       2       3       4       5         4.2       6232       6243       6253       6263       6274       6284       6294       6304       6314       6325       6335       1       2       3       4       5         4.3       6335       6345       6355       6365       6375       6385       6395       6405       6415       6425       6435       1       2       3       4       5													-				
3.9       5911       5922       5933       5944       5955       5966       5977       5988       5999       6010       6021       1       2       3       4       6         4.0       0.6021       6031       6042       6053       6064       6075       6085       6096       6107       6117       6128       1       2       3       4       5         4.1       6128       6138       6149       6160       6170       6180       6191       6201       6212       6232       6232       1       2       3       4       5         4.2       6232       6243       6253       6263       6274       6284       6294       6304       6314       6325       6335       1       2       3       4       5         4.3       6335       6345       6355       6365       6375       6385       6395       6405       6415       6425       6435       1       2       3       4       5         4.4       6435       6444       6454       6464       6474       6484       6493       6503       6518       6628       1       2       3       4       5														-		-	-
4.0       0.6021       6031       6042       6053       6064       6075       6085       6096       6107       6117       6128       1       2       3       4       5         4.1       6128       6138       6149       6160       6170       6180       6191       6201       6212       6222       6232       1       2       3       4       5         4.2       6232       6243       6253       6263       6274       6284       6294       6304       6314       6325       6335       1       2       3       4       5         4.3       6335       6345       6355       6365       6375       6385       6395       6405       6415       6425       6435       1       2       3       4       5         4.4       6435       6444       6454       6464       6474       6484       6493       6503       6513       6522       6532       1       2       3       4       5         4.5       6532       6542       6551       6561       6571       6580       6590       6599       6609       6618       6628       1       2       3       4															_	-	_
4.1       6128       6138       6149       6160       6170       6180       6191       6201       6212       6222       6232       1       2       3       4       5         4.2       6232       6243       6253       6263       6274       6284       6294       6304       6314       6325       6335       1       2       3       4       5         4.3       6335       6345       6355       6365       6375       6385       6395       6405       6415       6425       6435       1       2       3       4       5         4.4       6435       6444       6454       6464       6474       6484       6493       6503       6513       6522       6532       1       2       3       4       5         4.5       6532       6542       6551       6561       6571       6580       6590       6599       6609       6618       6628       1       2       3       4       5         4.6       6628       6637       6646       6656       6665       6665       6665       6675       6684       6693       6702       6712       6721       1       2 <td></td> <td>-</td> <td>-</td> <td>-</td>															-	-	-
4.2       6232       6243       6253       6263       6274       6284       6294       6304       6314       6325       6335       1       2       3       4       5         4.3       6335       6345       6355       6365       6375       6385       6395       6405       6415       6425       6435       1       2       3       4       5         4.4       6435       6444       6454       6464       6474       6484       6493       6503       6513       6522       6532       1       2       3       4       5         4.5       6532       6542       6551       6561       6571       6580       6590       6599       6609       6618       6628       1       2       3       4       5         4.6       6628       6637       6646       6656       6665       6665       66675       6684       6693       6702       6712       6721       1       2       3       4       5																-	
4.3       6335       6345       6355       6365       6375       6385       6395       6405       6415       6425       6435       1       2       3       4       5         4.4       6435       6444       6454       6464       6474       6484       6493       6503       6513       6522       6532       1       2       3       4       5         4.5       6532       6542       6551       6561       6571       6580       6590       6599       6609       6618       6628       1       2       3       4       5         4.6       6628       6637       6646       6656       6665       6665       6675       6684       6693       6702       6712       6721       1       2       3       4       5													_			•	
4.4       6435       6444       6454       6464       6474       6484       6493       6503       6513       6522       6532       1       2       3       4       5         4.5       6532       6542       6551       6561       6571       6580       6590       6599       6609       6618       6628       1       2       3       4       5         4.6       6628       6637       6646       6656       6665       6675       6684       6693       6702       6712       6721       1       2       3       4       5																-	-
4.5 6532 6542 6551 6561 6571 6580 6590 6599 6609 6618 6628 1 2 3 4 5 4.6 6628 6637 6646 6656 6665 6675 6684 6693 6702 6712 6721 1 2 3 4 5																	-
4.6 6628 6637 6646 6656 6665 6675 6684 6693 6702 6712 6721 1 2 3 4 5															_		
- 4.7 - 6771 - 6740 - 6740 - 6758 - 6767 - 6776 - 6785 - 6704 - 6817 - 1 - 7 - 7 - 7 - 7 - 7 - 7 - 7 - 7 -						• .										-	-
	4.7									6794		6812	1	2	3	4.	_
4.8 6812 6821 6830 6839 6848 6857 6866 6875 6884 6893 6902 1 2 3 4 4 4.9 6902 6911 6920 6928 6937 6946 6955 6964 6972 6981 6990 1 2 3 4 4																	2.7
4.9 6902 6911 6920 6928 6937 6946 6955 6964 6972 6981 6990 1 2 3 4 4 (74)	7.7	0904	OATT	0940	0740	0937			0704	09/4	0301	0990	•	4	3	4	4

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	0	1	2	3	4	5	6	7	8	9	10				4	
5.0	0.6990	6998	7007	7016		7033	7042	7050	7059	7067	7076	1	2	3	3	4
5.1	7076	7084	7093	7101	7110	7118	7126	7135	7143	7152	7160	1	2	3	3	4
5.2	7160	7168	7177	7185	7193	7202	7210			7235	7243	1	2	2	3	4
5.3	7243	7251	7259	7267	7275	7284	7292		7308	7316	7324	1	2		_	4
5.4	<b>7</b> 324	7332	7340	<b>7</b> 348	7356	7364	7372	7380	7388	7396	7404	1	2	2	3	4
5.5	7404	7412	7419	7427	7435	7443	7451	7459	7466	7474	7482	1	2		_	4
5.6	7482	7490	7497	7505		7520	7528	7536	7543	7551	7559	1	2			4
5.7	<b>7</b> 559	7566	7574	7582	7589	7597	7604	7612	7619	7627	7634	1	2	2	-	4
5.8	7634	7642	7649	7657	7664	7672	7679	7686	7694	7701	7709	1	1	2	_	4
5.9	7709	7716	7723	7731	7738	7745	7752	7760	7767	7774	7782	1	1	2	3	4
6.0	0.7782	7789	7796	7803	7810	7818	<b>7</b> 825	7832	7839	<b>7</b> 846	785 <b>3</b>	1	1	2	3	4
6.1	7853	7860	7868	7875	7882	7889	7896	7903	7910	7917	7924	1	1	2	3	4
6.2	7924	7931	7938	7945	7952	7959	7966	7973	7980	7987	7993	1	1	2	3	3
6.3	7993	8000	8007	8014		8028	8035	8041	8048	8055	8062	1	1	2	3	3
6.4	8062	8069	8075	8082	8089	8096	8102	8109	8116	8122	8129	1	1	2	3	3
6.5	8129	8136	8142	8149	8156	8162	8169	8176	8182	8189	8195	1	1	2	3	3
6.6	8195	8202	8209	8215	8222	8228	8235	8241	8248	8254	8261	1	1	2	3	3
6.7	8261	826 <b>7</b>	8274	8280		8293	8299	8306	8312	8319	8325	1	1	2	3	3
6.8	8325	8331	8338	8344	8351	8357	8363	8370	8376	8382	8388	1	1	2	3	3
6.9	8388	8395	8401	8407	8414	8420	8426	8432	8439	8445	8451	1	1	2	3	3
7.0	0.8451	8457	8463	8470	8476	8482	8488	8494	8500		8513	1	1	2	2	3
7.1	8513	8519	8525	8531		8543	8549	8555	8561		8573	1	1	2	2	3
7.2	8573	8579	8585		8597	8603	8609	8615	8621		8633	1	1	2	2	3
7.3	8633	8639	8645	8651		8663	8669	8675	8681	8686	8692	1	1	2	2	3
7.4	8692	8698	8704	8710		8722	8727	8733	8739		8751	1	1	2	2	3
7.5	8751	8756	8762	8768	8774	8779	8785	8791	8797	8802	8808	1	1	2	2	3
7.6	8808	8814	8820	8825	8831	8837	8842	8848	8854	8859	8865	1	1	2	2	3
7.7	8865	8871	8876	8882	8887	8893	8899	8904	8910	8915	8921	1	1	2	2	3
<b>7</b> .8	8921	8927	8932	8938	8943	8949	8954	8960	8965		8976	1	1	2	2	3
<b>7</b> .9	8976	8982	8987	8993	8998	9004	9009	9015	9020	9025	9031	1	1	2	2	3
8.0	0.9031	<b>9</b> 036	9042	9047	9053	9058	9063	9069	9074		9085	1	1	2	2	3
8.1	9085	9090	9096	9101	9106	9112	9117	9122	9128	9133	9138	1	1	2	2	3
8.2	9138	9143	9149	9154	9159	9165	9170	9175	9180	9186	9191	1	1	2	2	3
8.3	9191	9196	9201	9206	9212	9217	9222	9227	9232	9238	9243	1	1	2	2	3
8.4	9243	9248	9253	9258	9263	9269	9274	9279	9284		9294	1	1	2	2	3
8.5	9294	9299	9304	9309	9315	9320	9325	9330	9335	9340	9345	1	1	2	2	3
8.6	9345	9350	9355	9360	9365	9370	9375	9380	9385		9395	1	1	2	2	3
8.7	9395	9400	9405	9410	9415	9420	9425 9474	9430 9479	9435	9440	9445	0	1	1	2	2
8.8	9445	9450	9455	9460	9465	9469		9528	9484 9533	9489	9494	0	1	1	2	2
8.9	9494	<b>9</b> 499		9509		9518					9542	0	1	1	2	2
9.0	0.9542			9557		9566			9581		9590	0		1	_	2
9.1	9590	9595	9600	9605	9609	9614			9628		9638	0	1	1	2	2
9.2	9638			9652		9661			9675		9685	0	1	1	2	2
9.3	9685			9699		9708 9754			9722 9768		9731 977 <b>7</b>	0	1	1	2	2
9.4	9731			9745								0	1	1	2	2
9.5	9777			9791		9800 9845			9814 9859		9823	0	1	1	2	2
9.6	9823			9836					9903		9868	0	1	1	2	2
9.7	9868			9881 9926		9890 9934			9903 9948		9912 9956	0	1	1	2	2
9.8	9912	9917	227T	9926 9 <b>9</b> 69	9930	9934			9991		• 3330	0	1		2	2 2
9.9	9956	3301	3703	<del>2¥</del> U2	2217	221G		J J G I	J J J L	2230		•	-	-	~	4

# Logarithms to the Base e

These two pages give the natural (hyperbolic, or Napierian) logarithms of numbers between 1 and 10, correct to four places. Moving the decimal point places to the right (or left) in the number is equivalent to adding n times 2.3026 (or n times 3.6974) to the logarithm.

```
1 0.6974-3
       2.3026
1
2
3
4
                         0.3948 - 5
0.0922 - 7
0.7897 - 10
       4.6052
                    2
3
4
5
6
    6.9078
9.2103
11.5129
                         0.4871 - 12
0.1845 - 14
     13.8155
     16.1181
                     7
                          0.8819 - 17
                         0.5793 - 19
0.2767 - 21
     18.4207
                     8
     20.7233
```

Tenths of the Tabular Difference																
	0	1	2	3	4	5	6	7	8	9	10	1			4	
1.0	0.0000	0100	0198	0296	0392	0488	0583	0677	0770	0862	0.0953	10	19 :	29 :	38 4	48
1.1	0953	1044	1133	1222	1310	1398	1484	1570	1655	1740	1823	9	17 2	26	35 4	44
1.2	1823	1906	198 <b>9</b>	2070	2151	2231	2311	2390	2469	2546	2624	8	16	24	32 4	40
1.3	2624	2700	2776	2852	2927	3001	3075	3148	3221	3293	3365	7	15 3	22	30 3	37
1.4	3365	3436	3507	3577	3646	3716	3784	3853	3920	3988	4055	7	14 :	21 2	28 3	34
1.5	4055	4121	4187	4253	4318	4383	4447	4511	4574	4637	4700	6	13 ]	19 2	26 3	2
1.6	4700	4762	4824	4886	4947	5008	5068	5128	5188	5247	5306	6	12 ]	18 2	24 3	10
1.7	<b>5</b> 306	5365	5423	5481	5539	5596	5653	5710	5766	5822	5878	6	11 ]	17 2	23 2	29
1.8	5878	5933	5988	6043	6098	6152	6206	6259	6313	6366	6419	5	11 ]	16 2	22 2	27
1.9	6419	6471	6523	6575	6627	6678	6729	6780	6831	6881	0.6931	5	10 1	15 2	21 2	:6
2.0	0.6931	6981	7031	7080	7129	7178	7227	7275	7324	7372	7419	5	10 3	15 2	20 2	24
2.1	7419	7467	7514	7561	7608	<b>7</b> 65 <b>5</b>	7701	7747	7793	7839	7885	5	9 3	14 ]	19 2	23
2.2	7885	7930	7975	8020	8065	8109	8154	8198	8242	8286	8329	4	9 3	13 ]	18 2	:2
2.3	8329	8372	8416	8459	8502	8544	8587	8629	8671	8713	8755	4			17 2	
2.4	8755	8796	8838	8879	8920	8961	9002	9042	9083	9123	9163	4	8 ]	12 1	16 2	20
2.5	9163			9282	9322	9361	9400	9439	9478	9517	9555	4	8 ]	12 1	16 2	20
2.6	9555		9632	9670		9746	9783			9895	0.9933	4			15 1	
2.7	0.9933		0006			0116	0152	0188	0225	0260	1.0296	4	-		15 1	_
2.8	1.0296		0367		0438	0473	0508		0578	0613	0647	4	-		14 1	
2.9	0647	0682	0716	0750	0784	0818	0852	0886	0919	0953	1.0986	3	7	10 1	14 1	.7
3.0	1.0986	1019	1053	1086	1119	1151	1184	1217	1249	1282	1314	3	7	10 1	13 1	16
3.1	1314	1346	1378	1410	1442	1474	1506	1537	1569	1600	1632	3	6	10 1	13 1	16
3.2	1632	1663	1694	1725	1756	1787	1817	1848	1878	1909	1939	3			12 1	-
3.3	1939	1969	2000			2090	2119	2149	2179	2208	2238	3			12 1	
3.4	2238	2267	2296		2355	2384	2413	2442	2470	2499	2528	3	6	9 ]	12 1	4
<b>3.5</b>	2528	2556	2585	2613	2641	2669	2698	2726	2754	2782	2809	3	6		11 1	
3.6	2809	2837	2865	2892		2947	2975	3002	3029	3056	3083	3	5		11 1	
3.7	3083	3110	3137	3164		3218	3244	3271	3297	3324	3350	3	5		11 1	
3.8	3350	3376	3403		3455	3481	3507		3558	3584	3610	3	5		10 1	
3.9	3610	3635	3661	3686	3712	3737	3762	3788	3813	3838	1.3863	3	5	8.	10 1	13
4.0	1.3863	3888			3962	3987	4012	4036	4061	4085	4110	2	5	_	10 1	
4.1	4110	4134				4231	4255		4303	4327	4351	2	5		10 1	
4.2	4351	4375				4469	4493		4540		4586	2	5	-	9 1	
4.3	4586	4609				4702	4725	4748			4816	2	5	7	9 1	
4.4	4816	4839	4861	4884		4929	4951	4974			5041	2		.7	9 1	
4.5	5041	5063			•	5151	5173	5195	5217	5239	5261	2	4	7	9 1	
4.6	5261	5282		5326		5369	5390		5433		5476	2	4	_	91	
4.7	5476	5497				5581	5602			5665	5686	2	4		8 1	
4.8	5686		5728			°5790	5810		5851		5892	2	4	6	8 1	
4.9	5892	5913	5933	5953	5974	5994 77		6034	6054	6074	1.6094	2	4	6	8 1	M

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	0	1	2	3	4	5	6	7	8	9	10	,		3		
<b>5.0</b>	1.6094	6114	6134	6154	6174	6194	6214	6233	6253	6273	6292	2	4	6	8	10
5.1	6292		6332	6351		6390		6429		6467	6487	2	4	6	8	10
5.2	6487		6525		6563	6582 '		6620	6639		6677	2	4	6		10
5.3	6677		-	6734		6771		6808			6864	2	4	6	7	9
5.4	6864	6882	6901	6919	6938	6956	6974	6993	7011	7029	7047	2	4	6	7	9
5.5	7047	7066			7120	7138		7174		7210	7228	2	4	5	7	9
5.6	7228	7246	7263	7281	7299	7317	7334	7352	7370		7405	2	4	5	7	9
5.7	7405	7422	-	7457	7475	7492		7527	-		7579	2	3	5	7	9
5.8	7579		7613		7647	7664	7681	7699	7716	7733	7750	2	3	5	7	9
5.9	7750		7783		7817	7834	7851	7867	7884		1.7918	2	3	5	7	8
6.0	1.7918	7934	7951		7984	8001	8017	8034		8066	8083	$\frac{2}{2}$	3	5	7	8
6.1	8083	8099			8148	8165	8181	8197			8245		3	5	7	8
6.2	8245			8294		8326		8358			8405	2	3	5	6	8
6.3 6.4	8405 8563		8437	8610	8469	8485 8641		8516 8672			8563 8718 -	2	3	5 5	6	8
												2			6	8
6.5	8718	8733			8779	8795		8825			8871	2	3	5	6	8
6.6	8871			8916		8946		8976			9021	2	3	5		8
6.7 6.8	9021 9169	9184	9051	9213	9081 9228	9095 9242	9110 9257	-	9140 9286		9169 9315	1	3	4	6	7
6.9	9315			9359		9387	9402				1.9459	1	3	4	6	7 7
														-		-
7.0	1.9459	9473			9516	9530		9559 9699			9601 9741	1	3	4	6	7
7.1	9601	9615		9643 9782		9671 9810	9685				1.9879	1	3	4	6	7
7.2 7.3	9741 1.9879	9755 9892		9784		9947	9961				2.0015	1	3	4	6 5	7 7
7.3 7.4	2.0015	0028		0055	0069	0082		0109			0149	1	3	4	5	7
														-		-
7.5 7.6	0149	0162		0189 0321		0215 0347	0229 0360	0242 0373		0268 0399	0281 0412	1	3	4	5	7
7.0 7.7	0281 0412	0295 0425		0451		0347	0490		0516		0541	1	3	4	5 5	7 6
7.7 7.8	0541			0580		0605	0618	0631		0656	0669	i	3	4	5	6
7.9	0669			0707		0732	0744				2.0794	ī	3	4	5	6
8.0	2.0794	0807		0832		0857	0869	0882	0894		0919	1	2	4	5	6
8.1	0919	0931		0956		0980	0992	1005	1017		1041	1	2	4	5	6
8.2	1041	1054	1066	1078	1090	1102	1114		1138		1163	î	2	4	5	6
8.3	1163	1175	1187	1199	1211	1223	1235	1247	1258	1270	1282	ī	2	4	5	6
8.4	1282	1294		1318	1330	1342	1353	1365	1377	1389	1401	1	2	4	5	6
8.5	1401	1412	1424	1436	1448	1459	1471	1483	1494	1506	1518	1	2	4	5	6
8.6	1518	1529		1552		1576	1587	1599		1622	1633	ī	2	3	5	6
8.7	1633	1645	1656	1668	1679	1691	1702	1713	1725	1736	1748	1	2	3	5	6
8.8	1748	1759	1770	1782	1793	1804	1815	1827	1838	1849	1861	1	2	3	5	6
8.9	1861	1872	1883	1894	1905	1917	1928	1939	1950	1961	2.1972	1	2	3	4	6
9.0	2.1972	1983	1994	2006	2017	2028	2039	2050	2061	2072	2083	1	2	3	4	6
9.1	2083				2127	2138	2148	2159	2170	2181	2192			3		
9.2	2192	2203	2214	2225	2235	2246		2268			2300	1	2	3	4	5
9.3	2300			2332		2354		2375			2407	1	2	3	4	5
9.4	2407	2418	2428	2439	2450	2460		2481			2513	1	2	3	4	5
9.5	2513			2544		2565		2586			2618	1	2	3	4	5
9.6		2628				2670		2690			2721			3	4	5
9.7	2721			2752		2773		2793			2824			3		
9.8	2824					2875		2895			2925			3		
9.9	2925	2935	2946	_	2966			3996	3006	3016	2.3026	1	2	3	4	5
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# PART II

# THE USE OF THE DIAGRAMS

THE steam tables give values of the simultaneous physical coördinates (or properties) of steam, such as the pressure, specific volume, temperature, entropy, total heat, and internal energy. When certain of these physical coördinates are known, the remainder can be obtained from the tables, either directly, or by an interpolation. The values tabulated are for dry and saturated steam and for superheated steam; if the steam is wet, its properties must be calculated.

The simultaneous properties of steam can also be shown by the use of a steam diagram. The diagram may be drawn on a plane which has any independent pair of the properties as its coördinates; for example, the ordinates and abscissæ may be, respectively, pressures and specific volumes, or temperatures and entropies, or total heats and entropies, or total heats and pressures. Each point on such a plane represents steam in a perfectly definite condition: that is, with all its physical coördinates fixed. On such a plane it is possible to plot a steam diagram, or chart, consisting of a number of curves, each of which goes through all points on the plane having a certain constant value of some one physical coördinate. If a well-selected and sufficient number of such curves is drawn for each physical coördinate, then, for any point on the plane, all the properties of steam can be determined by reading the corresponding ordinate and abscissa, and by interpolation in the plotted families of curves. For example, on a pressure-volume plane on which families of constant entropy curves, and of constant total heat curves, are drawn, there can be read off by inspection the pressure, volume, entropy, and total heat, corresponding to any point on the plane.

The families of curves which are drawn may include curves of constant dryness factor (quality) of saturated steam; consequently the diagram may give by inspection the properties of wet steam. This is an advantage over the tables.

Of the various planes on which these diagrams may be drawn, some are more convenient than others. Any one of them will serve if the only purpose in view is to find single values of physical coördinates. For this purpose, the relative advantages of the various planes is a question only of the accuracy and ease with which the desired quantities can be read.

A diagram may, however, have uses other than merely showing the simultaneous properties of steam. It may be used for the solution of certain problems, if the proper plane is chosen and the necessary families of curves are drawn on it. It should be clearly borne in mind that the choice of a plane for this purpose has no relation to the choice of a plane on which to represent the cycle of operations of a steam

engine or other steam appliance. For the latter purpose two special planes are of particular value, (1) the pressure-volume plane, and (2) the temperature-entropy plane. The pressure-volume plane shows the amount of external work done while the steam is going through any series of changes; the temperature-entropy plane, in a similar way, shows the heat added to or abstracted from the steam. To find the work done or the heat exchange, it is only necessary that the steam cycle should be drawn on those planes; the presence of families of curves of the physical coordinates is of no use in finding those quantities. In other words, the plane alone is required for that purpose, not a steam diagram on that plane.

A steam diagram on the pressure-volume plane, or on the temperature-entropy plane, does not offer any particular advantages over other diagrams for finding steam quantities. For the solution of many problems of common occurrence such a diagram is decidedly less useful and convenient than a diagram in which the total heat of steam is one of the coördinates.

By the total heat of steam is meant the sum of its internal energy, E, and of the heat equivalent of the product of its pressure and specific volume, or

$$H = E + 144 A pv$$
.

(It should be noted that total heat defined in this way differs slightly from the total heat as found in Regnault's investigations of saturated steam and as usually given in steam tables; for a discussion of this, see page 101.)

The total heat of steam is a quantity which enters into a large number of problems. It represents the energy (other than kinetic energy) entering any piece of apparatus with every pound of steam that goes to it, and the energy (other than kinetic) leaving it with every pound of steam that leaves it. In most steam appliances, under steady conditions of operation, the weight of steam entering per unit of time is equal to the weight of steam leaving. In such an appliance if  $H_1$  is the total heat of one pound of the entering steam, and  $H_2$  is the total heat of one  $F_1$  und of the leaving steam, then  $H_1 - H_2$  is the energy given up in the apparatus by each pound of steam. In a steam engine  $H_1 - H_2$  is the sum of the work done and of the external heat-losses; in a boiler its value is negative and represents the heat supply per pound of steam formed; in a non-conducting steam nozzle it is the heat that is converted into kinetic energy; in a throttling calorimeter its value is zero because there is no external work done, no heat conduction, and no change in kinetic energy.

On a steam diagram on which the ordinates are total heats, the quantity  $\mathbf{H_1} - \mathbf{H_2}$  is represented by the vertical drop between the points representing the entering and leaving conditions. Vertical distances measure the energy given up in a steam appliance, with a constant scale all over the diagram. In flow of steam problems, this constancy of scale permits the immediate graphical determination of the velocity of flow by merely transferring the vertical distance  $\mathbf{H_1} - \mathbf{H_2}$  to a velocity scale at the side of the diagram. It is in this respect especially that a total heat-entropy diagram is greatly superior to a temperature-entropy diagram.

Two diagrams are presented, both with total heats as ordinates. By the superposition of three families of curves it would have been possible to give all the data on one diagram; but that would have led to confusion if the curves had been as closely spaced as is requisite for accurate interpolation.

The diagrams give information as to the total heat, entropy, and specific volume of wet and of superheated steam, within a pressure range from .5 to 600 lbs. per sq. in., and for steam in any condition between a quality of about .7 and a superheat of about 600° F. If the properties of water or the latent heat of steam come into the problem, the tables must be used to supplement the readings from the diagrams.

The principal advantages of the diagrams over the tables are that they give the properties of wet steam, and that they permit an expeditious solution of many problems without calculation and with a degree of accuracy which is sufficient for the ordinary purposes of the engineer.

The method of solution of some of the more commonly occurring problems is given below.

#### Properties of Steam

The two diagrams give the values of five of the physical coördinates of steam: pressure, quality,² entropy, total heat, and specific volume. If any two of these coördinates are known, the remaining three can be found by inspection. In some cases it will be more expeditious (and it will always be more accurate) to use the tables instead of the diagrams, but in other cases, as when wet steam is used, the diagrams will save time and calculation. Pressures, qualities, and total heats can be found on both diagrams; if entropy is involved, Diagram I must be used; if specific volume is involved, Diagram II must be used. The pressure scale on the top of Diagram II is more open than the pressure scale of Diagram I, and consequently somewhat greater accuracy is obtainable by using Diagram II in cases where either diagram can be used.

The method of finding a desired quantity is the same in all cases. The point of intersection of the lines (actual or interpolated) representing the two known quantities is located on the appropriate diagram; the position of this point with reference to the lines representing the desired quantity determines the actual value of that quantity.

## Examples.

1. A vessel of 4 cu. ft. capacity contains 0.2 lbs. of water and 0.8 lbs. of steam. What is the pressure?

In what follows, the word quality means, the dryness factor if the steam is saturated, the number of degrees of superheat if the steam is superheated. Pressures, throughout, are absolute pressures.

¹ The accuracy of a two-color diagram depends on the accuracy of registration of the two printings. The original drawings showed in no place an error of as much as  $\tau_0^1$  inch. The photographic reproduction of these drawings has resulted in minor local distortions, which in the lower corners of Diagram II amount to  $\tau_0^1$  inch. This is the maximum distortion, and it occurs in the least important part of the diagram.

The intersection of the steam quality line, .80, with the specific volume line, 4 cu. ft., on Diagram II, occurs at a steam pressure of 87 lbs. per sq. in. abs.

2. Measurements from an indicator card show that at a certain instant during expansion the volume of the steam is 1.6 cu. ft. and the pressure 40 lbs. per sq. in. abs. If the weight of steam in the cylinder is 0.20 lbs., what is the quality of the steam at that instant?

The specific volume of the steam is  $\frac{1.6}{.20}$  = 8 cu. ft. From Diagram II, steam of that volume and of 40 lbs. pressure has a quality of .364.

3. What is the entropy of 1 lb. of steam at 100 lbs. pressure and a temperature of 450° F.?

From the table on Diagram I, the temperature of saturated steam at 100 lbs. pressure is seen to be 328° F.; the steam is consequently superheated 450-328=122° F. From Diagram I, steam at 100 lbs. pressure, superheated 122° F., has an entropy 1.678.

4. An indicator (pressure-volume) card is to be redrawn on the temperatureentropy plane. What are the temperature and entropy corresponding to the condition defined in example 2?

Steam at 40 lbs. pressure has a temperature of  $267^{\circ}$  F., or  $267+460=727^{\circ}$  abs.

The entropy is seen, by Diagram I, to be 1.373.

5. What is the heat supply per lb. of steam to a boiler with feed water at 100° F., generating steam at 160 lbs. pressure and of a quality .99?

The total heat of steam (Diagram II) at 160 lbs. pressure and quality .99 is 1186 B. t. u.; the feed water contains approximately 100-32=68 B. t. u. The heat supply per lb. of steam is consequently 1186-68=1118 B. t. u.

6. What is the volume of 5 lbs. of steam at 1 lb. pressure and a quality .80?

The specific volume (Diagram II) is 265 cu. ft.; the volume of 5 lbs. is consequently 5×266=1330 cu. ft.

# Internal Energy

The internal energy of steam of known pressure, p, and specific volume, v, is given by the equation  $E=H-144 \ Apv.$ 

Example 7. A cylinder contains 1 lb. of steam at a pressure of 80 lbs. per sq. in. and occupying a volume of 7 cu. ft. What is the internal energy of the steam?

The total heat of the steam (Diagram II) is 1274 B. t. u. The internal energy is  $1274 - .1852 \times 80 \times 7 = 1170$  B. t. u.

#### Adiabatic Expansion

During adiabatic expansion, entropy is constant. Vertical lines on Diagram I are lines of constant entropy. A vertical line is consequently the locus of the points representing the condition of steam which is expanding adiabatically. Two of the three quantities, pressure, specific volume, and quality, will generally be known at some one point on the adiabatic curve; this suffices for finding the entropy. When the entropy and one other property of the steam are known, the condition of the steam is fixed.

To find the quality of steam which has expanded adiabatically to some *known* pressure, locate the intersection of the known entropy and pressure lines; its position with reference to the constant quality lines gives the desired quality.

Example 8. Steam at 120 lbs. pressure, superheated 100° F., expands adiabatically. Find its quality and the ratio of expansion when the pressure reaches 15 lbs. per sq. in.

The entropy of the steam (Diagram I) is 1.651; at 15 lbs. pressure, steam of the same entropy has a quality .928. The initial volume (Diagram II) was 4.33 cu. ft.; the final volume is 24.4 cu. ft. The ratio of expansion is

$$\frac{24.4}{4.33}$$
 = 5.63.

To find the pressure of steam which has expanded adiabatically to a *known quality*, locate the intersection of the known entropy and quality lines. The desired pressure is given by the position of the intersection with reference to the constant pressure lines.

Example 9. Steam at a pressure of 150 lbs. per sq. in., superheated 60° F., expands adiabatically. At what pressure will the steam become dry and saturated? The entropy (Diagram I) is 1.6105; the corresponding entropy line crosses the dry and saturated steam line at 90 lbs. pressure.

To find the pressure and quality of steam which has expanded adiabatically to a known volume, requires the use of both diagrams. The desired pressure and quality lie on the known constant entropy line of Diagram I, and on the known constant specific volume line of Diagram II. Find by inspection of the two diagrams the one pair of simultaneous values of pressure and quality which are common to both lines; or, assume various final pressures, find the corresponding final volumes, and interpolate.

Example 10. Steam of 140 lbs. pressure, superheated 120° F., expands adiabatically with a ratio of expansion of 6. What are the pressure and quality at the end of expansion?

The initial specific volume (Diagram II) is 3.85 cu. ft.; the final specific volume is  $6 \times 3.85 = 23.10$  cu. ft. The entropy (Diagram I) is 1.6503. With

this entropy, steam at 17 lbs. has a quality .934 corresponding to a volume of 21.8 cu. ft.; at 15 lbs. the quality is .927, and volume 24.4. The final pressure is evidently between 15 and 17 lbs. At 16 lbs. the quality is .931 and volume 23.0. By interpolation the desired pressure is 15.9 lbs. per sq. in., and the corresponding quality .930.

#### Work done during Adiabatic Expansion

The work done during adiabatic expansion cannot be taken directly from the diagrams. It is equal in amount but opposite in sign to the change of internal energy during expansion.

$$W_{12} = E_1 - E_2 = H_1 - H_2 - 144 A(p_1 v_1 - p_2 v_2)$$

The simplest way of obtaining the work done from the diagrams is to find  $H_1$ — $H_2$  for adiabatic expansion, and to subtract from it the second term in the equation given.

Example 11. How much work is done on unit mass of steam at 15 lbs. pressure and quality .90 when it is compressed adiabatically to one-fourth its original volume?

By a process similar to that given in example 10, the pressure at the end of compression is found to be 72 lbs. per sq. in., and the corresponding quality .988. The volumes at the beginning and end of the compression are 23.62 and 5.905 cu. ft. respectively.

The work done by the steam is

$$H_1 - H_2 - 144 A(p_1v_1 - p_2v_2)$$

$$= 1054 - 1169 - .1852(15 \times 23.62 - 72 \times 5.905)$$

$$= -115 - 13$$

$$= -128 B. t. u.$$

or the work done on the steam is 128 B. t. u.

#### Work done in the Rankine Ideal Cycle

In the Rankine cycle, steam is admitted at a constant pressure, expands adiabatically to the back pressure and is exhausted against a constant back pressure. The engine is supposed to have no clearance. It is an ideal steam-engine cycle, with no internal friction, no heat losses and no free or imperfectly resisted expansion. In such a cycle all the energy that is taken from the steam must be converted into work. The work done per lb. of steam is consequently  $H_1 - H_2$ . As the only expansion that takes place is adiabatic, the steam that is leaving has the same entropy as the entering steam.

To find the work done by unit mass of steam, in a Rankine cycle admitting steam of known quality and pressure, and expanding to a known back pressure, locate the

point representing the quality and pressure of the admission steam, and measure the vertical distance from this point to the known back pressure line. This distance represents the work done in B. t. u.

Example 12. Steam initially at 150 lbs. pressure, superheated 150° F., goes through a Rankine cycle with a back pressure of 2 lbs. per sq. in. How much work is done by unit mass of steam?

The total heat of steam at 150 lbs. pressure, superheated 150° F. (Diagram I), is 1275 B. t. u. Steam of the same entropy at 2 lbs. abs. pressure has a total heat of 964 B. t. u. The work of the Rankine cycle is

#### The Flow of Steam

In a steam engine the resistance to expansion is offered by the piston, and the useful work is done on the piston; in a steam nozzle the resistance to expansion is offered by the steam which is ahead, and consequently the work is done on the steam, and results in giving it kinetic energy.

If steam is admitted to a properly designed, non-conducting nozzle without internal friction, it will expand adiabatically. Since there is no heat loss, and no external work done, all the energy that is taken from the steam must be converted into kinetic energy. The kinetic energy of the escaping steam is consequently  $H_1 - H_2$ . The velocity corresponding to this kinetic energy of unit mass of steam can be read directly from the scale to the left of Diagram I. It is evident that the kinetic energy of the escaping steam is equal to the work that would have been done by the steam in a Rankine cycle with the same back pressure.

To find the velocity with which steam escapes from a properly designed frictionless nozzle, measure with a pair of compasses the change in the total heat of the steam during adiabatic expansion and transfer this measurement to the velocity scale.

Example 13. Steam at 100 lbs. pressure, superheated 60° F., expands in a nozzle to a pressure of 2 lbs. per sq. in. What is its final velocity?

The change in the total heat is 1219-954=266 B. t. u. This is seen by the scale on Diagram I to correspond to a velocity of 3650 ft. per second.

Example 14. A four-stage impulse turbine supplied with steam as in example 13 and with expansion to the same pressure, is designed for equal velocity of steam in each of the stages. What is that velocity?

The kinetic energy of the steam in each stage is  $\frac{266}{4}$  =66.5 B.t. u. This corresponds to a velocity of 1825 ft. per second.

## Designing a Nozzle

The design of a steam nozzle for a desired weight flow is determined by the throat (smallest cross section) of the nozzle. The pressure at the throat will be about .58 of the initial pressure whenever the ratio of the final pressure to the initial pressure is less than that quantity; for ratios greater than .58 the throat pressure is the same as the final pressure. To determine the throat area, find the velocity of the steam at the throat from Diagram I and its specific volume from Diagram II. The specific volume multiplied by the desired weight flow in lbs. per second is the volume flowing per second past the throat. This volume divided by the velocity at the throat is equal to the area of the throat, in square feet.

Example 15. 50 lbs. of steam at 160 lbs. pressure, superheated 100° F., flow per minute through a nozzle into the atmosphere (15 lbs. per sq. in.). What is the smallest cross section of the nozzle?

The entropy of the steam is 1.629 and its total heat 1251 B. t. u. At the throat the pressure is approximately  $160 \times .58 = 92.8$  lbs. per sq. in.; the total heat is 1202 B. t. u., and the specific volume is 4.98. The kinetic energy at the throat is 1251 - 1202 = 49 B. t. u., which corresponds to a velocity of 1575 ft. per second. The volume flowing per second past the

throat is  $\frac{50}{60} \times 4.98 = 4.15$  cu. ft. The throat area is consequently  $\frac{4.15}{1575} \times 144 = .380$  sq. ins.

## Throttling

If steam expands through a small orifice (or a porous plug) without the addition or abstraction of heat, and is brought finally to its initial velocity, its total heat will be unchanged. This must be the case because none of the heat is converted into external work or kinetic energy and no heat is added or abstracted, so that  $H_1 - H_2 = 0$ . The process is called throttling, and occurs when steam goes through a reducing valve and also in the throttling calorimeter. Horizontal lines on Diagrams I and II are lines of constant total heat and consequently show the changes in the condition of steam which result from throttling.

Example 16. Steam at 200 lbs. pressure, quality .99, passes through a reducing valve. At what pressure must the valve be set in order to discharge dry and saturated steam?

Inspection of Diagram I or II shows that dry and saturated steam at 119 lbs. has the same total heat as steam at 200 lbs. and quality .99.

Example 17. Steam in a throttling calorimeter has a pressure of 17 lbs. per sq. in. and a temperature of 265° F. The initial pressure of the steam was 100 lbs. per sq. in. What was its initial quality?

Saturated steam at 17 lbs. has a temperature of 219° F.; the superheat in the calorimeter is consequently 265-219=46° F. The initial quality of the steam is seen by inspection to be .987.

# Hirn's Analysis

In making Hirn's analysis of the performance of a steam engine it is necessary to find (from the measured pressure, volume, and weight of steam acting) the internal energy of the steam in the cylinder at admission, cut off, release, and compression. These quantities are readily found by the method already outlined.

## Temperature-Entropy Diagram

In redrawing an indicator (pressure-volume) diagram on the temperature-entropy plane, the assumption is made that the whole of the working substance remains in the cylinder throughout the cycle, and that heat is added to and abstracted from it while it is in the cylinder. That is, the boiler, cylinder, and condenser operations are all assumed to take place in the cylinder. It is most convenient, moreover, to draw the diagram for unit mass of steam, which is readily done after determining the proper scale of volumes for the indicator diagram. The process then becomes extremely simple: the temperature and entropy corresponding to a series of points on the indicator diagram are found as in example 4 and are plotted. It should be noted, however, that the diagrams do not give information for qualities below about .7. Consequently some of the points on the temperature-entropy diagram must be calculated.

#### Other Problems

Many special problems of less common occurrence than the foregoing can be easily solved by the use of the diagrams. For example, suppose it is proposed to spray into a gas-engine cylinder a certain weight of water at a certain instant, and it is desired to know what will be the resulting pressure and temperature in the cylinder. The partial pressure, temperature and total heat of the steam formed will be represented by the coördinates of some point on a definite constant specific volume line on Diagram II; the exact position of the point on the line can easily be determined from the conditions of the problem by trial and interpolation.

# PART III

# DISCUSSION OF SOURCES

THE computation of a steam table requires as its foundation experimental data of several different kinds. The most important are:

- 1. An evaluation of the absolute thermodynamic scale;
- 2. Data on the variation of the specific heat of water with temperature;
- 3. Data on the mechanical equivalent of heat;
- 4. Data on the pressure-temperature relation for saturated steam;
- 5. Data on the specific heat of superheated steam;
- 6. Data on the specific volume of superheated steam;
- 7. Data on the total heat of saturated steam.

Each of these subjects will be discussed in a separate section. Besides them one needs:

A comparison of the fundamental units of length and of weight in the English and metric systems;

Data on the density of water at various temperatures;

A value for the density of mercury at the temperature of melting ice.

In each of these last three cases there are trustworthy values so generally accepted as to need no discussion.

## § 1. Absolute Temperature

An evaluation of the absolute thermodynamic scale is necessary because of the use which must be made of absolute temperatures in the computation of entropies. Two distinct problems are involved. The first is the determination of the absolute temperature of melting ice, that is, the location of the absolute zero; and the second is the determination, degree by degree, of the difference between the absolute scale and that of the nitrogen-in-glass thermometer which is the usual standard in scientific work. For the present purpose the second of these problems need not be considered, for the variation of the nitrogen thermometer from the absolute scale is nowhere greater than a twentieth of a degree Fahrenheit between o' and 400°; above 400° even considerably larger errors in the temperature scale would be within the limit of error of the rest of the experimental data.

The determination of the absolute zero has recently been most satisfactorily accomplished. Three papers may be mentioned, which will themselves give references to many more, namely those of Berthelot, Buckingham, and Rose-Innes. Berthelot worked by two very different methods, the first based on the fact that as the pressure

- ¹ Trav. et Mém. Bur. Int., vol. 13 (1903).
- ² Bul. of the Bur. of Stan., vol. 3 (1907), pp. 237-293 (Reprint No. 57).
- ⁸ Phil. Mag. (6), vol. 15 (1908), pp. 301-316.

#### DISCUSSION OF SOURCES (\$\$1, 2)

in a gas thermometer approaches zero, the gas becomes more and more perfect, and the second based on the Joule-Thomson effect. Buckingham worked only from the Joule-Thomson effect. Rose-Innes also used the Joule-Thomson observations, but supplemented them as far as possible by much more accurate recent data on coefficients of expansion. The values which these investigators give for the temperature of the ice-point are:—

Author	YEAR	Мятнор	Gases	FINAL VALUE FOR ICE-POINT
Berthelot	1903	Extrapolation to p=o	H ₂ and N ₂	491.54° F.
"	1903	Joule-Thomson effect	H ₂ , N ₂ , CO ₂ and air.	491.63
Buckingham	1907	· · · · · · · · · · · · · · · · · · ·		491.71
Rose-Innes c	1908	JT. effect and other data	$H_2$ and $N_2$	401.64

Of these values the last is probably the best. Incidentally, it agrees almost exactly with the mean of the other three. Since the temperature of melting ice on the ordinary Fahrenheit scale is 32°, the value that must be added to temperatures on the ordinary scale to reduce them to absolute temperatures is

$$491^{\circ}.64 - 32^{\circ}.00 = 459^{\circ}.64$$

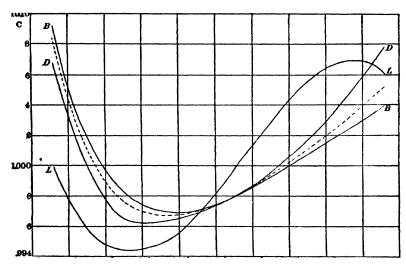


Fig. i.—The specific heat of water between the freezing and boiling points according to Barnes (B), Dieterici (D) and Lüdin (L). The dotted curve is (2B+D)/3,

# \$2. The Variation of the Specific Heat of Water with Temperature

The only sets of experiments available over the whole range from 32° to 212° F. are those of Lüdin, Barnes, and Dieterici. Since this part of the discussion is concerned only with the shape of the curve of variation of the specific heat, c, with tem-

¹ Inaug. Diss., Zurich, 1895: recomputed, Fortsch. d. Phys. vol. 5611 (1900), p. 304.

Phil. Trans., vol. 199A (1902), pp. 149-263.

³ Wied. Ann., (4) vol. 16 (1905), pp. 593-620.

## DISCUSSION OF SOURCES (§ 2)

perature, and not with its height, the actual values of each of these observers have been multiplied by such a constant as to make the average value of c between  $32^{\circ}$  and 212° exactly 1. This is equivalent to expressing each set of values in terms of the well-known Bunsen or mean calorie, if the temperatures are on the Centigrade scale, or in terms of a corresponding mean B.t.u., if the temperatures are on the Fahren-

heit scale. The resulting curves are shown in Figure 1. Lüdin's values are generally regarded as the least trustworthy, partly because of the difficulties inherent in calorimetry by the method of mixtures, and partly because his maximum just below the boiling point is not corroborated by either of the other observers, or by Regnault, either for water or for any other liquid. Of the other two pieces of work, Dieterici's is not as convincing as the extraordinarily good work of Barnes as regards either perfection of method or consistency of results. Barnes' values have therefore been given most weight in arriving at a representative curve. Lüdin's values have been given no direct weight whatever, but the fact that his curve and Dieterici's both differ from that of Barnes in the same direction throughout encourages one to give to Dieterici's values rather more weight in comparison with Barnes' than might otherwise have seemed desirable.1 The values finally chosen are a mean between those of Barnes and those

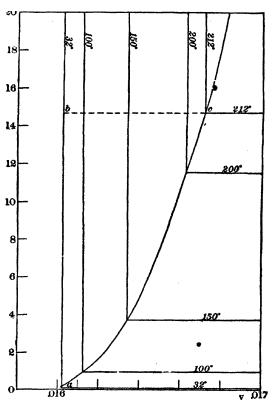


Fig. 2. - A large scale drawing of a piece out of the lower left-hand corner of the steam dome on the ordinary pv plane, illustrating the meaning of "the heat of the liquid." Abscissæ are in cu. ft.; ordinates are in lbs. per sq. in.; temperatures are on the Fahrenheit scale.

of Dieterici, giving the former twice as much weight as the latter. The curve representing these mean values is dotted in Figure 1, and its ordinates are tabulated in the sixth column of Table 6 at the end of Part I of this book. The values there given for temperatures below the freezing point are from the work of Barnes and Cooke.2 The values of the heat of the liquid, in Tables 1, 2 and 3, were obtained

 $h = \int_{32}^{t} c \ dt.$ by a step by step, numerical evaluation of the integral

¹ See also p. 91.

² Phys. Rev., vol. 15 (1902), pp. 65-72.

#### DISCUSSION OF SOURCES (§ 2)

It should be noticed that between  $32^{\circ}$  and  $212^{\circ}$  F. there are two theoretically distinct sets of numbers which could properly be given under the heading "the heat of the liquid" in a steam table, according to whether water at  $32^{\circ}$  and atmospheric pressure, or water at  $32^{\circ}$  and the pressure of its saturated vapor, is used as the zero of total heat. Figure 2 represents, drawn to scale, but much magnified, the lower left-hand corner of the steam dome on the usual pv plane. According to the first scheme, water at the point b is chosen as the zero of total heat, and the values of b which correspond to temperatures between  $32^{\circ}$  and  $212^{\circ}$  are those along the line bc. According to the second scheme, water at the point a is the zero of total heats, and the values of b given are those along the water-line bc. Since the internal energy, bc, of water at b is very nearly the same as that of water at b, practically all of the difference between the b at b and the b and the b at b and the b and the

$$h = e + 144 A pv$$
.

Graphically, this difference is the equivalent in heat units of the area of the rectangle between the vertical line ab of Figure 2 and the p axis; and in general the difference between the two possible values of h at any temperature is the area of a similar rectangle to the left of some vertical line between ac and bc.

A comparison of the two possible sets of h values with each other, and with the values of e along the same two lines, is given in the following table. The "mean B.t.u.," which is the heat unit employed, is, by definition, the one hundred and eightieth part of the change in total heat along bc.

	VALU	E AT	_
DESCRIPTION	32°	2 I 2 ⁰	RANGE
e along ac	0.00000	179.99813	179.99813
e along bc	0.00002	179.99813	179.99811
h alofig ac	0.00026	180.04362	180.04336
h along bc	0.04362	180.04362	180.0000

The distinction between the two possible sets of h values is of practical importance only in accurate calorimetry by the method of mixtures, and for that purpose h values along bc are preferable. They are given to two decimal places in Table 1 to facilitate this use of them. As a matter of convenience they have been reduced to b as the zero state, and satisfy the unusual but equally permissible equation of definition

$$h = e + 144 Apv - 0.04362$$

At high temperatures only values on the second scheme are possible, so that, in careful thinking, different interpretations of the phrase "heat of the liquid" are necessary in different temperature ranges.

Above 212° there are available only two investigations, Dieterici's and Regnault's.¹ The latter's observations were by the method of mixtures, the mean temperature of the cold water in the calorimeter varying from 55° to 70° F. Since the specific heat of

¹ Mém. de l'Inst. de France, vol. 21 (1847), pp. 729-748.

#### DISCUSSION OF SOURCES (§2)

water changes rapidly with the temperature in that range, it has seemed worth while to recompute Regnault's results on the basis of the curve just obtained for c below  $212^{\circ}$ . Figure 3 shows on a large scale the difference between the recomputed heat of the liquid from Regnault's data and that on the assumption that c is constant and equal to one. In other words, ordinates in Figure 3 are the increments that must be added to the mere temperature difference (t-212) to give, for any temperature t, the heat of the liquid above that at  $212^{\circ}$ . The curve R, representing Regnault's observations, does not approach zero at  $212^{\circ}$  as it should, which means that Regnault's experiments are inherently inconsistent with the c curve adopted above for the range from  $32^{\circ}$  to  $212^{\circ}$ . Regnault's experiments require the curve to be lower at room tempera-

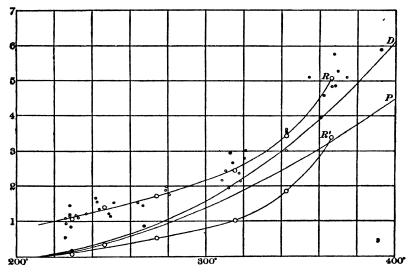


Fig. 3.— The heat of the liquid (h) above the boiling point. Abscissæ are temperatures on the Fahrenheit scale. Ordinates are  $\Delta h$  in B. t. u. where  $\Delta h$  is what must be added to (t-32) to give h. The recomputed results of Regnault's forty experiments are represented by small circles, and their means, in six groups, by large circles (curve R); curve R' is curve R scaled down to pass through o at  $t=212^\circ$ . Curve P is Peabody's recomputation of Regnault's curve, also scaled down to pass through o at  $t=212^\circ$ . Curve D represents Dieterici's formula and is the one used in this book. The black dots are five of Dieterici's twenty experimental means. The middle one of the five shown is the most inconsistent of the whole twenty. Dieterici's formula represents fairly well his other values at temperatures above  $400^\circ$  F.

tures and consequently higher near the boiling point than is the mean curve chosen above — that is, they require a curve still more like Dieterici's and still less like Barnes' than that chosen, thus justifying the decision that Dieterici's results should have a weight of at least one in three. Perhaps they should have had even more weight, but the work of Barnes has always been regarded as of such extraordinary excellence that this has not seemed best at the present time.

If Regnault's values are multiplied by such a constant factor as will make them approach zero at 212°, his curve lies below either Dieterici's or that marked P in Figure 3,

#### DISCUSSION OF SOURCES (\$52, 3)

which represents Peabody's version of Regnault's experiments, but turns sharply up across Peabody's curve toward Dieterici's near 400° F. The arbitrary nature of this scaling-down process is, however, an argument against the acceptance of the resulting curve.

Dieterici's curve is also open to objection in that his observed points do not lie as near it as might be wished, especially in the temperature range of Figure 3. The position of his curve is fixed largely by the points at higher temperatures.

The whole subject is still, therefore, in an unsatisfactory condition above 212°. Fortunately it makes very little difference in the properties of saturated steam which values are used for the heat of the liquid. For instance, the whole of the outstanding discrepancy at  $400^{\circ}$  would make about a thirtieth of one per cent difference in the entropy of saturated steam at that temperature. The values of Dieterici above 212° have, therefore, been chosen because of the great range covered by his experiments, even though this involves a slight discontinuity in dh/dt=c at 212°. His formula for the mean specific heat from  $32^{\circ}$  F. to  $t^{\circ}$  F. may be written

 $c_m = 0.9983 - 0.000 \text{ o28 } 8(t - 32) + 0.000 \text{ oo2 } 133(t - 32)^2 \text{ mean B. t. u.}$ 

Strictly speaking, this formula leads to values, not of h, but of e, but the difference is, in general, smaller than the outstanding uncertainties in either, being 0.046 B.t.u. at 212°, about 0.2 B.t.u. at 300°, and only 0.85 B.t.u. at 400°. Neglecting it, as has been done in these tables at temperatures below 450°, simply means using as standard a compromise (namely curve D on Figure 3) between the true Dieterici curve, which would lie somewhat higher than curve D, and Regnault's results as represented by either curve R or curve P. Above 450°, where the difference between e and h gets big, it has been allowed for.

## 53. The Mechanical Equivalent of Heat

The values of the specific heat of water discussed in the last section are in thermal units; some one of them must now be determined in mechanical units. For this purpose there are available the experiments of Rowland,² and of Reynolds and Moorby,⁸ by whom mechanical work was transformed directly into heat, and the experiments of Griffiths,⁴ of Schuster and Gannon,⁵ and of Barnes,⁶ by whom electrical energy was changed into heat. These investigations have recently been discussed by Smith,⁷ who accepts as most trustworthy the mean of the values of Reynolds and Moorby and of Barnes, namely

```
1 mean calorie = 4.1834 \times 10^7 ergs.
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- ¹ Reduced to mean B.t.u. by subtracting a seventh of one per cent.
- ² Proc. Amer. Acad., vol. 15 (1880), pp. 75-200.
- ^a Phil. Trans., vol. 190A (1898), pp. 301-422.

•

- 4 Phil. Trans., vol. 184A (1893), pp. 361-504.
- ⁸ Phil. Trans., vol. 186A (1895), pp. 415-467.
- ⁶ Phil. Trans., vol. 199A (1902), pp. 149-263.
- Monthly Weather Peview, October, 1907.

## DISCUSSION OF SOURCES (§§ 3, 4)

To change this into English units, one needs the conversion factor¹

$$1 \text{ kg.} = 2.204622 \text{ lbs.}$$

and a value of the gravitation constant g for which

$$g = 980.665$$
 cms. per sec.²

has been adopted as standard by international agreement.2 The result is

This value has been used in these tables.

#### §4. Pressures and Temperatures of Saturated Steam

The classical experiments on this subject were performed by Regnault ³ in the year 1847, and are even now models of accuracy. They covered the range from  $-27^{\circ}$  to 363° F. They have been recomputed with slightly varying results by several authors, among whom are Broch, ⁴ Peabody, ⁵ and Henning. ⁶ Since Regnault's time, many other investigations have been published, eleven of which are carefully discussed by Henning. ⁷ He uses as a standard of reference a formula of Thiesen, ⁸ which expresses p in mms. of mercury (at o° C.) as a function of t in degrees Centigrade, as follows: —

$$(t+273) \log \frac{p}{760} = 5.409 (t-100) - 0.508 \times 10^{-8} ((365-t)^4 - 265^4).$$

The deviations, from this formula, of Regnault's observations and of those of the eleven later investigators are plotted on a large scale in Henning's paper, and a correction curve for the formula obtained graphically. The conclusions reached in this paper were the basis of the original computations for these tables. The use of Thiesen's formula is greatly facilitated by a table in Henning's  $\mu$  aper, giving p in mms, of mercury for every degree from 0° to 200° C.

More recently, in August, 1908, Holborn and Henning have published the results of new experiments at the Reichsanstalt covering the range from 125° to 400° F. with extraordinary precision, and have proposed a new correction curve for Thiesen's

¹ See Fischer, Bul. of the Bur. of Stan., vol 1 (1904-5), p. 380.

² Troisième Conf. gen. des poids et mes., 1901, pp. 66-68.

³ Mém. de l'Inst. de France, vol. 21 (1847), pp. 465-633; for a most excellent account in English of these experiments see Risteen, The Locomotive, published by the Hartford Steam Boiler Inspection and Insurance Co., vol. 26 (July, 1906), pp. 85-94.

⁴ Trav. et Mém. Bur. Int., vol. 1A (1881), pp. 19-39.

⁵ Steam Tables, 7th ed. (1907), pp. 2-6.

⁶ Wied. Ann., (4) vol. 22 (1907), pp. 609-630.

⁷ Loc. cit.; see also Risteen, The Locomotive, vol. 26 (1907), pp. 183-190, 246-254; and vol. 27 (1908), pp. 54-62.

⁸ Wied. Ann., N. F., vol. 67 (1899), p. 692.

#### DISCUSSION OF SOURCES (§4)

formula based on their own work down to 125° F. and on Thiesen's experiments near the freezing point. Above 212° the new curve, Henning's 1907 curve, and the curve which represents Henning's recomputation of Regnault's observations, all agree within a twentieth of a degree Fahrenheit, so that the pressure-temperature relation may be regarded as satisfactorily known. Below 212° the new saturation temperatures run slightly higher than those of the 1907 paper, the greatest change being 0.12° F. at a pressure of 1 lb. Those parts of the tables which are affected by the change have been recomputed and corrected in page proof.

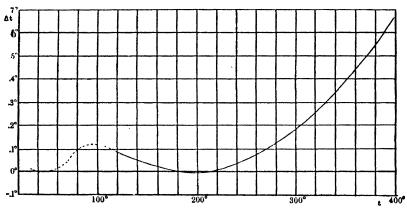


Fig. 4.—Correction curve for Thiesen's formula, according to Holborn and Henning (1908). Abscissæ are temperatures; ordinates are Δt = tobs.—teale.

To make Thiesen's formula available in English units, one needs the density of mercury at 0° C. According to Thiesen and Scheel ¹

In the computation of the condenser vacuum column in Table 1, giving p in inches of mercury, one needs also

Thiesen's formula, expressed in English units, is

$$(t+459.6) \log \frac{p}{14.70} = 5.409 (t-212) - 8.71 \times 10^{-10} ((689-t)^4 - 477^4),$$

where p is in lbs. per sq. in. and t is in ordinary Fahrenheit degrees. The correction curve of the 1908 paper of Holborn and Henning is plotted in English units in Figure 4, in which ordinates are  $\Delta t$ =observed temperature minus the t in Thiesen's

¹ Z. S. f. Instrkde., vol. 18 (1898), p. 138.

² This is the legal definition of the U. S. standard inch. See Fischer, Bul. of the Bur. of Stan. vol. 1 (1904-5), pp. 365-381, particularly p. 380.

## DISCUSSION OF SOURCES (\$54, 5)

formula. To use this curve to get the pressure corresponding to a given temperature  $t^o$ , one first *subtracts* from that t the  $\Delta t$  given by the curve, and then substitutes the remainder in Thiesen's formula.

At the very high temperatures considered at the end of Table 1, three researches are available, namely those of Battelli, of Cailletet and Colardeau, and of Knipp. The results of these observers are not in good agreement, as the following table shows. The values of Cailletet and Colardeau were used in the preparation of Table 1.*

TEMP.	Pressu	RE IN ATMOSPHERES ACCORD	ING TO
FAHR.	BATTELLI	C AND C.	Knipp
400°	16.8	16.8	
500°	48.6	46.6	47.₮
<b>6</b> 00°	109.7	107.1	112.5
<b>68</b> 0°	186.7	189.0	207.7

#### §5. The Specific Heat of Superheated Steam

Here, as before, the classical research is that of Regnault, 4 published in the year 1862. Contrary to an assumption sometimes seen in the literature, his work does not even seem to prove that the specific heat at constant pressure  $(C_s)$  of superheated steam is independent of either the pressure or the temperature, for he made only four series of experiments, and these were all at atmospheric pressure and covered nearly the same temperature range. He worked by the method of mixtures, injecting a known weight, first of slightly superheated steam, and then of highly superheated steam, into a calorimeter filled with water at room temperature. His computations are in error because, instead of weighing the cold water in the calorimeter, he measured it volumetrically in a suitable cast-iron tank. His justification of this was that although, by reason of the thermal expansion of the water as compared with that of the tank, there was less water by weight at room temperature than at oo C., which was his standard temperature, nevertheless the fact (which he thought to be true at low as well as at high temperatures) that the specific heat of water increased with the temperature, made the water in the calorimeter more effective thermally, gram for gram, and just about made up for neglecting its change of density. But we now know that at room temperatures the specific heat of water decreases with rising temperature. His data have, therefore, been recomputed, using his own value for the expansion coefficient of his sheet-iron tanks and modern data for the density and specific heat of water. This slightly reduces each of his four values of  $C_{\bullet}$  to the following figures:—

¹ Mem. d. R. Acc. d. Sc., Turin (2), vol. 43 (1892), pp. 63–98; see also Ann. de Chem. et de Phys. (6), vol. 26 (1892), pp. 410–425; and especially Risteen, The Locomotive, vol. 26 (October, 1906), pp. 116–126, and vol. 26 (July, 1907), pp. 213–219.

² Journ. de Phys. (2), vol. 10 (1891), pp. 333-340; also Ann. de Chem. et de Phys., vol. 25 (1892), pp. 519-534; also Physikalische Revue, vol. 1 (1892), pp. 14-21; also a short note in C. R. vol. 112 (1891), pp. 563-565; see Risteen, The Locomotive, vol. 26 (July, 1907), pp. 219-221.

Phys. Rev., vol. 11 (1900), pp. 141-144.

⁴ Mém. de l'Inst. de France, vol. 26 (1862), pp. 167-178.

^{*} See page 4.

## DISCUSSION OF SOURCES (§5)

	Temp. Range $(C^{\circ})$	R's Value of $C_p$	New Value of $C_p$
Series 1.	127.7-231.1	(0.46881) ¹	(0.4655)
Series 2.	137.7-225.9	0.48111	0.4769
Series 3.	124.3-210.4	0.48080	0.4736
Series 4.	122.8-216.0	0.47963	0.4780
	Mean of last three	0.48051	0.4762

It will be seen presently that the new figures agree better with modern work than do the older ones.

It is only within a few years that reliable determinations of  $C_{\rho}$  at other pressures than I atmosphere have been made. The best of these are probably those of Knoblauch and Jakob, which were carried out with great care by the electrical method. Steam from a boiler was superheated in an apparatus consisting of a long pipe some inches in diameter filled with a dense grid of resistance wire, wound on insulating frames. The energy necessary for superheating was introduced electrically in the first sections of this pipe and the rest of the resistance wire served to mix the steam and bring it into a homogeneous state. It then passed into a calorimeter where a small amount of additional energy was introduced electrically, careful measurements being made of the temperatures of the steam when entering and leaving this calorimeter. The losses due to radiation and conduction were determined by separate experiments. The  $C_{\rho}$  of the steam in the calorimeter could then be easily computed. The results of these experiments have been used as the basis for the computation of these tables.

They have, however, been modified in two respects. In the first place, the curve giving the  $C_{\rho}$  of steam at atmospheric pressure has been lowered in the high temperature region, so as to agree better with the values obtained by Holborn and Henning³ at very high temperatures. Their work, like Regnault's, was only at atmospheric pressure, but they reached temperatures as high as  $2450^{\circ}$  F., and others by different methods have gone even higher. All these results agree in giving smaller values of  $C_{\rho}$  than an extrapolation of Knoblauch and Jakob's atmospheric curve would indicate. It has therefore been lowered so as to join continuously with the curve of Holborn and Henning.⁴ The high

^{1 &}quot;...les résultats de la première série, qui m'inspirent moins de confiance que les autres...." Regnault, p. 178.

² Forscharb., Berlin, Hefte 35 and 36 (1906), pp. 109-152.

³ Wied, Ann., (4) vol. 18 (1905), pp. 730-756; and (4) vol. 23 (1907), pp. 809-845.

⁽Note added, June, 1912). The propriety of this change in the original curve of Knoblauch and Jakob has been justified since the first copies of this book were printed by the results of a new investigation by Knoblauch and Mollier (Z. V. D. I., 1911, pp. 665-674) covering the same range of pressure as their earlier investigation, but extending to over 1000° F. This work shows that their former  $C_{\rho}$  curve for 1 atmosphere rose too sharply near 650° F. and that the true curve lies nearly as it was drawn in figure 5. Their results run a little higher, however, than Holborn and Henning's, and it is therefore possible that the values of  $C_{\rho}$  used in this book for the highest temperatures are a little too low. No error of commercial importance is involved.

# DISCUSSION OF SOURCES (§ 5)

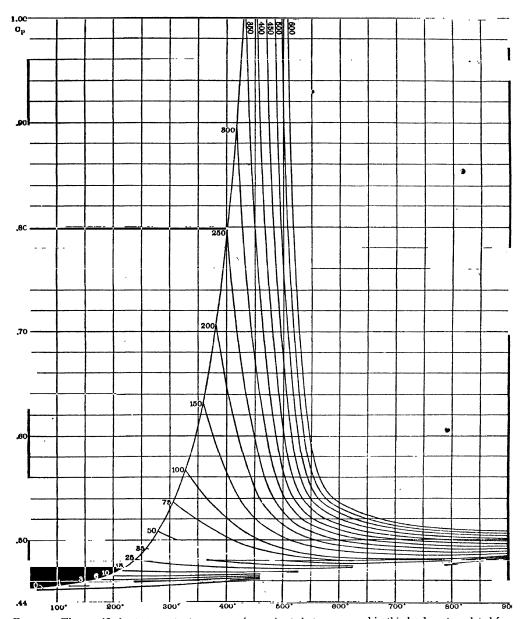


Fig. 5.— The specific heat at constant pressure of superheated steam as used in this book, extrapolated from Knoblauch's data. The saturation line is drawn according to his formula, and the curves at moderate pressures and superheats follow his curves as nearly as possible. The curves at very low pressures close to saturation are higher than Knoblauch's curves because of thermodynamic evidence, and because of Regnault's results at atmospheric pressure. The 15 lb. curve at high superheats follows Holborn and Henning's curve. The other curves are spaced at very high superheats in accordance with information derived from the Joule-Thomson effect.

# DISCUSSION OF SOURCES (\$5,6,7)

temperature ends of the other curves, for pressure higher than 15 lbs., have then been spaced in accordance with information which can be derived from a study of the Joule-Thomson effect in superheated steam and in other vapors.¹

The second modification of Knoblauch's curves is at the low temperature end of the 15 lb. curve and those near it. These run lower than even the recomputed results of Regnault's observations, to which considerable importance may well be attached in the present unsettled state of the subject. There are also certain theoretical considerations based on the thermodynamics of the Joule-Thomson effect which seem to set 0.45 as a lower limit to the lower end of the saturation line on the  $C_p$  diagram, a value also somewhat higher than Knoblauch's. For these reasons, the curves below 100 lbs. have all been slightly raised on the  $C_p$  diagram. The difference at 15 lbs. is only 0.007 B. t. u.

The finally accepted values of  $C_{\rho}$ , which were used in the preparation of these tables, are plotted in Figure 5. They have received additional confirmation from the fact that all of seven different kinds of large scale steam diagrams which have been plotted in the course of this work, and particularly the total heat-temperature diagram on which the lines of constant pressure seem to be very sensitive to inconsistencies in the assumed values of  $C_{\rho}$ , ran more smoothly with these values of  $C_{\rho}$  than with certain other suggested values which were first tried.

#### §6. The Specific Volume of Superheated Steam

Of the various sets of values of the specific volume of superheated steam at different pressures and temperatures, that of Knoblauch, Linde and Klebe ² seems to be the best, and has been used in this work.³ Linde's characteristic equation, ⁴ expressing v as a function of p and t, may be written

$$pv = 0.5962 \ T - p (1 + 0.0014 \ p) \left( \frac{150,300,000}{T^3} - 0.0833 \right),$$

where p is in lbs. per sq. in., v is in cu. ft., and T=t+459.6 is the absolute temperature on the Fahrenheit scale.

# §7. The Total Heat of Saturated Steam

It is in their values for the total heat of saturated steam that these tables differ most essentially from all that have preceded them. It has been the custom for makers of steam tables to use Regnault's classic formula, now sixty-one years old, which gives as the total heat of saturated steam

$$H = 1091.7 + 0.305 (t - 32).$$

- ¹ Davis, Proc. Am. Acad., vol. 44 (1909).
- ² Forscharb., Berlin, Heft 21 (1905), pp. 33-55.
- 3 But see p. 103.
- 4 Forscharb., Berlin, Heft 21 (1905), pp. 64-69.
- ⁵ Mém. de l'Inst. de France, vol. 21 (1847), pp. 635-728.

# DISCUSSION OF SOURCES (§7)

It has for some time been known that this formula was considerably in error, especially at low temperatures, and it is worth noticing that of the eight other vapors studied by Regnault, five gave curves of the second degree, concave downward, for H as a function of t.

Since Regnault's time, measurements of great value, either of the total heat itself, or of the heat of vaporization, which amounts to the same thing, have been made at various temperatures between 32° and 212° F. by Dieterici, Smith, Griffiths, Henning and Joly, all of which have been admirably discussed by Smith in the paper previously referred to. Their values as recomputed by him are given in the following table:—

Observer	TEMPERATURE DEGREES FAHR.	TOTAL HEAT  B. T. U.
C. Dieterici, Königl. Tech. Hochschule, Hanover, Germany. Wied. Ann., vol. 37 (1889), pp. 494-508.2	32.0	1073.4
A. W. Smith, University of Michigan, U. S. A. Phys. Rev., vol. 25 (1907), pp. 145-170.	57.1 70.1 82.5	1084.7 1090.7 1096.2
	103.6	1104.6
E. H. Griffiths, Cambridge, England. Phil. Trans., vol. 186A (1895), pp. 261-341.	86.0 104.3 76.9 103.9 121.7	1097.8 1104.9 1094.5* 1104.2* 1111.2*
F. Henning, Reichsanstalt, Berlin, Germany. Wied. Ann., (4) vol. 21 (1906), pp. 849–878.	86.2 120.5 148.7 171.2 192.7 213.1	1097.6* 1114.4 1124.7 1134.5 1144.0
J. Joly, Trinity College, Dublin, Ireland. In an appendix to Griffiths' paper above (p. 322).	211.9	1150.0

* These four values were considered by the experimenters less reliable than their other results.

These values have been plotted on a large scale and a graph drawn representing satisfactorily practically all of them, from which the values used in this book at temperatures below 212° were then read off. Regnault's formula, and those tables which are based on it, are right at 170° F., but are too high by 18 B. t. u. at 32° F.

Above  $212^{\circ}$ , Regnault's values may be replaced by a second degree equation recently proposed by one of the present authors on the basis of a recomputation of the throttling experiments of Grindley, Griessmann and Peake, with the help of the  $C_{\bullet}$  measurements of Knoblauch and Jakob, already referred to. The method used is illustrated by Figure 6, the left-hand half of which represents a throttling curve of the

¹ Monthly Weather Review, October, 1907.

² See also Wied. Ann., (4) vol. 16 (1905), pp. 593-620.

⁸ Davis, Proc. Am. Soc. of Mech. Engs., vol. 30 (November, 1908), pp. 1419-1432.

#### DISCUSSION OF SOURCES (§7)

sort published in the papers mentioned. Supposedly dry and saturated steam at the pressure and temperature corresponding to the point A is first throttled to a lower pressure and temperature corresponding to the point B; then in a later experiment in the same run, it is throttled from exactly the same initial condition A to the condition C; then to D and so on. The well-known law of throttling is that the total heat in the condition B, or C, or D, is equal to that in the initial condition A.

The point B represents superheated steam at the pressure  $p_B$ ; the point B' represents saturated steam at the same pressure; the amount of superheat at B is the known temperature there minus the temperature at B', which can be taken from a steam table. Also, by definition, the total heat at B equals that of saturated steam at the same pressure (point B') plus the amount of heat required to superheat it at constant pressure from B' to B. This is the integral of  $C_p$  from B' to B, or simply the mean  $C_p$  from saturation multiplied by the known superheat. If  $C_p$  is known, this integral or increment in the total heat between B' and B is easily evaluated.

The value obtained is not only the difference between the total heat of saturated steam at B' and that of superheated steam at B; it is also the difference between the total heat of saturated steam at B' and that of saturated steam at A; that is, between the two corresponding ordinates of a curve giving the total heat of saturated steam as a function of the temperature. To draw a piece of this curve, one chooses arbitrarily some horizontal line such as xy in Figure 6, and lays off below it, at the proper temperatures, the distances bb', cc', dd', etc., which represent on the desired H-scale the integrals or total heat differences between B' and B, C' and C, D' and D, etc. The curve ab'c'd' is an isolated piece of the true curve of total heat against temperature. The *relative* height of its points, that is, its shape, is accurately determined; its *absolute* height above the assumed zero of total heat, namely, water at  $32^{\circ}$  and atmospheric pressure, is not yet known.

In the paper referred to, twenty-four overlapping pieces of this sort were superposed and gave a well-defined curve. Its height was then so determined as to make it pass through the mean of the values near the boiling point of Henning and of Joly, each reduced to 212°. The resulting curve leads to the formula

$$H = 1150.3 + 0.3745(t - 212) - 0.000550(t - 212)^2$$
.

It agrees satisfactorily, in the range from 212° to 400° F., with the values which Linde ¹ computes from the volume measurements of Knoblauch, Linde and Klebe, and also with the values recently proposed by Henning ² on the basis of an extrapolation of a formula representing his results below 212°. It is certainly much better than Regnault's formula, and is probably within a tenth of one percent of the truth throughout the range considered. If it be even that much in error, it is probably because it runs too low at the high temperatures. It has been used for the range above 212° in these

¹ Forscharb., Berlin, Heft 21 (1905), pp. 69-72.

² Wied. Ann., (4) vol. 21 (1906), p. 870.

³ See also Peabody, Proc. Am. Soc. of Mech. Engs., vol. 31 (1909).

## DISCUSSION OF SOURCES (§7)

tables. It shows that Regnault's formula, and those tables which are based on it, are too high by 6 B.t. u. at  $175^{\circ}$ , are right at  $280^{\circ}$ , and are too low at higher temperatures, the error increasing as the square of (t-175).

It has been pointed out  1  that the "total heat of saturated steam" obtained in this way is, rigorously, slightly different from that measured by Regnault. The new H is defined by the equation already mentioned in section  2 ,

$$H=E+144 Apv-0.04$$
 mean B.t.u.,

where E is the internal energy of the saturated steam and v is its volume. Regnault's H was smaller by the amount of the feed-pump work required to force water at the

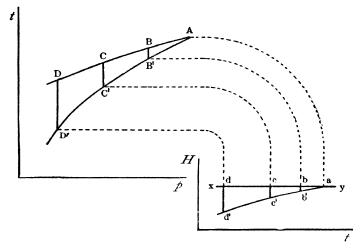


Fig. 6.—Showing how the total heat curve ab'c'd' is obtained from a throttling curve, ABCD.

temperature of the room into an enclosure against the pressure of the ligh temperature steam under investigation. Regnault's H gives accurately the heat required to turn feed water under pressure at his room temperature into steam in the delivery pipe, but is not as useful for other purposes as the H defined above; furthermore, it is not an accurately definable concept, depending as it does not only on the temperature of the saturated steam itself, but also on the temperature of the feed water. It is desirable, therefore, to displace it in both scientific and technical thinking by an H defined as above. This is the usual practice abroad.

From H it is easy to compute L, the latent heat of evaporation, by subtracting h, the heat of the liquid. L=H-h.

In many places in Tables 1 and 2, the values given for H, h and L will fail to satisfy this equation by one unit in the last place. This is because they were made to satisfy it when carried to an extra decimal place, the discrepancy coming in when the extra place was dropped.

¹ Heck, Jour. of the Am. Soc. of Mech. Engs., vol. 31 (1909), p. 301.

#### DISCUSSION OF SOURCES (\$\$ 7, 8)

At the end of Table 1, an attempt has been made to obtain by an extrapolation at least a qualitative idea of the variation of L and H with temperature in the range between  $400^{\circ}$  and the critical point. For this purpose L is easier to work with than H, because its behavior at the critical temperature itself is definitely known, at least if the usually accepted ideas about the critical point are assumed to be correct. These demand that at that point L=0 and dL/dt=minus infinity. As to H, it can be proved on the same hypotheses that dH/dt=minus infinity, but no information can be obtained as to the value of H itself. The two assumed facts about L led Thiesen 1 to suggest as an empirical formula

$$L=C (t_k-t)^n$$
,

where  $t_k$  is the critical temperature of water and C and n are constants to be determined experimentally. For n Thiesen used  $\frac{1}{3}$ , and Henning was led by his experiments below  $212^{\circ}$  F. to n=0.31249. A redetermination of this constant with the help of the new values above  $212^{\circ}$ , just described, leads to n=0.3150. If 138.81 B. t. u. be used for C, Thiesen's formula represents not only the seventeen values below  $212^{\circ}$  already tabulated, but also the eighteen mean values from which the new equation above  $212^{\circ}$  was obtained, with an average error of only one sixteenth of one per cent. It has, therefore, been used as the basis of an extrapolation to the critical point. The resulting values, which are given at the end of Table 1, are, of course, only qualitatively reliable. (See also page 4.)

#### §8. The Specific Volume of Saturated Steam

The adoption of a set of values for the total heat of saturated steam makes possible two useful computations. The first of these has already been mentioned on page 96, and gives  $C_{\mathfrak{p}}$  close to the saturation line by means of the formula ²

$$C_{p} = \frac{dH}{dt} - \frac{L}{T} + \frac{L}{u} \left(\frac{dv}{dt}\right)_{p}$$

The results of such a computation have been published elsewhere,³ and seem to justify the decision that Knoblauch's values of  $C_{\phi}$  are preferable to Thomas'.

Of much greater importance is the possibility of computing u, the change of volume during vaporization, by means of Clapyron's equation, where p is in lbs. per sq. in.

$$u = \frac{L}{144AT} \frac{1}{(dp/dt)_{\text{sat.}}}.$$

The necessary values of dp/dt were obtained by the method suggested in Henning's 1907 paper, the derivative of Thiesen's formula for p=j(t) being computed arith metically, and an unimportant correction factor being obtained graphically from the

- ¹ Verh. Phys. Ges. zu Berlin, vol. 16 (1897), pp. 80-82.
- For derivation, see, for example, Griessmann, Forscharb., Berlin, Heft 13 (1904), p. 8.
- ⁸ Davis, Proc. Am. Soc. of Mech. Engs., vol. 30 (November, 1908), pp. 1429-1431; and vol. 31 (February, 1909), pp. 309-310.

## DISCUSSION OF SOURCES (§§ 8, 9)

correction curve representing Henning's new results. To the values of u thus obtained must be added the specific volume, v', of water to give the specific volume, v, of saturated steam.

The results differ considerably from those obtainable from Regnault's total heats (see curve R of Figure 7). They agree remarkably well with the actual measurements of Knoblauch, Linde and Klebe between 212° and 360° F. (see curve K of Figure 7), the discrepancy only once reaching 0.2%, which is the limit of error assigned by the experimenters to their work.

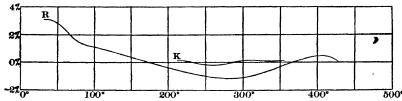


FIG. 7.—This figure shows the percentage deviation from the new values of the specific volume of saturated steam, first, of Regnault's values as given, for example, in the 1907 edition of Peabody's tables (curve R), and second of Knoblauch's experimental values (curve K). The irregularity below 100° is caused by the curious curvature in the lower part of the curve of Figure 4.

In Table 3 the values of v at saturation are the Clapyron values just described, while above 50° superheat, Linde's characteristic equation has been used. Between saturation and 50° superheat the values are such as to give a gradual transition. At high superheats Linde's equation is wholly an extrapolation, and the values of v should not be accepted with much confidence, the limit of error being uncertain.

#### §9. The Specific Volume of Steam at Very High Temperatures

The extrapolated values of the latent heat of vaporization discussed in section 6, together with the data on vapor tensions at very high temperatures discussed in section 4, make possible at least a qualitatively accurate computation, by Clapyron's equation, of the change of volume during vaporization up to and including the value u=0 at the critical point. Furthermore, the values of the specific volume of water in Landolt and Börnstein's tables run to about  $600^{\circ}$  F., so that up to that temperature the specific volume of saturated steam can be computed by the method used at ordinary temperatures.

Above 600° another device is furnished by a law proposed in 1886 by Cailletet and Mathias,² called "the law of the straight diameter." According to this law, if the means of the densities of a saturated vapor and its liquid at the same pressure and temperature are plotted (as abscissæ) against the corresponding temperatures (as ordinates), the resulting curve is so nearly straight and so nearly vertical up to and including the critical point itself, that its abscissa at even a somewhat uncertain

¹ The required values of the specific volume of water, v', were taken from the 3d (1905) edition of Landolt and Börnstein's "Physikalische Tabellen."

² Comptes Rendus, vol. 102 (1886), pp. 1202-1207; and vol. 104 (1887), pp. 1563-1568.

#### DISCUSSION OF SOURCES (§9)

critical temperature is a very good determination of the critical density. This law has been experimentally verified for many different substances by Mathias, Young, Guye, Tsuruta and others.¹ It is found that the diameter is usually not exactly straight, but that a second degree equation

$$s = s_0 + at + bt^2$$

represents even the most exact experimental data with satisfactory accuracy, except in the case of the alcohols, which require an additional term in  $t^3$ . The method is now regarded as furnishing by far the best attainable value of the critical density of a substance.

The application of this law to water, which seems to be new, is illustrated in Figure 8. This figure shows not only the diameter itself (large circles), but also the vapor and liquid densities (small circles) of which its points are the means. The steam dome on this figure is analogous to that on the ordinary pv plane except that right and left are interchanged, and that the shape of the top is much flattened because of the crowding of a large pressure range into a small temperature range. The curvature in the diameter is noticeable but regular, and its points can be represented well within the limit of error of the data by the formula

$$s = 28.424 - 0.016 \, 50(t - 320) - 0.000 \, 013 \, 2(t - 320)^2$$

The substitution in this formula of the critical temperature,  $t_c$ =689° F., gives for the critical density and volume the values

$$s_c$$
=20.5 lbs. per cu. ft.,  $v_c$ =0.049 cu. ft. per lb.*

These may be compared with the only values previously reported, namely Battelli's experimental value  $s_c = 13.0$  lbs. per cu. ft. (point B in Figure 8), Nadejdine's experimental value  $s_c = 26.8$  lbs. per cu. ft. (point N in Figure 8), and Dieterici's value  $s_c = 15.5$  lbs. per cu. ft. (point D in Figure 8). Neither of the experimental methods of the first two observers is, in general, comparable with that of Cailletet and Mathias for the accurate determination of a critical volume, although each is admirably adapted to the determination of a critical pressure. It is probable, therefore, that the new value of the critical density is much better than either of the older experimental ones. Dieterici's value was computed on the basis of Young's law that, for "normal sub-

Guye, Archives des Sci. Phys. et Nat. (3), vol. 31 (1894), pp. 43-46.

Tsuruta, Phys. Rev., vol. 10 (1900), pp. 116-118.

See also Young's "Stoichiometry," Longmans, 1908, pp. 165-170.

¹ Mathias, Ann. de la Fac. des Sci. de Toulouse, 1892; C. R., vol. 115 (1892), pp. 35-38; Mém. de la Soc. Roy. des Sci. de Liege (3), vol. 2 (1899); Journ. de Phys. (4), vol. 4 (1905), pp. 77-91. Young, Journ. of the Chem. Soc., vol. 63, trans. (1893), pp. 1237-1240; Phil. Mag., vol. 34 (1892), pp. 503-507; and vol. 50 (1900), pp. 291-305.

² Mem. dell. Ac. di Torino, (2) vol. 41 (1890), pp. 25-78; Physikalische Rev., vol. 2 (1892) pp. 1-32.

³ Universitätskija Investia Kiew, vol. 6 (1885), pp. 32-33.

⁴ Wied. Ann., (4) vol. 15 (1904), pp. 860-864.

^{*} These values should now (1916) by  $t_c=706.1^{\circ}$  F.,  $s_c=20.1$  lbs. per cu. ft.,  $v_c=0.050$  cu. ft. per lb.

#### DISCUSSION OF SOURCES (§9)

stances," the ratio of the actual density at the critical point to that predicted by the gas law is very nearly the same for all substances, an average value being 3.7. The discrepancy between the experimental value just found and the computed value is of the same sort as the well-established discrepancies in the case of methyl and ethyl alcohol and of acetic acid, which are regarded as indicating the existence of double

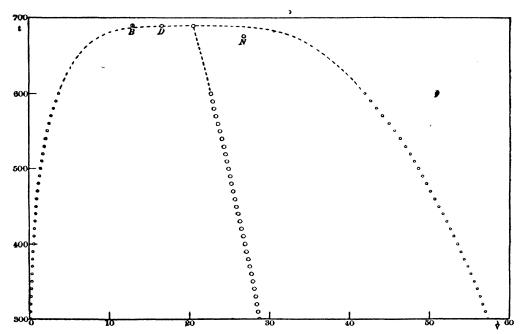


Fig. 8.—A determination by means of Cailletet and Mathias's law of the straight diameter of the critical volume of water and of the specific volumes of water and of steam at very high temperatures.

and triple molecules in those substances. A similar explanation in the case of water is very reasonable, since liquid water is known to be very highly associated at ordinary temperatures.

The equation for s, written above, gives at any temperature in the previously unknown range between 600° and 689° a value of

$$s = \frac{d_{st.} + d_{w.}}{2} = \frac{1}{2} \left( \frac{1}{v_{st.}} + \frac{1}{v_{w.}} \right)$$

Also Clapyron's equation gives a value of

$$u = v_{st} - v_{w}$$

A simple algebraic manipulation of s and u gives both  $v_{st}$  and  $v_{w}$ . The values at the end of Table 1 were obtained in this way. They are, of course, only qualitatively reliable because of the uncertainty in L and the efore in u.

## DISCUSSION OF SOURCES (§ 10)

#### § 10. The Computation of the Tables

The processes by which the various values set down in the tables were obtained from these experimental data are in most cases obvious. In Tables 1 and 2, the first eight columns depend directly on the data selected. The ninth column, giving the internal energy of evaporation, comes from the formula

$$I=L-144$$
 Apu;

and the tenth column, giving the internal energy of saturated steam, from the corresponding formula  $E=H-144 \ A pv$ .

The entropy of the liquid, in column eleven, was computed by a step by step, numerical evaluation of the integral

 $n = \int_{32}^{t} \frac{c}{T} dt$ 

up to 212°, and above 212° by an ordinary integration of Dieterici's second degree formula for c. The entropy of evaporation in column twelve is L/T. Column thirteen is the sum of columns eleven and twelve.

In all these cases, the required quantities were computed (usually to at least one extra significant figure) for each of a suitably selected set of standard pressures or temperatures, and the intermediate values filled in by interpolations involving, at times, differences of orders as high as the fifth. For such quantities as u and v, the interpolation is easier and more accurate if  $\log u$  and  $\log v$  are used instead of the quantities themselves.

In Table 3, the total heat and entropy increments from saturation at a number of standard pressures were computed by step by step numerical integrations of the  $C_{\rho}$  curves and the results plotted on a large scale. Smooth curves were then drawn for each of the superheats required and the increments read off for the intermediate pressures. A similar process was carried through for the specific volumes.

Since Holborn and Henning's observations on the  $C_{\rho}$  of superheated steam at atmospheric pressure run to very high temperatures, and since the spacing of the  $C_{\rho}$  curves for higher pressures is no more uncertain at 2000° superheat than at 600° superheat, it is possible to carry Table 3 to extremely high superheats with an accuracy limited chiefly by the errors already present below 600°. This has been done for several typical pressures in Table 4, and similar values for intermediate pressures can be obtained by interpolation.

The final values in all of the tables have been checked by the method of differences, by an independent computer, and as an additional precaution, many well-scattered numbers have been recomputed from the original formulæ by still another person not otherwise connected with the work. The authors will be glad to receive information as to any errors that may be discovered.